

IC Engines and Gas Turbines
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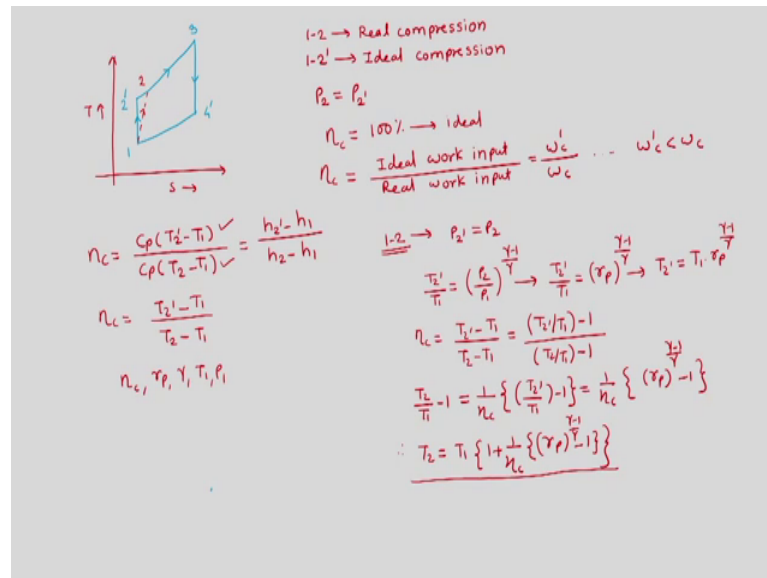
Lecture – 38
Real Brayton Cycle, Solved Example for Ideal Cycle

Welcome to the today's class. Today we are going to deal with Brayton cycle with non-ideal components. In the gist what we have covered till time, we have covered the ideal Brayton cycle, Brayton cycle with inter cooling, Brayton cycle with heat exchanger, Brayton cycle with reheating. We have seen there are advantages, why we should not have Brayton cycle with inter cooling, why we should have heat exchanger and what why we should have reheater. Every component has its own advantages and disadvantages.

Further we have also seen that if we integrate everything; like there is a single power plant with everything together; like heat exchanger, intercooler and reheater then what would happen, then how to do the cycle analysis that we have seen, but now in today's class we will be seeing that, if we are having the non-ideal components as part of a Brayton cycle. The fact to be understood over here is that, basically we have 4 components in Brayton cycle; one is compressor other is turbine, then we have a combustion chamber and then we have heat loss.

So, or in case of close cycle we have pre cooler, but within that we are having two components which are rotary machines and those two components are compressors and turbines. And now if these two components are non-ideal then how would be the cycle analysis? This is the topic of discussion for today's class and then we would see to solve some examples. So, let us see if we have Brayton cycle with non-ideal plants, non-ideal components.

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So, let us first consider the T S diagram as what we already always considered. So, we have T axis and we have S axis. So, the process initially what we would write, is all the processes what we already know, those processes we will plot for. So, we will initially plot for ideal cycle, so this is 1 to 2 is compression, so but will not say now two will say it has 2 dash is a compressor, then 2 to 3 is heat addition process then 3 to 4 is a expansion process in turbine. So, this is what we have already seen, but now we will not say it has 4, but we will say it as 4 dash. So, we have 1 2 3 4 as our cycle. Now having said this as our cycle we will see now if we are having non-ideal component. So, suppose compressor is non-ideal. So; that means, we are not going to reach the point 2 dash after the process of compression.

So, we mean that, what are the reasons of being non-ideal? The major reason what we will consider over here is a friction. So, frictional losses are there in the case of compressor due to which compressor would not let us go to the point 2 dash and then we would go to some other point and let it be some other point it is 2. So, instead of growing from 1 to 2 dash we went to wrong 1 to 2. We know that process 1 to 2 is a real process it is an irreversible process. So, 1 to 2 is showed by a dotted line

So, as what we know 1 to 2 is a real compression process and 1 to 2 dash is ideal compression process, but one point we have to keep it in mind that pressure 2 is equal to pressure 2 dash, we did not get landed in a different pressure condition. So, pressure at 2

which is a static pressure at 2 is equal to static pressure at 2 dash. So, this is what we have achieved by the still having non-ideal component, which is a compressor, but then when we say that we have compressor which is an ideal we mean that compressor thermal efficiency is 100 percent for ideal, but then what is the definition of compressor efficiency.

