

IC Engines and Gas Turbines
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Lecture - 46

Axial Compressor: Different factors, Degree of Reaction and Free Vortex Condition

So, welcome to the class. In the last class, we have seen that we started with Axial Compressor. And for axial compressor, we have seen how the velocity triangle is, how to find out the work interaction in case of axial compressor, and then how to find out stage temperature rise and pressure ratio for given conditions ok.

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Handwritten derivation of the pressure ratio formula for an axial compressor stage:

$$\frac{P_{03}}{P_{01}} = \left(1 + \eta_s \frac{\Delta T_{0s}}{T_{01}} \right)^{\frac{\gamma}{\gamma-1}}$$

$$\Delta T_{0s} = \frac{U}{C_p} (a_1 \tan \beta_1 - a_2 \tan \beta_2)$$

$$\therefore \frac{P_{03}}{P_{01}} = \left[1 + \eta_s \frac{U C_a}{T_{01} C_p} (\tan \beta_1 - \tan \beta_2) \right]^{\frac{\gamma}{\gamma-1}}$$

✓ \rightarrow axial velocity \rightarrow relative Mach no. $\frac{V_1}{a_1}$ $a_1 = \sqrt{\gamma R T_1}$
 ✓ \rightarrow blade speed \rightarrow centrifugal stress $\frac{T_{01}}{T_1} = 1 + \frac{\gamma-1}{2} M_1^2$
 ✓ \rightarrow deflection

Velocity triangle diagram showing the relationship between axial velocity (C_a), blade speed (U), and flow angles (β_1, β_2).

So, then we had obtained a formula in last class about the pressure rise as P_3 upon P_1 is equal to 1 plus stage efficiency into ΔT_s stage divided by T_1 bracket raised to γ upon γ minus 1. So, this is stage temperature rise. Rather we had found out that this stage temperature rise is U upon C_p into C_a into \tan of β_1 minus \tan of β_2 . So, this was our formula for stage temperature rise.

So, we got a formula for pressure ratio as P_3 upon P_1 , which is 1 plus efficiency stage efficiency divided by T_1 into $U C_a$ divided by C_p into \tan of β_1 minus \tan of β_2 bracket raised to γ upon γ minus 1. So, here we

can see that for a pressure rise to happen with required magnitude, there are different factors which affect.

First factor which affect is the axial velocity, which is C_a axial velocity. Axial velocity if it is more, then we can see that we can get more pressure rise. But, axial velocity is restricted or there is a limitation on axial velocity due to relative Mach number. And relative Mach number is defined as relative Mach number is defined as v_1 divided by a_1 . So, this is the relative Mach number at the blade, so entry. So, this number should be subsonic such that we should have minimum number of losses minimum amount of losses, so for that C_a will be restricted.

So, we basically need to find out, what is a_1 . So, basically we know that a_1 for gas is equal to $\sqrt{\gamma R T_1}$, and we should know what is T_1 . So, T_1 we know formula at T_∞ T_1 is equal to $T_\infty [1 + \frac{\gamma - 1}{2} M_1^2]$. So, we would know the Mach number at the entry, we would know the total temperature, then we can find out T_1 . Putting that T_1 , we will get a_1 . And then we will get the value of relative Mach number, which would have restriction to have any amount of axial velocity. So, only limited amount of axial velocity will be allowed.

