

IMPACT OF FLOW OF FLUIDS IN FOOD PROCESSING AND PRESERVATION

Lecture28

LECTURE 28 : PROBLEMS AND SOLUTIONS OF MOVING SURFACE FLOW

Good afternoon, my dear students, friends, boys and girls. Now we have done flow through surfaces, right? Where the surface was maybe inclined or vertical, that depends on what angle you are providing. But there the surface was stationary. Now, let us see what happens if there is surface which is also moving.

So, we term it as problems and solutions on moving surface fluid flow ok. So let us take a problem. The problem is like this. A coating experiment involving a flat photographic film that is being pulled up from a processing bath by rollers with a steady velocity u at an angle θ to the horizontal.



PROB:- A coating experiment involving a flat photographic film that is being pulled up from a processing bath by rollers with a steady velocity U at an angle θ to the horizontal. As the film leaves the bath, it entrains some liquid, and in this particular experiment it has reached the stage where: (a) the velocity of the liquid in contact with the film is $v_x = U$ at $y = 0$, (b) the thickness of the liquid is constant at a value δ , and (c) there is no net flow of liquid (as much is being pulled up by the film as is falling back by gravity). (Clearly, if the film were to retain a permanent coating, a net upwards flow of liquid would be needed.)



As the film leaves the bath, it entrains some liquid and in this particular experiment, it has reached the stage where number a, the velocity of the liquid in contact with the film is v_x is equal to u at y is equals to 0. And b, the thickness of the liquid is constant at a value δ . And see, there is no net flow of liquid as such is being pulled up by the film as is falling back by gravity. This means it is clearly if the film were to retain a permanent coating, a net upwards flow of liquid would be needed.

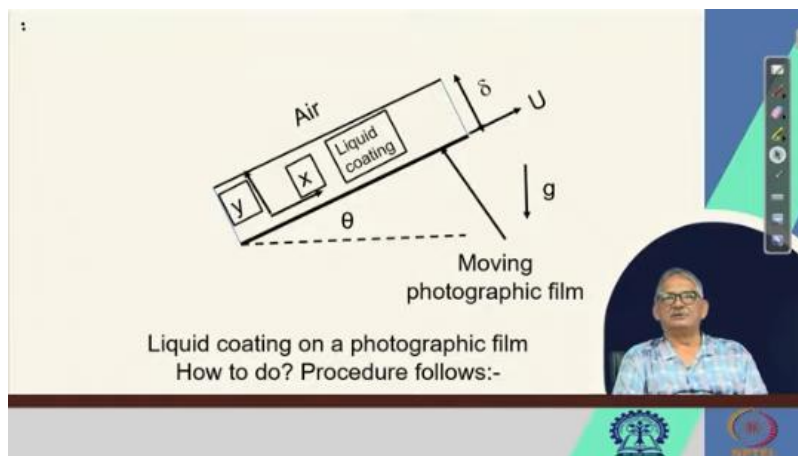
Right? I hope it is a big problem. Obviously, Not as simple as earlier cases, but definitely we have to handle, isn't it? This is something like that I don't know whether you have seen or not, even in X-ray films and other photographic films, they need to be treated with some solution.

So that is immersed into that solution and then taken away. So based on that phenomena, this problem looks similar. It is saying that a coating experiment involving a flat photographic film that is being pulled up from a processing bath by rollers with a steady velocity u at an angle θ to the horizontal. As the film leaves the bath,

it entrains some liquid and in this particular experiment, it has reached the stage number A), the velocity of the liquid in contact with the film is v_x is equals to u at y is equal to 0. Number B), the thickness of the liquid is constant at a value δ . And number C), there is no net flow of liquid as much is being pulled up by the film is falling back by gravity. So this says clearly that if the film were to retain a permanent coating, a net upwards flow of liquid would be needed, right.

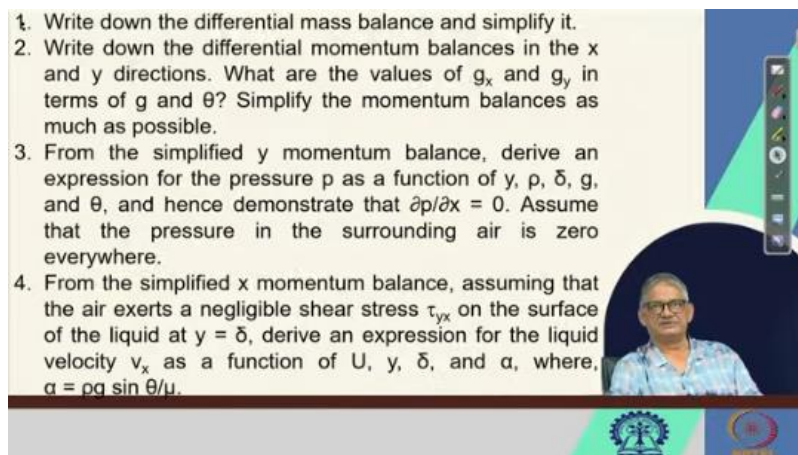
So, you have understood the problem. Now, let us see how this can be solved, ok. As you see, we have taken a volume element So, this is the liquid coating we have said that it is

having thickness δ and velocity is u in the x direction and the thickness is in the y direction δ . And the coating of the film



and the upper layer which is air. So, there is if you remember earlier we had said gas-liquid interface, liquid-liquid interface, liquid-solid interface, right? And this surface solid is moving that is the photographic film is moving with an angle with the horizon as theta. Like liquid coating on a photographic film, how to do?

