

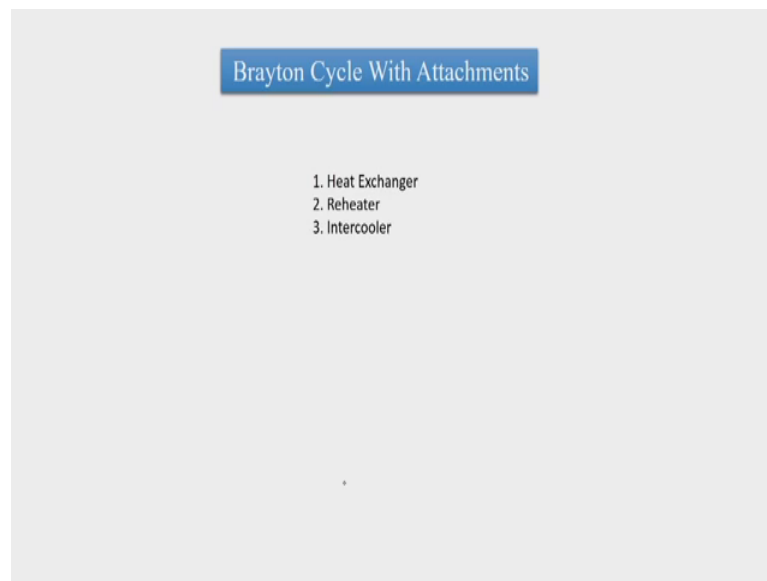
IC Engines and Gas Turbines
Dr. Vinayak N. Kulkarni
Department of Mechanical Engineering
Indian Institute of Technology, Guwahati

Lecture - 36

Brayton Cycle with Attachments: Heat Exchanger, Reheater, Intercooler

Welcome to the next class. In today's class, we will see about Brayton Cycle with some Attachments, and in previous class what we had seen was about Brayton cycle, its calculation for network output, its calculation for thermal efficiency and then we went on finding out what is the optimum condition when we can get maximum network of the Brayton cycle. And now we are supposed to find out what is the effect of different attachments on the Brayton cycle.

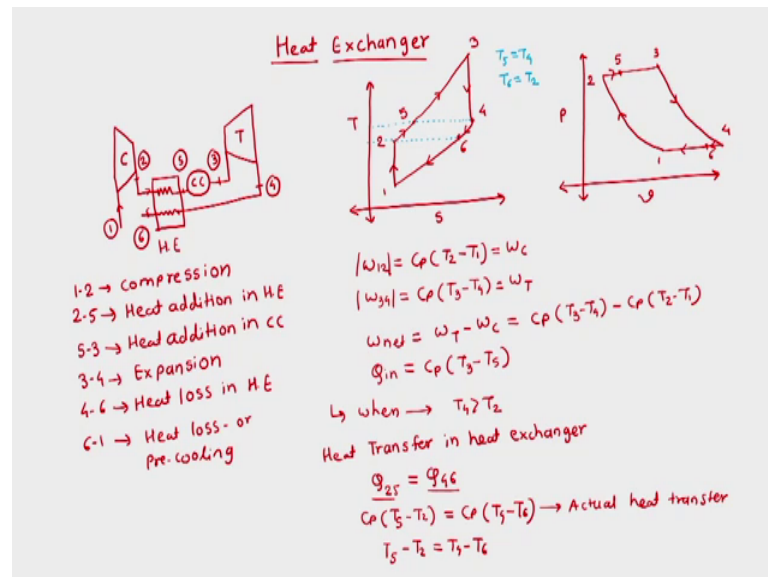
(Refer Slide Time: 01:13)



So, first attachment is Heat Exchanger, next attachment is Reheater and then Intercooler and then we will see what is the mixed or combined effect of all this thing. We should remember in our earlier lecture we had discussed about heat exchanger. We know that from last derivation efficiency of Brayton cycle depends upon pressure ratio. So, if we increase the pressure ratio or operating pressure ratio of the cycle efficiency of the cycle increases. Similarly, if we attach heat exchanger attachment of heat exchanger also increases the efficiency of the cycle. We had also seen that heat exchanger attachment is not that good idea if we go for high-pressure ratio since there are losses with it.

Attachment of reheater is more for getting more work output and attachment of intercooler is to reduce the work input. So, these 3 attachments have 3 different reasonings and then we will see one attachment each.

(Refer Slide Time: 02:27)



So, Brayton cycle with Heat Exchanger. So, let us see Brayton Cycle with Heat Exchanger, Cycle with Heat Exchanger. So, the attachment is this way if we see, we first have compressor, we know that there is a compressor. So, we will denote it as C. So, air comes in the compressor and then it goes out from the compressor to the combustion chamber, but while going out it will pass through a heat exchanger and then this is combustion chamber. Then air goes to the turbine, so this is turbine. And then turbine exhaust goes into the heat exchanger where there is heat exchange between the air which is actually going to the combustion chamber. So, this is heat exchanger.

