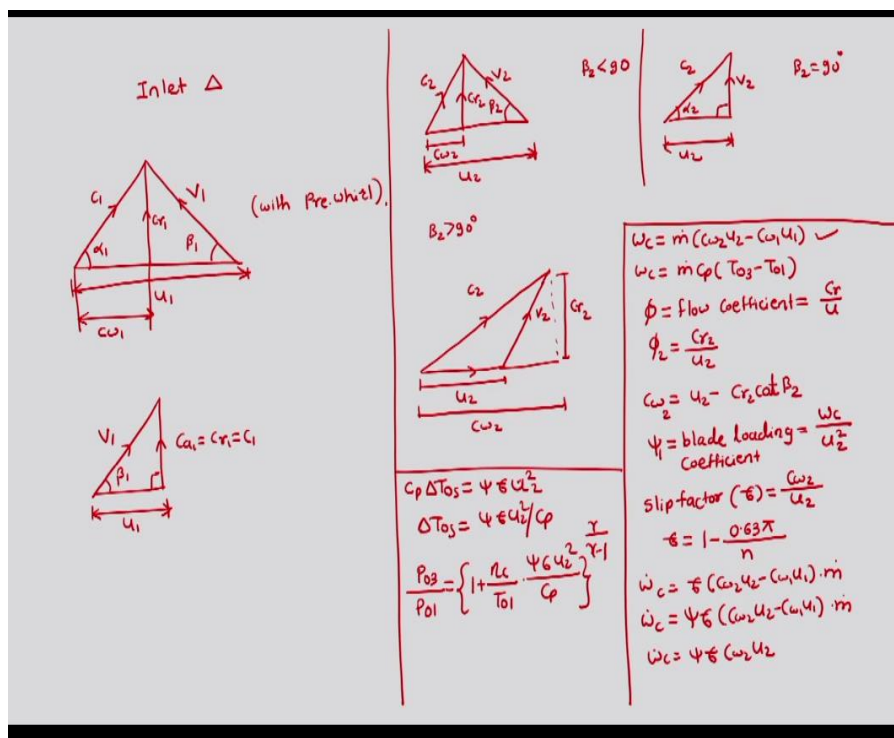


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**Lecture - 28**  
**Examples of Centrifugal Compressor**

Welcome to the class. We have till time seen about the centrifugal compressor and now we are going to go ahead with the examples on centrifugal compressor. So, before starting the examples, we will make recapitulation about the centrifugal compressor.

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What we know is inlet velocity triangle and inlet velocity triangle is like this for centrifugal compressor where we have this is  $C_{r1}$ , this is  $C_1$ , this is  $V_1$  and then big length is  $u_1$  and then this is  $C_{w1}$ . So, angle made by  $C_1$  is  $\alpha_1$  and  $v_1$  is  $\beta_1$ . So, this is inlet velocity triangle with prewhirl. If there is no prewhirl that is without guide when we know that the velocity triangle would be of this kind where we have  $C_{a1} = C_{r1} = C_1$ . This is  $v_1$ ,  $\alpha_1$  is 90 degree, this is  $\beta_1$  and then we have  $u_1$ .

Then, we have outlet velocity triangles, which are of 3 types. Outlet velocity triangle of this kind is for backward sweep which is  $\beta_2$  less than 90, so this is  $v_2$ , this is  $\beta_2$ , this is  $u_2$ , and this is  $C_2$  and  $c_{w2}$  where the central vertical line is  $C_{r2}$ . Then, for  $\beta$  equal to 90 which is for radial

case. For radial outlet, we have velocity triangle of this kind where we have this as  $u_2$ , this is  $v_2$  and this is  $c_2$ .

This is  $\alpha_2$ ,  $\beta_2$  is equal to 90 degree, then we have the velocity triangle which is for  $\beta_2$  greater than 90 degree, which is forward sweep and for forward sweep velocity triangle is of this kind where this is  $V_2$ , this is  $C_2$ , this is  $u_2$  and then we have this big as  $C_{w2}$  and then this is  $C_{r2}$ . So, this is about the velocity triangle for the centrifugal compressor. Then, we have some formulas what we had seen.

The first formula what we know is about compressor power where we have

$$\dot{m}(C_{w2} u_2 - C_{w1} u_1)$$

. Similarly, compressor power input is also

$$\dot{m}C_p(T_{03} - T_{01})$$

We have seen that  $\phi$  is flow coefficient and its definition we have made it as  $C_r/u$ . So, in general we needed  $\phi_2$  which was  $C_{r2}/u_2$  and then from the velocity triangle we can in general write  $C_{w2} = u_2 - c_{r2} \cot\beta_2$ .

