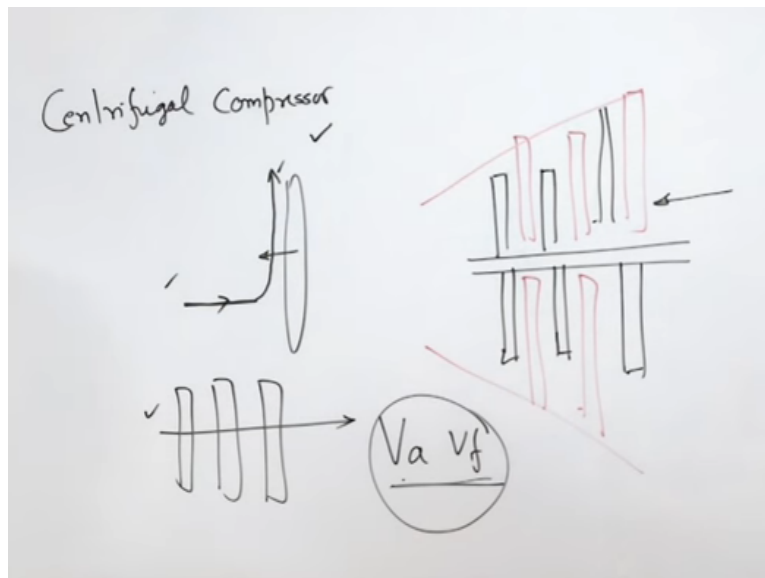


Steam and Gas Power Systems
Prof. Ravi Kumar
Department of Mechanical Industrial Engineering

Indian Institute of Technology - Roorkee
Module No # 08
Lecture No # 37
Axial Flow Compressor

I welcome you all in this course on steam and gas power systems today we shall start with Axial Flow Compressors. In the previous lecture we discussed the centrifugal compressor.

(Refer Slide Time: 00:35)



In centrifugal compressor, the fluid was entering along the shaft. There was an axial entry of the fluid or air and exit was radial. It was entering the compressor, there was an impeller, imparting energy or doing work on the incoming air and then air was compressed and finally, we got high pressure gas or air at the exit of the compressor. Now in axial flow compressor, the movement of the fluid is only in axial direction.

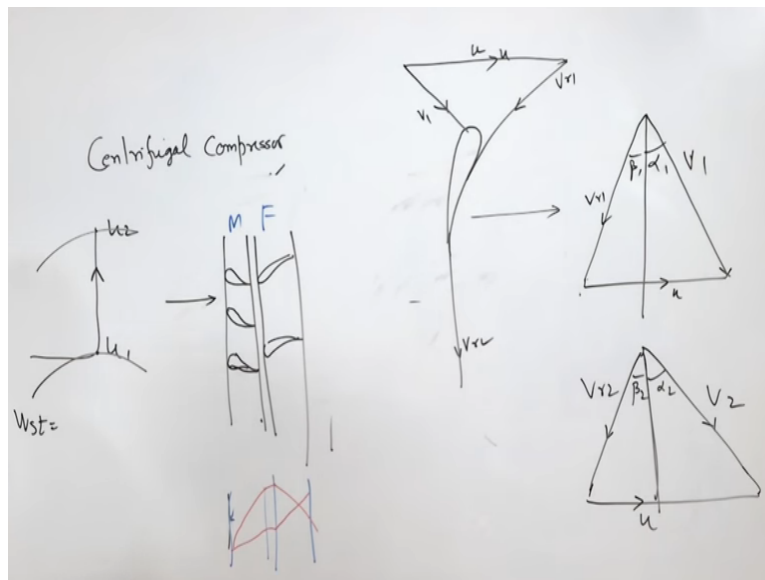
That is why because there is no change in direction that is why the efficiency of axial compressor is more than the centrifugal compressor. In axial compressor also like axial flow turbines, we have done the impulse turbine and impulse reaction turbine like that in axial flow compressor also there is several rings on stages each stage consists of fixed blades and moving blades.

