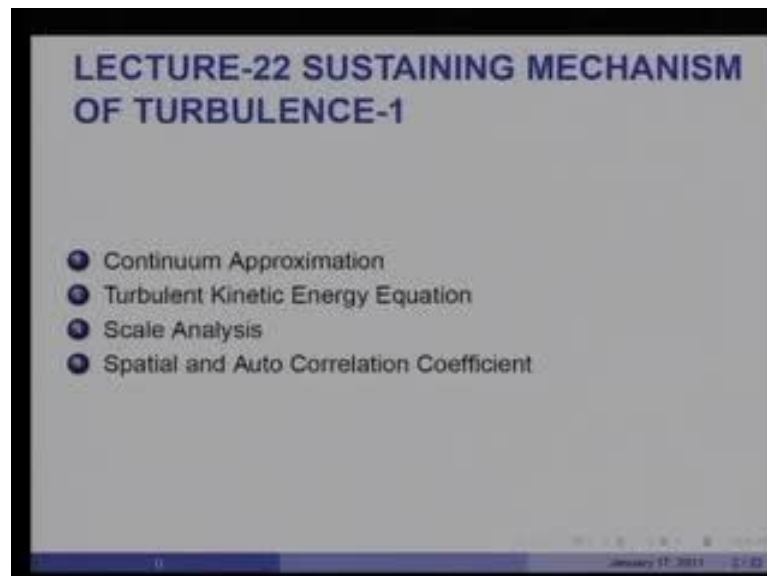


**Convective Heat and Mass Transfer**  
**Prof. A. W. Date**  
**Department of Mechanical Engineering**  
**Indian Institute of Technology, Bombay**

**Module No. # 01**  
**Lecture No. # 22A**  
**Sustaining Mechanism of Turbulence-I**

In the previous lecture, we made two important observations: one was the characteristics of turbulent flow significantly different from those of laminar flow and secondly, turbulence once generated - say, inside a pipe - somehow sustained itself right through the length of the pipe; **it does not die away** which means that there must be some pumping action, which feeds turbulence continuously to sustain itself, while viscosity is trying to kill it.

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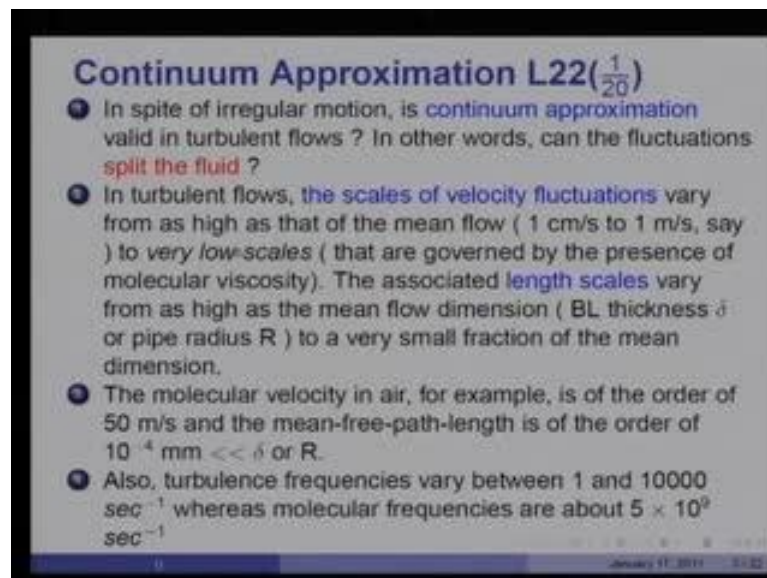


This lecture is the first of two lectures which will try and explain how turbulence sustains itself. We will do this firstly by some order - some magnitude analysis - by looking at and deriving the turbulent kinetic energy equation. Then, we will do scale analysis in

which we will introduce the idea of length and time scales of turbulent eddies through special and auto correlation coefficients.

The first question that arises is that turbulent fluctuations are extremely random and sharp as I showed you in the previous slide. Could it be that these fluctuations actually split the fluid? For example, if I had a paper in my hand and if I stretch it, subjecting it to very random motion, it is likely that the paper will split. Will the fluid split? That is a question, because of the stretching and torturing by the vortices. Can the fluid actually split? The question can be answered by considering orders or magnitude.