Further we know  $\Psi$  which is a blading coefficient, blade loading coefficient which is also called as pressure coefficient and this is  $W_c/u^2$ . Then, we have slip factor which is  $\sigma$  and for that we are knowing it is tangential velocity ratio divided by  $u_2$  and then this  $\sigma$  has a correlation as  $1 - 0.63 \phi/n$  where  $n$  is number of blades. Ideal work input whatever we have written was this.

But this work input with slip factor  $\sigma C_{w2} u_2 - C_{w1} u_1 \times \dot{m}$ . if there is frictional loss or windage then we have formula  $\Psi \sigma (C_{w2} u_2 - c_{w1}) u_1 \times \dot{m}$ . So, in a particular case, we can write down the formula without inlet prewhirl as

$$\dot{w} = \Psi \sigma C_{w2} u_2.$$

Further we have formula for stage temperature rise which is  $\Delta T_0$ s and then that we can write down for the radial exit as  $\Psi \sigma u_2^2$ .

So,  $\Delta T_0$ s was  $\Psi \sigma u_2^2 / C_p$ . Similarly, we have pressure ratio

$$\frac{P_{03}}{P_{01}} = \left( 1 + \left( \frac{\eta}{T_{01}} \right) \left( \frac{\Psi \sigma u_2^2}{C_p} \right) \right)^{\frac{\gamma}{\gamma-1}}$$

So, this is recapitulation of centrifugal compressor for velocity triangle on various diagrams.

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A centrifugal compressor runs at speed 11,500 rev/min. It takes air at 21°C and compresses it from 1 bar to 4 bar. Impeller diameter is 75cm and slip factor is 0.92. Find the isentropic efficiency of the compressor

given -  $N = 11,500 \text{ RPM}$     $T_{01} = 21^\circ\text{C} = 294 \text{ K}$     $P_{01} = 1 \text{ bar}$     $P_{03} = 4 \text{ bar}$   
 $\sigma = 0.92$     $D_2 = 75 \text{ cm} = 0.75 \text{ m}$     $\rightarrow \eta_c = ?$     $\gamma = 1$

$$\frac{P_{03}}{P_{01}} = \left\{ 1 + \frac{\eta_c \cdot \sigma \cdot u_2^2}{C_p T_{01}} \right\}^{\frac{\gamma}{\gamma-1}}$$

$$4 = \left\{ 1 + \frac{\eta_c \times 1 \times 0.92 \cdot u_2^2}{1005 \times 294} \right\}^{\frac{\gamma}{\gamma-1}}$$

$$u_2 = \frac{\pi D_2 N}{60} = \frac{3.14 \times 0.75 \times 11500}{60} = 451.37 \text{ m/s}$$

$$(4)^{\frac{\gamma-1}{\gamma}} = 1 + \frac{\eta_c \times 1 \times 0.92 \times (451.37)^2}{1005 \times 294}$$

$$\eta_c = 76.7\%$$

Now, will go ahead and solve the example. First example reads that a centrifugal compressor runs at a speed of 11,500 revolutions per minute. It takes air at 21°C and compresses it from 1 bar to 4 bar. Impeller diameter is 75 centimeter, slip factor is 0.92. Find isentropic efficiency of the compressor. So, we will see what are the given things. Given things in the example is N which is 11,500 rpm.

Then, we are given with T01 which is 21 degree Celsius. So, this is equal to 294 Kelvin, P01 is equal to 1 bar, P03 is equal to 4 bar. Then, we are given with slip factor  $\sigma$  as 0.92. We are told that diameter D2 is 75 centimeter, so it is 0.75 meter. We are supposed to find out what is compressor efficiency. If we look back, we are practically given everything from the formula which is

$$\frac{P_{03}}{P_{01}} = \left( 1 + \frac{\eta_c}{T_{01}} \left( \frac{\sigma \Psi u_2^2}{C_p} \right) \right)^{\frac{\gamma}{\gamma-1}}$$

So, we are just not knowing  $\eta_c$ , we are known with everything. For this example, we will take the losses due to friction as negligible so size equal to 1. So, left hand side P03 is 4, P01 is 1, so it is given so we have 1 plus eta c into size equal to 1 into sigma is equal to 0.92, we need to find u2 square divided by 1005 T01 is 294. Let us find out u2 where u2 is pi D2 N by 60 where we can take pi is 3.14, D2 is 0.75, N is 11,500 divided by 60.