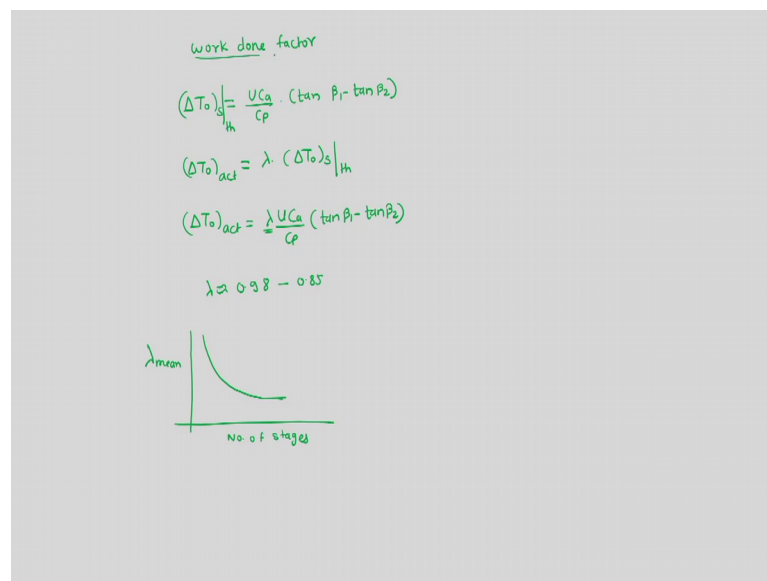
Then the second factor which can help to raise the pressure more is blade speed which is U , but blade speed is also restricted by stresses centrifugal stresses in the blade. And this stress is directly proportional with U^2 . So, there should not be again very high amount of blade speed. Third factor which is affecting is this which is called as deflection. We had seen in last class that $\beta_1 - \beta_2$ is called as a deflection. And if we can have larger deflection, then we can have larger pressure rise, but larger deflection would create the problem of flow separation, so there would be problem.

So, how would be the larger pressure direct larger pressure gradient created? Larger pressure ratio created, we can see here by creating deflection. This was the velocity triangle, which we had seen in earlier case in our earlier graph, we had seen that the velocity triangle is of this kind. So, same velocity triangle, we are trying to draw here. So, we have C_1 , and we have V_1 , we have C_2 , and we have V_2 . And this angle, we had called as $\beta_1 - \beta_2$, since this is α_1 , this is β_1 , then this is α_2 , and then this is β_2 .

Now, if we want to have higher deflection, then we should have our V velocity V_2 should be in the different place. So, we can have V_2 to be like this. If V_2 is like this, then we can see that there will be more deflection. If there is more deflection, then there will be more pressure rise. So, obviously we can also know that we would have more ΔC_w in this case. So, there will be more work absorb, and then there will be more pressure rise.

So, there are three factors which would affect the pressure ratio. One is axial velocity, but that is restricted by relative Mach number. One is blade speed, but that is restricted by stress in the blade. And another is deflection, and large deflection would lead to flow separation. So, these are the restrictions which will be we should be knowing which would affect the pressure rise in a stage.

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work done factor

$$(\Delta T_o)_s \Big|_{th} = \frac{U C_a}{C_p} (\tan \beta_1 - \tan \beta_2)$$

$$(\Delta T_o)_{act} = \lambda \cdot (\Delta T_o)_s \Big|_{th}$$

$$(\Delta T_o)_{act} = \frac{\lambda U C_a}{C_p} (\tan \beta_1 - \tan \beta_2)$$

$$\lambda \approx 0.98 - 0.85$$

λ_{mean}

No of stages

Now, we would see that there is a term which is called as work than factor. So, work done factor for the compressor, work done factor is related with the work supplied and work received. So, work received is always lesser than the work supplied. So, what we would have is ΔT_{naught} , ΔT_{naught} stage which we have we had found out as $U C_a$ upon C_p into \tan of β_1 minus \tan of β_2 . This is stage temperature rise, but that is ideal stage temperature rise, so we will get actual stage temperature rise is equal to λ into ΔT_{naught} stage or which is rather theoretical. So, this is theoretical.

And then this leads to $\Delta T_{\text{naught actual}}$ is equal to λ into U upon C_a divided by C_p into \tan of β_1 minus \tan of β_2 ok. And this λ actually has a range generally in between 0.98 to 0.85; this number is less than 1. So, actually we will get lesser temperature rise than the theoretically which we would have got, otherwise if there would be that much amount of work which would be have got stored in the compressor.

But, this λ as variation over number of stages, and this is mean value of λ , and this λ mean decreases over number of stages. So, as the number of stages increase, λ mean decreases. So, lesser and lesser temperature rise in actual case would be observed than the comparator compare theoretical value, if we have higher value of number of stages. So, this is one more term which we should be knowing in case of axial compressor.