So arrangement is like this only, there is a shaft on the blade are mounted and there are moving blades there are fixed blades also which are mounted in the casing this are fixed blades. So now in this case the energy is consumed by the compressor moves with the help of a motor the shaft rotates in a certain speed, air is sucked in and its gas compressed when it exits from the other end.

So air enters from here right, it will go from first stage, second stage, third stage it is shown converging because we have to maintain constant axial velocity. It is V_A or V_F , for designing the compressor. For the purpose of design of the compressor, this velocity has to remain constant. This direction the pressure is increasing, when the pressure is increasing velocity has to remain constant, will have to reduce the cross section area or size of the compressor.

That is why it is known to shown as converging passage right, it has number of the stages. Stages may go up to 18, 20, and 25. In this compressor if we look at the stages different stages, let us examine one stage of axial flow compressor.

(Refer Slide Time: 03:40)



So each stage has fixed blade and the moving blades. Suppose there is a fixed blade like this and then there is small gap between these two and then there is a moving blade. So there number of fixed blades and there is a number of moving blades and they have mounted on the shaft, the

shaft is parallel to this board and it rotates with a certain rotational speed. And the air moves in this direction axial flow direction.

Now in this compressor like impulse turbine, if it works as an impulse turbine then there is no pressure rise in moving blades. There is only pressure rise in fixed blades it works as a impulse turbine. That is in fix, these are fixed blades they are moving blades. Regarding velocity there will definitely increase in moving blades because the kinetic energy will be imparted to the moving air and these acts as a diffuser so velocity gets reduced.

But normally the axial flow compressors they work as reverse of impulse reaction turbine not impulse reaction turbine reverse of that. So here the pressure there is a pressure rise, if we see the pressure rise so there is pressure rise in moving blades and fixed blade as well and regarding the velocity the velocity increases in moving blades and it falls in fixed blade. Now first of all we will what will do will draw a velocity diagram for axial flow turbine then that will make things clearer.

So there is a blade in a axial compressor not turbine axial flow compressor velocity diagram for an axial flow compressor, the air is supposed to glide over the surface right. When the blade is moving in this direction, air is supposed to glide over the surface so this is VR_1 right and the blade is moving with certain velocity in this direction. So it is U , here we do not have V_1 and V_2 in centrifugal compressor because the radial flow.

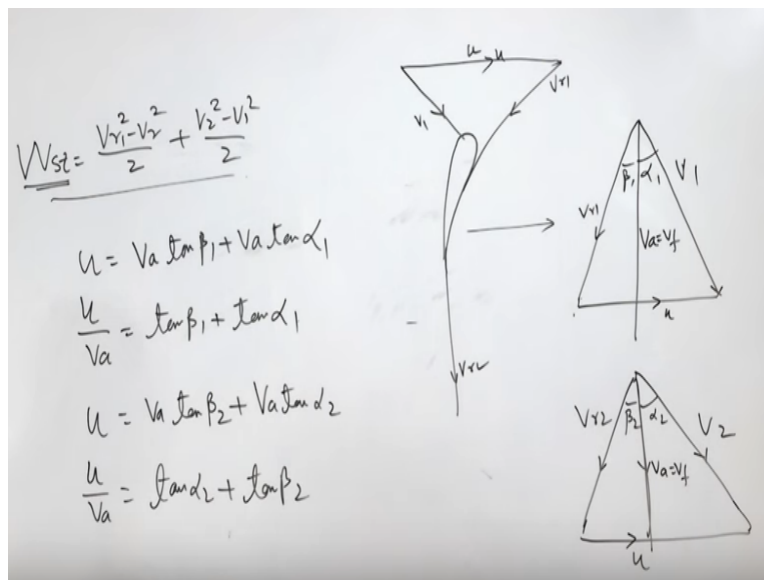
So we had U_1 and U_2 different peripheral velocity at the impeller. This inner diameter of the impeller and the outer diameter of the impeller because flow is taking place in axial direction. So there is only one peripheral velocity that is U and this is the absolute velocity of air through which it will be entering the blade. So in axial flow turbines the angles are the axis taken in the shaft axis is taken as a reference.

