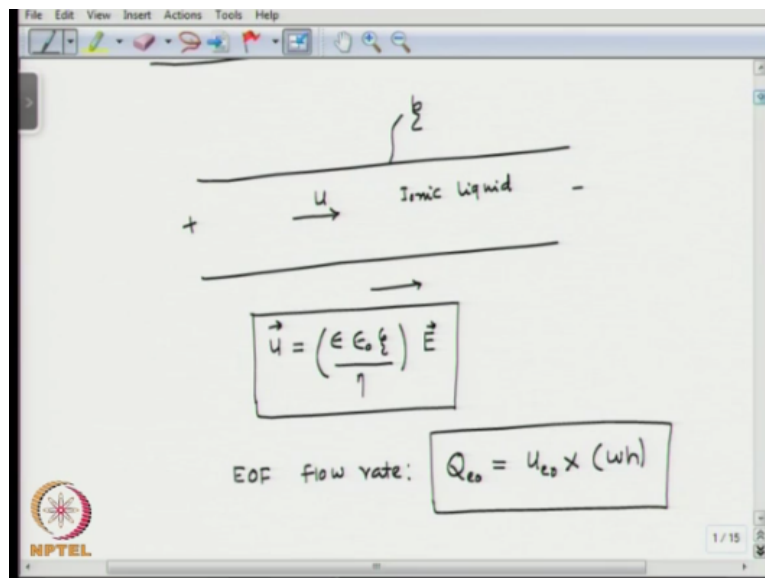


Microfluidics
Dr. Ashis Kumar Sen
Department of Mechanical Engineering
Indian Institute of Technology – Madras

Lecture - 29
Micropump

Okay, so let us continue a discussion on micropump, we have talked about the acoustic micropump, let us talk about electrokinetic micropump. We have already discussed that electrokinetic micropump operate on the principle of electro-osmosis and we have already discussed electro-osmosis in the previous lectures, so here will be briefly introducing to electro-osmosis and then talk about a design problem, okay.

(Refer Slide Time: 00:43)



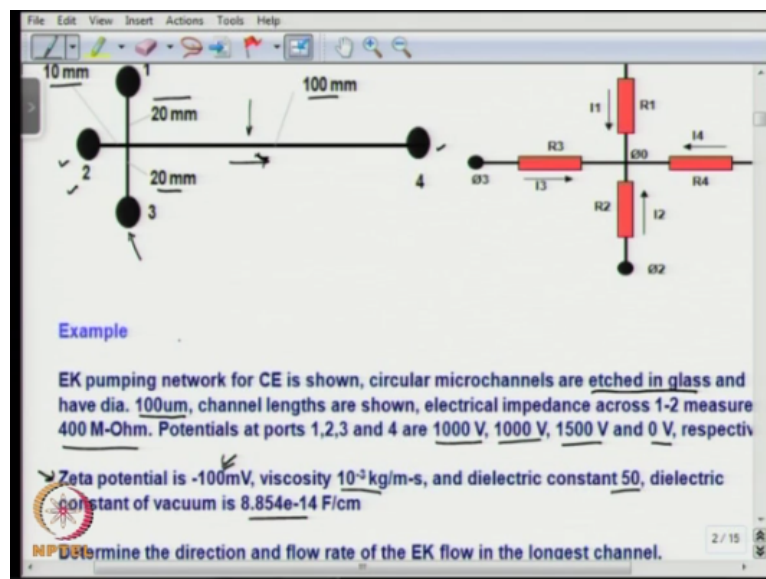
So, we talk about electrokinetic micropump, so here we have a channel which has some zeta potential, okay and here inside we have an ionic liquid, liquid with non0 conductivity and if we establish an electric field, okay then we induce a electro-osmotic flow, okay and this electro-osmotic flow velocity is given by epsilon epsilon 0, so that is the permittivity of free space, this is a dielectric constant of the liquid*zeta potential over the viscosity of the liquid*the electric field, okay.

So that is the expression for the electro-osmotic velocity. Now, knowing the area of cross-section of the channel, we can find the electro-osmotic flow rate. So the electro-osmotic flow rate for a rectangular channel, we have seen that the electro-osmotic flow rate is given by*the

area of cross-section per width*height, okay. So, let us consider a design problem, so you consider this situation here.

We are talking about electrokinetic pumping network for capillary electrophoresis. So this is a typical microchannel network use for capillary electrophoresis. Normally, you would have you know sample present in one of reservoirs, so here would be applying vacuum. So that the sample plug comes to junction and then by applying a voltage between this port, port 2 and port 4, the sample will get separated along this channel, okay.

(Refer Slide Time: 02:33)



So that is the principle of capillary electrophoresis. Here one such network is shown and we have circular microchannel cross-section that are etched in glass and have diameter of 100 micron and how do you make circular microchannels? We can have bulk etching of silicon to have hemispherical channel and we can bond 2 such microchannel to get a circular microchannel cross-section and here all the channel lengths are shown.

