

Computational Fluid Dynamics for Incompressible Flows

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Module 11: Finite Volume Method- 2

Lecture 1

Finite Volume Discretization of Steady Convection- Diffusion

Hello everyone, so in last module we discussed about the Finite Volume Discretization of diffusion equation. So now, we will add the convection term and we will discretize the steady convection diffusion equation using finite volume method in this module, in this lecture so, first let us write the governing equation.

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Finite Volume Discretization of Convection-Diffusion Equation

2-D steady convection-diffusion equation

$$\frac{\partial(\rho u \phi)}{\partial x} + \frac{\partial(\rho v \phi)}{\partial y} = \frac{\partial}{\partial x} \left(\Gamma \frac{\partial \phi}{\partial x} \right) + \frac{\partial}{\partial y} \left(\Gamma \frac{\partial \phi}{\partial y} \right) + S$$

For known velocity, the above equation is linear

$$\nabla \cdot (\rho \vec{u} \phi) = \nabla \cdot (\Gamma \nabla \phi) + S$$
$$\vec{u} = u \hat{i} + v \hat{j}$$
$$\nabla \cdot (\rho \vec{u} \phi - \Gamma \nabla \phi) = S$$
$$\nabla \cdot \vec{J} = S \quad \text{where } \vec{J} = \rho \vec{u} \phi - \Gamma \nabla \phi \rightarrow \text{flux vector}$$

So, we are considering 2D steady, so we have convection terms as well as diffusion term. So, convection diffusion equation so, the governing equation is $\rho u \phi$ by del x, where ρ is the fluid density and u is the velocity in x direction, then $\rho v \phi$ by del y, v is the velocity in y direction is equal to del of del x gamma del phi del x, gamma is the diffusion coefficient plus del of del y gamma del phi del y plus s .

So, we have written this governing equation for general variable ϕ and u , v are the velocities in x and y direction. So, if velocities are known, obviously this equation is linear. So, for known velocity, the above equation is linear.

So, we discussed that if this is your x direction, this is your y direction then, u is the velocity in x direction, v is the velocity in y direction and i is the unit vector in x direction and j is the unit vector in y direction. Now, let us consider this finite volume of cell P , so, you can see this is the main control volume, this P and the face centers are small e , small n , small w and small s .

So, we will integrate this governing equation over this control volume main cell P . So, let us write this governing equation in vector form first and write in terms of the flux vector. So, the governing equation you can write in vector form as divergence of $\rho u \phi$ is equal to divergence of $\Gamma \nabla \phi$ plus the source term. So, you can see that u is obviously your velocity vector and now we can write as divergence of $\rho u \phi$ and this diffusion term you bring in left hand side, so what you will get? Divergence of minus $\Gamma \nabla \phi$ is equal to S .

So, now we will introduce the flux vector j is equal to S where j is the flux vector $\rho u \phi$ minus $\Gamma \nabla \phi$ so, j is the flux vector. So, in last module you have seen this flux vector contain only the diffusion term, but in this lecture you can see the flux vector contains convection terms as well as the diffusion term.

So, the first term is the convection term and second term is the diffusion term and this equation divergence of j is equal to S , you have already discretize in last class and you know all the assumptions involved while integrating this equation in the main cell P . So, we will follow the same procedure, we will have the same assumptions valid here and we will write the discretize equation for this divergence of j is equal to S .

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Finite Volume Discretization of Convection-Diffusion Equation

$$\nabla \cdot \vec{j} = S$$

$$\int_V \nabla \cdot \vec{j} \, dV = \int_V S \, dV$$

Use Gauss divergence theorem

$$\int_A \vec{j} \cdot d\vec{S} = \int_V S \, dV$$

$$\sum \vec{j}_f \cdot \vec{S}_f = \bar{S} \Delta V$$

$$\vec{j}_e \cdot \vec{S}_e + \vec{j}_w \cdot \vec{S}_w + \vec{j}_n \cdot \vec{S}_n + \vec{j}_s \cdot \vec{S}_s = \bar{S} \Delta V$$

$$\vec{j}_e \cdot \vec{S}_e = (\rho u \phi)_e A_e - \Gamma \left(\frac{\partial \phi}{\partial x} \right)_e A_e$$