And this procedure it follows like this. Write down the differential mass balance and simplify it. Then write down the differential momentum balance in the x and y directions. What are the values of g_x and g_y in terms of g and θ ? Simplify the momentum balances as much as possible.

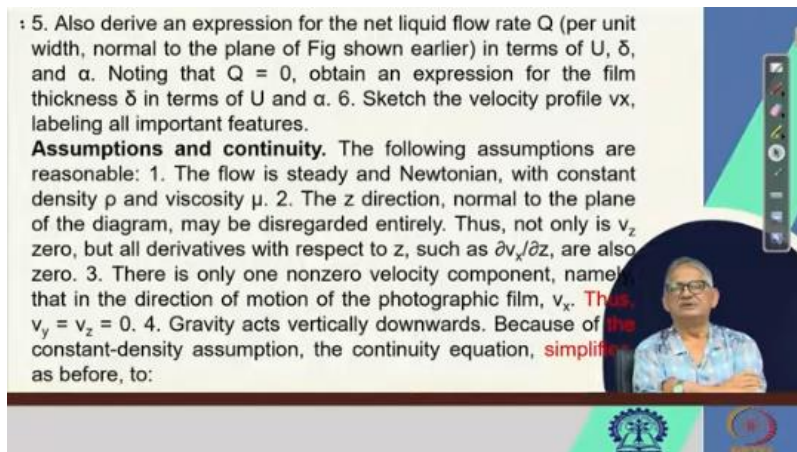


From the simplified y momentum balance, derive an expression for the pressure P as a function of y , ρ , δ and g , g and rather θ . And hence demonstrate that $\frac{\partial p}{\partial x}$ is zero. Assume that the pressure in the surrounding air is zero everywhere. From the simplified x momentum balance assuming that the air exerts negligible shear stress τ_{yx}

on the surface of the liquid at y is δ , derive an expression for the liquid velocity v_x as a function of u , y , δ and α .

where α is $\rho g \sin \theta$ by μ , right. α is $\rho g \sin \theta$ by μ . Then also derive an expression for the net liquid flow rate that is Q per unit width normal to the plane of the figure as we have shown it earlier. in terms of u , δ and α nothing that sorry noting that q is equal to 0 obtain an expression for the film thickness δ . in terms of u and α and last one is sketch the velocity profile v_x leveling all important features right.

So, we have described how you should tackle the problem, what are the steps you could And do accordingly. Right? Some assumptions also may be required like the following assumptions are reasonable. Number one, the flow is steady and Newtonian with constant density ρ and viscosity μ .



5. Also derive an expression for the net liquid flow rate Q (per unit width, normal to the plane of Fig shown earlier) in terms of U , δ , and α . Noting that $Q = 0$, obtain an expression for the film thickness δ in terms of U and α . 6. Sketch the velocity profile v_x , labeling all important features.

Assumptions and continuity. The following assumptions are reasonable: 1. The flow is steady and Newtonian, with constant density ρ and viscosity μ . 2. The z direction, normal to the plane of the diagram, may be disregarded entirely. Thus, not only is v_z zero, but all derivatives with respect to z , such as $\partial v_x / \partial z$, are also zero. 3. There is only one nonzero velocity component, namely, that in the direction of motion of the photographic film, v_x . Thus, $v_y = v_z = 0$. 4. Gravity acts vertically downwards. Because of the constant-density assumption, the continuity equation, simplified as before, to:

the z direction normal to the plane of the diagram may be disregarded entirely. Thus not only is v_z is 0, but all derivatives with respect to z such as $\partial v_x / \partial z$ are also 0. There is only one non-zero velocity component and that can be named as in the direction of motion of the photographic film v_x . Thus v_y , v_z is zero and gravity acts vertically downward because of the

constant density assumption, the continuity equation simplifies as like this. $\partial v_x / \partial x$ plus $\partial v_y / \partial y$ plus $\partial v_z / \partial z$ is equal to 0. Since v_y is v_z is equal to 0, it follows that $\partial v_x / \partial x$ is equal to zero. So, v_x is independent of distance x along the film.

: $\partial v_x / \partial x + \partial v_y / \partial y + \partial v_z / \partial z = 0 \dots (1)$. But since $v_y = v_z = 0$, it follows that $\partial v_x / \partial x = 0 \dots (2)$. So v_x is independent of distance x along the film. Further, v_x does not depend on z (assumption 2); thus, the velocity profile $v_x = v_x(y)$ depends only on y and will appear the same for all values of x .