In earlier in I mean in the reaction turbine or impulse reaction turbine, the peripheral direction of the peripheral velocity was taken as a plane of reference right. Here axial flow, axial direction is taken as plane of reference. So axial direction, when we take as a plane of reference then this

becomes V_1 right and this is VR_1 velocity U is this and is the velocity U is perpendicular to the axis of the shaft.

Now this is V_1 , this is VR_1 this is U , so this is angle α_1 , this is angle β_1 one regarding exit. Also regarding exit also the triangles are like this because this is VR_2 right. So regarding axis also this is V_2 and this is VR_2 . This is α_2 and this is β_2 and this is U and this is V_1 , V_2 . Now here in axial flow compressor, there is one more thing to discuss the work in a stage, is equal to axial flow compressors.

(Refer Slide Time: 09:26)



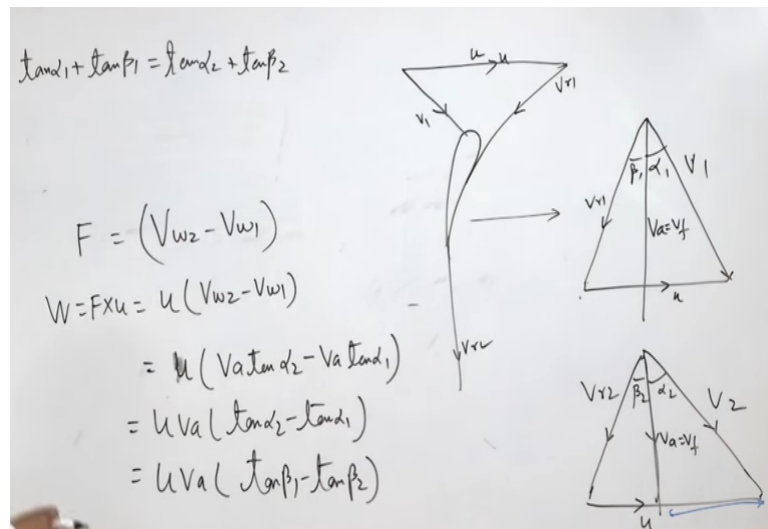
The work in a stage = VR_1 square - VR_2 square divide by 2 + V_2 square - V_1 square divide by 2, here peripheral velocity component is missing because there is nothing like U_1 and U_2 . There is only one constant peripheral velocity so energy imparted to the fluid by virtue of changing peripheral velocity is 0. So if we look at this then per stage work in axial flow system we can say is less than the per stage work in centrifugal compressors.

Now here this is axial velocity V_A or it is velocity of flow also V_A velocity of flow right. So U is equal to, if we take these two triangles then $U = V_A \tan \beta_1 + V_A \tan \beta_2$ or we can say U by $V_A = \tan \beta_1 + \tan \beta_2$. Similarly for this triangle $U = \beta_1$ and α_1 this is α_1 not $\tan \alpha_1$. Now in this triangle $V_A \tan \beta_1$, $\beta_2 + V_A \tan \alpha_2$.

So again we can take $U = V_1 \tan \alpha_2 + \tan \beta_2$ or we can say that these two if we compare these two then $\tan \alpha_1 + \tan \beta_1 = \tan \alpha_2 + \tan \beta_2$. So this relation is frequently used in analyses of axial flow compressors now we will calculate the tangential force required to compress the gas.