So, now, as our usual denotations this is 1, this point is 2, then this point we will say it as, we will denote this point as, this point as 2 as it was denoted earlier, then this point is 5 for us, since combustion exhaust is 3, turbine exhaust is 4, heat exchanger exhaust is 6. So, process 1 to 2, compressor Compression, process 2 to 5 is Heat addition, in heat exchanger process, 5 to 3, is Heat addition in combustion chamber process, 3 to 4 is Expansion, and then we have 4 to 6 this is in Heat loss in heat exchanger. Then, obviously, we will have 6 to 1 which is Heat loss, but we are considering in general open

cycle gas turbine power plant. But if it would have been closed cycle then obviously, we would have Heat loss or pre-cooler, pre- Pre-cooling.

Now, our job is to denote this cycle on the T S diagram. Suppose, this is T axis, this is S axis, now we have 1 to 2, 1 to 2 is compression, then we have process 2 to 5 is heat addition in heat exchanger, but that is at constant pressure. Again, 2 to 3 is sorry 2 to 5 heat addition in heat exchanger. Then, we have 5 to 6 same pressure or 5 to 3. It will continue with the same pressure. Then, we have 3 to 4, we have 3 to 4 and then we have 4 to 6. This is heat loss in heat exchanger and 6 to 1 is pre-cooler. This is however TS diagram would look like.

Now, if I draw P V diagram for the same cycle then P V diagram will look like, we have P axis, we have specific volume as V axis and 1 to 2 isentropic compression. So, 1 to 2 is isentropic compression. 2 to 3 is isobaric heat addition, so 2 to 3 in the heat exchanger, then 3 to 5 sorry 2 to 5 is heat exchanger heat addition, 5 to 3 is heat addition in combustion chamber, then 3 to we have 4 expansion in the turbine and then we have 4 to 6 heat loss in heat exchanger and 6 to 1 we have heat loss in, heat loss in pre-cooler. So, these are the P V diagrams.

Now, we have to find out the network and efficiency formulation for the attachment with heat exchanger, Brayton cycle with heat exchanger. So, first the process 1 to 2 we will have same, we will have 1 to 2, w 1 to 2 is unaltered. So, w 1 to 2 is absolute value is $C_p (T_2 - T_1)$. Again, this is for compressor, compressor work input. Similarly, w 3 4 which is $C_p (T_3 - T_4)$ which is turbine work this is also unaltered. So, if we see, w net which is w T minus w C is unaltered and that is $C_p (T_3 - T_4 - T_2 + T_1)$. So, this formula is unaltered with the attachment of heat exchanger.

But what is change then? The change thing is Q in, which is amount of heat added into the system. In olden case without heat exchanger heat addition was $C_p (T_3 - T_2)$, that is from external source, but now we have heat addition from external source by combustion is only $C_p (T_3 - T_5)$. So, this is the only amount of heat added into the process of heat transfer in combustion chamber. So, this is what it is going to be (Refer Time: 09:47) by an amount which is $C_p (T_5 - T_2)$.

So, we will have efficiency will be higher since for efficiency formula we have w_{net} upon Q_{in} , but formula for w_{net} is not changed, but formula for Q_{in} shows decrement in Q_{in} . So, efficiency of the cycle would increase. But then there are some issues which we should remember. Issue 1: when can we add heat exchanger? When? We had seen that attachment of heat exchanger is considered only for low-pressure ratio gas turbines, but when? For this when they seek requirement is you should have T_4 should be greater than T_2 , then only we can add the attachment for heat exchanger if T_4 is greater than T_2 then heat exchange is not possible to the air which is going to the combustion chamber, it is also clear from this T S diagram. So, for that we need T_2 to be, T_4 to be lesser than T_4 or T_4 to be greater than T_2 .

Then, what we next have to see is what is the heat transfer in heat exchanger, heat transfer in heat exchanger. There is, there are two elements in the heat exchanger one is air in the process 2 to 5. So, there is Q_{2-5} and that has to be equal to Q_{4-6} . Since this is heat loss other this is heat gain by the air which is going to the combustion chamber and this is heat loss by the gas which is going out from the turbine exhaust.

So, what is Q_{2-5} ? It is C_p into T_5 minus T_2 and this is equal to C_p into T_4 minus T_6 . So, this is equal. But C_p we are considering calorically perfect gas, so C_p is same. So, we practically get T_5 minus T_2 is equal to T_4 minus T_6 , this is what we are getting.

Next thing what we have to see is, there is a concept called as effectiveness of heat exchanger.