Momentum balances:- With the stated assumptions of a Newtonian fluid with constant density and viscosity, momentum eqⁿ gives the x and y momentum balances:

$$\begin{aligned} \rho (\partial v_x / \partial t + v_x \partial v_x / \partial x + v_y \partial v_x / \partial y + v_z \partial v_x / \partial z) &= -\partial p / \partial x \\ &+ \mu (\partial^2 v_x / \partial x^2 + \partial^2 v_x / \partial y^2 + \partial^2 v_x / \partial z^2) + \rho g_x \\ \rho (\partial v_y / \partial t + v_x \partial v_y / \partial x + v_y \partial v_y / \partial y + v_z \partial v_y / \partial z) &= -\partial p / \partial y \\ &+ \mu (\partial^2 v_y / \partial x^2 + \partial^2 v_y / \partial y^2 + \partial^2 v_y / \partial z^2) + \rho g_y \end{aligned}$$

Further, v_x does not depend on z , we have assumed earlier. Thus, the velocity profile v_x is a function of v_{xy} and this depends only on y and will appear the same for all values of x . Now, this was with the continuity equation. Now, with the momentum balance with the started assumptions of a Newtonian fluid With constant density and viscosity.

Momentum equation gives the x and y momentum balances. So we can write. ρ times $\partial v_x / \partial t$ plus $v_x \partial v_x / \partial x$ plus $v_y \partial v_x / \partial y$ plus $v_z \partial v_x / \partial z$. This is equal to minus $\partial p / \partial x$ plus μ $\partial^2 v_x / \partial x^2$ plus $\partial^2 v_x / \partial y^2$ plus $\partial^2 v_x / \partial z^2$ plus ρg_x . right. This is one and another one is ρ times $\partial v_y / \partial t$ plus $v_x \partial v_y / \partial x$ plus $v_y \partial v_y / \partial y$ plus $v_z \partial v_y / \partial z$ $\partial v_y / \partial z$ rather is equal to minus $\partial p / \partial y$ plus μ $\partial^2 v_y / \partial x^2$ plus $\partial^2 v_y / \partial y^2$ plus $\partial^2 v_y / \partial z^2$ plus ρg_y .

: $\partial v_x / \partial x + \partial v_y / \partial y + \partial v_z / \partial z = 0 \dots (1)$. But since $v_y = v_z = 0$, it follows that $\partial v_x / \partial x = 0 \dots (2)$. So v_x is independent of distance x along the film. Further, v_x does not depend on z (assumption 2); thus, the velocity profile $v_x = v_x(y)$ depends only on y and will appear the same for all values of x .

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over yeah $\partial^2 v_x / \partial x^2$ plus $\partial^2 v_y / \partial y^2$ plus $\partial^2 v_y / \partial z^2$ plus ρg_y . These are the two x and y momentum balances we get right. Then we note it here that g_x is nothing but minus $g \sin \theta$ and g_y is nothing but minus $g \cos \theta$. So, these

momentum balances simplify to $\frac{\partial P}{\partial x} + \rho g \sin \theta$ is equal to $\mu \frac{\partial^2 v_x}{\partial y^2}$ and $\frac{\partial p}{\partial y}$ is equal to $-\rho g \cos \theta$.

: Noting that $g_x = -g \sin \theta$ and $g_y = -g \cos \theta$, these momentum balances simplify to:
 $\frac{\partial p}{\partial x} + \rho g \sin \theta = \mu \left(\frac{\partial^2 v_x}{\partial y^2} \right) \dots (3)$, and
 $\frac{\partial p}{\partial y} = -\rho g \cos \theta \dots (4)$. Integrating eqⁿ (4) between the free surface at $y = \delta$ (where the gauge pressure is zero) and an arbitrary location y (where the pressure is p) gives:


$$\int_0^P dp = -\rho g \cos \theta \int_{\delta}^y dy + f(x) \dots (5)$$

$$\therefore P = \rho g \cos \theta (\delta - y) + f(x) \dots (6)$$


Now, integrating between, integrating 4 equations, this between the free surface at y is equal to δ , where the gauge pressure is 0 and an arbitrary location y , where the pressure is p . This gives integral of dp between 0 to p is equal to $-\rho g \cos \theta$, again between δ and y , integral of dy plus function of x . Therefore, we can write P on integration, $\rho g \cos \theta$ into δ minus y , we have taken care of minus, plus function of x , right? Again, let us look into that.