$$= (\rho u A)_e \phi_e - \Gamma_e A_e \frac{\phi_E - \phi_P}{(\delta x)_e}$$

$$= F_e \phi_e - D_e (\phi_E - \phi_P)$$

Mass flow rate, $F_e = \rho u_e A_e = \rho \frac{u_E + u_P}{2} A_e$ assuming uniform grid

$$\phi_e = \frac{\phi_E + \phi_P}{2} \rightarrow \text{Central Difference Convection scheme.}$$

for uniform grid

$F_e \phi_e$
convective coefficient convected variable

So, first integrate over this control volume so, divergence of j is equal to S where integrating over the main cell P divergence of $j \, dv$ plus, sorry equal to volumetrical $s \, dv$. Now, use Gauss divergence theorem so, you can write integral so, now we are converting the volume integral to surface integral.

So, $j \cdot ds$ is equal volume integral $s \, dv$. We followed the same procedure, till now we have not assumed anything, now we will assume that j varies linearly along the faces and the average value lies at the face center so, face center small e , small n , small w and small s and for the volume integral of the source term also we will have the average value lies at the cell center P .

So, with that now, we can write this integral over the faces that we can write summation of $j \cdot ds$ so, ds is the surface vector at the faces equal to \bar{S} is the average value lies at the cell center P and ΔV so, this now we can write j_e so, we have four faces for this two dimensional cases so, East, West, North and South so, we will write $J_e \cdot S_e$ plus $J_w \cdot S_w$ plus $J_n \cdot S_n$ plus $J_s \cdot S_s$ is equal to $\bar{S} \Delta V$.

So now, each flux vector at the faces we have two terms, one is convection and diffusion term. The diffusion term already you know how to discretize so, we will have the assumption that the flux, while calculating the flux vector we will assume that the value

of ϕ varies linearly between the cell centroids. So, obviously the gradient of ϕ at the face center will calculate using the neighbor cell centered value and its main control volume cell center value.

So, first let us see how that how we will calculate $J_e \cdot S_e$, then similarly we can write for other terms. So, $J_e \cdot S_e$, what is J ? So, J is $\rho u \phi$ minus $\gamma \nabla \phi$ so, now J_e will be $\rho u \phi$ at face E minus $\gamma \nabla \phi$ at face E , what is the surface vector? S_e , S_e is $A_e i$ so, now we can see this is your J_e , this is your S_e now, if you make the dot product, and what is $\nabla \phi$? $\nabla \phi$ is $\frac{\partial \phi}{\partial x} i + \frac{\partial \phi}{\partial y} j$.

So, now you make the dot product and write the terms so, convection term you see, this is the convection term $\rho u \phi$ so, u is again u_i plus v_j . So, if you make the dot product with u and S_e then you will get only $u_e A_e$, $u_e A_e$ because $i \cdot i$ will be 1 and $i \cdot j$ will be 0 so, only this term will remain $u_e A_e$. So, it will be $\rho u \phi$ at East face into A_e minus $\gamma \frac{\partial \phi}{\partial x}$ because it is $\nabla \phi$, $\frac{\partial \phi}{\partial x} i$ and you are making the dot product with A_e so, $\frac{\partial \phi}{\partial x}$ into A_e so, so $\frac{\partial \phi}{\partial x}$ at East face A_e .

So now, we can rearrange it so, we can write as $\rho u A_e$ at East face and ϕ_e you are taking outside of this and minus, now you can see γA_e and $\frac{\partial \phi}{\partial x}$ at face center E so, that we will use ϕ_E minus ϕ_P divided by the distance between this two cell centers. So, now this will represent as mass flow rate F_e into ϕ_e and γA_e by Δx_e will represent with D_e into ϕ_E minus ϕ_P . The last term you have already discretize in the earlier lectures but the first term now, we are introducing with the mass flow rate F_e so, we are introducing mass flow rate F_e is equal to $\rho U_e A_e$.

So, now you can see that U_e , the velocity at the face center E , this is not known because you might have the values available at the cell center P so, you can use a linear average so, you can use as ρ if you have a uniform grid then you can write U_e plus U_P divided by 2 into A_e where we are using, assuming uniform grid.