(Refer Slide Time: 12:43)

$$\begin{aligned}
 \eta_{HE} &= \frac{\text{Actual heat transfer}}{\text{Max. possible transfer}} = \frac{C_p (T_5 - T_2)}{C_p (T_4 - T_2)} \\
 \eta_{HE} &= \frac{T_5 - T_2}{T_4 - T_2} = 1 \rightarrow T_5 - T_2 = T_4 - T_2 \rightarrow \boxed{T_5 = T_4} \\
 \eta_{HE} &= \frac{T_4 - T_6}{T_4 - T_2} = 1 \rightarrow T_4 - T_6 = T_4 - T_2 \rightarrow \boxed{T_6 = T_2} \\
 W_{net} &= C_p (T_3 - T_4) - C_p (T_2 - T_1) \\
 Q_{in} &= C_p (T_3 - T_5) = C_p (T_3 - T_4) \\
 \eta_{th} &= \frac{W_{net}}{Q_{in}} = \frac{C_p (T_3 - T_4) - C_p (T_2 - T_1)}{C_p (T_3 - T_4)} = 1 - \frac{C_p (T_2 - T_1)}{C_p (T_3 - T_4)} \\
 \eta_{th} &= 1 - \frac{T_2 - T_1}{T_3 - T_4} = 1 - \frac{T_1 (r_p)^{\frac{\gamma-1}{\gamma}} - T_1}{T_3 - T_3 / (r_p)^{\frac{\gamma-1}{\gamma}}} = 1 - \frac{T_1}{T_3} \left[\frac{(r_p)^{\frac{\gamma-1}{\gamma}} - 1}{(r_p)^{\frac{\gamma-1}{\gamma}} - 1} \right] (r_p)^{\frac{\gamma-1}{\gamma}} \\
 \eta_{HE} = 1 &\rightarrow \boxed{\eta_{th} = 1 - \frac{(r_p)^{\frac{\gamma-1}{\gamma}}}{\beta}} \dots r_p = \frac{r_2}{r_1} \text{ or } r_p = \frac{\beta}{r_1} \text{ if } \beta = \frac{T_3}{T_1} = \frac{T_{max}}{T_{min}} \\
 &\quad r_p = \frac{r_{max}}{r_{min}}
 \end{aligned}$$

Effectiveness of heat exchanger, and effectiveness of heat exchanger is a Actual heat transfer by Maximum possible heat transfer. And what is actual heat transfer? Actual heat transfer is what we know it is from last slide. What is actual heat transfer? C P into T 5 minus T 2 is actual heat transfer or C P into T 4 minus T 6 is also actual heat transfer. So, actual heat transfer is C P into T 5 minus T 2. But what is maximum possible heat transfer? Maximum possible heat transfer is T 4 minus T 2. So, basically this is the maximum temperature in this at the in the heat exchanger divided by minimum temp minus minimum temperature in the heat exchanger. So, this is the maximum or big temperature difference in the heat exchanger. So, C P into T 4 minus T 2. So, this gives us the formula for effectiveness of heat exchanger. So, effectiveness of heat exchanger practically for us is by cancel C P we get T 5 minus T 2 divided by T 4 minus T 2.

Now, we are going to consider the cases where we will have ideal assumption for the heat exchanger. So, let us consider the heat exchanger to be ideal. So, heat exchanger will have efficiency which is 100 percent for effectiveness to be 1. So, let us consider that this to be 1. Once this is 1, it leads to T 5 minus T 2 is equal to T 4 minus T 2 and then this leads to T 5 is equal to T 4 this is one outcome. But effectiveness, can also be written as for the heat exchanger instead of T 5 minus T 2 it is also is equal to T 4 minus T 6 divided by T 4 minus T 2. This is also heat transfer in the heat exchanger we have seen it in the last slide. Heat transfer is either C P into T 5 minus T 2 or C P into T 4 minus T 6.

This is heat gain by the air from the exhaust and this is heat loss by the exhaust to the air. So, this is actual heat transfer both are we can say here as actual heat transfer. So, what we will have here is also for ideal case it is 1, and then this would lead to $T_4 - T_6$ is equal to $T_4 - T_2$. So, we will have T_6 is equal to T_2 for ideal case.

So, what is going to happen in ideal case? So, we will go back and we will see what is going to happen in ideal case. In the ideal case we will we can clearly see that there are few things which will be like this, in case we have ideal case leads to T_5 is equal to T_4 and T_6 is equal to T_2 . So, what we are having is T_5 is equal to T_4 and T_6 is equal to T_2 . So, temperature is same. So, this is how ideal heat exchanger would operate. So, we have to keep this point in mind.

