Lecture 65

So, I will take another maximum half an hour to solve two problems to make this thing clear, but before that I will tell you one thing that before solving a counter flow exchanger.

Now we will solve two problems on Heat Exchanger which will demonstrate our understanding of the discussion that which have been met just now in the earlier class.

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A counterflow heat exchanger of heat transfer area $A = 12.5\,\text{m}^2$ is to cool oil [$c_{ph} = 2000\,\text{J/(kg\,°C)}$] with water [$c_{pc} = 4170\,\text{J/(kg\,°C)}$]. The oil enters at $T_{h,in} = 100\,°C$ and $m_h = 2\,\text{kg/s}$, while the water enters at $T_{c,in} = 20\,°C$ and $m_c = 0.48\,\text{kg/s}$. The overall heat transfer coefficient is $U_m = 400\,\text{W/(m}^2\cdot°C)$. Calculate the exit temperature of water $T_{c,out}$ and the total heat transfer rate Q using both the LMTD and the ε-NTU method.

Now the first example is the counter flow heat exchanger of heat transfer area 12.5m square immediately you should strike that it is not a sizing problem that means size is given, that means a rating problem is to cool oil whose specific it is 2 kilo joule per kg degree Celsius. 2000 joule is taken from a book they have not written in the term of Kilo Joule. With water with specific it is 4.170J/kg degree Celsius.

Now oil is the hot fluid and water is the cold fluid. The oil enters at 100 degree Celsius that means in our nomenclature Th1 is 100 degree Celsius. Here it is written T h dot in. And the flow rate of the hot fluid that is oil is to 2kg/s, while the cold fluid enters that is T c dot in which is in

our nomenclature Tc1 is 20 degree Celsius and the cold fluid flow rate m_c is 0.48kg/s. The overall heat transfer coefficient is given.

This will be given for both the cases rating and sizing problem. 400W/ (m2 degree Celsius). Calculate the exit temperature of water and the total heat transfer rate Q using both LMTD and the Epsilon NTU method. Now an idiot will start with the any of Epsilon-- LMTD method but it is told that we have to do it, if nothing is told, so I can start with LMTD. Now you see LMTD how difficult it is.

(Refer Slide Time: 12:22)

Now what is m dot h, you tell me m dot h is 2kg, what is that, where it is written 2kg/s? 2 into- I am writing in terms of Kilo Joule it will be cancelled then Th1 is what, Th1 the oil enters 100 - th2 equals to what? Water enters at 20 degree Celsius 0.48. I have to find out Q. Good that is the mistake. I was discussing with people that I could not rectify though my teachers told me several times.

What is it flow rate? Flow rate is 0.48 into 4.17 (Tc2 – 20). Now LMTD is Delta T2 – Delta T1 divided by ln Delta T2 by Delta T1. Now what is Delta T2? Th2 – Tc2 nothing is known. Counter flow Th2 - Tc1 and Delta T1 is Th1 - Tc2. Now I cannot find out the LMTD because I don't know this Th2 Tc2. So what to do? We assume Tc2 or Th2. Let us assume Tc2 is equal to 60 degree Celsius.

It will be heated to a temperature, I assume something it is less than 100 definitely which maybe more than Th2 it cannot be more than Th1, let us assume 60 degree Celsius. Then I find out this and I find out Th2, so Th2 and Tc2 is found out. And I give that one superscript that is the first iteration. Accordingly, I find out LMTD with the first approximation of this. And when LMTD is found out this two are known-- I now found out Q as the first approximation.

When Q is found out I can use this with the unknown Th2 or this with the unknown Tc2 and try to match this Th2, Tc2 to found out with the earlier value, if they are differing again we put that value and we change this as superscript 2 next iteration and go and this loop will go until and unless these two matches. And finally depending upon your gauss value if 1 gives a gauss value by the magic of P. C. Sorcar, 85.6 degree Celsius.