This will give  $u_2$  as 451.37 meter per second. Having said this, we can write down 4 raise to  $\frac{\gamma-1}{\gamma} = 1 + \eta_c \times 1 \times 0.92 \times (451.37)^2 / (1005 \times 294)$ . So, this gives us  $\eta_c = 76.7\%$ . So, this is the isentropic efficiency of the compressor. So, this is how we would approach the example.

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A centrifugal compressor runs at speed 11,500 rev/min and delivers 35 kg of air per second with an efficiency of 80%. The pressure ratio of the compressor is 4.2. It takes air at 47°C and 1 bar. Impeller diameter is 76cm and radial velocity at the exit is 120 m/s. Find axial width of the compressor at the impeller tip.

given  $N = 11,500 \text{ rpm}$ ,  $\eta_c = 80\% = 0.8$ ,  $T_{01} = 47^\circ\text{C} = 320 \text{ K}$ ,  $\dot{m} = 35 \text{ kg/s}$ ,  $\frac{P_{02}}{P_{01}} = 4.2$ ,  $P_{01} = 1 \text{ bar}$   
 $D_2 = 76 \text{ cm} = 0.76 \text{ m}$ ,  $c_{r2} = 120 \text{ m/s}$

$\dot{m} = \rho_2 A V$   
 $\dot{m} = \rho_2 (\pi D_2 w_2) \cdot c_{r2}$

$u_2 = \frac{\pi D_2 N}{60} = \frac{3.14 \times 0.76 \times 11500}{60} = 457.4 \text{ m/s}$

$\frac{T_{03}}{T_{01}} = \left(\frac{P_{03}}{P_{01}}\right)^{\frac{\gamma-1}{\gamma}} = (4.2)^{0.286} = 1.5074 \rightarrow T_{03} = 482.4 \text{ K} = T_{02}$

$\eta_c = 0.8 = \frac{T_{02} - T_{01}}{T_{02} - 320} \rightarrow T_{02} = 523 \text{ K}$

$\rho_{02} \rightarrow \rho_2 \rightarrow \rho_2 = \frac{P_2}{R T_2} \approx \rho_2$   
 $\rho_2 = \frac{4.2 \times 10^5}{287 \times 523}$   
 $\rho_2 = 2.8 \text{ kg/m}^3$

$\dot{m} = \rho_2 (\pi D_2 w_2) \cdot c_{r2}$   
 $35 = 2.8 [3.14 \times 0.76 \times w_2] \times 120$   
 $w_2 = 43.6 \text{ cm}$

We will move on to the next example where it states that a centrifugal compressor runs at speed of 11,500 revolutions per minute and delivers 35 kg of air per second with an efficiency of 80%. The pressure ratio of the compressor is 4.2. It takes air at 47 degree Celsius and 1 bar. Impeller diameter is 76 centimeter; radial velocity at the exit is 120 meter per second. Find the axial width of the compressor at the impeller tip.

Here, we are given with few things, let us mention those. N is equal to 11,500 rpm, eta c is 80% which is equal to 0.8, T01 is equal to 47 degree Celsius which is 320 Kelvin, m dot is given as 35 kg per second, P03 upon P01 as 4.2 where P01 is given as 1 bar. D2 is given as 76 centimeter which is 0.76 meter, cr2 is told to be 120 meter per second. So, we are supposed to find out width of the impeller exit.

So, we know that  $\dot{m}$  is equal to  $\rho A \times \text{velocity}$ . So, here we are given with m dot, we are supposed to find out area but within area we know for the annular passage we can write down area as  $\phi D \times \text{width}$ , so diameter is given,  $\phi$  is given, we need to find out  $\rho$  and  $V$  at the outlet so which is basically

$$\dot{m} = \rho_2 \pi D_2 \times w_2 \times c_{r2}$$

where  $C_{r2}$  is given,  $\rho_2$  can be calculated and  $D_2$  is given.

We need to find out  $w_2$  for given  $\dot{m}$ . So, let us see first we need to find out  $u_2$  and  $u_2$  is  $\pi D_2 N/60$  and then this 3.14 into 0.76 into 11,500 divided by 60 which is 457.4 meter per second. So, this is the tangential velocity at the outlet. Now, we can find out, we need to find out density at outlet. For that, we need to know temperature at the outlet, so will proceed to find out temperature.