So, this keeping this point in mind we have to modify our formula for w_{net} and we have to modify our formula for efficiency of heat exchanger. So, let us write down the formula for network w_{net} . What we wrote is $C_p \text{ into } T_3 - T_4 - C_p \text{ into } T_2 - T_1$ there is no alteration in it, but Q_{in} is equal to $C_p \text{ into } T_3 - T_5$, but what is T_5 we can see this $C_p T_5 - T_3$ minus T_5 . So, what is T_5 ? We have seen T_5 is equal to T_4 . So, $C_p \text{ into } T_3 - T_4$. So, now, let us define the efficiency. Thermal efficiency with heat exchanger and then it is w_{net} upon Q_{in} . So, it is $C_p \text{ into } T_3 - T_4 - C_p \text{ into } T_2 - T_1$ divided by $C_p \text{ into } T_3 - T_4$. So, this would lead to $1 - C_p \text{ into } T_2 - T_1$ in divided by $C_p \text{ into } T_3 - T_4$, ok.

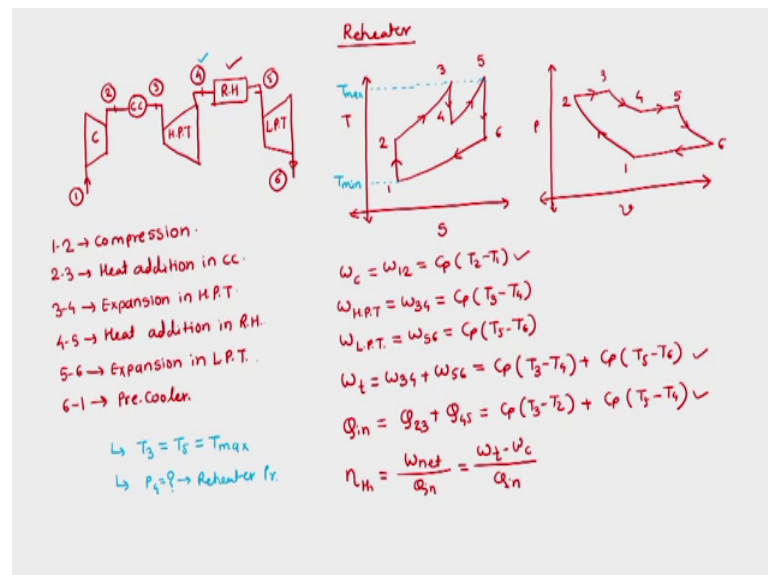
So, thermal efficiency of heat exchanger will equal to $1 - C_p C_p$ cancels out we have $T_2 - T_1$ divided by $T_3 - T_4$. So, we know formulas for T_2 and T_4 . We can use those formulas. And as per those formulas $1 - T_1$ into r_p , bracket raise to $\gamma - 1$ upon $\gamma - 1$ divided by $T_3 - T_3$ divided by r_p bracket raise to $\gamma - 1$ upon γ . So, this is equal to $1 -$ we can take T_1 common. So, T_1 we can take T_3 common, so T_3 . So, this in the bracket r_p bracket raise to $\gamma - 1$ upon $\gamma - 1$ divided by r_p bracket raise to $\gamma - 1$ upon γ minus 1, but then this r_p will go in that and then we will get r_p into bracket raise to $\gamma - 1$ upon γ .

So, thermal efficiency is equal to $1 - r_p$ bracket raise to $\gamma - 1$ upon γ divided by β , where we know r_p is equal to P_2 by P_1 or r_p is equal to P_3 by P_4 and β is equal to T_3 by T_1 or T_{max} by T_{min} . Similarly, r_p is equal to P

max by P min. So, this formula is for heat exchanger attachment for the Brayton cycle based power plant, but constraint it heat exchanger has effectiveness 100 percent or is in case heat exchanger effectiveness this formula is for heat exchanger effectiveness is equal to 1. So, this is the constraint.

Having said this, now if we are giving with an example or if we have to design a thermal power plant where we are supposed to use the heat exchanger then we can do the all the calculations and find out w_{net} and efficiency effect thermal efficiency of the power plant. Having done with the heat exchanger we will see the next attachment as Reheater.

(Refer Slide Time: 22:15)



Our next attachment is reheater. Brayton cycle based power plant with reheater. As I said earlier use of reheater is more for increasing the power of it of the Brayton cycle based power plant. So, here as well we will have compressor, here we will come into the compressor, so this is C from the compressor it will go to the combustion chamber, so it is C C then it goes to a turbine and we call it as highpressure turbine. So, initially air would go to high-pressure turbine. High pressure turbine exhaust is committed to a reheater. So, here is the concept of reheater. Then from reheater it goes to the low-pressure turbine. So, this is low-pressure turbine and then air is exhausted. So, this is how we will have Brayton cycle based power plant for the attachment with reheater.