So, compressor efficiency can be defined as ideal work input to real work input. We have to keep one point in mind and rather remember that compressor is a work input machine, so here we are giving some work input. Ideally we always would need less work for input than the real condition. So, ideal work being less what we call it as $w_{dash c}$ divided by w_c , but we know that $w_{dash c}$ is always less than w_c , so efficiency is always less than 100 percent. So, in real case we need to supply more pressure to get same pressure at the outlet of the compressor.

So, practically we are supplying more worker input to the compressor to get same pressure, but ideally we would need less work input to get the same pressure. In that aspect we know that compressor efficiency, we know work input to the compressor C_p into T_2 minus T_1 , this is real work, ideal work then C_p into $T_{2 dash}$ minus, sorry. So, we have $T_{2 dash}$ minus T_1 and T_2 minus T_1 . So, this is ideal work and this is real work

So, basically we would also have written it as $h_{2 dash}$ minus h_1 divided by h_2 minus h_1 this is the enthalpy based formulation for the work, we directly wrote and considering the gas to be a perfect gas with we are having and we are also assuming that C_p is and C_v is not function of temperature. So, we are having calorically perfect gas as an assumption if we go from here to here. So, compressor efficiency would ultimately become for calorically perfect gas as $h_{2 dash}$ minus h_1 divided by h_2 minus h_1 .

Then we will deal with the examples, then we would understand that compressor efficiency would be a known parameter for us. And parallely we also know that pressure ratio is also a known parameter for compressor. So, pressure ratio is known, compressor efficiency is known and then we would also know what are the inlet conditions of the compressor. So, practically what we would be knowing is, compressor efficiency, pressure ratio, γ and T_1 . These things are P_1 , these thing would be known to us. Having these things known our objective over here is to find out what is $T_{2 dash}$. Since

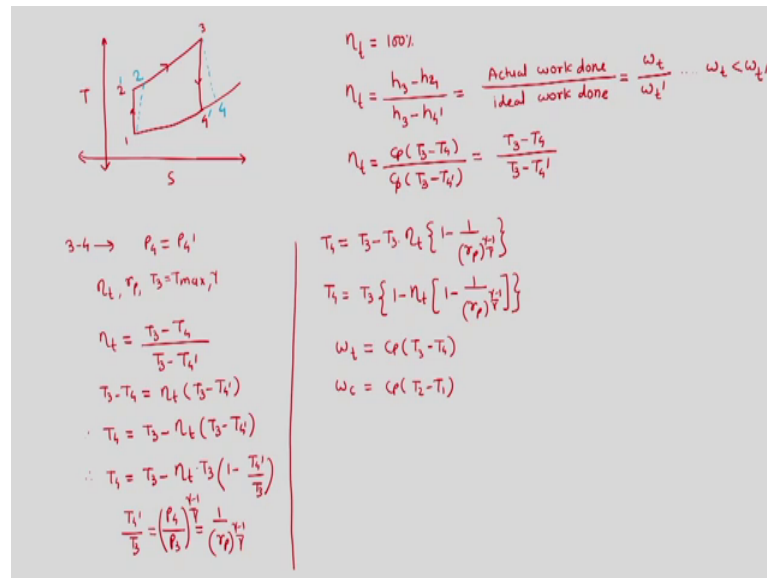
we are going to do some more derivations based upon the non-ideal components. So, we know that for process 1 to 2. We know that P_2 is equal to P_1 , this is known to us. And then now our objective is to find out what is T_2 so, but we know that T_2 upon T_1 is equal to P_2 upon P_1 bracket raised to $\gamma - 1$ upon γ . So, this is for the point 2 which is in an ideal point. So, we know that T_2 upon T_1 is r_p raised to $\gamma - 1$ upon γ .

