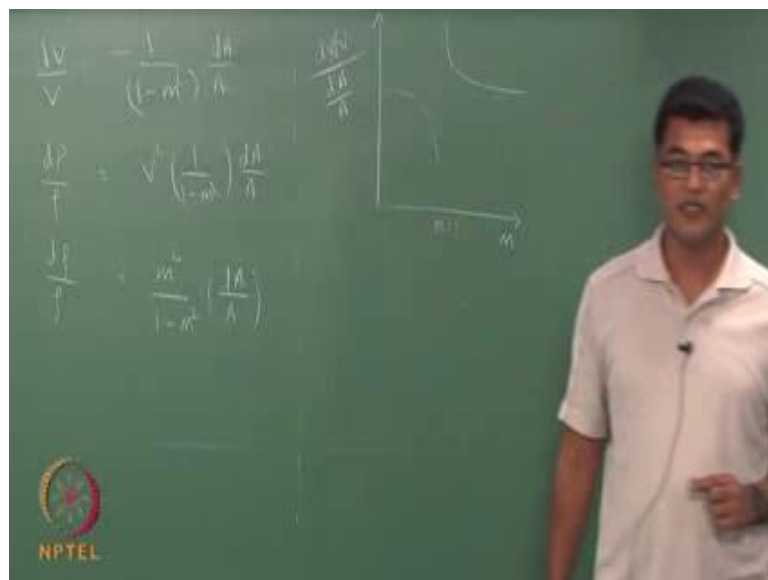


Fundamentals of Gas Dynamics
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Week – 05
Lecture – 15
Variable Area Adiabatic flow (cont'd)

This lecture is the continuation of variable area adiabatic flow. And we will try to see if the change in area can be represented in terms of Mach number, ok that is our aim. So, I will write the equations which we had seen in the other day.

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So, the first equation which we seen is this so will try to see how this quantity is varying with respect to mach number. So, if I take $\frac{dV}{V}$ by $\frac{dA}{A}$, this will vary according to this equation, which is going to be, some discontinuity happens at M equal 1. So, you would see something like this. So, if I have M in my x axis, and this quantity in my y axis I would get something. So, at M equals 1 there is something, that is happening which we had seen at M equals 1 there is no area change. So, can we use that information to get a reference value, or can we represent the changes in area in terms of M , at that area where there is no change in area due to the velocities. So, that is our aim.

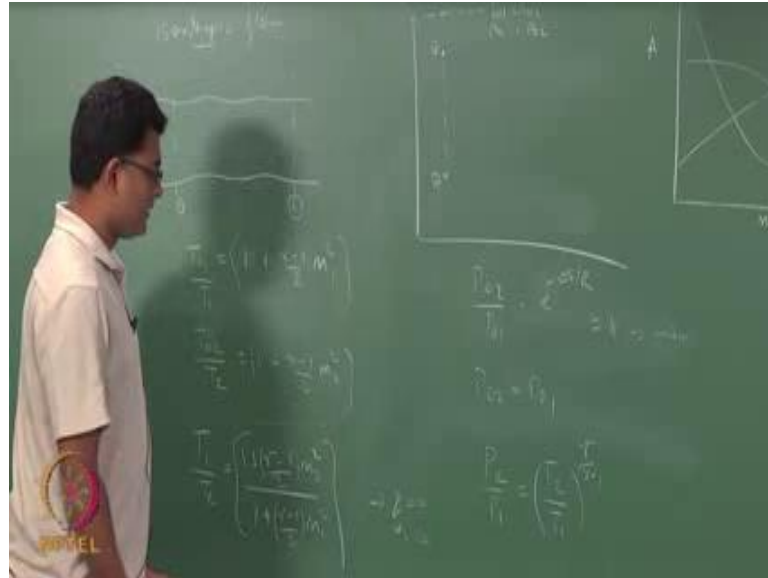
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So, if I plot m versus a , I would have a minimum at m equals 1 because that is the value where $d a$ is zero. So, my velocity would also go something like this, and the density would come down something like this. So, this is my area, this is my velocity this is my density or pressure. So, we will use these information what all we have learned in the other class, to evaluate the changes in area. So, this happens for some arbitrarily shaped body, whose areas changing. We have assumed q to be zero, w is to be zero, and evaluating this, and these flows are, we have also used the energy equation to get this relation. So, with this condition is what we are going to evaluate the area changes. So, for some particular area ratio can we describe this in terms of mach number.