So, here we will again number 1, we will number it as 2, we will number it as 3, we will number it as 4, 5, and 6. So, the process 1 to 2 is Compression, process 2 to 3 is Heat

addition, in combustion chamber then process 3 to 4 is Expansion, in High Pressure Turbine then process 4 to 5 is Heat addition in reheater and then process 5 to 6 (Refer Time: 24:39) power plant is Expansion in Low Pressure Turbine, but thermodynamically we will have process 6 to 1 in the Pre-Cooler.

So, now we have to draw thermodynamic cycle for this reheater attachment. Again we will draw T S diagram. So, this is T axis, this is S axis. So, process 1 to 2 process, 1 to 2 is isentropic compression, ok. So, then process 2 to 3 is isobaric heat addition, so this is 3. 3 to 4 isentropic expansion, so this is 4. Then 4 to 5 is isobaric heat addition, so this is 5; 5 to 6 is isentropic expansion, so this is 6. 6 to 1 is pre-cooler. So, here 1 to 2 is isobaric, 2 to 3 is 1 to 2 is isentropic, 2 to 3 is isobaric, 3 to 4 is isentropic, 4 to 5 is isobaric, 5 to 6 is isentropic, 6 to 1 is again isobaric. So, this is T S diagram for Brayton cycle with reheater attachment and this is the reheater.

Now, we can draw P V diagram for the same attachment. So, this is P, this is specific volume V in the P V diagram first we have 1 to 2 as isentropic compression, 2 to 3 is constant pressure heat addition, 3 to 4 is isentropic expansion, 4 to 5 is constant pressure heat addition, 5 to 6 is isentropic expansion and 6 to 1 we have isobaric heat rejection. So, this is Brayton cycle based power plant thermodynamic cycle for reheater arrangement.

Now, we have to again do the same calculation for w_{net} and Q_{in} and so we have to find out what is the thermal efficiency. We have to keep one point in mind that we have to use same formulas what we use to use for calculation of all corner quantities. So, if we know 3, T_3 and P_3 then we should be able to find out P_4 and T_4 from isentropic relations. Similarly, if we know everything at 4 then we can find out everything other thing at 5. However, there are certain constraints which would be known to us later on.

In this phase write w , now we will have w_c which is equal to w_{12} and that is equal to $C_p (T_2 - T_1)$ this is an altered. But w_T is changed now we have not just w_T we have $w_{HP \text{ Turbine}}$ and that is w_{34} that is $C_p (T_3 - T_4)$ and then we have $w_{LP \text{ Turbine}}$ that is w_{56} that is $C_p (T_5 - T_6)$. So, we have total turbine work w_T is equal to w_{34} plus w_{56} . So, we have $C_p (T_3 - T_4)$ plus $C_p (T_5 - T_6)$. Parallely we have Q_{in} and Q_{in} is equal to there are two heat addition processes, one is Q_{23} plus Q_{45} . So, we have $C_p (T_3 - T_2)$

plus C_p into T_4 sorry C_p into T_5 minus T_4 . So, these two formulas are changed. So, efficiency with thermal efficiency of Brayton cycle based power plant with reheater rearrangement it change.

And now we have w_{net} upon Q_{in} and w_{net} is equal to w_t minus w_c divided by Q_{in} . So, w_t can be found out from here, w_c can be found out from here, Q_{in} found can be found out from here, and then we can find out thermal efficiency of the Brayton cycle based power plant.

But for the reheater arrangement we have to know one thing rather there are two things. First thing, generally whenever we are using Brayton cycle based power plant with reheater arrangement then we should know one thing that we generally get T_3 is equal to T_5 is equal to T_{max} . These two temperatures are same. These two temperatures are same. So, having same temperatures we can have, so this is T_{max} , this is T_{max} and this is T_{min} .

There is one more point to be noted that what is P_4 ? What is the value of P_4 ? Means we should ask our self a question that when we should stop expanding the gas into the low pressure or as a high pressure turbine. At what condition it should enter into the reheater. So, what is the pressure of reheater? So, P_4 is reheater pressure. What is that? So, what is reheater pressure? So, this is a question and we will do a derivation for this question that how to find out what is the optimum condition for reheater, so that we can get a given objective to be achieved.

So, what is our objective in case of reheater based attachment? Our objective is that there is certain amount of oxygen remained into the air which is uncombusted. So, for it has not taken part in the combustions we have to burn that and by burning that we are going to get more work output. So, getting more work output is our basic objective function over here. So, for that we have to find out what is the P_4 , what is the condition in, what is the pressure of reheater such that it would lead us to maximum network. So, let us define this, so what our objective over here is to find out what is the reheater pressure which would lead to maximum network.