You can see this is 10 millimeter, this is 20 millimeter, this is 20 millimeter and the long channel is 100 millimeter. The electrical impedance across 1 to 2 is major, so you can measure the electrical impedance between port 1 and port 2. So that is measured to be 400 mega-Ohm, okay. Now, the potentials at the port 1, 2, 3 and 4 are given. So port 1, which is under 1000 volts, port 2 is 1000 volts, port 3 is 1500 volts and port 4 is 0 volts, okay.

So, it is also given the zeta potential of the channel (()) (04:42) is given is -100 millivolt, okay and the viscosity is 0.001 kilogram per meter second. The dielectric constant is 50 and

the dielectric constant of vacuum is 8.854×10^{-14} Faraday per centimeter. Now, we are interested to know the direction and flow rate of electrokinetic flow in the longest channel, okay.

So, we are interested to know in which direction, the electrokinetic flow is going to occur in the long channel and what is going to be the flow rate, okay. Now, how do we solve this. So, here we can assume that the fluid in the microchannel is homogenous, okay. So, we make an assumption is that the fluid in the microchannel is homogenous meaning the electrical properties are same throughout, okay.

So in that condition, the electrical impedance will be proportional to the channel length, okay and we can analyze the system as a network of resistors. So in that case, we can represent these network as an equivalent electrical network, okay. Now since we know the impedance between 1 to 2 that is 400 mega-Ohm, we can predict the resistances assuming that the fluid is uniform throughout, okay that is the assumption we make.

So, under that assumption we get R_1 as 200 mega-Ohm because from the length of this channel 1 junction and junction to 2, so 1 junction is having twice the length from junction to 2. Sorry, we are majoring 1 to 2, so this is actually 2, this is 3, okay. So, 1 junction and junction to 2 have same length 20 millimeter. So in that case, each will have resistance 200 mega-Ohm.

(Refer Slide Time: 05:37)

Assumption: Fluid in the microchannel is homogeneous
→ the elec. impedance of channel length

$R_1 = 200 \text{ M}\Omega$, $R_2 = 200 \text{ M}\Omega$, $R_3 = 100 \text{ M}\Omega$,
 $R_4 = 1000 \text{ M}\Omega$

→ Analyze the system as a resistor network

NPTEL

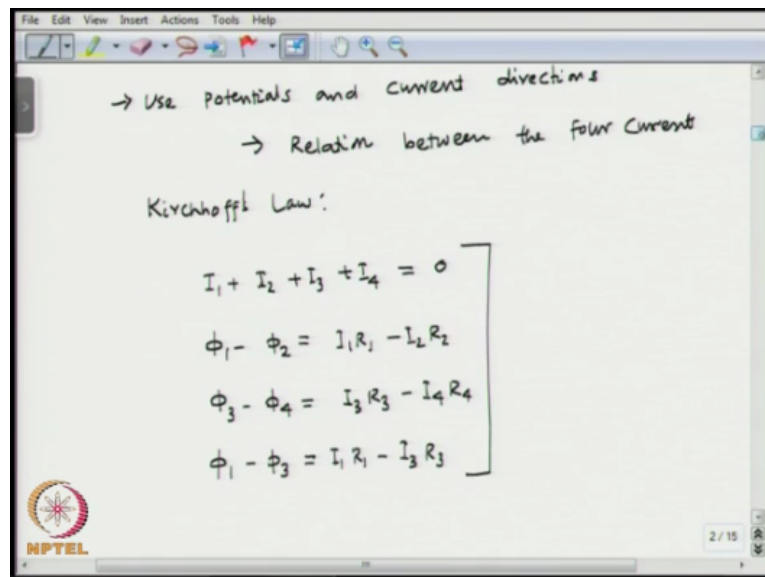
2 / 15

Because the total is 400 mega-Ohm, so R2 will be 200 mega-Ohm and R3 will be 100 mega-Ohm and R4 will be 1000 mega-Ohm. So R3 has half the channel length, okay. So R3 is only 10 millimeter, so it will be half of R12 junction, okay so that is 100 mega-Ohm and R4 is 10 times R3 so that will be 1000 mega-Ohm. So, we can analyze the system as a resistor network.

Now, if we consider the direction of the potential and current, we arbitrarily define the direction of the current and the potential, so this is at junction 1, it is ϕ_1 , so this is at 2, it is ϕ_2 , this is ϕ_3 , and that is ϕ_4 and we define the resistances R1, R2, R3 and R4 and the current I1, I2, I3, I4. So for convenience, we defined all the currents are coming towards the junction of course that will not happen due to Kirchhoff's law.

So, we will get some current in fact in the reverse direction. Now if we assume Kirchhoff's law for this electrical network, then we can arrive at a solution, okay. So, we use potentials and current directions, so using that we can establish the relation between the 4 currents and we can do that using the Kirchhoff's law, okay. So, we can write $I_1 + I_2 + I_3 + I_4$, so all the currents coming towards the junction, the summation of that is going to be 0.