So, I would start for an isentropic flow.

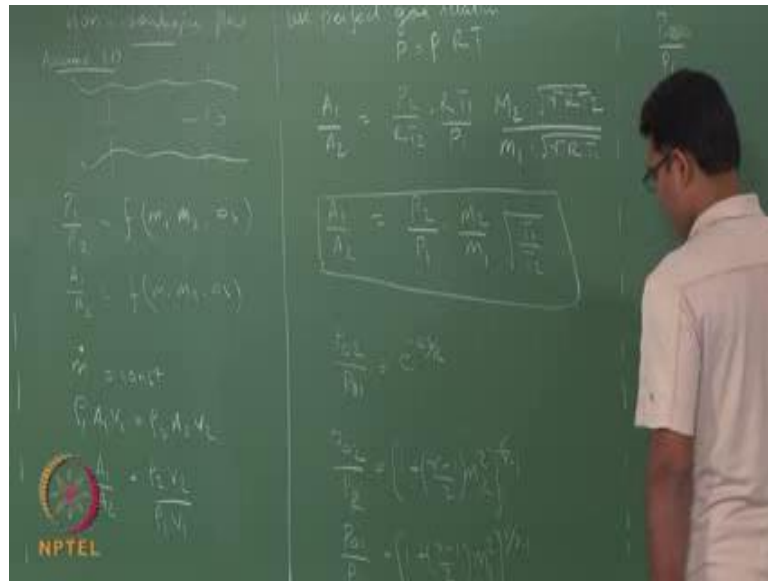
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Some flow at section 1 section 2, how did we see the process in the ds diagram, because it is an isentropic flow, we have $ds = 0$; say let say 1 has g_1 to 2 isentropically, associated with 1 I have a stagnation point, which 2 also I have a stagnation point, since it is isentropic $t_0 1$ equal $t_0 2$ and $p_0 1$ equals $p_0 2$. So, if I use that information t_1 we have $t_0 1$ by t_1 to be $1 + \frac{\gamma-1}{2} m_1^2$. Likewise point 2 has this relation. So, this is the isentropic process that happens at state 1, where the fluid is taken to a velocity 0 isentropically.

So, this relation holds. The same thing happens at station 2; this relation holds, because we know $t_0 1$ equals $t_0 2$ I can rewrite this equation in terms of t_1 and t_2 along. So, here we assumed w_q equals 0 w_s equals zero. and we have also seen $p_0 1$ $p_0 2$ by $p_0 1$ to be $e^{-\frac{\Delta s}{r}}$ which is now assumed 1, so your $p_0 2$ the same as $p_0 1$. So, this is isentropic. So, you can use isentropic relations here to find, say p_2 by p_1 equals t_2 by t_1 to the power $\frac{\gamma}{\gamma-1}$, which again you can write it in terms of m_1 and m_2 , but now if it is not isentropic.