(Refer Slide Time: 33:15)

$$\begin{aligned}
 W_{net} &= W_{HPT} + W_{LPT} - W_c \\
 W_{net} &= C_p (T_3 - T_4) + C_p (T_5 - T_6) - C_p (T_2 - T_1) \\
 W_{net} &= C_p [T_3 - T_4 + T_5 - T_6 - T_2 + T_1] \\
 \text{Constraint 1} &\rightarrow T_3 = T_5 = T_{max} \\
 \text{Constraint 2} &\rightarrow \frac{T_{max}}{T_{min}} = \beta = \text{constant} \quad \left. \vphantom{\frac{T_{max}}{T_{min}}} \right\} W_{net}|_{max} \\
 W_{net} &= C_p [T_3 - T_4 + T_3 - T_6 - T_2 + T_1] \\
 W_{net} &= C_p [2T_3 - T_4 - T_6 - T_2 + T_1] \\
 T_1 &\rightarrow \text{known by } C_p \text{ is known} \\
 W_{net} &= C_p T_1 \left[2 \frac{T_3}{T_1} - \frac{T_4}{T_1} - \frac{T_6}{T_1} - \frac{T_2}{T_1} + 1 \right] \\
 W_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{T_4}{T_3} \cdot \frac{T_3}{T_1} - \frac{T_6}{T_5} \cdot \frac{T_5}{T_1} - \frac{T_2}{T_1} \right] \\
 W_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{T_4}{T_3} \cdot \beta - \frac{T_6}{T_5} \cdot \beta - \frac{T_2}{T_1} \right] \\
 W_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{T_4}{T_3} \beta - \frac{T_6}{T_5} \beta - \frac{T_2}{T_1} \right]
 \end{aligned}$$

So, let us, work out what is w_{net} , w_{net} for us is w high pressure turbine plus w low pressure turbine minus w compressor. So, w_{net} it is equal to C_p . What is high pressure turbine work? It is T_3 minus T_4 we should remember it here. T_3 minus T_4 T_5 minus T_6 and T_2 minus T_1 . T_3 minus T_4 plus C_p into T_5 minus T_6 is low pressure turbine work and then we have compressor work is C_p into T_2 minus T_1 .

Now, having said this we can take C_p common and write down T_3 minus T_4 plus T_5 minus T_6 minus T_2 plus T_1 . Now, there is one more thing we will put here a constraint which says that T_3 is equal to T_5 or what we will write our constraint as T_3 is equal to T_5 is equal to T_{max} and we will also say the constraint 1, constraint 2. We have T_{max} upon T_{min} which is β and then that is constant. So, our objective is to find out what is the w_{net} max for these two constraints. If T_3 is equal to T_5 is equal to T_{max} and T_{max} upon T_{min} which is β is equal to constant. So, for these two constraint we will carry forward our derivation and as per that we have w_{net} is equal to C_p then T_3 minus T_4 , then we have T_5 , our T_5 is equal to T_3 minus T_6 minus T_2 plus T_1 . So, w_{net} is equal to C_p into twice T_3 minus T_4 minus T_6 minus T_2 plus T_1 , but we again know that conditions at the inlet are known, we know that conditions at the inlet are known, so for that all fact we have T_1 is known.

Similarly, C_p is known. So, we will continue this derivation and in that now we can get w_{net} is equal to C_p into T_1 divided by 2 into T_3 by T_1 minus T_4 by T_1 minus T_6

by T_1 minus T_2 by T_1 plus 1. So, w_{net} is equal to $C_P T_1$. So, we can write it as 2 into β . T_3 by T_1 is β . And similarly, T_5 by T_1 is also β minus, we can see here T_4 by T_3 into T_3 by T_1 . So, we have divided and multiplied by T_3 . Why did we do so? Since, we can see 4 and 3 are in isentropic line. So, there is a relation which is known between temperature at 4 and temperature at 3 and further by doing so, we got introduced with β . So, β is known which is T_3 by T_1 and then relation would have also be known. Similarly, T_6 is here, so we can replace it, we can replace it and say that this is basically T_6 divided by T_5 into T_5 divided by T_1 .

But what is T_5 ? T_5 is basically T_3 . What is T_5 is basically T_3 so, my plus 1. So, w_{net} is equal to $C_P T_1$ twice β minus T_4 by T_3 . What is T_4 by T_3 ? 1 upon r_P bracket raise to γ minus 1 upon γ into β , ok. So, minus T_6 by T_3 which is T_6 by basically T_5 . So, T_6 by T_5 , T_6 by T_5 is also same way we can say it as T_6 by T_5 is also 1 upon r_P bracket raise to γ minus 1 upon γ into β plus 1 . So, we get this formulation for the w_{net} .