So, now F_e is the mass flow rate and ϕ_e is the value of ϕ at the face center. So, this is also unknown, ϕ is also unknown because ϕ you are solving only at the cell centroids but you need to find the value of ϕ at the face center ϕ_e so, for simplicity let us use the central difference and ϕ_e we can use the value of ϕ_E plus ϕ_P divided by 2 so, this is known as central difference convection scheme.

If you see $F_e \phi$, the value of ϕ_e sometime we will determine depending on the value of F_e , whether it is positive or negative so, F_e is known as convective coefficient and ϕ_e is known as convected variable. So, you can see ϕ_e is the convected variable so, this mass flow rate whatever F_e is there it is known as convective coefficient and due to the mass flow rate this ϕ_e is transported, so that is why it is convected variable and to determine the value of ϕ_e from the sign of F_e , we will use some convection schemes and then we will discuss later in later classes.

So, now for these if you use the central difference convection scheme ϕ is equal to ϕ_e plus ϕ_P divided by 2 for uniform grid, for uniform grid then what you can write now $J_e \cdot S_e$ so, let us write down.

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Finite Volume Discretization of Convection-Diffusion Equation

$$\vec{J}_e \cdot \vec{S}_e = \frac{F_e}{2} (\phi_E + \phi_P) - D_e (\phi_E - \phi_P)$$

$$\vec{J}_w \cdot \vec{S}_w = -(\rho u \phi)_w A_w + \Gamma_w A_w \left(\frac{\partial \phi}{\partial x} \right)_w \quad \vec{J}_w = (\rho u)_w - (\Gamma \nabla \phi)_w$$

$$= -F_w \phi_w + \Gamma_w A_w \frac{(\phi_P - \phi_W)}{\Delta x} \quad \vec{S}_w = -A_w \hat{i}$$

$$= -\frac{F_w}{2} (\phi_P + \phi_W) + D_w (\phi_P - \phi_W) \quad \vec{S}_s = -A_s \hat{j}$$

$$\vec{J}_n \cdot \vec{S}_n = \frac{F_n}{2} (\phi_N + \phi_P) - D_n (\phi_N - \phi_P) \quad F_n = \rho v_n A_n$$

$$\vec{J}_s \cdot \vec{S}_s = -\frac{F_s}{2} (\phi_P + \phi_S) + D_s (\phi_P - \phi_S) \quad F_s = \rho v_s A_s$$

$$\vec{J}_e \cdot \vec{S}_e + \vec{J}_w \cdot \vec{S}_w + \vec{J}_n \cdot \vec{S}_n + \vec{J}_s \cdot \vec{S}_s = \bar{S} \Delta V$$

$$\frac{F_e}{2} (\phi_E + \phi_P) - D_e (\phi_E - \phi_P) - \frac{F_w}{2} (\phi_P + \phi_W) + D_w (\phi_P - \phi_W)$$

$$+ \frac{F_n}{2} (\phi_N + \phi_P) - D_n (\phi_N - \phi_P) - \frac{F_s}{2} (\phi_P + \phi_S) + D_s (\phi_P - \phi_S) = \bar{S} \Delta V$$

$$\left(D_e + \frac{F_e}{2} + D_w - \frac{F_w}{2} + D_n + \frac{F_n}{2} + D_s - \frac{F_s}{2} \right) \phi_P = (D_e - \frac{F_e}{2}) \phi_E + (D_w + \frac{F_w}{2}) \phi_W$$

$$+ (D_n - \frac{F_n}{2}) \phi_N + (D_s + \frac{F_s}{2}) \phi_S = \bar{S} \Delta V$$

$$a_P = D_e + \frac{F_e}{2} + D_w - \frac{F_w}{2} + D_n + \frac{F_n}{2} + D_s - \frac{F_s}{2}$$

$$= \underbrace{D_e - \frac{F_e}{2}}_{a_E} + \underbrace{D_w + \frac{F_w}{2}}_{a_W} + \underbrace{D_n - \frac{F_n}{2}}_{a_N} + \underbrace{D_s + \frac{F_s}{2}}_{a_S} + \bar{S} \Delta V$$