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**Continuum Approximation L22(1/20)**

- In spite of irregular motion, is **continuum approximation** valid in turbulent flows? In other words, can the fluctuations **split the fluid**?
- In turbulent flows, the **scales of velocity fluctuations** vary from as high as that of the mean flow ( 1 cm/s to 1 m/s, say ) to **very low-scales** ( that are governed by the presence of molecular viscosity). The associated **length scales** vary from as high as the mean flow dimension ( BL thickness  $\delta$  or pipe radius  $R$  ) to a very small fraction of the mean dimension.
- The molecular velocity in air, for example, is of the order of 50 m/s and the mean-free-path-length is of the order of  $10^{-4}$  mm  $\ll \delta$  or  $R$ .
- Also, turbulence frequencies vary between 1 and 10000  $\text{sec}^{-1}$  whereas molecular frequencies are about  $5 \times 10^9 \text{sec}^{-1}$

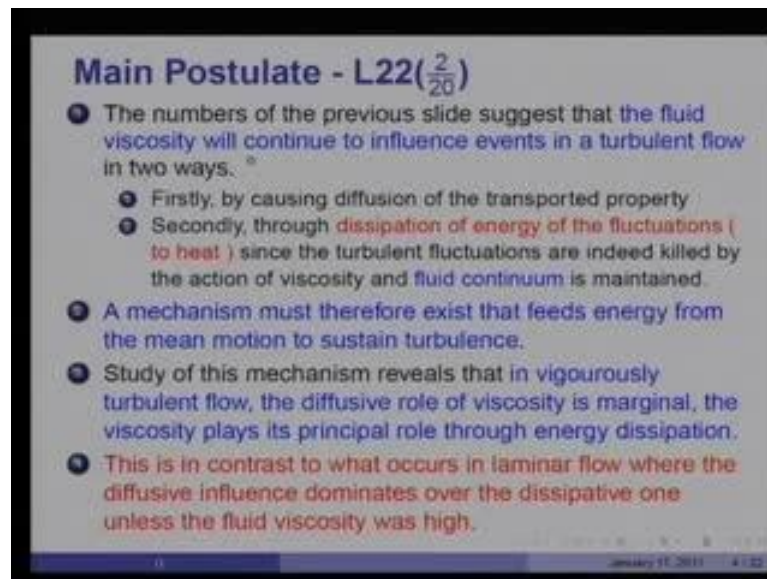
First of all, in turbulent flows, scales of velocity fluctuations vary from as high as that of the mean flow - say, in air, it could be anywhere up to 1 meter per second - to very low scales that are governed by the presence of molecular viscosity. The associated length scales would vary from as high as the mean flow dimension - say, boundary layer thickness or radius of a pipe - to a very small fraction of these quantities; the scales are associated with the turbulence fluid.

Let us ask ourselves what happens at the molecular level. For example, molecular velocity in air would be of the order of 50 meters per second, much greater than 1 meter per second. The mean-free-path-length would be of the order of  $10^{-4}$  millimeters of  $\delta$  and  $r$ ;  $\delta$  and  $r$  would be of the order of 1 millimeter to, let us say,

1 centimeter onwards. Velocity scales of a molecule are much greater than the mean flow velocity scales where the length scales are much smaller than the mean flow scales.

Similarly, in turbulence, frequencies of fluctuations are of the order of  $10^4$ , whereas the molecular frequencies are of the order of 5 billion; there is a vast difference between what happens at the molecular level and what happens in practical turbulence. You can see that this vast difference implies that the two must be completely uncorrelated. Turbulence behaves in its own way, molecules continue to behave in their own way, and therefore, we could safely assume that turbulence does not, in any way, destroy the basic characteristic of a fluid; the fluid will always remain as a continuum because of the presence of viscosity and no splits at the molecular level would occur. This is a very important observation about turbulence, to make progress with the theory of turbulence.

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**Main Postulate - L22( $\frac{2}{20}$ )**

- The numbers of the previous slide suggest that the fluid viscosity will continue to influence events in a turbulent flow in two ways. ◦
  - Firstly, by causing diffusion of the transported property
  - Secondly, through **dissipation of energy of the fluctuations ( to heat )** since the turbulent fluctuations are indeed killed by the action of viscosity and fluid continuum is maintained.
- A mechanism must therefore exist that feeds energy from the mean motion to sustain turbulence.
- Study of this mechanism reveals that in vigorously turbulent flow, the diffusive role of viscosity is marginal, the viscosity plays its principal role through energy dissipation.
- This is in contrast to what occurs in laminar flow where the **diffusive influence dominates over the dissipative one unless the fluid viscosity was high.**

The numbers of the previous slides suggest that the fluid viscosity will continue to influence events in turbulent flow in two ways. Firstly, by causing diffusion of the transported property - it can be a momentum, it can be temperature, or mass structure or anything; so, turbulence will cause because of viscosity causing diffusion. Secondly, through dissipation of energy of the fluctuations to heat, since turbulent fluctuations are indeed killed by the action of viscosity; therefore, the fluid continuum is maintained.