So, we know that T_2 is equal to T_1 into r_p bracket raised to the $\gamma - 1$ upon γ . This we have already seen, but now we know efficiency, so we are supposed to find out T_2 or T_2 . So, we know that efficiency is equal to T_2 minus T_1 divided by T_2 minus T_1 . So, here we can take, we can take T_1 as common then what we can get is T_2 upon T_1 minus 1 divided by T_2 upon T_1 minus 1 ok. So, what we can write as T_2 upon T_1 minus 1 is equal to 1 upon compressor efficiency into T_2 upon T_1 minus 1, but we know T_2 upon T_1 is equal to r_p raised to $\gamma - 1$ upon γ . So, this is equal to 1 upon compressor efficiency into r_p raised to $\gamma - 1$ upon γ minus 1.

So, we have T_2 is equal to T_1 into $1 + 1$ upon compressor efficiency into r_p bracket raised to $\gamma - 1$ upon γ minus 1 and then all brackets complete. So, this is the expression for calculating temperature at the exit to the non-ideal compressor. So, here all the quantities are known to us on the right hand side, so we can find out T_2 which is an actual temperature at the outlet of the compressor.

So, now we will go with the next point which is the non-ideal turbine. So, 3 is known to us by the way which is a T_{max} point or which is the point after the combustion chamber, we assume combustion chamber or heat addition and heat rejection processes are ideal, so we have to just work out with turbine.

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So, in the case of turbine what we will have, again we will try to draw the T S diagram for the next slide. So, we have T axis, we have s axis, then we have 1 to 2 compressor, then we have 2 to 3 and then 3 to 4, but what we are seeing now is non-ideal components. So, for non-ideal components we have 1 2, basically this is 2 dash, so 2, this is 4 dash, so this is 4. So, this is the non-ideal turbine case.

So, in case of non-ideal turbine now again we have know that we have known that, if the turbine efficiency for non-ideal ideal case will be again 100 percent. So, again we have to define what do we mean by efficiency of turbine. Again here we are considering the losses due to friction in the case of turbine. So, it is an isentropic efficiency of turbine. So, turbine efficiency, if we define in terms of enthalpy then it will be $h_3 - h_4$ divided by $h_3 - h_4'$. So, practically it means actual work done divided by ideal work done.

So, it means w_t divided by w_t' and then we know that w_t is always less than w_t' . We again would remember that turbine is our producing machine. So, in case of work producing machine we always would need the, we always would get lesser work output than the ideal case. So, turbines would have non hundred percent efficiencies.

Again if we try to again assume the gas to be calorically perfect then we will have turbine efficiency as $C_p(T_3 - T_4)$ divided by $C_p(T_3 - T_4')$. One more point to be remembered here that as in case of compressor we did not land in

different pressure. The pressure at 4 dash and pressure at 4 is same, turbine exit which having same pressure whether it is ideal expansion or non-ideal expansion. So, we have the expression for it efficiency of turbine is $T_3 - T_4$ divided by $T_3 - T_{4 \text{ dash}}$. Now, for the process 3 4 the same thing, what we did for earlier case for the process 3 4. We know that P_4 is equal to $P_{4 \text{ dash}}$, but for again finding out the temperature T_4 we know that we are knowing turbine efficiency, we are knowing pressure ratio, we would know T_3 which is a T_{max} by some means, then we know γ . So, these are things which are known to us

So, now what we can find out is turbine efficiency is equal to $T_3 - T_4$ divided by $T_3 - T_{4 \text{ dash}}$. Our objective is to find out T_4 , so $T_4 - T_3$ is equal to turbine efficiency into $T_3 - T_{4 \text{ dash}}$. So, T_4 is equal to $T_3 - 1$ second. So, this is equal to $T_3 - T_{4 \text{ dash}}$. So, we have $T_3 - T_4$ is equal. So, efficiency is equal to $T_3 - T_4$ divided by $T_3 - T_{4 \text{ dash}}$.