What we can know quickly is

$$\frac{T_{03}}{T_{01}} = \left(\frac{P_{03}}{P_{01}}\right)^{\frac{\gamma-1}{\gamma}}$$

This is 4.2 bracket raise to 0.286, this will be 1.5074. So, this gives us  $T_{03}$  dash and then that is basically 482.4 Kelvin. So, this is the temperature at exit. Basically, this is also equal to  $T_{02}$  dash since in the diffuser we have no work input, so total temperature would remain constant. So, having said this now we can use formula for efficiency, which is given as 0.28.

So, this will become  $(T_{02}' - T_{01}) / (T_{02} - T_{01})$  or this is as well  $T_{03}' - T_{01} / T_{03} - T_{01}$ . So, we have  $(T_{02}' - T_{01}) / (T_{02} - T_{01})$ . We know  $T_{02}'$ , it is 482.4 - 320 divided by  $T_{02} - 320$ . So, this gives us  $T_{02}$  is equal to 523 Kelvin. Now, velocities are low, so we can neglect the kinetic energy and we can feel that  $\rho_{02}$  is roughly is equal to  $\rho_2$  where  $\rho_{02}$  is equal to  $P_{02}$  upon  $RT_{02}$  and this is roughly is equal to  $\rho_2$ .

So,  $\rho_2$  is equal to 4.2 into 10 to the power 5 divided by 287 into 523. So, this gives us  $\rho_2$  is equal to 2.8 kg per meter cube. Having known with  $\rho_2$ , now we can go ahead with the formula for  $\dot{m}$  which is  $\rho_2 \pi D_2 \times w_2 \times C_{r2}$ . Here,  $\dot{m}$  is equal to 35,  $\rho_2$  is 2.8,  $\pi$  is 3.14,  $D_2$  is given as 0.76 into width at the exit into radial velocity which is given as 120. So, this gives us width at the exit for the impeller as 4.36 centimeter.


This is the way we have to make use of different known factors. We learnt few things from here that we have to use the formula for mass flow rate at the exit if we need to calculate the width at the outlet of the impeller.

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A centrifugal compressor has inlet eye diameter of 15 cm. It runs at speed 20,000 rpm and takes air at 107m/s axial speed. Inlet stagnation conditions are 294 K and 1.03 bar. Find the blade angle at inlet and Mach number at the tip of the impeller eye.

given  $\rightarrow D_1 = 15 \text{ cm} = 0.15 \text{ m}$     $N = 20,000 \text{ rpm}$     $C_{a1} = 107 \text{ m/s}$     $T_{01} = 294 \text{ K}$     $P_{01} = 1.03 \text{ bar}$

$$u_1 = \frac{\pi D_1 N}{60} = \frac{3.14 \times 0.15 \times 20,000}{60} = 157 \text{ m/s}$$



$$\tan(\beta_1) = \frac{C_{a1}}{u_1} = \frac{C_1}{u_1} = \frac{107}{157} \rightarrow \beta_1 = 34.27^\circ$$

$$M_1 = \frac{V_1}{a_1} \rightarrow V_1 = \sqrt{C_{a1}^2 + u_1^2} = 190 \text{ m/s} \quad \left. \vphantom{M_1} \right\} M_1 = 0.55$$

$$a_1 = \sqrt{\gamma R T_{01}} = 343.7 \text{ m/s}$$

$$a_1 = \sqrt{\gamma R T_1}$$

$$T_{01} = T_1 + \frac{C_{a1}^2}{2 C_p}$$

$$\therefore T_1 = T_{01} - \frac{C_{a1}^2}{2 C_p} = 288.3 \text{ K} \rightarrow M_1 = \frac{V_1}{a_1} = 0.55$$

Let us go with the next example. This example reads that centrifugal compressor has inlet eye diameter of 15 centimeter. It runs at 20,000 rpm and takes air at 107 meter per second axial speed. Inlet stagnation conditions are 294 Kelvin and 1.03 bar. Find the blade angle at the inlet and Mach number at the tip of the impeller eye. Here, everything told to us to calculate is at the inlet itself.

So, we will write down the given things first. In the given things, we are told diameter at the inlet of the eye that is  $D_1$  is equal to 15 centimeter, so it is 0.15 meter and is told to be 20,000 rpm, axial velocity is given as 107 meter per second.  $T_{01}$  is 294 Kelvin and  $P_{01}$  is equal to 1.03 bar. So, knowing this we can find out  $u_1$ , which is  $\pi D_1 N/60$ , so we have 3.14,  $D_1$  is 0.15,  $N$  is 20,000 divided by 60 and this gives us  $u_1$  as 157 meter per second.