In other words, fluctuations are no longer allowed by viscosity to sustain themselves and they are simply killed by viscosity. Therefore, the molecular behavior remains completely unaffected by turbulence.

Having made this observation that the continuum is maintained, we now turn to the main point that a mechanism must therefore exist that feeds energy from the mean motion to sustain turbulence, while viscosity kills turbulence.

Study of this mechanism reveals that in vigorously turbulent flows, the diffusive role of viscosity is marginal - that is the first one. But the viscosity plays its principal role through energy dissipation - that is, the motions are killed and therefore, the kinetic energy is dissipated.

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**Instantaneous KE Eqn - 1 - L22( $\frac{3}{20}$ )**

The Eqn for IKE  $\hat{E} \equiv \hat{u}_i \hat{u}_i / 2$  is derived from the N-S Eqns by first multiplying instantaneous momentum equations by  $\hat{u}_i$  and then adding the three equations.

$$\rho \frac{D\hat{E}}{Dt} = -\frac{\partial}{\partial x_i} (\hat{p}\hat{u}_i) + \frac{\partial}{\partial x_i} (\hat{u}_i \hat{\tau}_{ij}) - \mu \hat{\Phi}_v$$

$$\hat{\tau}_{ij} = \mu \hat{S}_{ij} = \mu \left[ \frac{\partial \hat{u}_i}{\partial x_j} + \frac{\partial \hat{u}_j}{\partial x_i} \right]$$

$$\mu \hat{\Phi}_v = \hat{\tau}_{ij} \frac{\partial \hat{u}_i}{\partial x_j}$$

Now, this is in contrast to what occurs in laminar flow, where the diffusive influence dominates over the dissipative one unless the fluid viscosity was very high, as in oil flows. That is something we have already studied while considering laminar flows.

In order to explain whatever I have said through the Navier-Stokes equations, the first thing to appreciate is that the Navier-Stokes equation is written for an instantaneous velocity,  $\hat{u}$ , which is a valid description of turbulent flow. Because the continuum prevails, all derivatives can be resolved for the instantaneous velocities, and therefore, the equations are valid. So, this is a fundamental assumption on which we will proceed.

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For example, I can develop an equation for instantaneous kinetic energy. This is the equation for  $\hat{u}_i \hat{u}_i$  by 2 which essentially means  $u_1$  square plus  $u_2$  square plus  $u_3$  square divided by 2 is the instantaneous kinetic energy. How do I derive then? Recall that the instantaneous momentum equation is  $D \hat{u}_i$  by  $D t$  equal to minus  $d p$  cap by  $d x_i$  plus  $d \tau_{ji}$  cap  $d x_j$ . If I multiply this equation by  $\hat{u}_i$  – that is,  $\hat{u}_i$  and  $\hat{u}_i$  – throughout, then you will notice that this will be  $\rho$  times  $D \hat{u}_i \hat{u}_i$  divided by 2 by  $d t$  which is nothing but  $\rho D \hat{E}$  cap by  $D t$ . This will equal minus  $\hat{u}_i d p$  cap by  $d x_i$  plus  $\hat{u}_i d \tau_{ji}$  cap by  $d x_j$ . Therefore,  $\rho$  times  $D \hat{E}$  cap by  $D t$  would be equal to minus  $p$  absorbing  $\hat{u}$  inside by  $d x_i$  plus  $p$  cap  $d \hat{u}_i$   $d x_i$  plus again observing this inside  $d$  by  $d x_j$  of  $\hat{u}_i \tau_{ji}$  cap minus  $\tau_{ji} d \hat{u}_i$   $d x_j$  this is what it will be. But remember from continuity equation which also applies the instantaneous velocities this term will be 0 and that is why you get this equation, that is what I have written here  $D \hat{E}$  by  $D t$  equal to  $d$  by  $d x_i$   $p$  by  $\hat{u}_i$  plus  $d$  by  $d x_i$  of  $\hat{u}_j d \hat{u}_i$   $d x_j$  minus  $\mu \phi v$ , this is  $\mu \phi v$  the viscous dissipation term.