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Degree of reaction

$$R = \frac{\text{static temp rise in rotor}}{\text{total temp rise in stage}}$$

$$R = \frac{\Delta T_{12}}{(\Delta T_0)_{13}}$$

$$T_{01} = T_1 + \frac{C_{a1}^2}{2C_p}$$

$$T_{03} = T_3 + \frac{C_{a3}^2}{2C_p}$$

$$C_{a1} = C_{a3}$$

$$(\Delta T_0)_{13} = (\Delta T)_{13}$$

$$R = \frac{(\Delta T)_{12}}{(\Delta T)_{13}} = \frac{(\Delta T)_{12}}{(\Delta T)_{12} + (\Delta T)_{23}}$$

Now, moving on to the next topic of discussion, which is called as degree of reaction degree of reaction. We would define degree of reaction as a R , suppose an R is degree of reaction or in some places degree of reaction is also defined as λ , so that we would term as capital λ maybe as in other case. Here it is also small λ , and then we will define this as R or maybe capital λ .

So, degree of reaction is defined as temperature rise in the rotor which is static temperature rise in the rotor, static temperature rise in rotor divided by total temperature rise in stage. So, this is the definition of degree of reaction or static enthalpy rise in the

rotor divided by total enthalpy rise in the stage. So, this is what, so it is so it is comparing the pressure rise in the rotor divided by total complete pressure rise in the stage. So, this is how degree of reaction is defined.

Now, what we should be remembering is what we have in case of axial compressor is like this; we first have a rotor, then have stator. So, then this is 1, this is 2, and this is 3 for us ok. So, 1 to 2 is rotor, 2 to 3 is stage. So, we would say that this is ΔT_A , so temperature rise static temperature rise is ΔT_A , and this static temperature rise or rather we can call it as ΔT_{12} , and this is ΔT_{23} . So, this is what the temperature rise which would be taken place in the rotor, and the stator ok.

And then we know that at one, we have $T_{\text{naught one}}$ total temperature, at 2 we have $T_{\text{naught two}}$ total temperature, at 3 we should have $T_{\text{naught three}}$, but $T_{\text{naught three}}$ is equal to $T_{\text{naught one}}$. Since in the stator, there is no work interaction only, there is diffusion of the energy, and it would rise the pressure. So, we have this as a variation of total temperature in a stage, this is the change in static temperature in the stage. So, we have basically static temperature rise in the rotor divided by total temperature rise in the stator as the formula for degree of reaction.

So, we have ΔT_{12} divided by $\Delta T_{\text{naught one three}}$ $\Delta T_{\text{naught one three}}$. We should keep it in mind that there is no total temperature in the numerator, total temperature used only in the denominator for the fact that total temperature rise take place only in the rotor, otherwise degree of reaction would have been always one ok.

So, now we will see that we know $T_{\text{naught one}}$ is equal to T_1 plus C_a^2 divided by twice C_p , axial velocity square divided by twice C_p , this is the temperature, total temperature in stage 1 ok. We are assuming that the flow is axial completely at the inlet. So, we are having similarly $T_{\text{naught two}}$ is equal to T_2 plus C_a^2 upon twice C_p , which is a rather if we go to 3. If we go to 3, then we can write $T_{\text{naught three}}$ is equal to T_3 plus C_{a1}^2 C_{a3}^2 divided by twice C_p . C_{a3} is here it is entry to the next stage, but we know that C_{a1} is equal to C_{a3} .

So, in that particular case, what we would have is $\Delta T_{\text{naught one three}}$ is equal to ΔT_{13} . So, total temperature rise in the stage is equal to static temperature rise in the stage, so degree of reaction R can again be written ΔT_{12} divided by ΔT_{13} . So, we will

have ΔT_{12} divided by $\Delta T_{12} + \Delta T_{23}$, so this would be the formula for the degree of reaction.