Now, we have to do few things about evaluation of this formula. So, let us work out, ok. So, what we can do here? That we can write w_{net} is equal to $C_P T_1$ is equal to 2 into β , we can take this one closure 2 into β plus 1 minus T_4 divided by T_3 . We are going to rearrange this term which is T_4 by T_1 as T_4 divided by T_3 into T_3 divided by T_1 minus. Similarly, we can do it for 6. T_4 by T_3 is for high pressure turbine and T_6 by T_5 is for low-pressure turbine. So, we can do it for here also which is T_6 by T_5 into T_5 by T_1 minus T_2 by T_1 plus, so this plus 1 is accounted. So, we will have bracket complete. So, w_{net} practically would be $C_P T_1$ into twice β plus 1 minus T_4 by T_3 into β T_3 by T_1 is β minus T_6 by T_5 . What is T_5 ? T_5 is T_3 by T_1 minus T_2 by T_1 . So, w_{net} is equal to $C_P T_1$ in the bracket 2β plus 1 minus T_4 by T_3 into β minus T_6 by T_5 into β minus T_2 by T_1 . This is the derivation for w_{net} .

Now, we did not achieve our objective, yet we have to continue. So, let us continue we will take this w_{net} here. So, w_{net} is basically equal to $C_P T_1$ into twice β plus 1 minus T_4 by T_3 into β minus T_6 by T_5 into β minus T_2 by T_1 and then bracket complete. So, we have 1, 2, 3 and 4 terms and then we have 1, 2, 3 and 4 term correct.

(Refer Slide Time: 41:51)

$$\begin{aligned}
 w_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{T_3}{T_3} \beta - \frac{T_4}{T_4} \beta - \frac{T_5}{T_1} \right] \\
 t &= \frac{T_2}{T_1} \quad t_1 = \frac{T_3}{T_4} \quad t_2 = \frac{T_5}{T_6} \\
 \checkmark \quad \frac{T_2}{T_1} &= \left(r_p \right)^{\frac{\gamma-1}{\gamma}} \quad \frac{T_3}{T_4} = \left(\frac{P_3}{P_4} \right)^{\frac{\gamma-1}{\gamma}} = \left(r_p \right)^{\frac{\gamma-1}{\gamma}} \quad \frac{T_5}{T_6} = \left(\frac{P_5}{P_6} \right)^{\frac{\gamma-1}{\gamma}} = \left(r_p \right)^{\frac{\gamma-1}{\gamma}} \\
 \downarrow & \quad \downarrow \quad \downarrow \\
 t &= (r_p)^{\frac{\gamma-1}{\gamma}} \quad t_1 = (r_p)^{\frac{\gamma-1}{\gamma}} \quad t_2 = (r_p)^{\frac{\gamma-1}{\gamma}} \\
 r_p &= \frac{P_2}{P_1} \quad r_{p1} = \frac{P_3}{P_4} \quad r_{p2} = \frac{P_5}{P_6} \\
 r_{p1} \cdot r_{p2} &= \frac{P_3}{P_4} \cdot \frac{P_5}{P_6} = \frac{P_3}{P_6} = \frac{P_2}{P_1} = r_p \rightarrow r_p = r_{p1} \cdot r_{p2} \\
 & \quad t = t_1 \cdot t_2 \checkmark \\
 w_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{1}{t_1} \beta - \frac{1}{t_2} \beta - t \right] \\
 \text{constraints} &\rightarrow \beta = \text{constant}, C_p, T_1 \rightarrow \text{known}, r_p \text{ or } t \text{ is known} \\
 w_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{1}{t_1} \beta - \frac{1}{t/t_1} \beta - t \right] \\
 w_{net} &= C_p T_1 \left[(2\beta + 1) - \frac{\beta}{t_1} - \frac{t_1 \beta}{t} - t \right]
 \end{aligned}$$

So, here let us start seeing let us redraw the diagram reconsider the diagram. And here let us see that this is for compressor this is T 2 by T 1, for high-pressure turbine this is T 3 by T 4 and for low pressure turbine this is T 5 by T 6. So, let us write this.

So, let t be the temperature ratio which is for compressor, let T_1 be the temperature ratio for high pressure turbine, let T_2 be the temperature ratio for low pressure turbine what we are going to achieve with this, we are going to achieve it this way. So, w_{net} formula we can directly replace it by this. Here what we will have is this way. Basically, we know r_p temperature T 2 by T 1 is equal to r_p bracket raise to gamma minus 1 upon gamma. Similarly, we know T 3 by T 4 is P_3 by P_4 bracket raise to gamma minus 1 upon gamma. Let us say that P_3 by P_4 is r_{p1} then that is equal to bracket raise to gamma minus 1 upon gamma. Then, we have T 5 by T 6 is equal to P_5 by P_6 bracket raise to gamma minus 1 upon gamma.