From the velocity triangle, we know that this is  $\alpha_1$ , this is  $u_1$ , this is  $\beta_1$ , this is  $v_1$  and this is  $C_{a1}$  is equal to  $C_1$ . So, we know that  $\tan \beta_1$  is equal to  $C_{a1}/u_1$  which is  $C_1/u_1$ , so it is 107 divided by 157 and this gives us  $\beta_1$  is equal to 34.27 degrees. So, this is the value of  $\beta_1$ . We are supposed to find out Mach number at the tip of the impeller eye. So, we know Mach number  $M_1$  is equal to  $V_1/a_1$ .

We are supposed to find out relative Mach number, so this relative Mach number can be calculated if we know  $V_1$  and  $a_1$ , we can find out  $V_1$  from this velocity triangle which says that it is equal to square root of  $(C_{a1}^2 + u_1^2)$  and then this turns out to be 190 meters per second. Now, we are supposed to find out  $a_1$ ,  $a_1$  is equal to square root of  $\gamma R T_1$ . Now, instead of taking

this as static temperature, if we take it as total temperature, we can get a1 as 343.7 meter per second.

And then this combination gives us M1 as 0.55 but if we do not take a1 using total temperature and if we calculate static temperature required for calculation of a1, we need to use the formula for calculation of total temperature as

$$T_{01} = T_1 + \frac{C_{a1}^2}{2C_p}$$

So,  $T_1 = T_{01} - C_{a1}^2 / 2C_p$ . So, this gives us T1 as 288.3 Kelvin. So, this is the static temperature at the inlet.

Now, we can calculate

$$M_1 = v_1/a_1$$

and this also becomes close to 0.55 since total temperature and static temperature are very close by.

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A one sided centrifugal compressor delivers air at the rate of 14 kg/s with pressure ratio of 4:1 at the speed of 12,000 rev/min. Stagnation conditions in the inlet are 288 K and 1.033 bar. Consider 0.9 slip factor and 80% isentropic efficiency for determining the overall diameter of the impeller.

given  $\dot{m} = 14 \text{ kg/s}$   $N = 12000 \text{ rpm}$   $T_{01} = 288 \text{ K}$   $P_{01} = 1.033 \text{ bar}$   $\sigma = 0.9$   $\eta_c = 0.8$ ,  $\frac{P_{02}}{P_{01}} = 4$

$$\frac{P_{02}}{P_{01}} = \left\{ 1 + \frac{\eta_c \cdot \psi \cdot u_2^2}{T_{01} \cdot C_p} \right\}^{\frac{\gamma}{\gamma-1}} \Rightarrow (4) = 1 + \frac{0.8 \times 1 \times 0.9 \times u_2^2}{288 \times 1005} \rightarrow u_2 = 442.2 \text{ m/s}$$

$$u_2 = \frac{\pi D_2 N}{60} \rightarrow D_2 = \frac{60 \times u_2}{\pi \times N} \rightarrow \underline{\underline{D_2 = 0.70 \text{ m}}}$$

Having known this, we can move ahead with the next example and this example reads that a one sided centrifugal compressor delivers air at the rate of 14 kg per second with pressure ratio of 4 is to 1 at the speed of 12,000 revolutions per minute. Stagnation conditions at the inlet at 288 Kelvin and 1.033 bar. Consider 0.9 as slip factor and efficiency as 80% for determining overall diameter of the impeller.

So, we are given in this example as  $\dot{m}$  is 14 kg per second and then revolutions  $N$  as 12,000 rpm,  $T_{01}$  is 288 Kelvin,  $P_{01}$  is 1.033 bar, slip factor  $\sigma$  is 0.9, efficiency is 0.8. Having known this, we can use formula  $P_{03}$  upon  $P_{01}$  since we are given as  $P_{03}$  upon  $P_{01}$  as 4. So, this is equal

$$= \left( 1 + \frac{\eta_c}{T_{01}} \left( \frac{\sigma \Psi u^2}{C_p} \right) \right)^{\frac{\gamma}{\gamma-1}}$$

In this formula, we can take  $\Psi$  is equal to 1, so we will have  $P_{03}/P_{01}$  is 4 raise to  $0.286 = 1 + 0.8 \times 1 \times 0.9$  into  $u^2 / (288 \times 1005)$ . This gives us  $u_2 = 442.2$  meter per second. We know that  $u_2 = \pi D_2 N / 60$ , so  $D_2 = 60 \times u / \pi N$ . So, we get  $D_2$  from the know quantities as 0.70 meter. So, here in this example, we were expected to find out the diameter.