

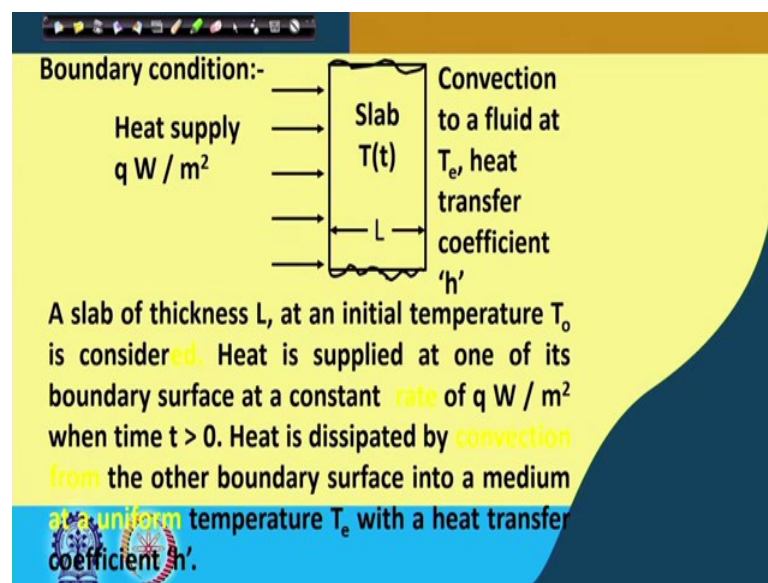
Thermal Operations in Food Process Engineering: Theory and Applications
Prof. Tridib Kumar Goswami
Department of Agricultural and Food Engineering
Indian Institute of Technology, Kharagpur

Lecture - 23
Transient Heat Transfer (Contd.)

In the previous class we have seen that lumped system analysis how it can be done, 'right'. And, today we will do another that is where the boundary conditions are given, 'right'. Boundary conditions if are given, then we can solve it analytically. We will do that today and in the previous class we were discussing about the problem, that a slab is bounded in the two sides; one with a convective boundary condition and the other with the constant heat flux boundary condition, 'right'.

So, under that situation if the slab is having a thickness L , then what will be the temperature distribution in the body that we can find out by solving it, 'right'.

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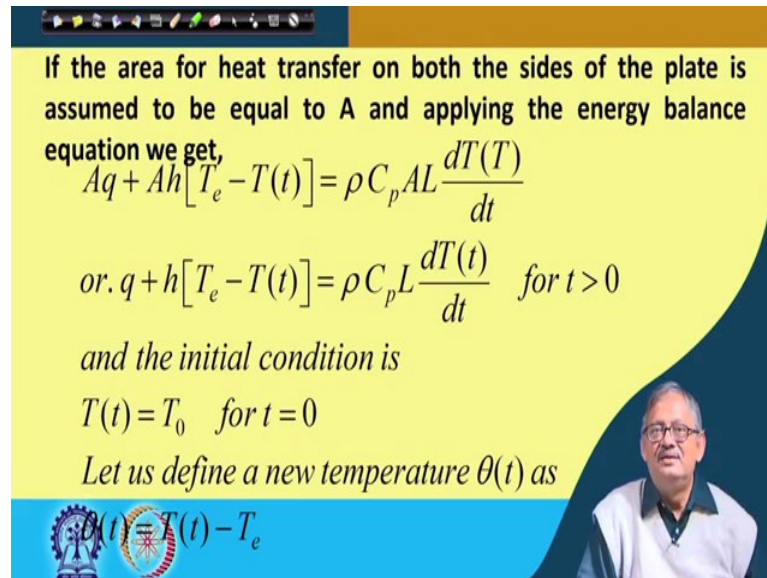


So, we come to this that if the boundary conditions are given, that we have a heat flux of q watt per meter square, in a slab of thickness L and the other boundary is a convective boundary with the heat transfer coefficient of h and the temperature is T_e .