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: Note that since a partial differential equation is being integrated, a function of integration, $f(x)$, is again introduced. Another way of looking at it is to observe that if eqⁿ (6) is differentiated with respect to y , we would recover the original equation (4), because $\partial f(x)/\partial y = 0$. However, since $p = 0$ at $y = \delta$ (the air / liquid interface) for all values of x , the function $f(x)$ must be zero. Hence, the pressure distribution: $P = (\delta - y)\rho g \cos \theta \dots (7)$ and it shows that P is not a function of x . In view of this last result, we may now substitute $\partial p/\partial x = 0$ into the x momentum balance, eqⁿ. (3), which becomes: $d^2 v_x / dy^2 = \rho g / \mu \sin \theta = \alpha \dots (8)$



Since a partial differential equation is being integrated, a function of the integration, that is $f(x)$ is again introduced. Another way of looking into it, as looking into it, as it is, rather to observe, at it is to observe that if the earlier equation number 6 which is this one, earlier equation number 6 is differentiated with respect to y . We would recover the original equation that is equation number 4.

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Where is that? Let us go back a little, equation number 4, 1, 2, 3, 4 yeah, this is the equation number 4 ok. Then This is why, because $\frac{\partial P}{\partial x}$ is equal to 0. However, since P is 0 at y is δ ,

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That is because the air-liquid interface for all values of x , the function $f(x)$ must be 0. Hence, the pressure distribution P , that is, equals to $\delta - y$ $\rho g \cos \theta$. And it shows that P is not a function of x . In view of this last result, we may now substitute $\frac{\partial P}{\partial x}$ is equal to 0 into the x momentum balance, that is in equation 3, right. So, let us look into equation 3.

: Note that since a partial differential equation is being integrated, a function of integration, $f(x)$, is again introduced. Another way of looking at it is to observe that if eqⁿ (6) is differentiated with respect to y , we would recover the original equation (4), because $\partial f(x) / \partial y = 0$. However, since $p = 0$ at $y = \delta$ (the air / liquid interface) for all values of x , the function $f(x)$ must be zero. Hence, the pressure distribution: $P = (\delta - y)\rho g \cos \theta \dots$ (7) and it shows that P is not a function of x .

In view of this last result, we may now substitute $\frac{\partial p}{\partial x} = 0$ into the x momentum balance, eqⁿ. (3), which becomes: $\frac{d^2 v_x}{dy^2} = \rho g / \mu \sin \theta = \alpha \dots$ (8)

So, this was equation $P \frac{\partial P}{\partial x} + \rho g \sin \theta = \mu \frac{d^2 v_x}{dy^2}$. right. So, if we put, hence, if we put, we may substitute $\frac{\partial P}{\partial x}$ is equal to 0 into the x momentum balance which becomes $\frac{d^2 v_x}{dy^2} = \frac{\rho g \sin \theta}{\mu}$. This is equal to $\frac{\rho g \sin \theta}{\mu}$ that is α .

: Noting that $g_x = -g \sin \theta$ and $g_y = -g \cos \theta$, these momentum balances simplify to:
 $\partial p / \partial x + \rho g \sin \theta = \mu (\partial^2 v_x / \partial y^2) \dots (3)$, and
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$$\int_0^P dp = -\rho g \cos \theta \int_{\delta}^y dy + f(x) \dots (5)$$

$$\therefore P = \rho g \cos \theta (\delta - y) + f(x) \dots (6)$$

This alpha, we have defined earlier, just see, here we have redefined, $\rho g \sin \theta$ by μ , that is, alpha, right ok. ρg by $\mu \sin \theta$ is alpha. Then we get that equation number 8 is, $d^2 v_x / dy^2$ is equal to ρg over $\mu \sin \theta$, that is alpha, ok. Now, this on simplification we note that the constant alpha has been introduced to denote $\rho g \sin \theta$ by μ and observe that the second derivative of the velocity now it appears as a total derivative.

: 5. Also derive an expression for the net liquid flow rate Q (per unit width, normal to the plane of Fig shown earlier) in terms of U , δ , and α . Noting that $Q = 0$, obtain an expression for the film thickness δ in terms of U and α . 6. Sketch the velocity profile v_x , labeling all important features.

Assumptions and continuity. The following assumptions are reasonable: 1. The flow is steady and Newtonian, with constant density ρ and viscosity μ . 2. The z direction, normal to the plane of the diagram, may be disregarded entirely. Thus, not only is v_z zero, but all derivatives with respect to z , such as $\partial v_x / \partial z$, are also zero. 3. There is only one nonzero velocity component, namely, that in the direction of motion of the photographic film, v_x . Thus, $v_y = v_z = 0$. 4. Gravity acts vertically downwards. Because of the constant-density assumption, the continuity equation, simplifies, as before, to:

: $\partial v_x / \partial x + \partial v_y / \partial y + \partial v_z / \partial z = 0 \dots (1)$. But since $v_y = v_z = 0$, it follows that $\partial v_x / \partial x = 0 \dots (2)$. So v_x is independent of distance x along the film. Further, v_x does not depend on z (assumption 2); thus, the velocity profile $v_x = v_x(y)$ depends only on y and will appear the same for all values of x .

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: Note that since a partial differential equation is being integrated, a function of integration, $f(x)$, is again introduced. Another way of looking at it is to observe that if eqⁿ (6) is differentiated with respect to y , we would recover the original equation (4), because $\partial f(x) / \partial y = 0$. However, since $p = 0$ at $y = \delta$ (the air / liquid interface) for all values of x , the function $f(x)$ must be zero. Hence, the pressure distribution: $P = (\delta - y) \rho g \cos \theta \dots (7)$ and it shows that P is not a function of x .