(Refer Slide Time: 12:11)

Tangential
 V_{w1} for the
 one kg per
 will be
 mass flow
 work is F
 V_{w1} and
 component

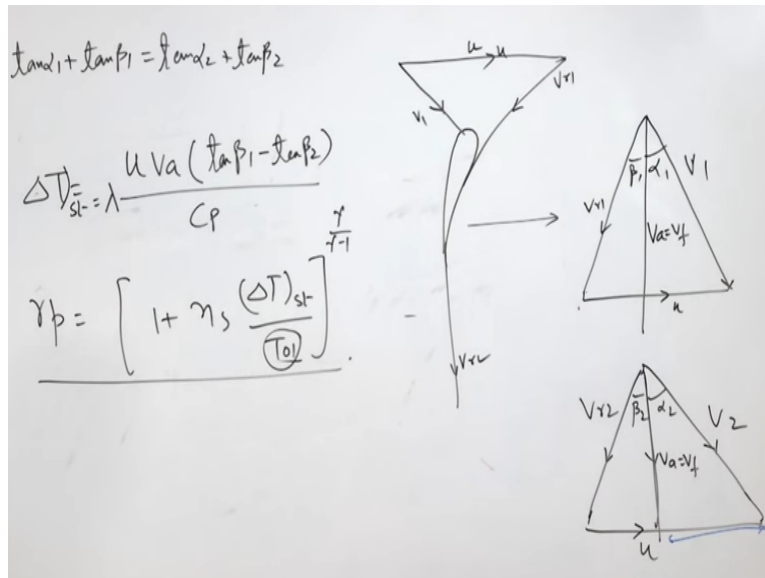


force is V_{w2} -
 mass flow rate of
 second, otherwise it
 multiplied by the
 rate. Also and then
 into $U = U V_{w2} -$
 V_{w1} is will
 at angle. This 1

$V_{w2} = V_2 \sin \alpha_2$ so U is there $V_2 \tan \alpha_2$, V_2 is axial velocity - $V_2 \tan \alpha_1$, and then we can say it is $U V_2 \tan \alpha_2 - \tan \alpha_1$.

If we use this analyzation then work is $U V_2 \tan \alpha_2 - \tan \alpha_1 \tan \beta_1 - \tan \beta_2$. So either of these expressions can be used for finding out work done on the gas or air during compression in an axial flow compressor. Now temperature change in a stage because in compressor normally we have to find the temperatures and different stages.

(Refer Slide Time: 14:13)



So temperature change in a stage $\Delta T =$ we will take the work $\tan \beta_1 - \tan \beta_2$, let us say $\tan \beta_1$ and $\tan \beta_2$, and ΔT per stage is $C_p \Delta T$. So divided by C_p that will give the change in temperature in a stage, there is an expression we will discuss it later on, that is work done factor it will be multiplied by then you want to have an actual temperature rise. It will be multiplied by the work done factor and if you want to have pressure ratio in the stage that is going to be $1 + \left(\frac{\Delta T}{T_0} \right)^{\frac{\gamma}{\gamma-1}}$ (15:03) of the stage.

ΔT stage divided by $T_0 \left(\frac{\gamma}{\gamma-1} \right)$ we have taken stagnation temperature at inlet because we have considered the kinetic energy also. So when we consider the kinetic energy is converted into the pressure energy so this will result in the rise in temperature. So this is the expression for pressure ratio in a stage now we will do the pressure rise, so what we have calculated done so far.

(Refer Slide Time: 15:41)

- Working principle
- Velocity diagram
- Work output
- Pressure rise and aerodynamic force
- Worked example

We have just discussed the working principle, we have discussed the velocity diagram, we have discussed the work output. Now pressure rise in aerodynamic force in a stage of axial flow compressor.

(Refer Slide Time: 15:56)

The image shows a handwritten derivation of the pressure rise and aerodynamic force in a stage of an axial flow compressor. The derivation starts with Bernoulli's theorem:

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} = \frac{P_2}{\rho} + \frac{V_2^2}{2}$$

$$\Delta P = \frac{1}{2} \rho (V_1^2 - V_2^2)$$

$$= \frac{1}{2} \rho (V_a^2 + V_{w1}^2 - V_a^2 - V_{w2}^2)$$

$$= \frac{1}{2} \rho (V_{w1}^2 - V_{w2}^2)$$

$$\Delta P = \frac{1}{2} \rho V_a^2 (\tan^2 \alpha_1 - \tan^2 \alpha_2)$$

$$F_x = s l_b \rho V_a^2 (\tan \alpha_1 - \tan \alpha_2) \tan \alpha_m$$

Two velocity diagrams are shown on the right. The top diagram is for the inlet stage, showing a velocity triangle with axial velocity V_a , tangential velocity V_w , and resultant velocity V_1 . The angle between the axial velocity and the resultant velocity is α_1 . The bottom diagram is for the outlet stage, showing a velocity triangle with axial velocity V_a , tangential velocity V_w , and resultant velocity V_2 . The angle between the axial velocity and the resultant velocity is α_2 .