Then a slab of constant with the thickness of L at an initial temperature of T_0 is considered and heat is supplied at one end of its boundary surface at the constant rate of

heat flux that is q watt per meter square, when time is greater than 0 or t is greater than 0. Heat is dissipated by convection into the other boundary surface into your medium at uniform temperature of T_e with a heat transfer coefficient of h , 'right'.

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If the area for heat transfer on both the sides of the plate is assumed to be equal to A and applying the energy balance equation we get,

$$Aq + Ah[T_e - T(t)] = \rho C_p AL \frac{dT(T)}{dt}$$

or. $q + h[T_e - T(t)] = \rho C_p L \frac{dT(t)}{dt}$ for $t > 0$

and the initial condition is

$$T(t) = T_0 \quad \text{for } t = 0$$

Let us define a new temperature $\theta(t)$ as

$$\theta(t) = T(t) - T_e$$

Perhaps a similar problem we have done earlier also, 'right';. If the area for heat transfer on both the sides of this plate is assumed to be equal to A and applying the energy balance equation we can write, that

$$Aq + Ah[T_e - T(t)] = \rho C_p AL \frac{dT(T)}{dt}$$

or. $q + h[T_e - T(t)] = \rho C_p L \frac{dT(t)}{dt}$ for $t > 0$

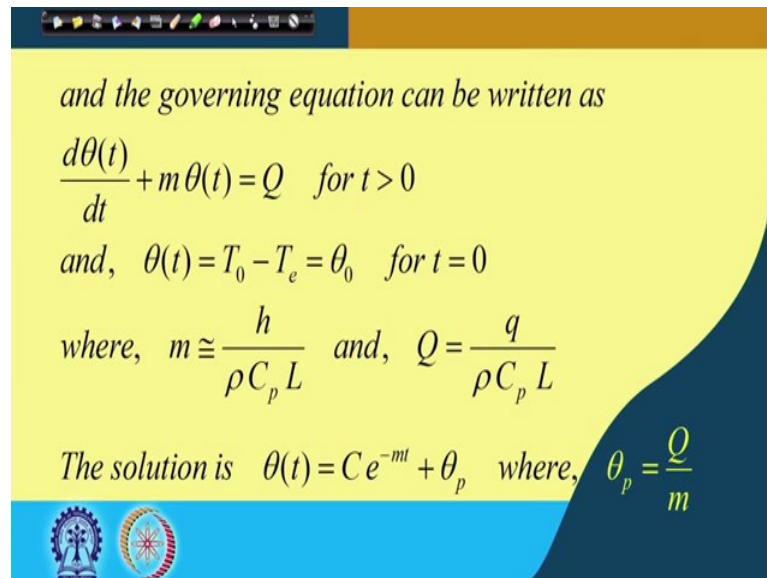
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and the governing equation can be written as

$$\frac{d\theta(t)}{dt} + m\theta(t) = Q \quad \text{for } t > 0$$

and, $\theta(t) = T_0 - T_e = \theta_0$ for $t = 0$

where, $m \cong \frac{h}{\rho C_p L}$ and, $Q = \frac{q}{\rho C_p L}$

The solution is $\theta(t) = C e^{-mt} + \theta_p$ where, $\theta_p = \frac{Q}{m}$