In view of this last result, we may now substitute $\partial p / \partial x = 0$ into the x momentum balance, eqⁿ. (3), which becomes:

$$d^2 v_x / dy^2 = \rho g / \mu \sin \theta = \alpha \dots (8)$$

since v_x depends only on y right. A first integration of the equation 8, just now we have seen with respect to y , it gives dv_x / dy is equal to αy plus C_1 integration constant. So, to find out this integration constant, we need to get a boundary so that this C_1 can be calculated. The boundary condition of zero shear stress at the free surface is now invoked. At the free surface, we also said earlier also, that the shear stress is zero.

: in which the constant α has been introduced to denote $\rho g \sin \theta / \mu$. Observe that the second derivative of the velocity now appears as a total derivative, since v_x depends on y only.

A first integration of Eqn. (8) with respect to y gives:

$$dv_x / dy = \alpha y + c_1 \dots (9)$$

The boundary condition of zero shear stress at the free surface is now invoked: $\tau_{yx} = \mu (\partial v_y / \partial x + \partial v_x / \partial y) = \mu dv_x / dy = 0 \dots (10)$

Thus, from eqⁿ (9) and (10) at $y = \delta$, the first constant of integration can be determined:

$dv_x / dy = \alpha \delta + c_1 = 0$; or, $c_1 = -\alpha \delta \dots (11)$

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So, that can be brought into that τ_{yx} is equal to $\mu \, dv_x / dy$. That is equal to $\mu \, dv_x / dy$ is equal to 0. right. So, thus from this equation 9, and equation 10, at y is equal to δ , the first constant of integration can be determined as dv_x / dy is $\alpha \delta + c_1$, dv_x / dy is $\alpha \delta + c_1$ is equal to 0. Therefore, c_1 is equal to $\alpha \delta$ minus $\alpha \delta$, c_1 is equal to minus $\alpha \delta$.

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$$dv_x / dy = \alpha \delta + c_1 = 0; \text{ or, } c_1 = -\alpha \delta \dots (11)$$


So, a second integration of equation 9 with respect to y this gives v_x is equal to $\alpha y^2 / 2 - \alpha \delta y + C_2$. So, the second constant of integration C_2 this can be determined by using the boundary that the liquid velocity at y is equal to 0 equals that of the moving photographic film right. Here I repeat the second constant of integration C_2 that can be determined by using the boundary condition that the liquid velocity at

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 The second constant of integration, c_2 , can be determined by using the boundary condition that the liquid velocity at $y = 0$ equals that of the moving photographic film. That is, $v_x = U$ at $y = 0$, yielding $c_2 = U$; thus, the final velocity profile is: $v_x = U - \alpha y (\delta - (y / 2)) \dots$ (13)



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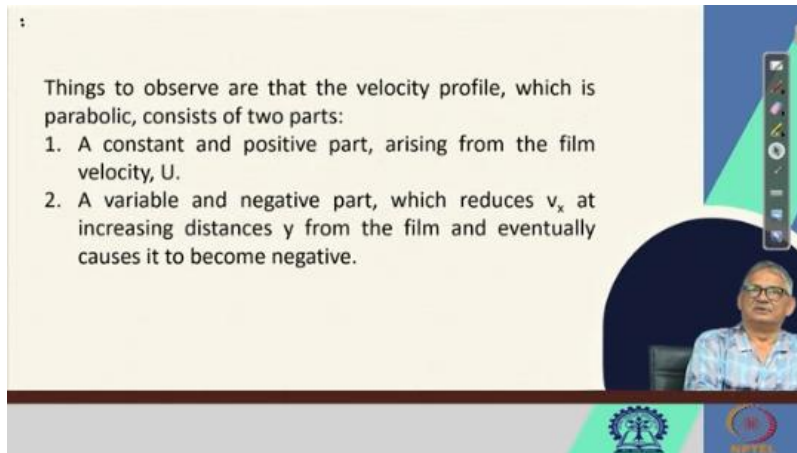


y is equal to 0 equals that of the moving photographic film that is v_x is u at y is equal to 0. Because our photographic film that is the surface is also moving with a velocity u and that is the v_x right. and that is at y is equal to 0 because y is the other side y is equal to δ which is the free end. So, yielding C_2 is equals to u thus we can write the final velocity profile is v_x is equal to u minus αy into δ minus y by 2. right.

So, we found out the velocity profile that is whatever velocity was there u minus αy into δ minus y by 2 is the v_x . So, here we have to keep in mind that The velocity profile which is parabolic consists of two parts. Number one, a constant positive part arising from the film velocity u and a variable and negative part which reduces v_x at increasing distance y from the film and eventually causes it to be or to become negative right. I repeat that the things which we have to keep in mind here is that the velocity profile is parabolic.