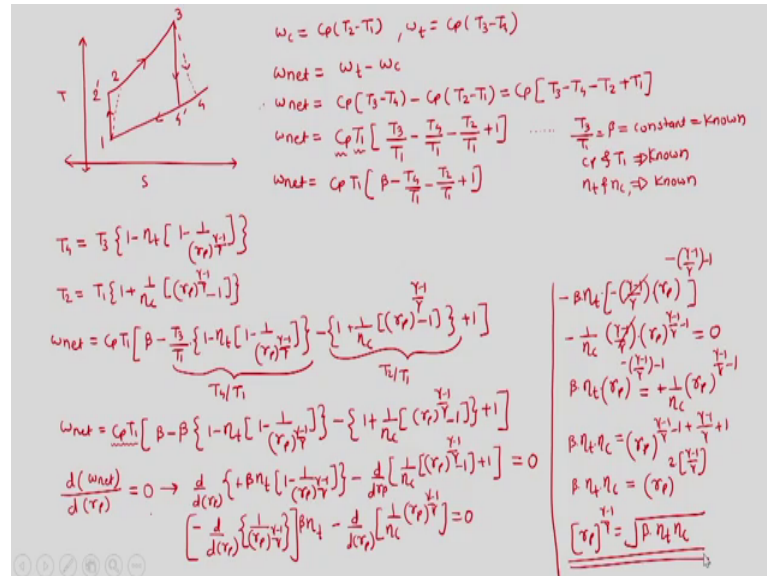
So, we want to find out T_4 . So, for that $T_3 - T_4$ is equal to efficiency into $T_3 - T_{4 \text{ dash}}$. So, T_4 is equal to $T_3 - \text{efficiency into } T_3 - T_{4 \text{ dash}}$. So, what we would have is, T_4 is equal to $T_3 - \text{turbine efficiency into } T_3 \text{ into } 1 - T_{4 \text{ dash upon } T_3}$, but we know that $T_{4 \text{ dash upon } T_3}$ is equal to $P_4 \text{ upon } P_3$ bracket raised to $\gamma - 1$ upon γ and that is $1 \text{ upon } r_p$ bracket raised to $\gamma - 1$ upon γ . So, what we ultimately would have is $T_{4 \text{ dash}}$, T_4 is equal to $T_3 - T_3 \text{ into turbine efficiency into } 1 - 1 \text{ upon } r_p \text{ raised to } \gamma - 1 \text{ upon } \gamma$.

So, T_4 is equal to $T_3 \text{ into } 1 - \text{turbine efficiency into } 1 - 1 \text{ upon } r_p \text{ raised to } \gamma - 1 \text{ upon } \gamma$. So, this is the formula for finding out temperature at the exit of the turbine. Here we know all the quantities; like again we know what is the pressure ratio, what is the γ what is the turbine efficiency and what is a T_3 which is T_{max} . So, having known this we can find out the actual corner properties which are take temperature and pressure

So, now we know what is turbine work output? Turbine work output is $T C_p$ into $T_3 - T_4$. So, T_4 is known to us, similarly compressor work C_p into $T_2 - T_1$ again T_2 new formula for T_2 in terms of compressor efficiency is known to us. Having known these things we should now find out what is the optimum condition for the

maximum work output in case of the compressor and turbine based plant where both are non-ideal. So, having said this we should find out w_{net} . So, let us work for this.

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So, we are now having non-ideal plant where we have turbine and compressors with non-ideal efficiencies. So, what we have, this is a, this is a turbine and then what we have, this is a compressor; 1 to 2 dash 1 to 2 1 to 2 to 3 3 to 4 and 3 to 4 dash. So, these are the processes in case of non-ideal. And we saw that compressor work is C_p into T_2 minus T_1 and turbine work is C_p into T_3 minus T_4 . Now, we are supposed to find out w_{net} . We know that w_{net} is w_t minus w_c , so w_{net} is C_p into T_3 minus T_4 minus C_p into T_2 minus T_1 .

So, what we have is C_p into T_3 minus T_4 minus T_2 plus T_1 . So, w_{net} is equal to. Known quantities are taken out, so we have T_3 upon T_1 minus T_4 upon T_1 minus T_2 upon T_1 plus 1. Here C_p is known to us T_1 is known to us. Practically T_3 is also known to us. So, we know that we have used T_3 upon T_1 as β and then that is constant or that is known

Similarly, C_p and T_1 are also known. So, we are working out the w_{net} formulation or constraint for maximum w_{net} with these fix things. So, w_{net} is equal to $C_p T_1$ into β minus T_4 . We can write T_4 by, we can write T_4 by T_1 minus T_2 by T_1 plus 1, but what we know? What we know is T_4 is equal to, from last slide we can take it T_4 is equal to T_3 into $1 - \eta_t$ T_1 raised to γ minus 1 upon γ . So, this is T_4 .