(Refer Slide Time: 09:55)



→ Use potentials and current directions
→ Relation between the four currents

Kirchhoff's Law:

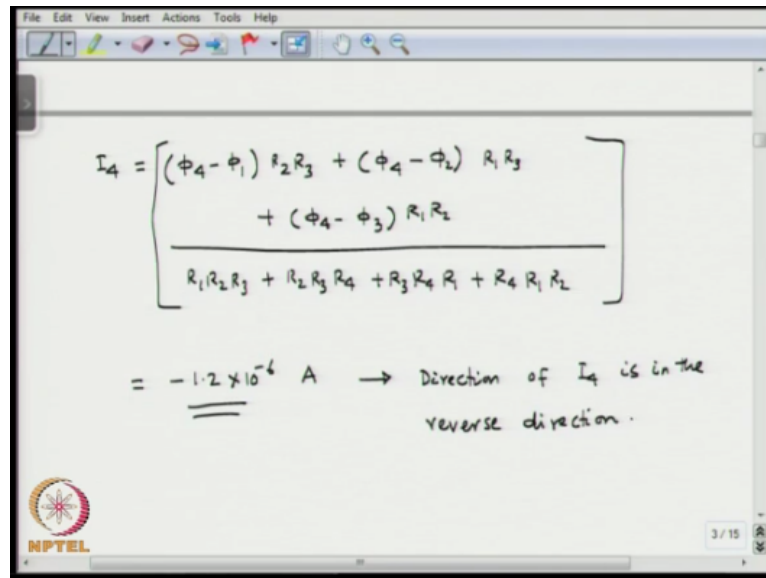
$$\left[\begin{array}{l} I_1 + I_2 + I_3 + I_4 = 0 \\ \phi_1 - \phi_2 = I_1 R_1 - I_2 R_2 \\ \phi_3 - \phi_4 = I_3 R_3 - I_4 R_4 \\ \phi_1 - \phi_3 = I_1 R_1 - I_3 R_3 \end{array} \right]$$

NPTEL

Now, $\phi_1 - \phi_2$, so here $\phi_1 - \phi_2$ is going to be $I_1 R_1 - I_2 R_2$, because the direction of I2 is in this direction, so it will be $-I_2 R_2$, so $I_1 R_1 - I_2 R_2$. Similarly, we would have $\phi_3 - \phi_4$ will be $I_3 R_3 - I_4 R_4$ and we have $\phi_1 - \phi_3$ as $I_1 R_1 - I_3 R_3$. So, here we have 4 equations and we have 4 unknowns. The unknowns are I1, I2, I3 and I4, everything else is known. So, if you solve the 4 equations simultaneously, we can get an expression for I4, okay.

So, we can solve for I_4 , I_4 will be $\phi_4 - \phi_1 \cdot R_2 R_3 + \phi_4 - \phi_2 \cdot R_1 R_3 + \phi_4 - \phi_3 \cdot R_1 R_2$ divided by $R_1 R_2 R_3 + R_2 R_3 R_4 + R_3 R_4 R_1 + R_4 R_1 R_2$, okay. So, this is going to be the expression for I_4 . So if we plug in the values, we know all the values here. So if we plug in the values, we can calculate I_4 is -1.2×10^{-6} ampere. So, this is negative because here if you see here, we have taken I_4 to be in this direction, but in reality the current is going to be in this direction, okay.

(Refer Slide Time: 12:16)



$$I_4 = \frac{(\phi_4 - \phi_1) R_2 R_3 + (\phi_4 - \phi_2) R_1 R_3 + (\phi_4 - \phi_3) R_1 R_2}{R_1 R_2 R_3 + R_2 R_3 R_4 + R_3 R_4 R_1 + R_4 R_1 R_2}$$

$$= \underline{\underline{-1.2 \times 10^{-6} \text{ A}}} \rightarrow \text{Direction of } I_4 \text{ is in the reverse direction.}$$

So that will be same as the direction of the flow, okay. So, what that means is direction of I_4 is in the reverse direction. So, it is going from the junction towards the port 4, is in the reverse direction. Now, you can find the electric field strength in the longest channel, which is going to be ϕ_0 , ϕ_0 is the potential at the center - ϕ_4 divided by L . So, this is going to be $I_4 R_4$ divided by L .

(Refer Slide Time: 14:22)

Electric field strength in the longest channel:

$$E_{el,4} = \left(\frac{\phi_1 - \phi_4}{L} \right) = \left(\frac{I_4 R_4}{L} \right)$$

$$= \frac{(1.2 \times 10^{-6}) \times (1000 \times 10^6)}{(100 \times 10^{-3})} = \underline{\underline{11.9 \times 10^3 \text{ V/m}}}$$

NPTEL

So you have all the values, we can substitute I_4 is going to be 1.2×10^{-6} , so that is from the junction towards port 4. R_4 is 1000 mega-Ohm, so 10^6 Ohm divided by the length of the channel is 100 millimeter, so 10^{-3} , so that would be 11.9×10^3 volt per meter, okay. So that will be from the junction towards the port 4 that will be the direction of the electric field.