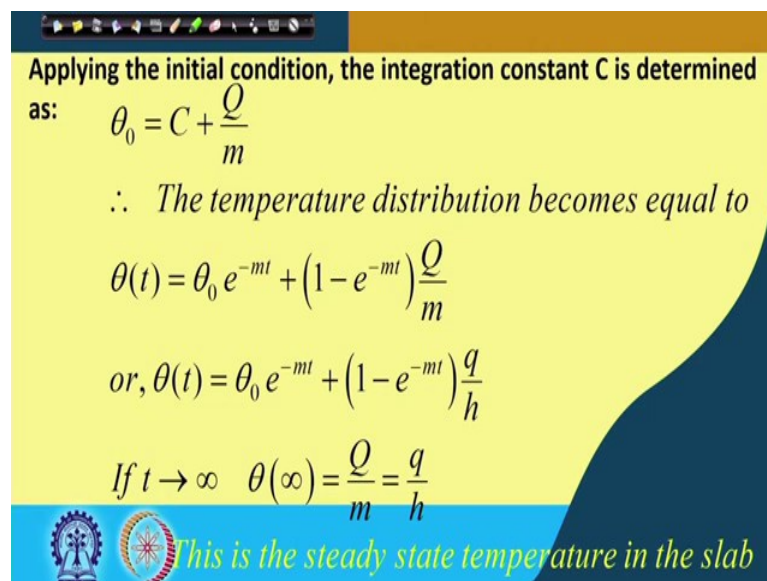
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(Refer Slide Time: 04:51) The solution is $\theta(t) = C e^{-mt} + \theta_p$ where, $\theta_p = \frac{Q}{m}$



Applying the initial condition, the integration constant C is determined as:

$$\theta_0 = C + \frac{Q}{m}$$

\therefore The temperature distribution becomes equal to

$$\theta(t) = \theta_0 e^{-mt} + (1 - e^{-mt}) \frac{Q}{m}$$

or, $\theta(t) = \theta_0 e^{-mt} + (1 - e^{-mt}) \frac{q}{h}$

If $t \rightarrow \infty$ $\theta(\infty) = \frac{Q}{m} = \frac{q}{h}$

This is the steady state temperature in the slab

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And, this is the steady state temperature in the slab that is where theta tends to infinity is the steady state temperature.

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Prob:- An electric iron has a steel base having $\rho = 7800 \text{ kg / m}^3$, $C_p = 400 \text{ J / kg }^\circ\text{C}$, $k = 80 \text{ W / m }^\circ\text{C}$, weight $M = 1.0 \text{ kg}$, ironing surface area $A = 0.03 \text{ m}^2$ is heated from the other surface with a 300 W heating element. The initial temperature of the iron is $T_i = 25 \text{ }^\circ\text{C}$ and the heating starts suddenly. The iron starts dissipating heat by convection from the ironing surface into an ambient at $T_e = 25 \text{ }^\circ\text{C}$ with a heat transfer coefficient $h = 60 \text{ W / m}^2 \text{ }^\circ\text{C}$. What is the temperature of the iron when $t = 5 \text{ min}$ after the start of heating? What would be the equilibrium temperature of the iron if the control did not switch off the current?

An electric iron has a steel base having density $\rho = 7800 \text{ kg/m}^3$, C_p that is specific heat $C_p = 400 \text{ J / kg }^\circ\text{C}$, conductivity $= 80 \text{ W / m}^2 \text{ }^\circ\text{C}$, weight M is 1.2 kg, ironing surface area A is 0.03 meter square, perhaps this problem we have not done. A similar solution might have been, but this problem we have not done, 0.03 meter square is heated from the other surface with a 300 watt per watt heating element.

The initial temperature of the iron is $T_i = 25^\circ\text{C}$ and the heating starts suddenly. The iron starts dissipating heat by convection from the ironing surface into an ambient at T_e is equal to 25°C with a heat transfer coefficient h equal to $60 \text{ W / m}^2 \text{ }^\circ\text{C}$. What is the temperature of the iron when t is 5 minute after the start of the heating? What would be the equilibrium temperature of the iron if the control did not switch off the current?

How it is coming into this unsteady, because you see after time 0 suddenly you have put one iron, which is starting heating, 'right'. That you everybody you or every one of us do that while ironing you put the switch on, 'right'. So, you in that iron down below, there will be some electrical resistance through which this electricity process and by which that $i^2 r$ is that is that element is heated, 'right'.