So, $\vec{J}_e \cdot \vec{S}_e$ now, we can write F_e by 2 then we have a average value ϕ_E plus ϕ_P minus D_e convection term and ϕ_E minus ϕ_P . So, we have written this flux vector dot product with the surface vector at the East face. Now, let us write for West face. So, $\vec{J}_w \cdot \vec{S}_w$, similarly now you can see it will be $\rho u \phi$ at West face. Now, if you make that dot product with \vec{J}_w with the \vec{S}_w . So, \vec{J}_w is $\rho u \phi_w$ minus $\gamma w \phi$ at w and \vec{S}_w is $-\hat{i}$.

So, this you have to remember because this is minus because at this space you face normal in negative x direction so, that is why it is minus $A_w \hat{i}$ so, now if you make a dot product obviously it will become minus A_w similarly, here also you will get minus 1 convection term is there and another minus will come it will be a dot product and you will get plus and you write $\gamma w A_w$ and $\frac{\partial \phi}{\partial x}$ at w . So now, you can write it so, now you use the convection minus $F_w \phi_w$ and plus $\gamma w A_w$. Now, $\frac{\partial \phi}{\partial x}$ at w so, it will be ϕ_P minus ϕ_W divided by Δx_w .

So, now rearrange it so, you will get F_w will take the convection scheme, central difference convection scheme, so minus F_w by 2 so, it will average ϕ_P plus ϕ_W by 2. So, it is ϕ_P plus ϕ_W and this is your plus D_e and ϕ_P minus ϕ_W . Now, similarly if you do $\vec{J}_n \cdot \vec{S}_n$ so, you can write as F_n by 2 ϕ_N plus ϕ_P minus $D_n \phi_N$ minus ϕ_P .

So, this is your convection term, diffusion term where F_n is now you have ρV_n into A_n because now you have the u velocity and $J S_n$ is your ρJ . So, now if you make a dot product so it will be $v J \cdot n$ so it will be $V A_n$ and that $\rho V_n A_n$ we are writing as the mass flow rate at North face F_n .

So, similarly you can write $J_s \cdot S_s$ so, it will be F_s by 2 so, you remember we are using central difference convection scheme, it will be $\phi_P + \phi_S$ and here minus sign will be there because S_s will be minus $A_s J$ so, due to that minus sign will come and you have plus $D_s \phi_P - \phi_S$. So, we have written all the terms.

Now, let us put in the summation of $J \cdot S F$ is equal to S equation. So, we have $J_e \cdot S_e$ so, your F_s will be $\rho V_s A_s$ so, $S_e + J_w \cdot S_w + J_n \cdot S_n + J_s \cdot S_s$ equal to $\bar{S} \Delta V$. So, now let us put all this values so, you can see here it will be F_e by 2 $\phi_E + \phi_P - D_e \phi_E - \phi_P$. So, this is your $J_e \cdot S_e + J_w \cdot S_w$, this one you write so, you can write minus F_w by 2 $\phi_P + \phi_W$ plus, sorry, here it will be D_w so, it will be $D_w \phi_P - \phi_W$. So, this for the West face.

Now, for the North face the flux is, plus F_n by 2 $\phi_N + \phi_P - D_n \phi_N - \phi_P - F_s$ by 2 $\phi_P + \phi_S$ and you have plus $D_s \phi_P - \phi_S$ equal to $\bar{S} \Delta V$. So now, we will write this equation in the form of $A_p \phi_p$ so, you collect all the terms of ϕ_p in the left hand side and the rest all other terms you take in the right hand side.

So, which are the p terms? So, this is so, these are the ϕ_p terms so, all this coefficient will write in the left hand side. So, if you write that so, you see it will be F_e by 2 and minus minus plus so, this will be plus D_e so, we will write $D_e + F_e$ by 2, similarly here you see this is your $D_w + D_w$ so, plus D_w and here p coefficient minus F_w .

So, minus F_w by 2, for north face you can see this is your minus minus plus so it will be $D_n + F_n$ by 2 plus for South, so it will be ϕ_p so, it will be D_s and it will be minus F_s by 2. These are the coefficient of ϕ_P , so this is your diagonal coefficient equal to now, other terms you take in the right hand side so, if you take ϕ_e term then you take ϕ_w , then you take ϕ_n and then you take ϕ_s in the right hand side.