Now, the electro-osmotic mobility can be determined as, so new electro-osmolality is going to be $\epsilon \epsilon_0 \xi / \eta$. So this is 50 that is the dielectric constant of the liquid that is given and of the vacuum is 8.854×10^{-14} , so ξ is given which is 100×10^{-3} , 100 millivolt thus given and viscosity is 10^{-3} . So that is going to be 4.43×10^{-8} meter square per volt second, right.

(Refer Slide Time: 15:56)

EO mobility $\mu_{eo} = \left(\frac{\epsilon \epsilon_0 \xi}{\eta} \right) = \frac{50 \times (8.854 \times 10^{-14}) \times (100 \times 10^{-3})}{10^{-3}}$

$$= 4.43 \times 10^{-8} \text{ m}^2/\text{V}\cdot\text{s}$$

EO flow velocity in the longest channel:

$$u = \mu_{eo} E_{el,4}$$

$$= (4.43 \times 10^{-8}) \times (11.9 \times 10^3)$$

$$= 527 \text{ nm/s}$$

NPTEL

So, you can find the electro-osmotic flow velocity in the longest channel, so u is going to be $\mu_{\text{electro-osmotic}} \times \text{the electric field}$ which is going to be $4.43 \times 10^{-8} \times 11.9 \times 10^3$ to the power 3, so that will be 527 micron per second. So, knowing the electro-osmotic flow velocity, we can find the flow rate, okay. So, the electro-osmotic flow rate is going to be, so that is in channel 4 is going to be u_4 .

(Refer Slide Time: 18:09)

EO flow velocity

$$u_4 = \mu_{eo} E_{el,4}$$

$$= (4.43 \times 10^{-8}) \times (11.9 \times 10^3)$$

$$= 527 \mu\text{m/s}$$

EO flow rate : $Q_{eo,4} = u_4 A$

$$= 527 \times \pi (50 \times 10^{-6})^2 = 248 \text{ nL/min}$$

$$Q_{eo,4} = 248 \text{ nL/min}$$

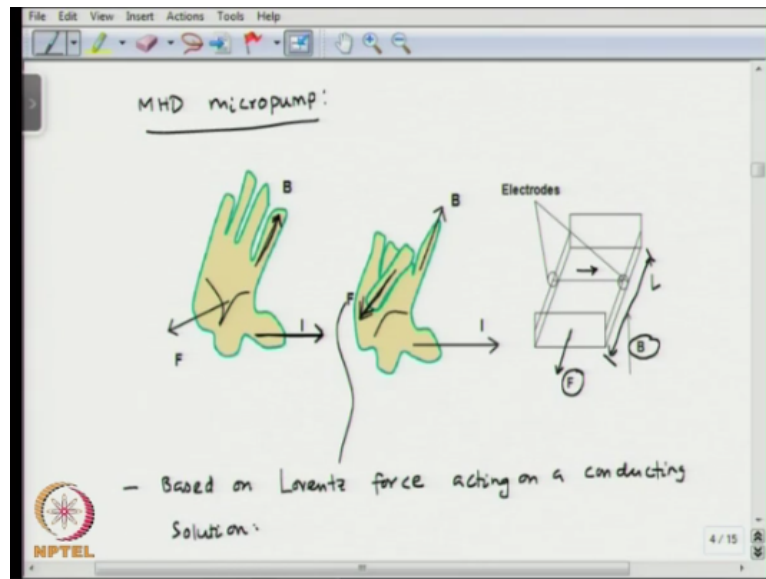
NPTEL

3/15

So this is in velocity in channel 4*the area of cross-section is $527 \times \text{the area of cross-section}$, this is 50 micron radius, $\pi \times 50 \times 10^{-6} \text{ square}$, so that is going to be 248 nanoliter per minute. So, $Q_{\text{electro-osmotic}}$ is 248 nanoliter per minute, okay. So, that gives you an example how to solve for the electro-osmotic flow rate in a typical microfluidic network when you are electro-osmosis for capillary electrophoresis applications, okay.

Now, let us talk about magneto-hydrodynamic micropump. So, we talk about magneto-hydrodynamic micropump, MHD micropump, okay. So, magneto-hydrodynamic micropumps work on the principle of Lorentz force. So, typically if you have a channel and you are applying a magnetic field, you have an electrode through which you are applying the current through the fluid, okay.

(Refer Slide Time: 19:30)



So, if you have a channel such that you are applying a current in the thumb direction and you are applying a magnetic field along the index finger, the liquid will be subjected to a force along the middle finger, okay. So that is the principle based on which the magneto-hydrodynamic pumping works. So as we can see here, so this is the direction of the current and this is the direction of the magnetic field.

