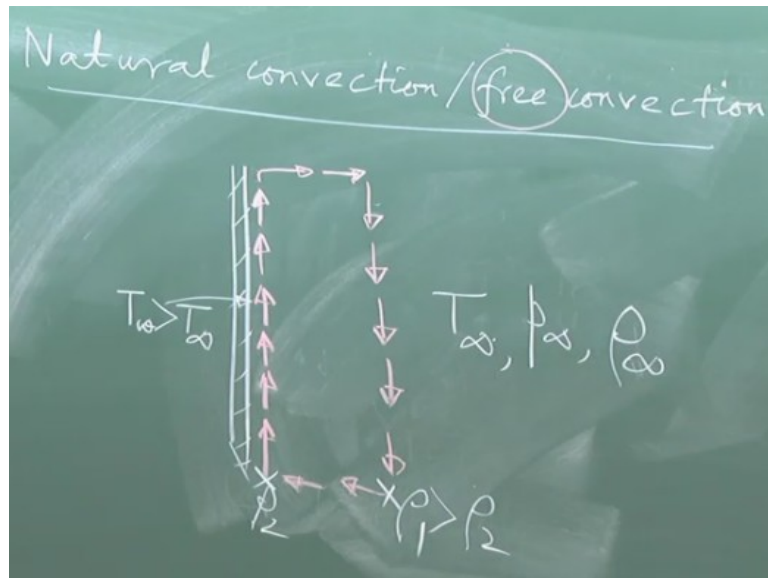


**Conduction and Convection Heat Transfer**  
**Prof. S.K. Som**  
**Prof. Suman Chakraborty**  
**Department of Mechanical Engineering**  
**Indian Institute of Technology- Kharagpur**

**Lecture-53**  
**Natural Convection – I**

So far, we had discussed about force convection, where the objective is to have a convection by driving fluid flow by a force mechanism like, for example by a pressure gradient or by some external forcing mechanism. On the other hand, there may be situations, when you do not have an external forcing mechanism, but you can still drive a fluid flow and one such example is natural convection or free convection.

**(Refer Slide Time: 01:11)**



So, let me give you some physical insight on natural convection, before we entered into the mathematical analysis. So, let us say that you have a vertical plate like this, although we give an example of vertical plate or a vertical surface mostly to introduce natural convection, it does not mean that it has to be a vertical surface always to have the effect of natural convection.

But this is a classical demonstrative example by virtue of which we can show that how convection current can be generated without any external driving flow? So how that is possible? let us say that the ambient temperature is  $T_\infty$ , ambient pressure is  $p_\infty$  and the density is  $\rho_\infty$ . Let us say that the temperature of the wall is  $T_w$ , which is greater than  $T_\infty$ .

The medium can be any fluid, let us say there is air, okay, which is the very common medium and why we are considering this? Because, see one of the terminology is associated with this, this is free convection. So, free is an English word, which resembles the situation when we are getting something free of cost, whether we actually getting free of cost or not, is something which is the matter of further consideration.

But at least air we can get free of cost, one vertical plate you can put free of cost, you are not able to heat a vertical plate free of cost. But I mean there can be see scenarios when there can be a boundary which is heated free of cost like, for example, in sunlight, if you expose a surface to solar energy or something like that, actually you do not pay any cost.

Let us say there is any heating within an electronic device. So, there is an electrical or electronic device, because of Joule effect, there is a heating. So, then you can get a heated surface, say heated printed circuit board, you can get; that you can get, that heating is free of cost. Because you did not intend to get a heating, that heating is an artifact of Joule effect. So, let us say that, it has the situation is like this.

Now if the air which is in contact with the solid boundary, air again, I am giving an example, it can be some other fluid, it gets hot, it gets lighter, right. If it gets hot, its density decreases and it tends to go up. Now when it reaches here, it still has its inertia, right. Because it was going up, now one possibility is that by maintaining its inertia, it can go to the left or it can go towards the right.

It cannot be penetrated the solid boundary to the left, so it has the only option of going toward the right, it cannot go further up, because heating is stopped here. But then, once this effect is gone, then gravity will play its role and it will come down, so once it comes down, it has to complete the loop to satisfy continuity. Because when fluid has gone from here, some other fluid should replenish back to maintain continuity.