So, you can see, if you write the coefficient of ϕ_e then you can see ϕ is here minus $D_e \phi$, so, right hand side if you take it will be positive D and here if you see F_e by 2 ϕ so, it will be minus F_e by 2 so, it is coefficient of ϕ similarly now you see ϕ_w so, here minus $D_w \phi_w$ so, it will be, right hand side if you bring it, it will be D_w and here you have minus F_w by 2 so, it will become plus F_w by 2.

Similarly, for North it is D_n , it will be minus because the left hand side you are bringing it in to the right hand side so, minus F_n by 2 ϕ_N and ϕ_S , so it will be plus D_s plus F_s by 2 ϕ_S is equal to $S \bar{\Delta} V$. So now, these coefficient you just write it as coefficient a_e , this is as a_w , this is as a_n and this coefficient as a_s . So, if you write that then what you can write the left hand side term, this first coefficient you can see so, we will denote it as a_p , so this will denote as a_p , so a_p you can write as D_e plus F_e by 2 plus D_w minus F_w by 2 plus D_n plus F_n by 2 plus D_s minus F_s by 2.

So, we will rearrange it now, you can see a_e is D_e minus F_e by 2 so, we will write first this terms as D_e minus F_e by 2. So, if you write D_e minus F_e by 2 then another F_e by 2 we have to add so, F_e by 2 plus F_e by 2. This will get cancelled so, F_e by 2 will remain. Now, this together you can see it is F_e , this is F_e . So, similarly you can write D_w so, now we have in a_w coefficient D_w plus F_w by 2 so we will write F_w by 2 and we will subtract F_w by 2 and another minus F_w by 2 is there, so now this together will give minus F_w .

Similarly, D_n so n counters minus F_n by 2 so, we will write minus F_n by 2 plus F_n by 2 and another F_n by 2 is there so this together will give F_n and plus D_s plus F_s by 2 and we have now subtract minus F_s by 2 and another F_s by 2 is there so, this together will give F_s . So, now this a_p we can write as this term, this is a_n , this is term this is your A_w , this is your A_n and this is your A_s , so, we can write as a_E plus this is your a_W plus a_N plus a_S so, these are the coefficient and we have now this together, this together will give plus F_e minus F_w plus F_n minus F_s .

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Finite Volume Discretization of Convection-Diffusion Equation

$$a_p = a_E + a_W + a_N + a_S + F_e - F_w + F_n - F_s$$

$$= \sum a_{nb} + \sum F_f$$

$$\sum F_f = F_e - F_w + F_n - F_s$$

$$= \rho u_e \Delta y - \rho u_w \Delta y + \rho v_n \Delta x - \rho v_s \Delta x$$

$$= \text{net mass outflow from the cell P.}$$

$$a_p \phi_p = a_E \phi_E$$

Finite Volume Discretization of Convection-Diffusion Equation

$$\vec{J}_e \cdot \vec{S}_e = \frac{F_e}{2} (\phi_E + \phi_P) - D_e (\phi_E - \phi_P)$$

$$\vec{J}_w \cdot \vec{S}_w = -(\rho u \phi)_w A_w + \Gamma_w A_w \left(\frac{\partial \phi}{\partial x} \right)_w$$

$$= -F_w \phi_w + \Gamma_w A_w \frac{(\phi_P - \phi_W)}{(\Delta x)_w}$$

$$= -\frac{F_w}{2} (\phi_P + \phi_W) + D_w (\phi_P - \phi_W)$$

$$\vec{J}_n \cdot \vec{S}_n = \frac{F_n}{2} (\phi_N + \phi_P) - D_n (\phi_N - \phi_P)$$

$$\vec{J}_s \cdot \vec{S}_s = -\frac{F_s}{2} (\phi_P + \phi_S) + D_s (\phi_P - \phi_S)$$

$$\vec{J}_e \cdot \vec{S}_e + \vec{J}_w \cdot \vec{S}_w + \vec{J}_n \cdot \vec{S}_n + \vec{J}_s \cdot \vec{S}_s = \bar{S} \Delta V$$