So we will start with Bernoulli's theorem, P_1 by $\rho = V_1$ square by 2 = P_2 stage divided by $\rho + V_2$ square by 2 because it is moving in horizontal direction prudentially production energy is 0. So ΔP is half ρV_1 square - V_2 square ΔP .

This minus this = half ρV_1 square - V_2 square = half ρ , now if you draw again this diagram this is V_1 V_{R1} U β_1 α_1 , So ash this is V_w and this is V_a . So it is V one is V_a

square + VW square in same fashion, if we take into account this diagram Alpha 2 Beta 2 VR2 V2 and U. Here also the V2 square is VA square - VW square and then this will be cancelled out it is going to be half Rho.

VW 1 square - VW2 square or it is half Rho VA square and the VW is nothing but VA Tan Alpha 1. So Tan square Alpha 1 - Tan square Alpha 2. So only axial velocity is with us and density is with us. We can find the pressure rise in this stage, so axial force now once we have the pressure rise pressure multiplied by area will give the force.

So axial force is SLB is the length of the blade Rho VA square Tan Alpha 1 - Tan Alpha 2 Tan Alpha 1 + Tan Alpha 2 divided by 2 or this is mean blade angle Alpha 1 Tan Alpha one plus Tan Alpha 1. So we can replace this by Tan Alpha M it is not the angle of mean of the angle but mean of the Tans of the angle so this is axial force. Now the compressor will also experience.

(Refer Slide Time: 19:17)

The image shows a handwritten derivation of axial force and two velocity triangles. The derivation starts with the axial force equation:

$$F_{axis} = \dot{m} (V_{w1} - V_{w2})$$

$$= \rho V_a \sin \alpha \rho (V_{w1} - V_{w2})$$

$$F = \int \rho V_a^2 \sin \alpha (\tan \alpha_1 - \tan \alpha_2)$$

$$= \frac{1}{2} \rho (V_a^2 + V_{w1}^2 - V_a^2 - V_{w2}^2)$$

$$= \frac{1}{2} \rho (V_{w1}^2 - V_{w2}^2)$$

$$\Delta P = \frac{1}{2} \rho V_a^2 (\tan^2 \alpha_1 - \tan^2 \alpha_2)$$

$$F_x = S L_b \rho V_a^2 (\tan \alpha_1 - \tan \alpha_2) \tan \alpha_m$$

Two velocity triangles are shown on the right. The top triangle is for stage 1, with axial velocity V_a , tangential velocity V_{w1} , and angle α_1 . The bottom triangle is for stage 2, with axial velocity V_a , tangential velocity V_{w2} , and angle α_2 . A note indicates $\frac{F_x}{F_{axis}} = \tan \alpha_m$.

The willing force which is perpendicular to this one sorry this is an compressor, so compressor will have the force will be exerted in the axial direction force will also be exerted in willing direction and that force is mass flow rate multiplied by VW 1 - VW2 and that is V F S L N Rho. This is volume, this is density VW1 - VW2 and the net energy consumed by the axial flow compressor will be Pythagorean sum of this means net force.

It is going to be equal to under root this force square of this plus square of this and the direction of the force will be the ratio of these two and that is going to be, this F_X divided by F_{WSIFX} divided by $FWIS$ and that is going to be = $\tan \alpha_M$ because these terms will be cancelled out this is V_A . So these terms will be cancelled out and we will be getting the ratio of these two as $\tan \alpha_M$.