Similarly T_2 is equal to is known to us, T_1 into $1 + \frac{1}{\eta_c}$ plus compressor efficiency r_p raised to $\gamma - 1$ upon $\gamma - 1$, 1 upon compressor efficiency.

So, these two things are known to us, so we can use them to find out the w_{net} . So, w_{net} is equal to $C_p T_1$ into $\beta - \frac{T_4}{T_1}$. So, that will be T_3 by T_1 into $1 - \eta_T$ T_1 into $1 - \frac{1}{r_p^{\frac{1}{\gamma}}}$ upon γ . Then we have minus T_2 by T_1 , so we have $1 + \frac{1}{\eta_c}$ into $r_p^{\frac{1}{\gamma}} - 1$ upon $\gamma - 1$ plus 1 then bracket complete. So, this is basically T_4 by T_1 , and this is practically T_2 by T_1

Then now we need to differentiate this formula with respect to r_p , but before that we know that w_{net} is equal to the quantities with constants can be separated or known quantities can be separated. So, we have $C_p T_1$ into $\beta - \beta$ into $1 - \eta_T$ T_1 into $1 - \frac{1}{r_p^{\frac{1}{\gamma}}}$ upon γ bracket complete minus $1 - \frac{1}{r_p^{\frac{1}{\gamma}}}$ upon compressor efficiency r_p raised to $\gamma - 1$ upon $\gamma - 1$ plus 1 . So, having said this we know that β is a constant. So, since β is a constant its differentiation with respect to r_p will be 0 .

So, here we have to keep in mind that apart from our things η_c and η_T are also known. Having these things known we can now differentiate $d w_{net}$ by $d r_p$, and then we can equate it to 0 . So, having said this what we will get. So, this quantity is a constant, so $C_p T_1$ is a constant, its differentiation would be 0 , so we can neglect that and then we will have this also to be 0 . So, we directly would end up in this way $C_p d r_p$ of minus minus minus plus β into it η_T into $1 - \frac{1}{r_p^{\frac{1}{\gamma}}}$ bracket raised to $\gamma - 1$ upon γ minus. So, this differentiation will be 0 , so minus minus plus. So, d by $d r_p$ of $1 - \frac{1}{r_p^{\frac{1}{\gamma}}}$ upon compressor efficiency and $2 r_p^{\frac{1}{\gamma} - 1}$ upon $\gamma - 1$ plus 1 and then this, this equal to 0

So, having said this we can differentiate it and then we can find out that within that this first two quantities when would multiplied with 1 , they will have their differentiation to be 0 . So, what we ultimately would have is minus d upon $d r_p$ of $1 - r_p^{\frac{1}{\gamma}}$ raised to $\gamma - 1$ upon γ , and then this quantity would be multiplied by η_T plus and β plus. Then we would again have, differentiation will be 0 for this one. So, we will have d upon $d r_p$ of only this quantity which is 1 upon η_c into $r_p^{\frac{1}{\gamma}}$ raised to

$\gamma - 1$ upon γ , and this term would be equal to 0. Having said this we can differentiate it and then find out what is happening.

So, its differentiation will be $\beta - \beta \eta T$ into $-\gamma - 1$ upon γ into $r p$ bracket raised to $-\gamma - 1$ upon $\gamma - 1$. So, this is the differentiation of this term and then differentiation of this term would lead to 1 upon ηc into $r p$ into $\gamma - 1$ upon γ into $r p$ bracket raised to $\gamma - 1$ upon $\gamma - 1$ equal to 0. So, the term in the bracket which is $\gamma - 1$ upon γ would get cancelled

So, what we would have is $\beta \eta T$ into $r p$ bracket raised to $-\gamma - 1$ upon $\gamma - 1$ is equal to -1 upon ηc into $r p$ bracket raised to $\gamma - 1$ upon $\gamma - 1$. So, we have $\beta, \eta t, \eta c$ in equal to $r p$ raised to here we will have $\gamma - 1$ upon $\gamma - 1$ plus we will have $\gamma - 1$ upon γ plus 1 ok. So, there is a slight mistake, here it is 1 plus 1 upon ηc , so here it should be 1 plus 1 upon ηc . So, here it will be minus, here it will be minus, so here it will be minus accordingly and then this will lead to minus over here, and then it would lead to plus over here then we will have $\beta \eta T \eta c$ is equal to $r p$ raised to 2 into $\gamma - 1$ upon γ .