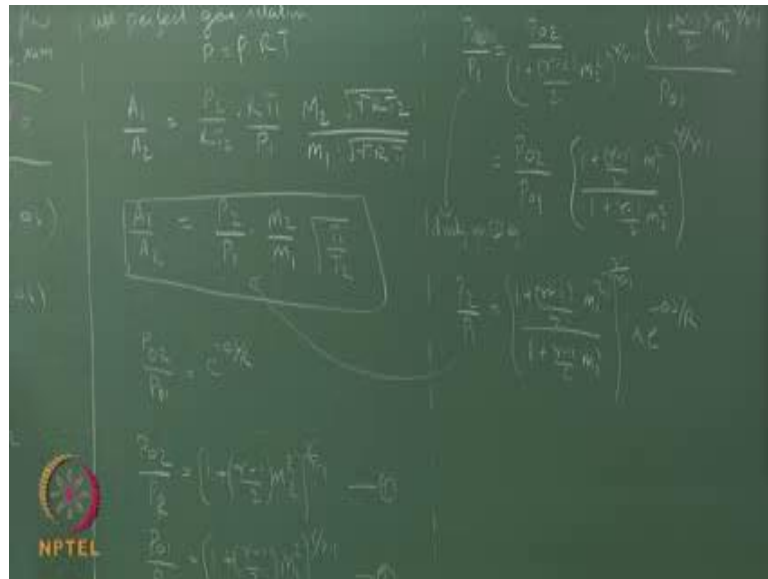
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Let us consider a non isentropic flow. So, I have a flow here, my ratio p_1 by p_2 will be a function of m_1 m_2 and Δs and of course, γ or r . If that is true then my a_1 by a_2 also depends on m_1 m_2 and Δs . My $m \cdot$ is constant. So, I can write $\rho_1 a_1 v_1$ equals $\rho_2 a_2 v_2$, assume 1 d flow. So, if I write, if I want to find a_1 by a_2 , I would write $\rho_2 v_2$ by $\rho_1 v_1$. Now I substitute ρ_1 and v_1 from perfect gas relation. So, my a_1 by a_2 is replaced by ρ_2 , as p_2 by $r t_2$ multiplied by $r t_1$ by p_1 into v_2 is replaced as m_2 into a_2 is $\gamma r t_2$ divided by $m_1 \cdot \gamma r t_1$, which gives me a relation p_2 by p_1 into m_2 by m_1 into root of t_1 by t_2 .

So, between the process p_1 and p_2 , I have this. There is entropy change, between location 1, and 2, $p_0 2$ by p_1 is $1 + \gamma$ minus 1 by $2 m_2$ square to the power γ by γ minus 1 . Likewise I have $p_0 1$ by $p_0 p_1$ equals $1 + \gamma$ minus 1 by 2 into m_1 square to the power γ by γ minus 1 . Now I use these three relation to write; p_2 by p_1 . So, p_2 by p_1 , p_2 by p_1 as $p_0 2$ by $1 + \gamma$ minus 1 by $2 m_2$ square to the power γ by γ minus 1 into p_1 is $1 + \gamma$ minus 1 by $2 m_1$ square to the power γ by γ minus 1 divided by $p_0 1$ which are replace it as $p_0 2$ by $p_0 1$ in $1 + \gamma$ minus 1 by $2 m_1$ square divided by $1 + \gamma$ minus 1 by $2 m_2$ square to the power γ by γ minus 1 .

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So, I taken this 2 relation, I divided 2 by 1. So, this is dividing equation 2 a 1 now I replace $p_0 2$ by $p_0 1$ with this relation. So, my p_2 by p_1 is $1 + \gamma - 1$ by $2 m_1$ square divided by $1 + \gamma - 1$ by $2 m_2$ square to the power γ by $\gamma - 1$ into e power minus Δs by r . So, this is the pressure ratio p_2 by p_1 with this. So, if it is an isentropic flow, this is 1, and hence you would get this relation which is same as what you have got from your isentropic relation from t_1 and t_2 . Now, I substitute this into this t_1 and t_2 anyway I can get it from that relation. So, there is there is no q , no w s . So, t_1 by t_2 has this equation, where you have obtained using isentropic relation, but p_1 by p_2 there is an reversibility irreversibility and hence you have to use this equation.