So, you would have a force induced in this direction, okay. So, you can see this is the length of the channel, okay and this is the direction of the magnetic field and you have a current which is going in this direction between the 2 electrodes, so induced the force F in this direction. So, magneto-hydrodynamic pumping is based on the Lorentz force, okay. So, this force is called Lorentz force that is acting on a conducting solution.

So, you need a conducting solution because you need to pass current through it, okay. So the force, F is going to be $\text{current} \times \text{cross magnetic field}$, so that means force is going to be on the third direction, okay. So, current is along one direction and magnetic field along the direction 2, so this will be along the third direction, okay* w , right. So here, I is the current and B is the magnetic flux intensity, okay and w is the distance between the electrodes, okay.

(Refer Slide Time: 22:06)

$$\vec{F} = (\vec{I} \times \vec{B}) w$$
 where w is distance between electrodes.

$$p_{\max} = J B L$$
 where J is current density, B is mag. flux intensity, and L is channel length.

Max. pressure

So, you can find out the expression for the pressure and flow, so the maximum pressure P_{\max} has been estimated as $J \cdot B \cdot L$, okay. So, J is the current density, okay and B is the magnetic flux intensity which is defined here and L is the channel length, okay and the maximum flow rate Q can be defined as $J \cdot B \cdot \pi D_h^4$ divided by 128, okay. So that is the expression for the flow rate.

(Refer Slide Time: 24:09)

$$Q = J B \left(\frac{\pi D_h^4}{128 \mu} \right)$$

- Lorentz force acts on bulk fluids and creates pr. gradient

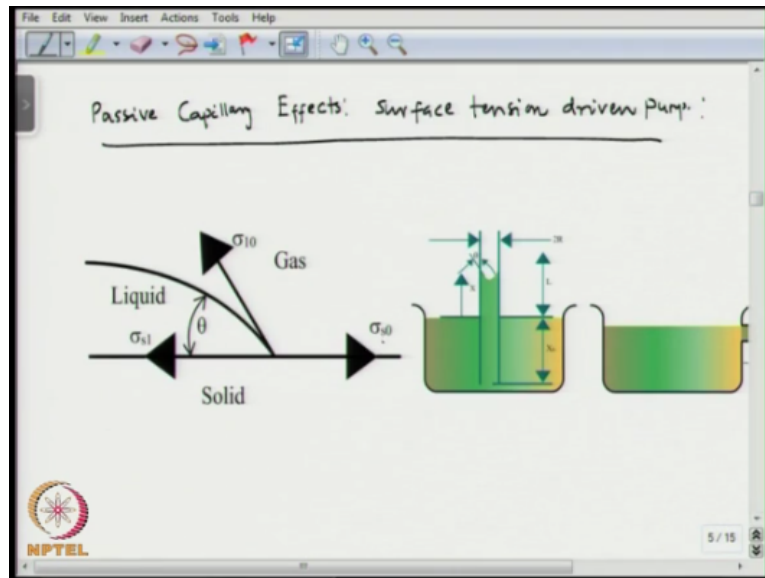
→ MHD pump generates parabolic velocity profile similar to pr. driven flow

So, the Lorentz force what it does is, it induces a pressure gradient in the bulk of the fluid, okay. So, since it induces a pressure gradient, the flow induced because in the magnetohydrodynamic effects is parabolic in nature, okay similar to that is encountered in pressure driven flow, okay. So, the Lorentz force acts on bulk fluids and creates a pressure gradient, so the velocity profile similar to that obtained for pressure driven flow.

So the magneto-hydrodynamic pump generates parabolic velocity profile similar to pressure driven flow, okay. So that finishes our discussion on magneto-hydrodynamic pump, now let us talk about the micropump based on surface tension driven effects, okay. So, we first talk about passive capillary effect, okay. So typically, when we have a liquid droplet present on a solid surface, this is the contact line that we encounter.

So here, we have the surface tension between solid gas and surface tension between solid liquid and surface tension between liquid gas, okay and this angle is known as the contact angle. So, we can write the force balance at the interface. So if you do force balance along the interface, we can write $\sigma_{sg} - \sigma_{sl} \cos \theta = \sigma_{lg}$.

(Refer Slide Time: 26:28)