So, $r p$ raised to $\gamma - 1$ upon γ is equal to square root of $\beta \eta t \eta c$. So, this is the constraint on the optimum pressure ratio for the maximum network in case of non-ideal components of the Brayton cycle. So, if we have non-ideal components of the Brayton cycle, we would get ultimately the pressure ratio is equal to square root of pressure 2 raised to $\gamma - 1$ upon γ is equal to square root of $\beta \eta t$ into ηc as constraint on optimum pressure ratio. So, such pressure ratio which satisfies this is called as optimum pressure ratio. As what we would remember that if these efficiencies are 100 percent, then we had seen that for ideal cycle we had $r p$ optimum bracket raised to $\gamma - 1$ upon γ was square root of β . So, we just got an additional components with β as ηt and ηc

So, here we practically end the part what we were talking about, as if we are having non-ideal components. So, we have to keep again a point in mind that the things will not change, except what we will have is a turbine and compressor efficiencies. So, those turbine and compressor efficiencies will be used to find out the temperature at the end of

the turbine or temperature at the end of the compressor, rest of the things would remain same. There is one more point to note that now heat addition would not start from 2 dash, but it will start from 3 to, so heat addition will be C_p into T_3 minus T_2 .

Similarly in case of heat rejection it will not start from T_4 dash, but it will start from T_4 , then Q_{out} is equal to $T_4 C_p$ into T_4 minus T_1 . So, efficiency would accordingly change. So, efficiency would be 1 minus Q_{out} upon Q_{in} . So, 1 minus C_p into T_4 minus T_1 divided by C_p into T_3 minus T_2 . So, we know now T_3 , we know now T_2 , we know now T_4 and we know T_1 , so accordingly we can find out efficiency. So, this is how the chapter or the part for non-ideal components is. Now we will see some examples

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Example

A gas turbine operates on a pressure ratio 6. The inlet air temperature to the compressor is 300K and the air enters the turbine at 577°C. If the volume flow rate of the air is 240 m³/s calculate power output in MW for the Gas turbine power plant

given $\rightarrow r_p = 6.0, \eta_c = \eta_t = 100\%, C_p = 1.005 \text{ kJ/kg K}, \gamma = 1.4, P_1 = 1 \text{ bar}$

$\frac{P_2}{P_1} = r_p = 6.0, T_1 = 300\text{K}, T_3 = 577^\circ\text{C} = (577 + 273)\text{K}$

Volume flow rate = 240 m³/sec

$\omega_{net} = ? \text{ (MW)}$

$\omega_{net} = \omega_t - \omega_c = C_p(T_3 - T_2) - C_p(T_2 - T_1)$

$\frac{T_2}{T_1} = (r_p)^{\frac{\gamma-1}{\gamma}} \rightarrow T_2 = T_1 (r_p)^{\frac{\gamma-1}{\gamma}} \rightarrow T_2 = \text{known}$

$\frac{T_3}{T_4} = (r_p)^{\frac{\gamma-1}{\gamma}} \rightarrow T_4 = \frac{T_3}{(r_p)^{\frac{\gamma-1}{\gamma}}} \rightarrow T_4 = \text{known}$

$\omega_{net} \rightarrow \text{kJ/kg} \rightarrow \text{known}$

mass flow rate = Volume flow rate $\times$ density

$\omega_{net} \text{ (MW)} = \omega_{net} \text{ (kJ/kg)} \cdot \text{mass flow rate (kg/s)}$

We will here see how to solve the example or what are the things which would be given in general in an example. So, an example says that there is a gas turbine which operates on a pressure ratio 6. The inlet air temperature to the compressor is 300 Kelvin and the air enters the turbine at 577 degree Celsius. If volume flow rate of air is 240 meter cube per second then calculate power output in megawatt for the gas turbine power plant. So, what is given to us, so what is given to us is given in the example. In the example we are given with r_p and that r_p is equal to 6.