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So, I am rewriting that equation here; a_1 by a_2 is p_1 . instead of p_2 by p_1 I replace that with this equation m_2 by m_1 . now root of t_1 by t_2 I use this equation, which t_1 by t_2 is $1 + \frac{\gamma - 1}{2} m_2^2$ divided by $1 + \frac{\gamma - 1}{2} m_1^2$, which into $\frac{p_1}{p_2} = \frac{p_1}{p_2} \left(\frac{1 + \frac{\gamma - 1}{2} m_2^2}{1 + \frac{\gamma - 1}{2} m_1^2} \right)^{\frac{\gamma}{\gamma - 1}}$. So, this I can reduce it further to $1 + \frac{\gamma - 1}{2} m_1^2$ square divided by $1 + \frac{\gamma - 1}{2} m_2^2$ square to the power to the power $\frac{\gamma}{\gamma - 1}$, there is a $1 + \frac{\gamma - 1}{2}$ here there is a $1 + \frac{\gamma - 1}{2}$ there that is the root of t_1 by t_2 . So, there is a $1 + \frac{\gamma - 1}{2}$ there. So, this would be $\frac{p_1}{p_2} = \frac{p_1}{p_2} \left(\frac{1 + \frac{\gamma - 1}{2} m_1^2}{1 + \frac{\gamma - 1}{2} m_2^2} \right)^{\frac{\gamma}{\gamma - 1}}$. So, this would be $\frac{p_1}{p_2} = \frac{p_1}{p_2} \left(\frac{1 + \frac{\gamma - 1}{2} m_1^2}{1 + \frac{\gamma - 1}{2} m_2^2} \right)^{\frac{\gamma}{\gamma - 1}}$. So, this $\frac{p_1}{p_2}$ is $\frac{p_1}{p_2} \left(\frac{1 + \frac{\gamma - 1}{2} m_1^2}{1 + \frac{\gamma - 1}{2} m_2^2} \right)^{\frac{\gamma}{\gamma - 1}}$ into m_2 by m_1 into $e^{-\frac{\gamma - 1}{2} m_2^2}$ by $e^{-\frac{\gamma - 1}{2} m_1^2}$ which is my a_1 by a_2 .

So, my area ratio is a function of m_1 , m_2 , γ and r and Δs . So, it is depends on the fluid m_1 , m_2 and your irreversibility. So, if this is the area ration, you can try to see if there is a reference quantity with this. So, I am going to introduce a new reference quantity which is called A^* . The star condition is like our stagnation point star condition is when fluid is isentropically taken to $m = 1$ condition, which means in the $t-s$ diagram from point 1. So, I have a state 1, I take it to velocity 0 is my stagnation

point. So, if I take the point isentropically to v equals zero, then I get my stagnation point. So, this is my m equals zero. Now instead of m equals 0 if I take it to m equals 1. So, let say somewhere here; then I have my star condition. So, I take it isentropically that is very important.

So, if you can actually take the flow to m equals 1 in hundred different ways, but the 1 that is, that you are talking about is when it when it is reduced to m equals 1 or I mean or increased to 1 m equals 1 isentropically, if you do that is your star condition. So, what is your star condition? We will try to understand what is our star condition. So, we use this relation to evaluate further.

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So, let say this star condition can be present in the flow, or it can be completely imaginary point. So, if it is a converging diverging nozzle, your star condition is the (()) area where your d is going to be zero, and your m equals 1. So, that is also your star condition. We will come to that in few lectures from now, but now let us concentrate on this arbitrarily shaped d value. So, this is 1. So, along at there is a mach number associated with the station 1, this is a 1 d flow now I take this fluid to an imaginary value,, where m equals 1 and that value is your star condition and that area is your A star. So, the area associates. So, if I write a 1 by a 2 as this, and I take a 2 as my A star,

stagnation reference.

We will see in the next lecture, we will see further information on star conditions, how we can define what is the relation between t^* , v^* and p^* and the other things.