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The image shows a handwritten derivation of the degree of reaction R for an axial compressor stage. The derivation starts with the relationship between temperature drops and work, then uses the steady flow energy equation between stations 1 and 2 to find the enthalpy difference. Finally, it expresses the degree of reaction R in terms of velocity, axial velocity, and blade angles.

$$\begin{aligned}
 (\Delta T_0)_B = (\Delta T)_B &\Rightarrow W_s = C_p (\Delta T_0)_B = U C_a (\tan \beta_1 - \tan \beta_2) \checkmark \\
 (\Delta T_0)_B = (\Delta T)_B = (\Delta T_0)_B &= \frac{U C_a}{C_p} (\tan \beta_1 - \tan \beta_2) \\
 \text{1 2 3} \\
 \text{R | S} \\
 h_1 + \frac{C_1^2}{2} + q &= h_2 + \frac{C_2^2}{2} + w \\
 h_1 + \frac{C_1^2}{2} &= h_2 + \frac{C_2^2}{2} - W_s \\
 h_2 - h_1 &= \frac{C_1^2}{2} - \frac{C_2^2}{2} + W_s \\
 C_p (\Delta T)_{12} &= W_s - \frac{1}{2} (C_2^2 - C_1^2) \checkmark \\
 R = \frac{(\Delta T)_{12} \cdot C_p}{(\Delta T_0)_{12} \cdot C_p} &= \frac{W_s - \frac{1}{2} (C_2^2 - C_1^2)}{W_s} = 1 - \frac{\frac{1}{2} (C_2^2 - C_1^2)}{W_s} = 1 - \frac{(C_2^2 - C_1^2)}{2 U C_a (\tan \beta_1 - \tan \beta_2)} \\
 R &= 1 - \frac{(C_a^2 \sec^2 \alpha_2 - C_a^2 \sec^2 \alpha_1)}{2 U C_a (\tan \beta_1 - \tan \beta_2)} = 1 - \frac{C_a}{2 U} \frac{(\tan^2 \alpha_2 - \tan^2 \alpha_1)}{(\tan \beta_1 - \tan \beta_2)} \rightarrow \frac{\tan \alpha_1 + \tan \beta_1 = \tan \alpha_2 + \tan \beta_2}{\tan \beta_1 - \tan \beta_2 = \tan \alpha_2 - \tan \alpha_1} \\
 R &= 1 - \frac{C_a}{2 U} \frac{\tan^2 \alpha_2 - \tan^2 \alpha_1}{\tan \alpha_2 - \tan \alpha_1} = 1 - \frac{C_a}{2 U} (\tan \alpha_2 + \tan \alpha_1) \checkmark
 \end{aligned}$$

Now, we should be knowing rather the ΔT naught 1 3 in case of axial compressor. So, ΔT naught 1 3 which is equal to ΔT_{13} is equal to or rather can be found out from stage work, which is C_p into ΔT naught stage. And then that is for our case, this is $U C_a$ into \tan of β_1 minus \tan of β_2 . So, we knew that ΔT naught stage is equal to $U C_a$ divided by C_p into \tan of β_1 minus \tan of β_2 . So, we know how to find out ΔT naught stage, which is ΔT naught 13, and which is equal to ΔT_{13} .

Now, we got the formula of R like this. So, we found out the denominator, we need to find out the numerator. So, numerator can be found out by considering the energy equation between the rotor, and the stator such that we know that this is rotor, this is stator this is 1, 2, and 3. Let us apply energy equation between steady flow energy equation between point station 1 and station 2. We can write down that $h_1 + \frac{C_1^2}{2} + q$ is equal to $h_2 + \frac{C_2^2}{2} + w$, but this is an adiabatic process, so q is not there. Further this w is received by the system, so we have $h_1 + \frac{C_1^2}{2}$ is equal to $h_2 + \frac{C_2^2}{2} - w$ stage.