First we should always draw the T S diagram and this example, since we are not given with turbine and compressor efficiencies we can assume turbine efficiency and compressor efficiencies as 100 percent, so they are one. So, for us we are working with

ideal gas turbine power plant 1 2 3 4. So, what is given to us is r_p . So, we are knowing P_2 by P_1 is equal to r_p is equal to 6.

So, we parallelly know the inlet air temperature to the compressor means, we know T_1 is equal to 300 Kelvin and then we know turbine entry temperature which is T_3 , T_3 is equal to 577 degree Celsius, so it is 577 plus 273 Kelvin. So, I am just explaining the process what we are given is volume flow rate and volume flow rate is 240 meter cube per second, and we are supposed to find out what is w_{net} , but the usual formula of ours would lead w_{net} in kilo Joule per k g, but here we are supposed to find out w_{net} in megawatt. So, this we have to remember. So, what we can do

We need, we know that w_{net} is equal to w_t minus w_c . So, we know that w_t is equal to C_p into T_3 minus T_2 minus C_p into T_2 minus T_1 . We again should know that C_p for air is 1.005 kilo Joule per k g Kelvin. This is information which either would be known to us or would be given to us. So, sorry, so turbine work is T_3 . So, turbine work is T_3 minus T_4 and compressor work is C_p into T_2 minus T_1 . Then for us we do not know what is T_4 and we do not know what is T_2 , but we know T_2 by T_1 is r_p raised to γ minus 1 upon γ .

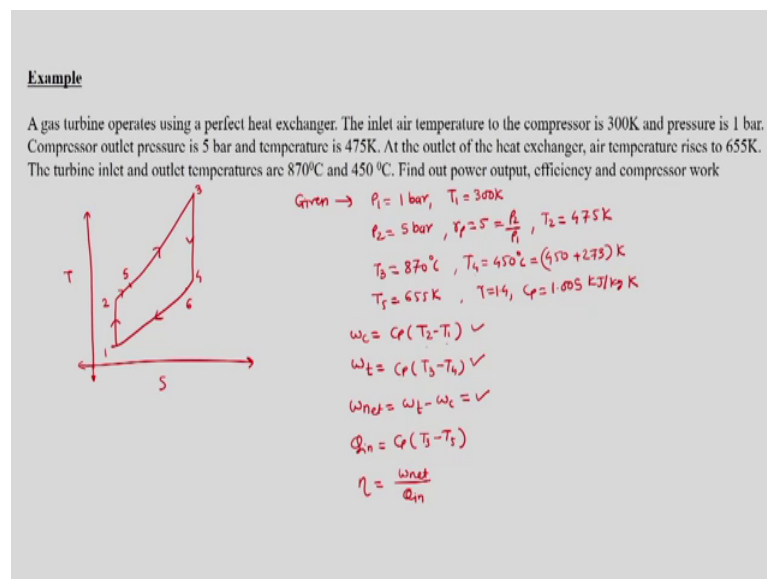
So, we know r_p , we know T_1 , we can find out T_2 . So, T_2 is equal to T_1 into r_p bracket raised to γ minus 1 upon γ , since we are told with air. For air γ is 1.4, so we know r_p , we know γ , we know T_1 . So, now, T_2 is known to us, then T_2 is known to us, then T_3 is also given to us as it is told. So, now, we just have to find out T_4 . So, for T_4 also we know formula T_3 by T_4 is r_p raised to γ minus 1 upon γ , but this leads to T_4 is equal to T_3 upon r_p bracket raised to γ minus 1 upon γ . So, here as well T_3 is known to us, γ is known to us, r_p is known to us

So, now T_3 is known to us. Knowing T_3 , T_3 not T_4 is known to us. So, knowing T_4 , knowing T_2 , knowing T_3 and T_1 we can find out w_{net} , but this w_{net} in kilo Joule per k g is known. Our object over here is to find out what is the w_{net} in megawatt. So, here we have to multiply it with mass flow rate or volume flow rate. So, what is the volume flow rate? Volume flow rate is given to us which is 240 meter cube per second, but this is volume flow rate. So, we have to find out mass flow rate. So, for mass flow rate we have to multiply by density.