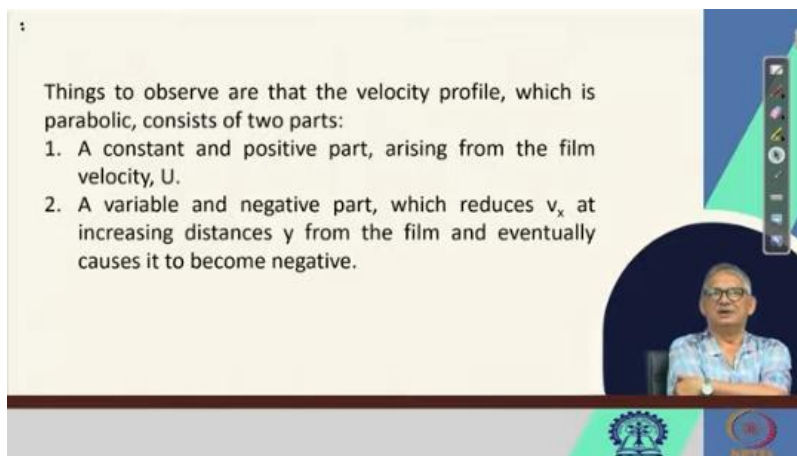
Things to observe are that the velocity profile, which is parabolic, consists of two parts:

1. A constant and positive part, arising from the film velocity, U .
2. A variable and negative part, which reduces v_x at increasing distances y from the film and eventually causes it to become negative.



Things to observe are that the velocity profile, which is parabolic, consists of two parts:

1. A constant and positive part, arising from the film velocity, U .
2. A variable and negative part, which reduces v_x at increasing distances y from the film and eventually causes it to become negative.

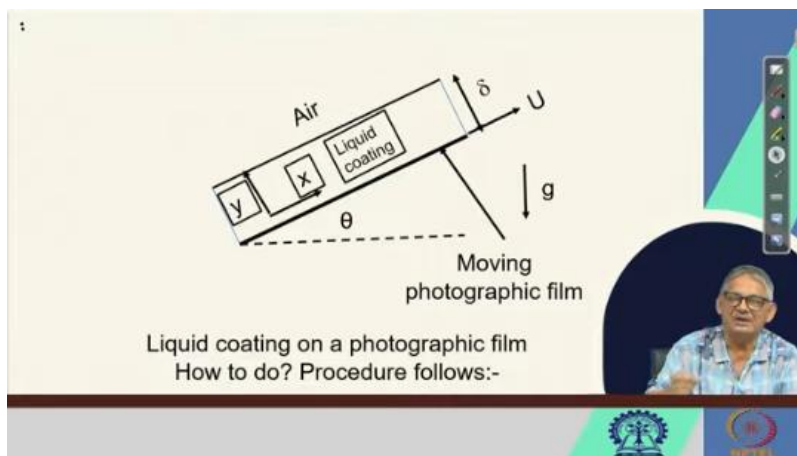
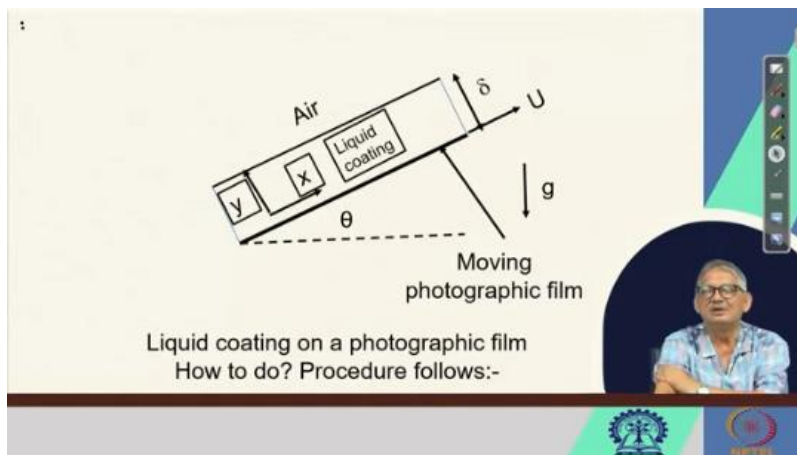


And it consists of two parts. First part is constant and a positive part arising from the film velocity u . A variable and negative part which reduces v_x at increasing distance y from the film and eventually causes it to become 0. So, let us look into v_x again that v_x is u minus αy into $\frac{\Delta}{2}$ right. As y is increasing