Now before dividing it we can write V_F or V_A square S length of the blade, $\rho V W 1$ is the V_1 that is why square has come here. This is $\tan \alpha_1 - \tan \alpha_2$ now they will be cancelled, now if we take the ratio of this and in order to find the direction then we will get all this terms. They will be cancelled out and this will also be cancelled out and what we are going to get is $\tan \alpha_M$.

So we have calculated work force required in a axial direction to compress the gas force required in the peripheral direction. This is the force in axial direction, this is the force in peripheral direction and then Pythagorean sum of these two forces will give the net force required for compressing the gas and there ratio will give the direction right. Now we will solve one worked example of axial flow compressors.

(Refer Slide Time: 22:33)

Calculate the pressure rise and work done by a rotating cascade of axial flow compressor for following data:
 $u = 200 \text{ m/s}$, $V_f = 186 \text{ m/s}$, $\alpha_1 = 45^\circ$, $\alpha_2 = 14^\circ$, $\rho = 1 \text{ kg/m}^3$
 Assume isentropic compression.

Calculate the pressure rise and work done by rotating cascade of axial flow compressor for following data peripheral velocity 200 meters per second flow, velocity is or V_A axial velocity is

186 meter per second and Alpha 1 and Alpha 2 are given Rho = 1, that is density of air or working fluid assume isentropic compression.

(Refer Slide Time: 22:58)

The image shows handwritten mathematical derivations for pressure rise and work done. The first part calculates the pressure rise ΔP using the formula $\Delta P = \frac{1}{2} \rho V_f^2 (\tan^2 \alpha_1 - \tan^2 \alpha_2)$. Substituting $\rho = 1$, $V_f = 186$, $\alpha_1 = 45^\circ$, and $\alpha_2 = 14^\circ$, the result is $\Delta P = 16.22 \text{ kPa}$. The second part calculates the work done W using the formula $W = U V_f (\tan \alpha_1 - \tan \alpha_2)$. Substituting $U = 200$, $V_f = 186$, $\alpha_1 = 45^\circ$, and $\alpha_2 = 14^\circ$, the result is $W = 27.9 \text{ kW}$.

$$\Delta P = \frac{1}{2} \rho V_f^2 (\tan^2 \alpha_1 - \tan^2 \alpha_2)$$
$$\Delta P = \frac{1}{2} \times 1 \times 186^2 (\tan^2 45 - \tan^2 14)$$
$$= \underline{16.22 \text{ kPa}}$$
$$W = U V_f (\tan \alpha_1 - \tan \alpha_2)$$
$$= 200 \times 186 (\tan 45 - \tan 14)$$
$$= \underline{27.9 \text{ kW}}$$

So Delta T pressure rise is half Rho PF square Tan square Alpha 1 - Tan square Alpha two we have already done that. Now here Delta P = half Rho is given here one velocity of flow is 186 square Tan square Alpha 1 is 45 - Tan square Alpha 2 is fourteen and this case the pressure rise as 16.22 kilopascal that is the pressure rise.

Calculate the pressure rise at work done by rotating so work done is UVF tan alpha 1 - Tan Alpha 2. Simply we will put the values U is 200 meters per second, 200 - VF1 8645 - Tan 14 and this give will the work done as 25.9 kilowatt. This is the work or energy consumed by compressor in for the movement of air or for the compression of air and after this we will take another numerical which is a little lengthier.

(Refer Slide Time: 25:01)

In an eight stage axial flow compressor the over all pressure ratio is 5:1 and the over all efficiency is 90%. The temperature and pressure at inlet is 20 °C and 100 kPa. The work is divided equally between the stages. The mean blade velocity is 175 m/s and 50% reaction design is used. The axial velocity through the compressor is constant and is equal to 100 m/s. Calculate the power required and blade angles.

In eight stage axial flow compressor, so there is a axial flow compressor consisting of eight stages the overall pressure ratio is 5 is to 1. So compressor has number of stages right and cumulative effect of pressure rise is 5 is to 1 and the overall efficiency of the compressor is 90% the temperature and pressure at inlet will write down here. So that later on time is saved, so the temperature and pressure at the inlet.