So, in this way, a circulation is created. This is called as natural convection circulation. Okay. So, these kind of flow is, although we are saying natural, but it is actually again a pressure driven flow fundamental. Why it is a pressure driven flow? Here you have, let us say here

you have density  $\rho_1$ , here you have density  $\rho_2$ . Which density is more?  $\rho_1$ , let us assume for the time being that these air is treated as an ideal gas, so  $p/\rho$  is  $RT$ , right.

So that means, this density  $\rho_1$  greater than  $\rho_2$  means,  $p_1$  greater than  $p_2$ , so that means, there is actually a driving pressure gradient that is driving the flow. But the catch of the story is that this driving pressure gradient is not an externally impose pressure gradient, but an intrinsically created pressure gradient, because of density gradient which in turn is created, because of the temperature gradient within the domain.

So, it is possible that because of temperature gradient, there is a density gradient and that drives the flow, but density gradient can be created because of other gradients also, for example, there can be solutal concentration gradient in a multi component system. So, let us say there is a salt water system and the salt water system is freezing. So, when the salt water system is freezing, then there is a concentration gradient being created all the time as the salt water system is freezing.

As the concentration gradient is created, there is a density gradient created. Because, depending on the salt concentration, the density of the mixture would change. So, it is possible that there is a density gradient created not just because of temperature gradient, but may be because of a solutal concentration gradient, but whatever may be the reason.

If there is a natural or intrinsic density gradient that is created and that can drive this kind of flow may be due to temperature gradient, may be due to concentration gradient that we call as natural convection. Okay. Now what are the important intricacy of these natural convection, we will understand, natural convection for mathematical analysis is much more involved topic than force convection.

So, in the under-graduate level, we will not get into all the details of mathematical analysis of natural convection, but at least we will try to identify or try to derive the basic governing equations and do some order of magnitude analysis. We figure out that what are the various parameters which affect the heat transfer? So, one of the important thing to consider is that when you have a force convection, we have seen that the Nusselt number is the function of Reynolds number and Prandtl number, that much you have learn by this time.

Now here the Reynolds number is no more important, because there is no forced mechanism of driving the flow. So, the Nusselt number, of course it is expected to be a function of Prandtl number, it may or may not be, we will see, but in addition to that, the Nusselt number is likely to be a function of some other dimensionless number instead of Reynolds number. What are those dimensionless numbers and how the Nusselt number is related to that?

**(Refer Slide Time: 09:47)**

Steady, 2-D incompressible flow

Continuity:  $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$

x-mom:  $\rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \rho \left( \nu \frac{\partial^2 u}{\partial x^2} + \nu \frac{\partial^2 u}{\partial y^2} \right) - \frac{\partial p}{\partial x}$

y-mom:  $\rho \left( u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = \rho \left( \nu \frac{\partial^2 v}{\partial x^2} + \nu \frac{\partial^2 v}{\partial y^2} \right) - \frac{\partial p}{\partial y} - \rho g$

Energy:  $u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$

That will be one of the objectives of our further investigation. So, we will try to figure out, so let us figure out the governing equations; let us say that it is a 2-dimensional incompressible flow, so when I am telling that it is incompressible flow, you can pounce on me immediately and say that on one side, you are saying density is changing, on another side, how can you say that it is a incompressible flow? Right?

So, if you recall that during one of our preliminary discussions on recapitulation of fluid mechanics; I have talked about one example, which is called variable density incompressible flow. So, this is an example, where we are talking about that, so the incompressible flow does not necessarily mean that the density has to be constant, incompressible flow means that the volumetric strain rate is 0.

So, constant density flow is a special case of incompressible flow, so we are assuming steady 2-dimensional incompressible flow. Of course, you can have natural convection with unsteady 3 dimensional compressible; all these additional complexities taken into consideration, but to begin with; I don't want to complicate the situation with those and again just captured the essential physics of interest of natural convection.

So, the continuity equation; now let us say our x axis and y axis, say this is a x axis, this is y axis and we will be considering a boundary layer type of flow just like we have consider the flow over horizontal flat plate. Instead of horizontal flat plate, it is the vertical flat plate. So, why we are made it vertical? Is to make sure that the body force is important assuming that gravity in these direction.