$$\frac{F_e}{2} (\phi_E + \phi_P) - D_e (\phi_E - \phi_P) - \frac{F_w}{2} (\phi_P + \phi_W) + D_w (\phi_P - \phi_W)$$

$$+ \frac{F_n}{2} (\phi_N + \phi_P) - D_n (\phi_N - \phi_P) - \frac{F_s}{2} (\phi_P + \phi_S) + D_s (\phi_P - \phi_S) = \bar{S} \Delta V$$

$$\left(D_e + \frac{F_e}{2} + D_w - \frac{F_w}{2} + D_n + \frac{F_n}{2} + D_s - \frac{F_s}{2} \right) \phi_P = (D_e - \frac{F_e}{2}) \phi_E + (D_w + \frac{F_w}{2}) \phi_W$$

$$+ (D_n - \frac{F_n}{2}) \phi_N + (D_s + \frac{F_s}{2}) \phi_S + \bar{S} \Delta V$$

$$a_p = D_e + \frac{F_e}{2} + D_w - \frac{F_w}{2} + D_n + \frac{F_n}{2} + D_s - \frac{F_s}{2}$$

$$= D_e - \frac{F_e}{2} + \frac{F_e + F_e}{2} + D_w + \frac{F_w}{2} - \frac{F_w - F_w}{2} + D_n - \frac{F_n}{2} + \frac{F_n + F_n}{2} + D_s + \frac{F_s}{2} - \frac{F_s - F_s}{2}$$

$$= a_E + a_W + a_N + a_S + F_e - F_w + F_n - F_s$$

Finite Volume Discretization of Convection-Diffusion Equation

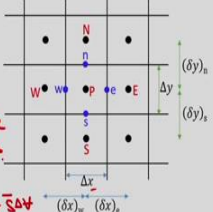
$$a_p = a_E + a_W + a_N + a_S + F_e - F_w + F_n - F_s$$

$$= \sum a_{nb} + \sum F_f$$

$$\sum F_f = F_e - F_w + F_n - F_s$$

$$= \rho U_e \Delta y - \rho U_w \Delta y + \rho V_n \Delta x - \rho V_s \Delta x$$

$$= \text{net mass outflow from the cell P.}$$



$$a_p \phi_p = a_E \phi_E + a_W \phi_W + a_N \phi_N + a_S \phi_S + \bar{S} \Delta V$$

$$a_p \phi_p = \sum_{nb} a_{nb} \phi_{nb} + b_p$$

$$b_p = \bar{S} \Delta V \quad a_E = D_e - \frac{F_e}{2} \quad a_W = D_w + \frac{F_w}{2} \quad a_N = D_n - \frac{F_n}{2} \quad a_S = D_s + \frac{F_s}{2}$$

$$a_p = a_E + a_W + a_N + a_S + F_e - F_w + F_n - F_s$$

$$a_p = \sum a_{nb} + \sum F_f$$

$$F_e = \rho U_e A_e$$

$$F_w = \rho U_w A_w$$

$$F_n = \rho V_n A_n$$

$$F_s = \rho V_s A_s$$

$$D_e = \frac{\Gamma_e A_e}{(\delta x)_e}$$

$$D_w = \frac{\Gamma_w A_w}{(\delta x)_w}$$

$$D_n = \frac{\Gamma_n A_n}{(\delta y)_n}$$

$$D_s = \frac{\Gamma_s A_s}{(\delta y)_s}$$

$$A_e = A_w = \Delta y$$

$$A_n = A_s = \Delta x$$

$$\phi_p \rightarrow \phi_{i,j}$$

$$\phi_E \rightarrow \phi_{i+1,j}$$

$$\phi_W \rightarrow \phi_{i-1,j}$$

$$\phi_N \rightarrow \phi_{i,j+1}$$

$$\phi_S \rightarrow \phi_{i,j-1}$$

So now, you can write F_e as a_E plus a_W plus a_N plus a_S plus F_e minus F_w plus F_n minus F_s and this you can write as summation of a_{nb} because all the neighbor coefficient summation plus summation of F_f , what is F_f ? So, what does it signify? F_e minus F_w minus F_n minus F_s , so this is the net outflow from the control volume P.