(Refer Slide Time: 25:10)

$t_1 = 20^\circ\text{C} = 273 + 20$
 $T_1 = 293\text{K}$
 $P_1 = 100\text{ kPa}$
 $u = 175\text{ m/s}$
 $R = 50\%$
 $T_{02} = 464$
 $\alpha_1 = \beta_2$
 $\alpha_2 = \beta_1$
 $V_f = V_a = 100\text{ m/s}$
 $Z = 8$

$$\frac{T_{02}}{T_{01}} = \left(\frac{P_{02}}{P_{01}}\right)^{\frac{\gamma-1}{\gamma}}$$

$$T_{02} = T_{01} \left(\frac{P_{02}}{P_{01}}\right)^{\frac{\gamma-1}{\gamma}} = 293 (5)^{0.286} = 464\text{ K}$$

So $T_1 = 20$ degree or 293 Kelvin we will just add 273, here $273 + 20 = 293$ Kelvin that is T_1 and 100 kilopascal pressure $P_1 = 100$ kilopascal. The work is divided equally between the stage, so each stage on each stage same amount of work is being done on the gas. The mean blade velocity is 175 meters per second and 50% reaction design is used.

When there is a reaction is 50% then $\alpha_1 = \beta_2$ and $\alpha_2 = \beta_1$ as we did in the case of turbine, same thing will be done here. Also in axial flow compressor, if the degree of reaction is 50%. Then this nozzle inlet angle is equal to blade outlet angle and nozzle outlet angle is equal to blade inlet angle.

The axial velocity throughout the compressor is constant is equal to or $V_F = V_A = 100$ meters per second okay. So we assume that eight how many stages are there eight stages though Z is denoted by this stage. So $Z = 8$ there is a pressure rise in each stage and the temperature at the outlet of the compressor T_{OZ} by T_{O1} to Z means after the eighth stage that is P_{OZ} by P_{O1} raise to power $\gamma - 1$ over γ .

If the compression index is not given we assume it to be γ . So $T_{OZ} = T_{O1} P_{OZ}$ by P_{O1} raise to power $\gamma - 1$ over γ because index of compression is not given. We will assume it to be $\gamma = 1.4$ T_{O1} is 293 P_{OZ} by P_{O1} is 50.986 this $\gamma = 1.4 - 1$ divided by $1.4 = 0.286$.

So directly we have put the values and the T_{OZ} , we are getting 464 Kelvin. So T_{OZ} 464 Kelvin and the compression is not isentropic because the efficiency is given is 90% overall efficiency is 90%.

(Refer Slide Time: 28:25)

$$\begin{aligned}
 t_1 &= 20^\circ\text{C} = 273 + 20 \\
 T_1 &= 293\text{K} \\
 P_1 &= 100\text{ kPa} \\
 u &= 175\text{ m/s} \\
 R &= 50\% \quad T_{02} = 464\text{K} \\
 \alpha_1 &= \beta_2 \quad T_{02}' = 483\text{K} \\
 \alpha_2 &= \beta_1 \\
 V_f &= V_a = 100\text{ m/s} \\
 Z &= 8
 \end{aligned}$$

$$\begin{aligned}
 \eta_0 &= \frac{T_{02} - T_1}{T_{02}' - T_1} \\
 T_{02}' &= T_1 + \frac{T_{02} - T_1}{\eta_0} \\
 &= 293 + \frac{464 - 293}{0.9} \\
 &= 483\text{K}
 \end{aligned}$$

So = $T_{02} - T_1$ divided by $T_{02}' - T_1$ $T_{02}' = T_1 + T_{02} - T_1$ divided by T_1 is $293 + T_{02}$. We have taken as $464 - 293$ divided by $.9$ and that gives T_{02}' as 483 Kelvin. So T_{02}' is 483 Kelvin same thing. We have done as we did earlier also.