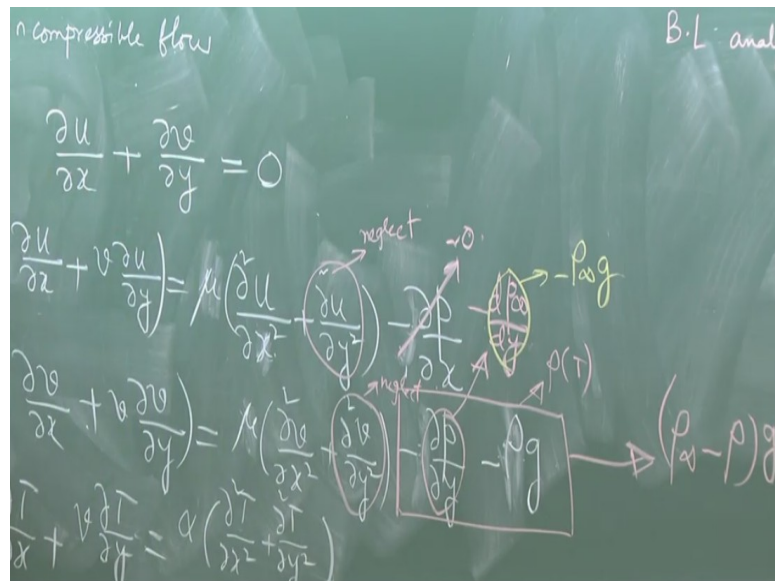
X momentum; let us write  $\frac{dp}{dx}$  for pressure gradient along x. The X momentum will not be important. Let us also write the energy equation; let us write all the equations. There is a rho; because rho is an important parameter here, let us prefer to keep the rho in the left-hand side and multiply all the terms by rho, so that you know, because rho is an important variable here.

I want to preserve the sanctity of rho. So, this will become mu, and this is rho, this is mu, okay. Now first let us try to qualitatively understand the inter linkage of these equations. First of all, these rho is a function of what? These rho is a function of temperature. How will you get temperature? You will get the temperature from the energy equation. Therefore, in the momentum equation, you have a term which contains temperature.

This rho, may be say polynomial function of temperature. So, rho be the function of temperature, you cannot now decouple the momentum equation and energy equation, so far in force convection, what we have done? We have solved the fluid flow velocity profile, we are substituted that velocity profile in the energy equation to get the temperature distribution, that is what we have done.

Now here we cannot do that, because while solving the fluid flow through the continuity and the momentum equations, you have a term which depends on temperature. So, the energy equation and the momentum equation becomes explicitly coupled not that you can solve the momentum equation separately and substitute that in the energy equation to get the temperature; that you cannot do for it in this case.

(Refer Slide Time: 17:59)



Now, question is that can we make certain simplifications, of course we cannot decouple these, but just for further analysis, can we make certain simplifications? So, one simplification is the boundary layer analysis. So, in the boundary layer analysis, first of all, out of these 2 terms which term will be important? What is the x reference length scale, that is the boundary layer thickness and what is the y reference length scale? That is the height of the plate.

Let us say, height of the plate is  $h$ . so assuming that  $\delta_R$ ,  $\delta_T$ , that is either the hydrodynamic or thermal boundary layer thickness is much less than the height of the plate, which is very similar to the kind of assumption that we made for force convection boundary layer. We can neglect this. Similarly, for y momentum equation, also we can neglect this. What is the other important substitution?

Whatever is the pressure gradient; see out of these 2 momentum equations just from pure intuition, can you tell which momentum equation is going to be more important for you? Y momentum equation, right. Because that is where the body force is coming into the picture. So, in the y momentum equation, so in the momentum equation for the dominant flow direction, if you have a pressure gradient, that pressure gradient is, a pressure gradient that is imposed from outside the boundary layer.

Just like so in the for the force convection over a flat plate, where the direction of plate was x direction, then you had the  $-\frac{dp}{dx} = -\frac{dp}{dx}$ . So here similarly, for the boundary layer analysis  $-\frac{\partial p}{\partial y}$  is  $-\frac{dp}{dy}$  and this  $\frac{\partial p}{\partial x}$  will be 0. Just draw the analogy with force convection over horizontal flat plate and natural convection over a vertical plate. I am only a little bit confusing to you.