So, that means it is the continuity equation, so if you integrate the continuity equation over this volume then you will get this so, that means summation of F_f is F_e minus F_w plus F_n minus F_s , and you know what is F_e ? F_e is $\rho U_e A_e$, A_e is your Δy minus F_w is $\rho U_w \Delta y$ plus ρV_n , V_n and the area is Δx and minus ρV_s into Δx and this is the net mass outflow from the cell P. Net mass outflow from the cell P so, you can see that if your flow field satisfy the continuity equation, then summation of F_f will become 0, so, generally at convergence summation of F_f will be tending to 0.

So now, you can write the final form of the discretize equation, so we can write $a_P \phi_P$ is equal to a_E , so you look this one so, this is your discretize equation so, you can write $a_E \phi_E$ plus $a_W \phi_W$ plus $a_N \phi_N$ plus $a_S \phi_S$, sorry this will be plus so, plus $\bar{S} \Delta V$, so we can write $a_E \phi_E$ plus $a_W \phi_W$ plus $a_N \phi_N$ plus $a_S \phi_S$ plus $\bar{S} \Delta V$.

So, this now you can write as $a_P \phi_P$ is equal to summation of $a_{nb} \phi_{nb}$ all the neighbor, $a_{nb} \phi_{nb}$ plus, so $\bar{S} \Delta V$ will denote as b . So, you have b is equal to $\bar{S} \Delta V$.

a_E is your D_e minus F_e by 2, a_W is D_w plus F_w by 2, a_N is D_n minus F_n by 2 and a_S is D_s plus F_s by 2 and the diagonal coefficient will be just a_E plus a_W plus a_N plus a_S minus summation or plus F_e minus F_w plus F_n minus F_s . So, you can write a_P as summation of all the neighbor coefficient plus summation of F_f .

And what about your F_e F_w ? So, F_e is $\rho U_e A_e$, A is nothing but your Δy , F_w is $\rho U_w A_w$, F_n is $\rho V_n A_n$, and F_s is $\rho V_s A_s$, and you have D_e , so D_e will be $\frac{\gamma_e A_e}{\Delta x_e}$, D_w is $\frac{\gamma_w A_w}{\Delta x_w}$ and D_n is $\frac{\gamma_n A_n}{\Delta x_n}$ and D_s is $\frac{\gamma_s A_s}{\Delta y}$, sorry here Δy .

So, this is your Δy and $\frac{\gamma_s A_s}{\Delta y}$ where A_e is equal to A_w is equal to, this is the surface area so this is your Δy and A_{north} is equal to A_{south} is this distance so, this will be Δx , so it will be Δx . So, you can see so, this is the final algebraic equation for this steady convection diffusion equation and this you need to solve using some linear solver and where P , ϕ_P denotes ϕ_{ij} , ϕ_E denotes ϕ_{i+1j} , ϕ_W denotes ϕ_{i-1j} , and ϕ_N denotes ϕ_{ij+1} and ϕ_S denotes ϕ_{ij-1} .

So, in today's class we discretize steady convection diffusion equation, so we considered two dimensional case and we introduce the flux vector which contains diffusion term as well as the convection term. Then we integrated this over the control volume P and we have converted the volume integral to surface integral using Gauss divergence theorem.

Then each flux vector at each faces, the flux vector dot product with the surface vector, we have calculate at each faces East, West, North and South and we defined mass flow rate F_e as $\rho U_e A_e$ and similarly for the north face F_n is equal to $\rho V_n A_n$ and finally after rearranging we have written the discretize form in the form of $a_P \phi_P$.

So, we have written $a_P \phi_P$ is equal to summation $a_n \phi_n$ plus b , where a_P is the diagonal coefficient and this diagonal coefficient a_P is equal to summation of all the neighbor coefficient, a_P is equal to a_E plus a_W plus a_{north} plus a_{south} plus the summation of F_f , where summation of F_f denotes the net mass flow outlet from the cell P

and it actually is the discretize form of the continuity equation. So, if you flow field satisfy the continuity, then the summation of F_f will become 0. Thank you.