(Refer Slide Time: 29:24)

$$\begin{aligned}
 t_1 &= 20^\circ\text{C} = 273 + 20 \\
 T_1 &= 293\text{K} \\
 P_1 &= 100\text{ kPa} \\
 u &= 175\text{ m/s} \\
 R &= 50\% \quad T_{02} = 464\text{K} \\
 \alpha_1 &= \beta_2 \quad T_{02}' = 483\text{K} \\
 \alpha_2 &= \beta_1 \\
 V_f &= V_a = 100\text{ m/s} \\
 Z &= 8
 \end{aligned}$$

$$\begin{aligned}
 W &= CP (T_{02}' - T_{01}) \\
 &= (V_{w2} - V_{w1}) u Z \\
 W &= V_f (T_{02}' - T_{01}) u Z \\
 T_{02}' - T_{01} &= 13639
 \end{aligned}$$

Now work is if we take as a thermodynamic process then work = $CP, T_{02}' - T_{01}$. This is the work done on the gas and this is equal to $V W_2 - V W_1$ multiplied by U that is one in one stage multiplied by number of stages. This is the work, this is not the work in the entire compressor because this will component is only for one stage. So this work multiplied by the peripheral velocity multiplied by the work number of stages.

This will give $V_f \tan \alpha_1 - \tan \alpha_1 U_Z$ okay. Now here we can get the value of $\tan \alpha_2 - \tan \alpha_1$ because this is = W . Now here we have the value of T_{OZ} dash 483 Kelvin to 1293 Kelvin and U is also given 175 meters per second.

So this is 175 and this one is 474 and T_{O1} is 293 and this is equal to this one both are equal from here we will get the value of $\tan \alpha_2 - \tan \alpha_1$ and $\tan \alpha_2 - \tan \alpha_1$ is 1.3639 okay. That is equation one, and second and second third second one.

(Refer Slide Time: 31:51)

$t_1 = 20^\circ\text{C} = 293 + 20 = 293\text{K}$
 $T_1 = 293\text{K}$
 $P_1 = 100 \text{ kPa}$
 75 m/s
 $\beta_1 = 57.4^\circ = \alpha_2$
 $\alpha_1 = 10.95^\circ = \beta_2$
 $T_{OZ} = 464\text{K}$
 $T_{OZ}' = 483\text{K}$
 $\tan \beta_1 = \frac{1.3639 + 1.75}{2}$
 $\beta_1 = 57.4^\circ$
 $\tan \alpha_2 - \tan \alpha_1 = 1.3639$

We know that $U = V_f \tan \alpha_1 + \tan \beta_1$ if you look at the velocity triangle α_1 and this is β_1 and this is V_1 V_{R1} and this is U . So $U =$ this is V_f . So $U = V_f \tan \alpha_1 + \tan \beta_1$ or $U = 175$ and V_f is $100 = \tan \alpha_1 + \tan \beta_1$ and this = $\tan \alpha_1 + \tan \beta_1 = 1.75$ by 100 .

Now add these two you will get $\tan \alpha_2$ minus plus $\tan \beta_1$. So if you add these two this will be cancelled out if you add these two, then this will be cancelled out then $\tan \beta_1 + \tan \alpha_2 = \tan \beta_1 + \tan \alpha_1$ and $\beta_2 = \beta_1 = \alpha_2$. So we can comfortably say that $\tan \beta_1 = 1.3639 + 1.75$ divided by 2 and from here we will get the value of β_1 and the β_1 is 57.4 degree. So β_1 is 57.4 degree.

Now once we have the value of Beta 1, we can either take the equation from either of the equation. We can calculate the value of which angle is required Kelvin power required blade angles. So Beta 1 is with us, we can calculate the value of Alpha 1 and once Alpha 1 Beta 1 are with us. We can find the value of Alpha 2 and Beta 2. So here the Alpha 1 is 10.95 degree it is = Beta 2 and this is equal to Alpha 2.

So all blade angles are known here that is all for today and in the next class we will start with the characteristics of axial flow compressors.