Then you did not have to do any iteration, that means you will get a value of Th2 such and LMTD such and accordingly Q which will exactly match this value. But it is very difficult only the magician can do. So, some iteration will be there. But this problem if you solve by NTU Epsilon method, so therefore we see this is a tedious method, but what is NTU LMTD method?
(Refer Slide Time: 16:20)

$$2 \times 2 \times (100 - T_{h_2}) = 0.48 \times 4.17 (T_{c_2} - 20)$$

$$NTU = \frac{uA}{C_{min}}$$

$$= \frac{400 \times 12.5}{2002} = 2.5$$

$$\varepsilon = 0.82 \qquad \varepsilon = \frac{T_{c_2} - 20}{100 - 20}$$

$$T_{c_2} = 85.6°C$$

NTU is known, what is NTU? uA/C min. What is C? 2*2=4 and this is 0.48*4 that means which one is minimum? That one, right hand side is minimum. So if you do that minimum then you

find out C min—sorry NTU is uA/C min then we find out NTU as Au, u is what? What is u? What is A? 12.5 And what is C min? I just see that multiplication is difficult for me 2002 what means 2, because this Joule unit has to be there.

Because this unit has to be consistent, here I can write Kilo Joule because both the side it will be balanced. Be careful with this unit. NTU is a non-dimensional. u is what per meter square K or meter square degree Celsius. A is meter square, so here C min has to be in Joule. Do not be that smart to put it here and finally come with a wrong result I will be giving 80% marks, if you are happy than it's alright. So therefore, NTU comes out to be what? Where is NTU? 2.5.

That means if you clear it NTU then Epsilon for a counter flow heat exchanger expression there if you put NTU it is an explicit calculation by a small calculator you can do it and Epsilon comes straightforward value if Epsilon comes 0.82. Now when Epsilon is 0.82 Epsilon will be the temperature difference of the minimum fluid Tc2 – 20 divided by Th1 – Tc1 that means maximum temperature 100 – 20. And this gives Tc2 is equal to 85.6. Explicitly done. So you see that a rating problem is explicitly done by this.

Anybody has feel that LMTD method is not at all valid or you cannot do it for the rating problem? No, we can do it. But it is not explicit. And in today's world both are almost same. By putting into calculator just making a small program and do it nothing is there. But it is explicit and there it is implicit by iteration that is the only difference. Now the next problem, problem 2, this is an interesting problem.

(Refer Slide Time: 20:12)

Water is heated from 30 °C to 90 °C in a counterflow double-pipe heat exchanger. Water flows at the rate of 1.2kg/s. The heating is accomplished by a geothermal fluid which enters the heat exchanger at 160 °C at a mass flow rate of 2kg/s. The inner tube is thin walled and has a diameter of 15mm. If the overall heat transfer coefficient of the heat exchanger is $600 \text{W}/(\text{m}^2 \text{°C})$, determine the length of the heat exchanger required for the purpose. The specific heats of water and geothermal fluid are 4.18 and $4.31 \text{kJ}/(\text{kg °C})$ respectively. Use both (a) the LMTD method and (b) the ε-NTU method.

Water is heated to 30 to 90. Two temperatures are given. In a counter flow double-pipe heat exchanger. Water flows at the rate of 1.2kg/s that means total load is given. The heating is accomplished by a geothermal fluid which enters the exchanger at 160°C at a mass flow rate of 2kg/s, that means everything is explicit we know all the temperatures, the heat transfer everything is given, because by heat balance, we can find out the exact temperature of the geothermal fluid.

Specifics are not given – no specifics are given at the end. The inner tube is thin walled and has a diameter of 15mm. Thin wall, this is extra language that means we can neglect this wall resistance. It is not required because overall heat transfer coefficient is given. If the overall heat transfer coefficient of the exchanger is 600 Watt per meter square degree Celsius, determine the length of the heat exchanger required, -- Oh! That is why it has given thin.

Because area is to be find out then area divided by pie the is the length that's why the thinness is required otherwise it will be difficult. The specific heats of water and geothermal fluid as give use both the LMTD and Epsilon. Here, this is the reverse LMTD is very simple. Epsilon NTU is done. Why? Because the temperatures are known. Let me write, very simple. Tell me, you dictate will write.