Because of the fact that in a force convection case, we consider the x axis to be along the plate, now y axis is along the plate, that is the only difference. But if you are more comfortable with putting x axis along the plate, you can do that. I mean it should not matter, because which term is important or not, that should be decided from the physics and not from whether it is x or y. So that should be kept in mind.

So, you can see, now what is  $\frac{dp}{dy}$ ? What is infinity here? So, there is a heated flat plate, there is a convection current close to the plate but far away from plate what is there? Far away from plate, there is no motion of the fluid, right. So, there is a big difference between natural convection and force convection. Force convection at the edge of the boundary layer,  $u$  is  $u_{\infty}$ , right.

Force convection over a flat plate, but in natural convection at the edge of the boundary layer, what is  $u$ ?  $u$  is 0,  $u$  means here  $v$ ; here instead of  $u$ , you have to consider  $v$ . So, the velocity outside the boundary layer is 0, because there is no mechanism that is forcefully driving the flow. On the other hand, for force convection, you have  $u = u_{\infty}$  at  $y = \delta$ , basically  $y$  or  $x$  depending on the coding.

So then if there is no fluid motion in the fast stream, then what is  $\frac{dp}{dy}$ ? This is governed by what? This is governed by fluid statics, right, because their fluid is under rest, so if fluid is under rest, what is  $\frac{dp}{dy}$ ?  $-\rho_{\infty} g$ , right. This is the fluid statics, possibly the first chapter in fluid mechanics that you have studied. So, if you consider these 2 terms together, so what is the net term?

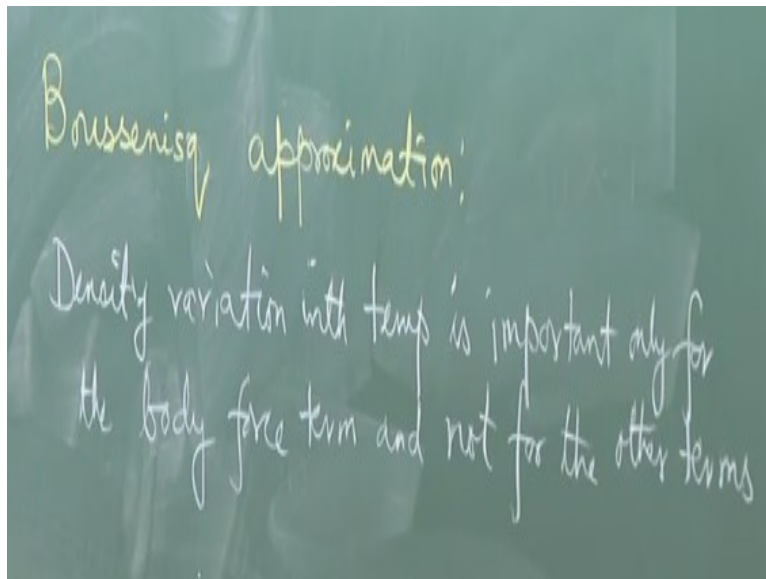
These  $-$  with these  $-$ , will become  $+$ , so  $\rho_{\infty} - \rho g$ . Question is that when we are having a  $\rho$  which is a function of temperature, then in the left-hand side also there is a  $\rho$  which should be a function of temperature, but out of these 2 effects, which effect is primary?

Which effect is secondary? right. The question is that if rho is a function of temperature for governing the physics of the problem.

Rho is the function of temperature in these term or rho is the function of temperature in these term, which is the primary effect and which is the secondary effect? Which is actually driving the flow? See, this body force that is driving the flow, so this rho being the function of temperature, is the primary effect, these rho being the function of temperature is also a physical effect but that is the secondary effect to the problem.

The primary effect in these rhos being the function of temperature. So, to simplify the problem, one important assumption was done, made by Boussinesq, what he made is an, he made an assumption that he considers the density variation with temperature to be important only for the body force term and not for the other term. So here, he considers  $\rho = \rho_{\infty}$ , this is an assumption.

**(Refer Slide Time: 25:55)**



This is not the reality, here also rho will change, but you know these are certain levels of simplifications to make your analysis more and more mathematically tractable.