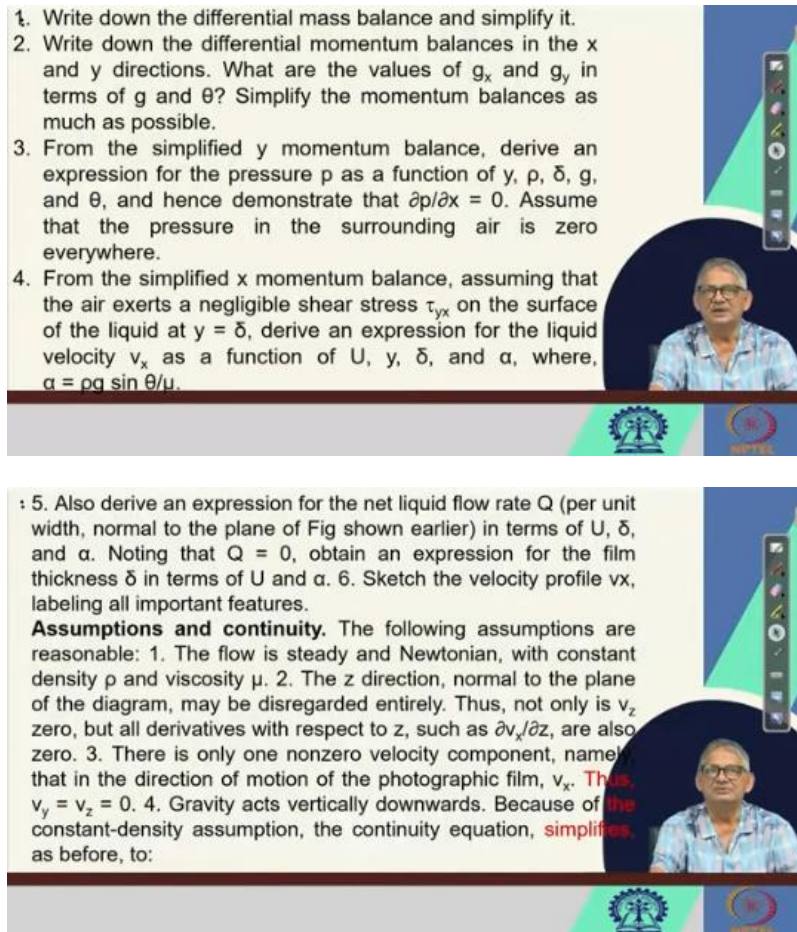
$\frac{\Delta}{2}$ is also decreasing right. So, that is why we have said we can say that eventually causing it to become negative ok. before going further because now the time is also not so much. So, let us recapitulate again so that it becomes easier for us to understand. First, the problem we have understood.

PROB:- A coating experiment involving a flat photographic film that is being pulled up from a processing bath by rollers with a steady velocity U at an angle θ to the horizontal. As the film leaves the bath, it entrains some liquid, and in this particular experiment it has reached the stage where: (a) the velocity of the liquid in contact with the film is $v_x = U$ at $y = 0$, (b) the thickness of the liquid is constant at a value δ , and (c) there is no net flow of liquid (as much is being pulled up by the film as is falling back by gravity). (Clearly, if the film were to retain a permanent coating, a net upwards flow of liquid would be needed.)

Second, we have drawn that film which is moving right with an angle of theta with the horizon and the upper part is air interface. So, we have taken that two dimensions Y and X. Y is up to del that is the film and X is the direction of the flow. having a velocity already u, right? And another is the gravitational pull, right?



We have discussed with the how it should be done. Then we have found out Some assumptions which is also very valid assumptions, flow is steady and Newtonian, constant density and viscosity and z direction normal to the plane that has nothing to do. So, all z components are taken off. one non-zero velocity component that the direction of motion of the photographic film that is v_x .



1. Write down the differential mass balance and simplify it.

2. Write down the differential momentum balances in the x and y directions. What are the values of g_x and g_y in terms of g and θ ? Simplify the momentum balances as much as possible.

3. From the simplified y momentum balance, derive an expression for the pressure p as a function of y , ρ , δ , g , and θ , and hence demonstrate that $\partial p / \partial x = 0$. Assume that the pressure in the surrounding air is zero everywhere.

4. From the simplified x momentum balance, assuming that the air exerts a negligible shear stress τ_{yx} on the surface of the liquid at $y = \delta$, derive an expression for the liquid velocity v_x as a function of U , y , δ , and α , where, $\alpha = \rho g \sin \theta / \mu$.

5. Also derive an expression for the net liquid flow rate Q (per unit width, normal to the plane of Fig shown earlier) in terms of U , δ , and α . Noting that $Q = 0$, obtain an expression for the film thickness δ in terms of U and α .

6. Sketch the velocity profile v_x , labeling all important features.

Assumptions and continuity. The following assumptions are reasonable:

1. The flow is steady and Newtonian, with constant density ρ and viscosity μ .
2. The z direction, normal to the plane of the diagram, may be disregarded entirely. Thus, not only is v_z zero, but all derivatives with respect to z, such as $\partial v_x / \partial z$, are also zero.
3. There is only one nonzero velocity component, namely, that in the direction of motion of the photographic film, v_x . Thus, $v_y = v_z = 0$.
4. Gravity acts vertically downwards. Because of the constant-density assumption, the continuity equation, simplifies, as before, to:

So, v_y if v_z all are equal to 0 right. So, like this simplifies we started with finding out from the continuity equation and then momentum balance. We found out some relations and then integrating them with the limit once for pressure for 0 to P and the y direction that is δ . So, you got pressure relation P is also with a function of x, right?