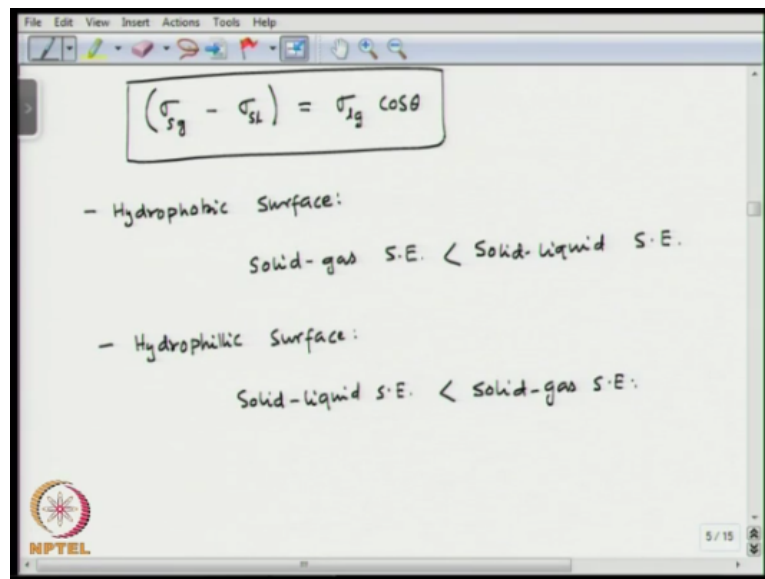


So, you make a component of σ_{lg} in this direction and that is what the force balance is at the contact line, okay. So, you know if you have a hydrophobic surface what that means is that the surface energy between a solid gas interface is $<$ that between a solid liquid interface, okay. So, the surface does not like liquid to wait, okay. If you have a hydrophilic surface, then the surface energy between a solid liquid interface is $<$ that between the solid gas interface, okay.

So, if we have a hydrophobic surface, then the solid gas surface energy is $<$ the solid liquid surface energy, okay and if you have a hydrophilic surface, then the solid liquid surface energy is $<$ the solid gas surface energy, okay. So, you know the surface tension between the

liquid gas interface can be obtained using a capillary tube experiment that we have seen in previous lecture, so here we just briefly revisit that.

(Refer Slide Time: 27:50)



$$(\sigma_{sg} - \sigma_{sl}) = \sigma_{lg} \cos \theta$$

- Hydrophobic Surface:
Solid-gas S.E. < Solid-liquid S.E.
- Hydrophilic Surface:
Solid-liquid S.E. < Solid-gas S.E.

NPTEL

So as you can see, in a vertical tube put in a liquid bath, if we do force balance at the interface, so say that the liquid gas surface tension can be determined by capillary rise experiment and if you do force balance at the interface, then it will be $2\pi R \cdot \sigma_{\text{solid gas}} - \sigma_{\text{solid liquid}}$ will be $\Delta P \cdot \pi R^2$, okay. So, you can find σ_{lg} as ρ , so this you can express in terms of $\sigma_{lg} \cos \theta$.

So this will be $\rho g l R$ divided by $2 \cos \theta$, okay. So, this is the expression for the liquid gas surface tension, okay. So here, you see we have 2 configuration, here the tube is connected vertically, so this is the vertical configuration, here the capillary tube it is inserted horizontally to the liquid container, okay. Now, this vertical capillary rise and horizontal capillary advancement have different applications.

(Refer Slide Time: 30:51)

Force balance at the interface:

$$2\pi R(\sigma_{lg} - \sigma_{sl}) = \Delta p \times \pi R^2$$

$$\Rightarrow \sigma_{lg} = \frac{\rho g L R}{2 \cos \theta}$$

← Liq-gas surface tension

Vertical capillary rise is used when you want to collect some sample from a container using a capillary and horizontal capillary advancement is used in case of a filling of microchannel for lab-on-a-chip applications, okay. So, you have 2 cases here, the vertical tube configuration is used for sample collection and the horizontal tube configuration is used for the self filling of microchannels in lab-on-a-chip application, okay.

(Refer Slide Time: 33:33)

Vertical tube Config. → Sample collection

Horizontal tube Config. → Self-filling of microchannels
in lab-on-chip application

So, let us look at first case where the liquid is trying to raise in the vertical tube configuration, okay. So, we consider passive capillary in vertical configuration, here we do balance of different forces, okay. So, when this liquid column is trying to move off, because of the capillary action we can do a force balance on this liquid column, okay. So, what is the different forces that are acting?

(Refer Slide Time: 34:48)

Passive Capillary in vertical Config.:

→ Balance of forces:

Gravitational force, inertia, interfacial, and viscous forces

$$\frac{d}{dt} \left(m \frac{dx}{dt} \right) = -m_1 g - 2 \pi R (x+x_0) \tau + 2 \pi R \sigma_{lg} \cos \theta$$

$$F_i = F_g + F_v + F_s$$

NPTEL

We have gravitational force, then we have inertia force, we have interfacial force and viscous forces, okay. So, we can write down the expression for these forces, so we can write $d/dt \cdot m \cdot dx/dt - m_1 g - 2 \tau \pi R \cdot x + x_0 + 2 \pi R \sigma_{lg} \cos \theta$. So, this is the inertia force, so this is nothing but mass*acceleration as mass is changing with time, so we have d/dt outside the bracket.

This one is the gravitational force, okay, $m_1 \cdot g$, where m_1 is the mass of the liquid column over the outside liquid surface. So, anything ever so this mass will be ever this line, this mass will be m_1 , okay and this is you know the viscous force and this is the surface tension force, okay. So this is the inertia, this is the gravitational force and this is the viscous force, okay and this is the surface tension force, okay.