Let us say P_5 by P_6 as r_{p2} bracket raise to gamma minus 1 upon gamma. So, t is equal to from this, t is equal to r_p raise to gamma minus 1 upon gamma. So, from here t_1 is equal to r_{p1} bracket raise to gamma minus 1 upon gamma. From here we have t_2 is equal to r_{p2} bracket raise to gamma minus 1 upon gamma. But what is r_p ? r_p is equal to P_2 by P_1 . What is r_{p1} we wrote? r_{p1} is P_3 by P_4 . What is r_{p2} we wrote? We wrote it as P_5 by P_6 . Then what is r_p into r_{p2} ? It is P_3 by P_4 into P_5 by P_6 , but if we go back and see the diagram then P_4 is equal to P_5 this we should remember. So, if

P_4 is equal to P_5 this will cancel out, we will get it as P_3 divided by P_6 . But what is P_3 ? What is P_3 ? P_3 is equal to P_2 . P_6 is equal to P_1 . So, P_3 is equal to P_2 P_6 is equal to P_1 . So, this is rP . So, we get rP is equal to rP_1 into rP_2 .

So, if we put this in the formulations for temperature over here in this row we will get t is equal to t_1 into t_2 . We can prove this there is no problem, rP we will we can do this bracket raise to gamma minus 1 upon gamma, then bracket raise to gamma minus 1 upon gamma, bracket raise to gamma minus 1 upon gamma then we can get t is equal to t_1 into t_2 . So, this is how we can use this. That is why w_{net} is equal to $C_P T_1$ twice beta plus 1 minus T_3 by T_4 by T_3 , and T_4 by T_3 is 1 upon T_1 for us into beta minus T_6 by T_5 . This is 1 upon T_2 for us into beta minus T .

But we can consider that we were working with, we will assume one more thing over here that we are working along with other constraints as for constraints, total number of constraints as what we said beta constant, $C_P T_1$ known, similarly rP or t is known. So, if this constraint is there then t is a constant for this derivation, and then for this case we can get w_{net} is equal to $C_P T_1$ twice beta plus 1 minus 1 upon t_1 into beta. We can replace this T_2 by this expression which is T_2 is equal to 1 upon t by t_1 into beta minus t . So, w_{net} is equal to $C_P T_1$ twice beta plus 1 minus beta upon t_1 minus t_1 beta upon t minus t . So, this expression we have to remember. We have to keep it forward and then we can differentiate these w_{net} with respect to T_1 .

(Refer Slide Time: 49:07)

$$\begin{aligned}
 w_{net} &= C_P T_1 \left[(2\beta + 1) - \frac{\beta}{t_1} - \frac{\beta t_1}{t} - t \right] \\
 \frac{d}{dt_1} [w_{net}] &= 0 \rightarrow w_{net}|_{max} \\
 + \frac{\beta}{t_1^2} - \frac{\beta}{t} &= 0 \\
 t_1 &= \sqrt{\frac{\beta}{t}} \quad t_1, t_2 = t \\
 t_2 &= \sqrt{\frac{\beta}{t}} \\
 \boxed{t_1 = t_2 = \sqrt{\frac{\beta}{t}}} &\rightarrow w_{net}|_{max} \\
 w_{net}|_{max} &= C_P T_1 \left[(2\beta + 1) - \frac{\beta}{\sqrt{\frac{\beta}{t}}} - \frac{\beta}{\sqrt{\frac{\beta}{t}}} - t \right]
 \end{aligned}$$

So, from this expression w_{net} is equal to $C_p T_1 [2\beta + 1 - \beta \frac{T_1}{T_2}]$, minus we have $\beta \frac{T_1}{T_2}$ upon T_2 minus T_1 . Then for getting maximum w_{net} let us differentiate this with respect to T_2 and then we create it to 0, so that we can get w_{net} maximum. So, there are few term, if where we have to equate it to 0 $C_p T_1$ being constant it will go β is a constant, T_1 is a constant.

So, this term in the bracket would have zero derivative, this term will also have zero derivative. So, practically we have only two terms to get differentiated. So, we will have minus β into plus β upon T_2^2 square, plus β upon T_2^2 square. This is differentiation of first term, minus $\beta \frac{T_1}{T_2}$ is equal to 0. So, $\beta \frac{T_1}{T_2}$ would cancel out. So, we get T_2 is equal to square root of T_1 , T_2 is equal to square root of T_1 . But what we know? We know T_1 into T_2 is equal to T_1 . So, it leads to T_2 is also equal to square root of T_1 . So, it leads to T_2 equal to T_1 equal to square root of T_1 . So, this is the constraint for which we can get w_{net} maximum.

So, $w_{net max}$ is equal to $C_p T_1 [2\beta + 1 - \beta \frac{T_1}{T_2}]$ divided by square root of T_1 minus β divided by again square root of T_1 minus T_1 . So, this is the expression for maximum w_{net} . So, this is how we can arrive and the constraint for the (Refer Time: 51:56) based Brayton cycle power plant where we can get maximum w_{net} . So, the arrangement for intercooler and rest of the thing we will see in the next class.