: $\partial v_x / \partial x + \partial v_y / \partial y + \partial v_z / \partial z = 0 \dots (1)$. But since $v_y = v_z = 0$, it follows that $\partial v_x / \partial x = 0 \dots (2)$. So v_x is independent of distance x along the film. Further, v_x does not depend on z (assumption 2); thus, the velocity profile $v_x = v_x(y)$ depends only on y and will appear the same for all values of x .

Momentum balances:- With the stated assumptions of a Newtonian fluid with constant density and viscosity, momentum eqⁿ gives the x and y momentum balances:
 $\rho (\partial v_x / \partial t + v_x \partial v_x / \partial x + v_y \partial v_x / \partial y + v_z \partial v_x / \partial z) = -\partial p / \partial x + \mu (\partial^2 v_x / \partial x^2 + \partial^2 v_x / \partial y^2 + \partial^2 v_x / \partial z^2) + \rho g_x$
 $\rho (\partial v_y / \partial t + v_x \partial v_y / \partial x + v_y \partial v_y / \partial y + v_z \partial v_y / \partial z) = -\partial p / \partial y + \mu (\partial^2 v_y / \partial x^2 + \partial^2 v_y / \partial y^2 + \partial^2 v_y / \partial z^2) + \rho g_y$

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: Noting that $g_x = -g \sin \theta$ and $g_y = -g \cos \theta$, these momentum balances simplify to:
 $\partial p / \partial x + \rho g \sin \theta = \mu (\partial^2 v_x / \partial y^2) \dots (3)$, and
 $\partial p / \partial y = -\rho g \cos \theta \dots (4)$. Integrating eqⁿ (4) between the free surface at $y = \delta$ (where the gauge pressure is zero) and an arbitrary location y (where the pressure is p) gives:

$$\int_0^P dp = -\rho g \cos \theta \int_{\delta}^y dy + f(x) \dots (5)$$



$$\therefore P = \rho g \cos \theta (\delta - y) + f(x) \dots (6)$$

And then we integrated and shown that the $\partial^2 v_x / \partial y^2$ is $\rho g \sin \theta / \mu$ and we named this $\rho g \sin \theta / \mu$ as α . Then we found out that $dv_x / dy = \alpha y + C_1$ and we found out C_1 to be $-\alpha \delta$. Like that we found out the other equation by integrating and we found out the integration constant and that is, C_2 is u . So,

we got the velocity profile v_x is u minus αy into y by 2 that is 1 and from there we interpreted that this profile is parabolic in nature, but it has two components.

: Note that since a partial differential equation is being integrated, a function of integration, $f(x)$, is again introduced. Another way of looking at it is to observe that if eqⁿ (6) is differentiated with respect to y , we would recover the original equation (4), because $\partial f(x)/\partial y = 0$. However, since $p = 0$ at $y = \delta$ (the air / liquid interface) for all values of x , the function $f(x)$ must be zero. Hence, the pressure distribution: $P = (\delta - y)\rho g \cos \theta \dots$ (7) and it shows that P is not a function of x .

In view of this last result, we may now substitute $\partial p/\partial x = 0$ into the x momentum balance, eqⁿ. (3), which becomes:

$$d^2v_x / dy^2 = \rho g / \mu \sin \theta = \alpha \dots$$
 (8)




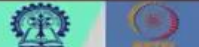
: in which the constant α has been introduced to denote $\rho g \sin \theta / \mu$. Observe that the second derivative of the velocity now appears as a total derivative, since v_x depends on y only.

A first integration of Eqn. (8) with respect to y gives:

$$dv_x / dy = \alpha y + c_1 \dots$$
 (9)



The boundary condition of zero shear stress at the free surface is now invoked: $\tau_{yx} = \mu (\partial v_y / \partial x + \partial v_x / \partial y) = \mu dv_x / dy = 0 \dots$ (10)

Thus, from eqⁿ (9) and (10) at $y = \delta$, the first constant of integration can be determined:

$$dv_x / dy = \alpha \delta + c_1 = 0; \text{ or, } c_1 = -\alpha \delta \dots$$
 (11)



: A second integration, of eqⁿ. (9) with respect to y , gives: $v_x = \alpha (y^2 / 2 - y\delta) + c_2 \dots$ (12)

The second constant of integration, c_2 , can be determined by using the boundary condition that the liquid velocity at $y = 0$ equals that of the moving photographic film. That is, $v_x = U$ at $y = 0$, yielding $c_2 = U$; thus, the final velocity profile is: $v_x = U - \alpha y (\delta - (y / 2)) \dots$ (13)

One is the positive part arising from the film velocity u and another one is variable and negative part which reduces v_x at increasing distance y from the film and eventually causes

it to become negative ok. Now, the time is up. Thank you for listening and we will continue with it in the next class. Okay.

Thank you very much.