Here, the x is the position variable and x_0 is going to be the immersed length, τ is the shear stress, m is the mass of the liquid column, so total liquid column from the bottom to the top is m and m_1 is the mass of the liquid column above reservoir surface, okay. So now, we can simplify this equation, we can write $d/dt \cdot \rho \pi R^2$, so we write the expression for $m \pi R^2 \cdot x + x_0 \cdot dx/dt$ will be $= - \rho \pi R^2 \cdot x \cdot g - \pi R^2 \cdot dP/dx$, this is pressure gradient $\cdot x + x_0$, okay.

(Refer Slide Time: 37:59)

F_i F_g F_v

x = position variable, m = mass of liquid column
 x_0 = immersed length, m_1 = mass of liquid column above reservoir surface
 z = shear stress

$\frac{d}{dt} \left[\rho \pi R^2 (x+x_0) \frac{dx}{dt} \right] = - \left(\rho \pi R^2 x \right) g - \pi R^2 \left(\frac{dp}{dx} \right) (x+x_0) + 2 \pi R \sigma_{lg} \cos \theta$

NPTEL 6/15

So, this is the pressure gradient, this is the viscous force and $+ 2 \pi R \sigma_{lg} \cos \theta$, okay. So here, what we have used? We have used the expression for the pressure gradient in this expression. So now, if we use Hagen-Poiseuille model for pressure drop, then we can write dp over dx , the pressure gradient can be written as 8μ over R^2 times dx over dt , right so this is the Hagen-Poiseuille model.

That we can substitute in this equation now, so we get this equation, $\frac{d^2 x}{dt^2} + \frac{1}{x+x_0} \left(\frac{dx}{dt} \right)^2 + \frac{8 \mu}{R^2 \rho} \left(\frac{dx}{dt} \right) + g \left(\frac{x}{x+x_0} \right) = \frac{2 \sigma_{lg} \cos \theta}{\rho R}$, right. So this is the inertia term and this is the viscous term $+ g \cdot x$ divided by $x + x_0$ and this is the gravitational force term, which will be $= 2 \sigma_{lg} \cos \theta$ divided by $\rho R \cdot 1$ over $x + x_0$, okay.

(Refer Slide Time: 40:28)

$+ 2 \pi R \sigma_{lg} \cos \theta$

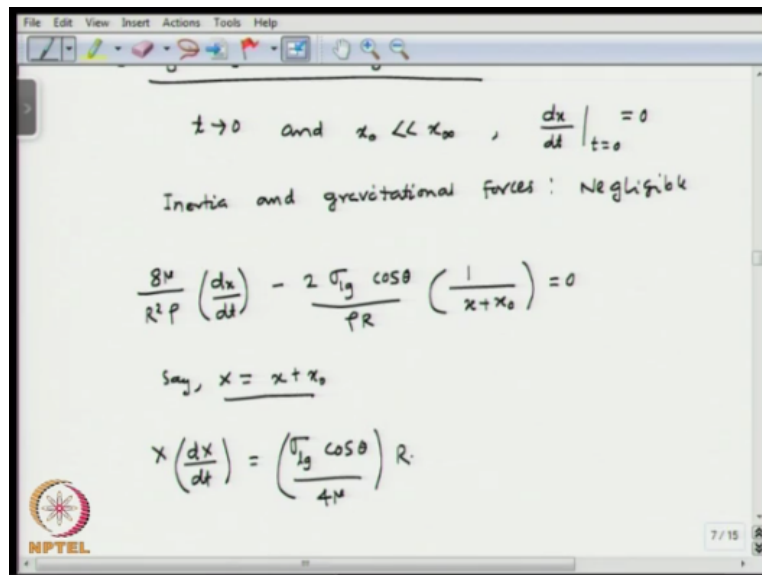
Hagen Poiseuille model:
 $\left(\frac{dp}{dx} \right) = \frac{8 \mu}{R^2} \left(\frac{dx}{dt} \right)$

$\Rightarrow \underbrace{\frac{d^2 x}{dt^2} + \left(\frac{1}{x+x_0} \right) \left(\frac{dx}{dt} \right)^2}_{F_i} + \underbrace{\frac{8 \mu}{R^2 \rho} \left(\frac{dx}{dt} \right)}_{F_v} + \underbrace{g \left(\frac{x}{x+x_0} \right)}_{F_g} = \frac{2 \sigma_{lg} \cos \theta}{\rho R} \left(\frac{1}{x+x_0} \right)$

NPTEL 6/15

So that is the equation we have, this is the surface tension force, okay. Now, we can be obtained for the solution for the 2 extents, one when the time scale is you know very less, so it is basically the beginning of the capillary filling process and the second time step is towards the end of the capillary filling process, so solution can be obtained for 2 extremes, okay. $t \rightarrow 0$, $x_0 \ll x$ infinity, so that is the beginning of the filling process.