So, you were heating and then doing the ironing and after doing you forgot to switch it off, 'right'. So, what will be the effect? is it that if that iron will go on increasing the temperature? Perhaps not i.e., what is the problem, that is why it is that a little unsteady and the solution we have to find out through the analytical solution. Because, in this type of thing Biot number will not come into, because hl/k is that if you see it will be very high, it is not less than 0.1. Though here we have not shown typically in this problem, but the solution itself says that it is almost equal to that solution of unsteady and the iron is the example for that, 'right'.

So, if we look at the problem once more then it becomes easier, more clear to you that an electrical iron has a steel base having density of 7800 kg/m^3 , specific heat of $400 \text{ J / kg } ^\circ\text{C}$. So, conductivity k is $80 \text{ W/m}^\circ\text{C}$ weight of the material is 1.2 kg , ironing surface area through which we are ironing you see most of the iron is like that, this end is little constricted and gradually it is expanding, 'right' one end is narrow or pointed so, 'right'.

So, the total area of iron is 0.03 m^2 , heated from the out other surface with a 300 watt heating element. Initial temperature of the iron is $25 \text{ }^\circ\text{C}$ and the heating starts suddenly, because you switched off suddenly or switched on suddenly so, that you can iron it, 'right'.

The iron starts dissipating heat by convection from the ironing surface into an ambient where the temperature is $25 \text{ }^\circ\text{C}$ with a transfer coefficient of $60 \text{ W/m}^2\text{ }^\circ\text{C}$. What is the temperature of the iron when t is 5 minutes you have been ironing you have been put on the switch for 5 minutes your system is on, what will be the temperature?

That is number 1, after the start of the heating, ok. What it would be the equilibrium temperature of the iron, if the control did not switch off the current? If the problem we have defined in a different way actually it is like that.

So, you were doing that ironing sometime after doing that few you have suddenly forgotten to switch off and you left the place, 'right', that is what equivalent to that, what will be the equilibrium temperature of the iron if the control did not switch off the current? That means, you have not switched off the current. If that be the condition what will be the maximum and that is what we call it to be the steady state temperature, because that iron will not go on increasing the temperature, rather then it will become red hot and then suddenly burst like that it does not happen, 'right'. So, that is a real example or real problem which we are solving, 'right'.

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Sol:- The characteristic length dimension is

$$L_s = \frac{V}{A} = \frac{M}{A\rho} = \frac{1}{0.03 \times 7800} = 4.3 \times 10^{-3} \text{ m}$$

The Biot number is

$$Bi = \frac{hL}{k} = \frac{60 \times 4.3 \times 10^{-3}}{80} = 3.2 \times 10^{-3}$$

Applying lumped system analysis,

$$\theta(t) = \theta_0 e^{-mt} + (1 - e^{-mt}) \frac{q}{h}$$

where, $\theta_0 = T_i - T_e = 25 - 25 = 0$

$$q = \frac{300}{0.03} = 10000 \text{ W/m}^2$$

So, we have understood the problem and the solution of heat we can say, that here also we are finding out first

$$L_s = \frac{V}{A} = \frac{M}{A\rho} = \frac{1}{0.03 \times 7800} = 4.3 \times 10^{-3} \text{ m}$$

So, Biot number is 0.003. So, if it is 0.003 similar to that earlier we can use the lamp system, 'right'.

$$Bi = \frac{hL}{k} = \frac{60 \times 4.3 \times 10^{-3}}{80} = 3.2 \times 10^{-3}$$

So, here that lamp system was the solution

$$\theta(t) = \theta_0 e^{-mt} + (1 - e^{-mt}) \frac{q}{h}$$

$$\text{where, } \theta_0 = T_i - T_e = 25 - 25 = 0$$

$$q = \frac{300}{0.03} = 10000 \text{ W/m}^2$$

If that be true initial and the temperature which was there let me see where is the where is the pen with this side I have kept, ok. So, if we see that so, initial temperature was given 25 and environmental temperature is also 25, 'right'. And, the earlier that area was 0.03, conductivity was 80, this we have changed to m and the other things remaining same.