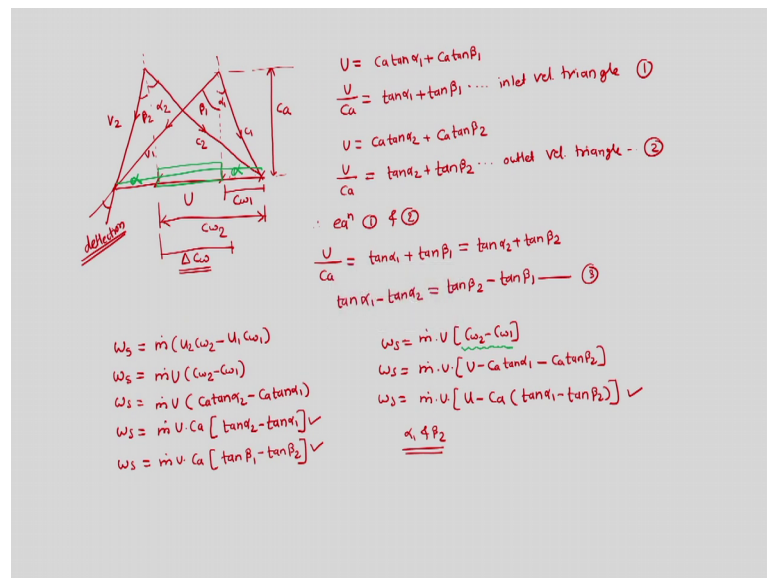
So, we would have $h_2 - h_1$ is equal to rather, we would have w stage $h_2 - h_1$ is equal to $\frac{C_1^2}{2} - \frac{C_2^2}{2} + w$ s ok. So, we have C_p into ΔT

T_1^2 is equal to w stage plus or we can also write it as $\frac{C_2^2}{2}$ here, and then we can write it as $\frac{C_2^2 - C_1^2}{2}$. So, this is the formula, till now what we have got. So, here we got the numerator, here we got the denominator.

So, now R is equal to ΔT_1^2 which is equal to $\Delta T_{naught 1}^2$ is equal to w s minus half. So, we can multiply both the sides by C_p , so we will get C_p into $\Delta T_{naught 1}^2$ divided by C_p into $\Delta T_{naught 1}^2$, so this is here. So, we can write it as w s minus half C_2^2 minus C_1^2 , but this factor is w s.

So, we will have w s. So, what we get is $\frac{1}{2} (1 - \frac{C_2^2}{C_1^2}) w$ s into C_2^2 minus C_1^2 , but we can know that w s is equal to this. So, we can use that and say that $\frac{1}{2} (1 - \frac{C_2^2}{C_1^2}) w$ s divided by $U C_a$ into $2 \tan \beta_1$ minus $\tan \beta_2$ ok. So, this is the formula till time for R .

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Now, we have to find out what is C_a , what is C_1 . We will go back to the velocity triangle, what we had drawn. So, in this velocity triangle if we see what is C_1 , and what is C_2 . So, C_1 is $C_a \sec \alpha_1$, and C_2 is equal to $C_a \sec \alpha_2$. So, from the velocity triangle, we know that C_1 is equal to C_1 is equal to R is equal to $\frac{1}{2} (1 - \frac{C_a^2 \sec^2 \alpha_2 - C_a^2 \sec^2 \alpha_1}{2})$ into U into C_a divided by $\tan \beta_1$ minus $\tan \beta_2$.

So, we have R is equal to $1 - \tan^2 \alpha_1$, then this formula can be further replaced $\sec^2 \alpha_1$ in $\tan^2 \alpha_1$, and then we can get it again replaced using the relation of \sec and \tan , we can get it as $C_a \frac{U}{2} \frac{\tan^2 \alpha_2 - \tan^2 \alpha_1}{\tan \alpha_2 - \tan \alpha_1}$.

But, in earlier sections, what we had seen from the velocity triangle that there is a relation which says that $\tan \alpha_1 + \tan \beta_1 = \tan \alpha_2 + \tan \beta_2$. So, we can write down that relation which says that $\tan \alpha_1 + \tan \beta_1 = \tan \alpha_2 + \tan \beta_2$. So, we get $\tan \beta_1 - \tan \beta_2 = \tan \alpha_2 - \tan \alpha_1$.

So, we can write down it over here, and we can say that R is equal to $1 - C_a \frac{U}{2} \frac{\tan^2 \alpha_2 - \tan^2 \alpha_1}{\tan \alpha_2 - \tan \alpha_1}$. [noise So, we get $1 - C_a \frac{U}{2} \frac{\tan^2 \alpha_2 - \tan^2 \alpha_1}{\tan \alpha_2 - \tan \alpha_1}$]. So, this is our formula for R , further this formula can also be reduced in terms of betas. So, this is how we can find out R for the compressor, which is the degree of reaction for a compressor.