(Refer Slide Time: 42:54)



Handwritten notes on a whiteboard showing the initial conditions and force balance for capillary filling:

$$t \rightarrow 0 \text{ and } x_0 \ll x_\infty, \quad \left. \frac{dx}{dt} \right|_{t=0} = 0$$

Inertia and gravitational forces: Negligible

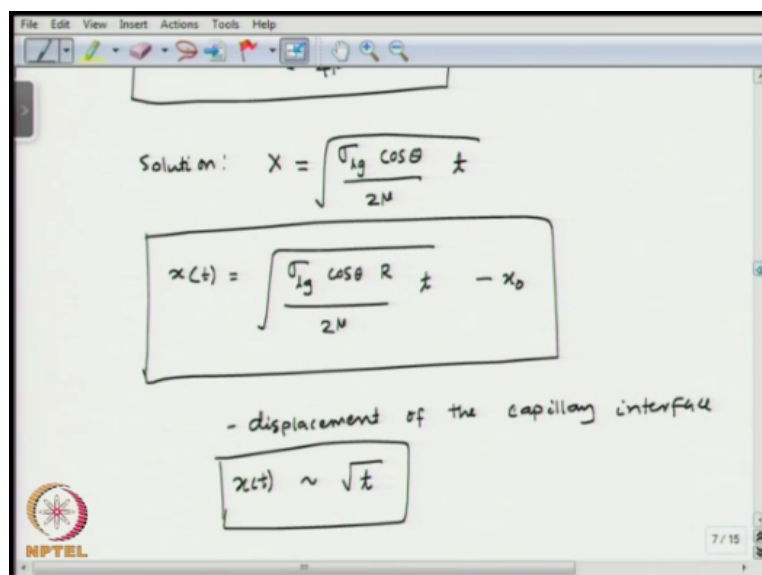
$$\frac{8\mu}{R^2 P} \left(\frac{dx}{dt} \right) - \frac{2\sigma_{lg} \cos\theta}{PR} \left(\frac{1}{x+x_0} \right) = 0$$

Say, $x = x + x_0$

$$x \left(\frac{dx}{dt} \right) = \left(\frac{\sigma_{lg} \cos\theta}{4\mu} \right) R$$

The second process is t tends to infinity and x infinity tends to L , okay. So first let us talk about the beginning of the filling process, so beginning of the filling process t tends to 0 and $x_0 \ll x$ infinity and also dx over dt at $t = 0$ is going to be 0. So in this case, the inertia and the gravitational force going to be negligible, okay. Since we are talking about the beginning of the filling process, the fluid had just started to move.

(Refer Slide Time: 46:40)



Handwritten notes on a whiteboard showing the solution for the displacement of the capillary interface:

Solution: $x = \sqrt{\frac{\sigma_{lg} \cos\theta}{2\mu} t}$

$$x(t) = \sqrt{\frac{\sigma_{lg} \cos\theta R}{2\mu} t} - x_0$$

- displacement of the capillary interface

$$x(t) \sim \sqrt{t}$$

So, the inertia and the gravitational force are going to be negligible, so this is the general equation we work on and for the beginning process, we drop the inertia and the gravitational force from this equation and if we do that we get $\frac{8\mu}{R^2} \frac{dx}{dt} - 2 \frac{\sigma \lg \cos \theta}{R} \frac{1}{x + x_0}$ is going to be 0. So, we can do a conversion of a variable, we can say X is $x + x_0$, okay.

So, if we say that then we can write $X \frac{dx}{dt}$ will be $\frac{\sigma \lg \cos \theta}{4\mu R}$, okay. So this is the equation we get which is easy to solve, so we can get the solution as this. The solution would be X is going to be $\frac{\sigma \lg \cos \theta}{2\mu} t$, okay or we can convert back to the original variable, in that case we can say x is going to be $\frac{\sigma \lg \cos \theta}{2\mu} R$ divided by $2\mu - x_0$, okay.

So, what we see here is at the beginning of the filling process, the displacement is going to vary as square root of t , okay. So, the displacement of the capillary interface varies as square root of t , right.

So next, we will look at what happens at the end of the filling process. So at the end of the filling process, since the liquid column is going to slow down and the driving force which is the surface tension force is going to die down, the inertia and the surface tension forces are going to be negligible. So in the general equation, we drop the inertia and the surface tension force from the equation.

(Refer Slide Time: 48:23)

② At the end of the filling process:

Inertia and Surface tension are negligible

$$\left(\frac{4\gamma}{g R^2} \right) \left(\frac{d^2 x}{dt^2} \right) + (x - x_0) = 0$$

Let $x_0 = x_0 + L$

consider $\chi = (x_0 - x)$

$\chi \downarrow$

NPTEL

7/15

So at the end of the filling process, the inertia and the surface tension are negligible, okay. So in that case, we can get $\frac{4\nu}{gR^2} \frac{dx^2}{dt} + x - x_\infty$ is going to be 0 and here, we define x_∞ as $x_0 + L$, okay. So, now if we consider a parameter x as $x_\infty - x$ and in that case, we can convert this into an equation in terms of the new variable and try to solve that. We will continue with this in the subsequent lecture.