(Refer Slide Time: 22:08)

$$2 \times 4.3 \times (160 - T_{h_2}) = 1.2 \times 4.18 \times (90 - 30)$$

$$T_{h_2} = 125.10°C.$$

$$\Delta T_2 = 125.10 - 30 = 95.10°C$$

$$\Delta T_1 = 160 - 90 = 70°C$$

$$LMTD = 81.91°C \qquad L = \frac{A}{\pi D}$$

$$A = \frac{Q}{u(LMTD)} \qquad A = 6.12\,m^2 \qquad = 129.87\,m.$$

Water is 1.2 or the hot fluid first, hot fluid is; what is the flow rate? 2 into You tell me, you dictate me I will write, I will not see. First heat balance, $2 * 4.3 * (160 – Th2) = 1.2 * 4.18 * (90-30)$. What is the value of Th2? Nobody can tell without calculating it. Th2 is 120.10oC. Then Delta T2 125 -- sorry 125.10 – 130 is equal to 95.10 degree Celsius this is meaningless but still I am doing. Delta T1 is Th1 = 160 - Tc2 that is 90 that is equal to 70 degrees Celsius.

With this value the LMTD will come as 81.91 degree Celsius. This is the main temperature, 81.91 degree Celsius. Then A is Q /u LMTD in the dominator. So, Q is this one either this one or this one you put u is given, what is the value of u? u is 600 Watt per meter square degree Celsius and LMTD is 81.91 degree Celsius which gives A if you put the value which gives A as 6.12m square. And L is equal to A by pie D and D is given as diameter is 15mm.

We have to put into meter that means 0.15 m and A is m square finally it is thin walled so diameter outer and inner is same and finally we get L = 129.87 meter. So therefore, is just the reverse. LMTD is straightforward. Clear? Because it is sizing problem. But to do it with Epsilon NTU what you have to do. Because here Epsilon is known but NTU has to be found out. Here Epsilon is known NTU has to be found out. In Epsilon NTU method, what is Epsilon?

(Refer Slide Time: 25:55)

$$\varepsilon = \frac{1 - \exp[-NTU(1-C)]}{1 - C \exp[-NTU(1-C)]}$$

$$\varepsilon = \frac{90 - 30}{160 - 30} = 0.461$$

$$NTU = f(\varepsilon)$$

$$NTU = \frac{1}{C-1} \ln\left(\frac{\varepsilon - 1}{\varepsilon C - 1}\right)$$

Minimum fluid is which one? What is Epsilon? Minimum fluid is m dot c dot, this is the minimum fluid, so Epsilon will be 90 – 30 divided by 160 – 30. So, Epsilon will be 90 – 30. This is the minimum. So this is the Epsilon So Epsilon becomes 0.461. Now, problem is that Epsilon is known, you have to find out surface area and finally length. That means I have to express NTU is a function of Epsilon, for that little more labour you have to out.

We express Epsilon as a function of NTU, that function if you just write other way NTU is equal 1 by C-1 into ln just you do it, Epsilon minus 1 divided by Epsilon C-1? What is C? C mean by C. We express Epsilon as a function of NTU. Here I write by rubbing this, if we recall just now I told. Epsilon in a counter flow is 1 minus exponential minus NTU into 1 minus C that is the ratio into 1 – C again exponential minus NTU into 1 – C.

So you see, this expression this capital C is C mean by C. You have to first from here express NTU, this is tough but it can be done, sometime this is not possible to express NTU as a function of Epsilon explicitly than the problem face, that means then we have to go for iteration. But luckily with a little labour work one can rearrange this function to do that NTU is this. Now when Epsilon is known 0.46 you just put it and ratio C min by C max or C.

You know and you straightforward find out NTU and find out area, area will come exactly the same 6.12-meter square and L will be 129.87. Now you have been able to appreciate that LMTD

method is simple and explicit when we go for sizing, rating is given. But when the size is given NTU Epsilon method is explicit and simple because we have an explicit relationship of NTU with Epsilon where from Epsilon we can find out the rating which was, which is unknown for this type of problem. So, with this I will finish my lecture on Heat Exchanger. Okay.