So, mass flow rate is equal to volume flow rate into density. Then where we have to find out density? We have to find out density at 1. So, we know we will take pressure as 1 bar at the inlet and then we know temperature 300 Kelvin then we can find out density. So, for that we will assume P_1 is equal to 1 bar. So, if we take P_1 as 1 bar then we know P is equal to $\rho r t$. Then knowing the pressure and knowing the temperature we can find out density at the inlet.

So, we know, once we know the density at the inlet we know volume flow rate, then we know mass flow rate, then w_{net} in megawatt is equal to w_{net} in kilo Joule per k g in mass into mass flow rate which is k g per second. So, this is how we can solve this example where we are supposed to find out what is the power output in megawatt. So, having said this, we will see how the next example is.

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In the next example we are again told that there is a gas turbine which operates on a perfect heat exchanger. So, this example is with a gas turbine with heat exchanger. The inlet air temperature to the compressor is 300 Kelvin and pressure is 1 bar, compressor outlet pressure is 5 bar and temperature is 475 Kelvin. At the outlet of the heat exchanger air temperature rises to 655 Kelvin, the turbine inlet and outlet temperatures are 870 celsius and 450 celsius, find out power if output and efficiency of and compressor work. So, here as well first we will start with T S diagram. So, as per T S diagram we are at 1 2,

but 2 to 3 is a heat exchange process then 3 to 4. So, we did not name it as 3 v 3 4, here we have 5 and then here we have 6. So, this is the ideal cycle with heat exchanger

So, now in the given things we are given with P_1 which is 1 bar T_1 which is 300 Kelvin, we are again told that P_2 is 5 bar. So, practically r_p is 5 which is P_2 by P_1 it is given to us, but we are also given that T_2 is equal to 475 Kelvin. We are told that T_3 is equal to 870 degree Celsius and T_4 is 450 degree Celsius. So, keep this point in mind T_2 is 475 Kelvin, but T_4 is 450 plus 273 Kelvin for heat exchanger cooperate we always know that T_4 has to be greater than T_2 , but we are told that T_5 is 655 Kelvin which is a temperature at the outlet of the heat exchanger.

Now, we are supposed to find out power output and efficiency and compressor work, which is compressor work is simple to find out w_c is equal to C_p into T_2 minus T_1 . Again for all this case we have to take γ is equal to 1.4 C_p . For air 1.005 kilo Joule per kg Kelvin and then we know C_p , we know T_2 and we know T_1 , so compressor work can be easily found out. Similarly for turbine work is also C_p into T_3 minus T_4 T_3 is also given, T_4 is also given, C_p is also known. So, turbine work can also be found out. So, w_{net} is equal to w_t minus w_c . So, turbine work is known, compressor work is known, then we can find out w_{net} , but what is that we have to find out is efficiency. So, for efficiency there is only one glitch, only one problem that we have to find out Q_{in}

So, Q_{in} is C_p into T_3 minus T_5 and its not T_2 that is what we have to remember, since combustion chamber entry temperature is T_5 . So, T_3 is known to us, T_5 is known to us, C_p is known to us. We know Q_{in} , then efficiency is w_{net} upon Q_{in} . Thus we can find out how the different parameters of the cycle can be found out for every case. One thing we have to remember that first we have to draw the $T-S$ diagram or $P-V$ diagram of the cycle, then we have to find out what are the given things. From the given things we have to find out all the corner parameters like $T_2 P_2 T_3 P_3 T_4 P_4$.

Once those parameters are found out then we can find out heat and work interaction in each process; like compressor work, like turbine work, like Q_{in} and Q_{out} . And then we can find out what is the resultant performance parameters of the cycle which are efficiency w_{net} like parameters. So, this is the fact which we should remember and we

end here with the lectures for the fact where we were dealing with the compressor turbine, if they are non-ideal then how would be they affect the Brayton cycle.

Thank you.