This formula can further be utilized to understand, how the R is going to vary with respect to the blade height. So, here we know that our formula for degree of reaction is this. And here we have $C_a \tan \alpha_2$ and $C_a \tan \alpha_1$ ok, we will do it. After one more derivation which is called as the free vortex theory ok. So, till time what we were trying to do was for the two dimensional case, where we had seen that we were working with the velocity triangle on a plane which is parallel to the axis of the compressor. So, we were having this analysis as two dimensional.

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Free vortex condition

Radial eqⁿ $\rightarrow \frac{1}{r} \frac{dp}{dr} = \frac{C_w^2}{r}$

$h_0 = h + \frac{C_w^2}{2} = h + \frac{1}{2} (C_{w1}^2 + C_{w2}^2)$

$\frac{dh_0}{dr} = \frac{dh}{dr} + C_{w1} \frac{dC_{w1}}{dr} + C_{w2} \frac{dC_{w2}}{dr} \quad \text{--- (1)}$

$T ds = dh - v dp = dh - \frac{dp}{\sigma}$

$dh = T ds + \frac{dp}{\sigma}$

$\frac{dh}{dr} = T \frac{ds}{dr} + \frac{dp}{\sigma dr} + \frac{1}{\sigma} \frac{dp}{dr} - \frac{1}{\sigma^2} \frac{dp}{dr} \frac{dp}{dr}$

$\frac{dh}{dr} = T \frac{ds}{dr} + \frac{C_w^2}{r} \quad \text{--- (2)}$

$\frac{dh_0}{dr} = T \frac{ds}{dr} + \frac{C_w^2}{r} + C_{w1} \frac{dC_{w1}}{dr} + C_{w2} \frac{dC_{w2}}{dr}$

$\frac{C_w^2}{r} = -C_{w1} \frac{dC_{w1}}{dr}$

$-\frac{dr}{r} = \frac{dC_{w1}}{C_{w1}}$

$C_{w1} r = \text{const}$

$R = 1 - \frac{C_{w1}}{2U} [\tan \alpha_2 + \tan \alpha_1]$

$R = 1 - \frac{1}{2U} [C_{w1} \tan \alpha_1 + C_{w2} \tan \alpha_2]$

$R = 1 - \frac{1}{2U} [C_{w1} + C_{w2}]$

$R = 1 - \frac{1}{2U} [C_{w1} + C_{w2}] = 1 - \frac{[C_{w1} + C_{w2}]}{2U}$

$R = 1 - \frac{K_1}{rU} \quad V = \frac{\pi DN}{60} = \frac{\pi r N}{60}$

$R = 1 - \frac{K_2}{r^2}$

But, we can do further a glimpse of three dimensional analysis, where we will use a theory which is called as free vortex condition or free vortex theory ok. So, we will say that this is free vortex condition. And we will derive this condition, as per this condition. Now, this condition is applied for the compressor axial compressor as well as for the axial turbine. So, this part of discussion is common between axial compressor and axial turbine.

So, what do we mean by free vortex condition, we using this condition we are trying to find out the relation between the triangle velocity triangles, whatever we would have drawn in a plane at a condition. So, this is the blade as we know, this is a blade, and this is a stator, this is rotor, this is stator. We know that we are working at this height of the blade. So, if we are working at this height of the blade, then we are drawing the velocity triangle here and here, then knowing the velocity triangle at these locations how to find out the velocity triangle at other locations or the of the rotor. So, this is what our objective through this free vortex condition is.

So, for that we practically are considering this radial variation. And since this is an axial compressor or more intention was that it has only axial velocity. So, it is not having any radial velocity, but with this non-radial velocity being accounted, we will try to derive a constraint. So, for that we will first consider, there exist a radial equilibrium and radial equilibrium leads to $\frac{1}{r} \frac{dp}{dr} = \frac{C_w^2}{r}$ by $\frac{dp}{dr} = C_w^2$ by $\frac{dp}{dr} = C_w^2$ by r . So,

centrifugal force is balanced by the pressure gradient in the r direction for the compressor at a location ok . So, this is our assumption we could have derived that, but this can be taken to start with as a [vocalized-] assumption for radial equilibrium to derive the free vortex condition.