So, we have found out Bi and then now we are finding out the solution this solution we have already found out earlier and Bi we have found out to be equal to $0.3 \cdot 0.2 \cdot 10$ to the power minus 3 that is 0.003, 'right'. So, 0.003 say applying the lumped system analysis, we found out θ is $\theta_0 \cdot e^{-\frac{mt}{hA}}$ plus 1 minus $e^{-\frac{mt}{hA}}$ into q by h , this we have just solved it with the boundary, 'right'. Where θ_0 is $T_i - T_e$ that is 25 minus 25 that is equal to 0, 'right'.

So, θ_0 is 0 and q the value of q which was not given which was given 300 watt that much of supply heat being supplied 300 watt, but q is a flux. So, that is watt per meter square, 'right' so, to get the q what we need to do we have to divide with the area. So, that is what we have done q is 300 by 0.03 that becomes equal to 10000, that is 10,000 watt per meter square, that we have found out. Because we were given that heat is supplied equivalent to 300 watt, 'right'.

So, that 300 watt we are now converting it to the heat flux, which is watt per meter square. So, by dividing that with the area of the heat transfer that is 0.03. So, 300 by 0.3 is nothing, but 10,000, 'right', so that we have found out.

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$h = 60 \text{ W / m}^2 \text{ }^\circ\text{C}$
 $m = \frac{h}{\rho C_p L} = \frac{60}{7800 \times 400 \times 4.3 \times 10^{-3}} = 4.47 \times 10^{-3}$
 $mt = 4.47 \times 10^{-3} \times 5 \times 60 = 1.341$
 $\therefore \theta(t) = (1 - e^{-1.341}) \frac{10000}{60} = 123 \text{ }^\circ\text{C}$
 So, $T(t) = \theta(t) + T_e = 123 + 25 = 148 \text{ }^\circ\text{C}$
 and the equilibrium temperature becomes equal to
 $\theta(\infty) = \frac{q}{h} = \frac{10000}{60} = 166.66 \text{ }^\circ\text{C}$

Now, we have to find out the temperature distribution 'right'.

$$h = 60 \text{ W / m}^2 \text{ }^\circ\text{C}$$

$$m = \frac{h}{\rho C_p L} = \frac{60}{7800 \times 400 \times 4.3 \times 10^{-3}} = 4.47 \times 10^{-3}$$

$$mt = 4.47 \times 10^{-3} \times 5 \times 60 = 1.341$$

$$\therefore \theta(t) = (1 - e^{-1.341}) \frac{10000}{60} = 123 \text{ }^\circ\text{C}$$

$$\text{So, } T(t) = \theta(t) + T_e = 123 + 25 = 148 \text{ }^\circ\text{C}$$

and the equilibrium temperature becomes equal to

$$\theta(\infty) = \frac{q}{h} = \frac{10000}{60} = 166.66 \text{ }^\circ\text{C}$$

So, value of q was watt per unit of q was watt per meter square and unit of h is watt per meter square degree centigrade. So, this goes out; so degree centigrade is the unit. So, that becomes 166.66 degree centigrade. So, the equilibrium temperature; that means, if you have not put the power supply off, then the temperature will rise from 148 to 166 and it will be at that temperature only, 'right'.

Because, why you are not changing the 300 that 3 you remember that, you are not changing the heat source that is 300 watt; that means, that it is i square r, there is i you are not changing, v you are not changing, r you are not changing, so that is fixed. So, correspondingly your watt supply is also 300.

So, it will come to your steady that is 166.66 and where it will remain, if we do not put it up it will not go beyond that temperature, 'right'. So, hopefully we could have explained the situation and we have come to the end of the class for this. So, let us call it a day.

Thank you.