Now, let us consider h_{naught} is the total enthalpy at a station which is equal to h plus C^2 , but we know that C can be decomposed into two components which is C_a^2 plus C_w^2 , further we can differentiate this h_{naught} , and then we get dh_{naught}/dr is equal to dh/dr plus C_a into dC_a/dr plus C_w into dC_w/dr plus C_w into dc_w/dr , this is equation number 1.

Now, we know our thermodynamic relation which is combined first law and second law as per that Tds is equal to dh minus vdp , so that can be written as dh minus dp/ρ , then we can write here as dh is equal to Tds plus dp/ρ . Now, here we can see that there is a term dh/dr . So, we can differentiate this equation, then we can get dh/dr , so T into ds/dr plus ds into dT/dr plus $1/\rho$ into dp/dr minus, we would have $1/\rho^2$ into dp into $d\rho/dr$, this would be the term.

But, then this term is a second order, further this term is also second order will for the sake of convenience, we will neglect them being their magnitudes to be very small. So, we get dh/dr is equal to T into ds/dr plus $1/\rho$ dp/dr , but we know that $1/\rho$ dp/dr is equal to C_w^2/r .

So, what we get after this putting equation 2 in equation 1, we get dh_{naught}/dr is equal to T into ds/dr plus C_w^2/r plus C_a into dC_a/dr plus C_w into dC_w/dr . Now, we know that when we are considering centrifugal compressor our C_a is taken as constant with respect to r . So, this term is negligible in magnitude or 0 for us.

Further we are considering subsonic compressors. So, there is no entropy variation in r direction. So, these two terms would get cancelled. Further we are also considering that the dh_{naught}/dr is negligible which is saying that we are having equal amount of work to be taken by the compressor at different heights. So, considering these terms to be negligible in the respect of other two terms, we get C_w^2/r is equal to minus C_w into dC_w/dr , so which says that dr/r is equal to dC_w/C_w .

After integration, this expression leads to the fact that C_w into r is equal to constant. So, if we know C_w at a height, then we can find out C_w at some other height. So, this is how this formula helps us to work out for finding out the velocity triangle known at one point to be finding out velocity triangle to be evaluated or estimated at the other height.

This formula can be having thought to having relation with the formula for what we have derived for the degree of reaction. So, degree of reaction formula, what recently we derived has $1 - \frac{C_a}{2U} \tan \alpha_2$ plus $\tan \alpha_1$. So, r is equal to $1 - \frac{U}{2C_a} \tan \alpha_2$ plus $\tan \alpha_1$, so it is R is equal to R is equal to C_a by U C_a by U . So, we have $1 - \frac{U}{2C_a} \tan \alpha_2$ plus $\tan \alpha_1$ into C_a .

If we see velocity triangle, so $C_a \tan \alpha_1$, $C_a \tan \alpha_1$ would be C_{w1} . So, R is equal to $1 - \frac{U}{2C_a} \tan \alpha_2$, and this is C_{w1} plus C_{w2} . And now we will multiply both the numerator and denominator by R . So, we will get $1 - \frac{U}{2C_a} \tan \alpha_2$ plus C_{w1} plus C_{w2} , which would lead to $1 - \frac{U}{2C_a} \tan \alpha_2$ plus C_{w1} plus C_{w2} divided by r into U . Then we know that r_1 , and we can write it as r_2 , since r_1 and r_2 are same, but this is a constant. Since this is a constant.

We get R is equal to $1 - \frac{U}{2C_a} \tan \alpha_2$ plus C_{w1} plus C_{w2} that this constant is K_1 , but we know that U is equal to $\pi D N$ by 60. So, U is equal to $\pi r N$ into 2 by 60. So, it turns out that R is $1 - \frac{K_2}{r^2}$ upon r square. So, this is the relation of degree of reaction with respect to R . So, if R is increased, degree of reaction will increase. If R is decreased, degree of reaction will decrease.

So, this is how we when do our 2D analysis for the velocity using the velocity triangle at mid bed height, free vortex theory helps us to translate that analysis with the constraint that we are having negligible change in axial velocity, we are having negligible change in the total enthalpy in the radial direction. So, we can take that C_w into R is equal to constant. So, these are the topics which we will be needing for understanding the axial compression. And here we end the topic on axial compressor. We will meet for the next topic in the next class.

Thank you.