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**Instantaneous KE Eqn - 1 - L22( $\frac{3}{20}$ )**

The Eqn for IKE  $\hat{E} \equiv \hat{u}_i \hat{u}_i / 2$  is derived from the N-S Eqns by first multiplying instantaneous momentum equations by  $\hat{u}_i$  and then adding the three equations.

$$\rho \frac{D\hat{E}}{Dt} = -\frac{\partial}{\partial x_i} (\hat{p}\hat{u}_i) + \frac{\partial}{\partial x_i} (\hat{u}_i \hat{\tau}_{ij}) - \mu \hat{\Phi}_v$$
$$\hat{\tau}_{ij} = \mu \hat{S}_{ij} = \mu \left[ \frac{\partial \hat{u}_i}{\partial x_j} + \frac{\partial \hat{u}_j}{\partial x_i} \right]$$
$$\mu \hat{\Phi}_v = \hat{\tau}_{ij} \frac{\partial \hat{u}_i}{\partial x_j}$$

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Essentially, what the equation says is the rate of change of instantaneous kinetic energy is the rate net rate of work done by pressure forces plus the net rate of work done by the stresses  $\tau_{ij} = \mu S_{ij}$ ;  $S_{ij}$  is the strength rate  $d u_i / d x_j$  plus  $d u_j / d x_i$  minus viscous dissipation.

So, turbulent energy increases because of these terms, which can be positive or negative does not matter, but when they are positive it increases but  $\mu \Phi_v$  by definition would being positive would always decrease instantaneous kinetic energy. So, viscosity plays the role of destroying instantaneous kinetic energy.

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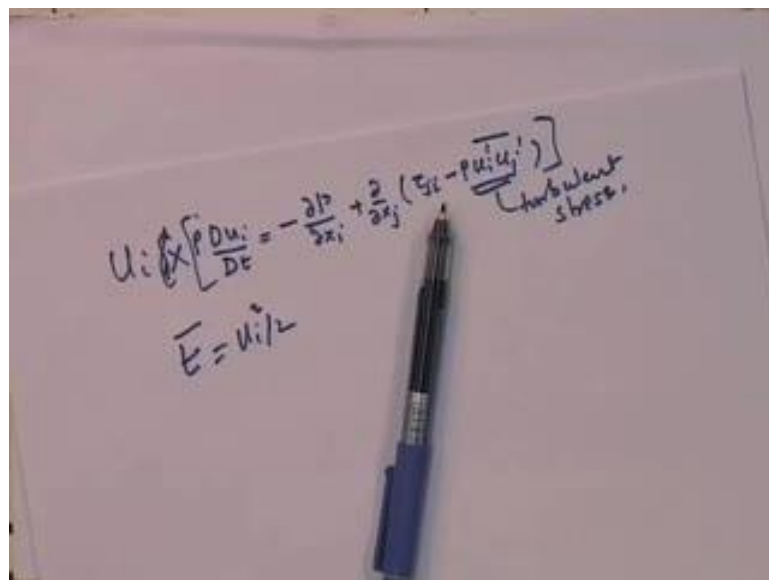
**Mean KE Eqn - 2 - L22( $\frac{4}{20}$ )**

The Eqn for MKE ( $E = \overline{u_i u_i} / 2$ ) is derived from time-averaged N-S Eqns by first multiplying by  $u_i$  and then adding the three equations.

$$\rho \frac{DE}{Dt} = \underbrace{-\frac{\partial}{\partial x_i} (\rho u_i)}_{(a)} + \underbrace{\frac{\partial}{\partial x_j} (\tau_{ji} u_i)}_{(c)} + \underbrace{\frac{\partial}{\partial x_j} (-\rho \overline{u_i' u_j'} u_i)}_{(d)} - \underbrace{\mu \Phi_v}_{(e)} - \underbrace{(-\rho \overline{u_i' u_j'} \frac{\partial u_i}{\partial x_j})}_{(f)}$$

The total rate of change of mean E ( a ) = the rate of work done by pressure forces ( b ) + by viscous stresses ( c ) + by turbulent stresses ( d ) - the rate of energy dissipated by viscous action ( e ) - the rate of energy transferred to turbulence by the mean motion ( f ).

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I do the same thing now to derive mean kinetic energy equation, but in this case what I will do is I will begin by writing the RANS equations where  $D u_i / D t$  equal to minus  $d p / d x_i$  plus  $d$  by  $d x_j$  of  $\tau_{ji}$  minus  $\rho u_i' u_j' d x_j$  plus the body forces, which I am presently in ignoring and these where the turbulence stresses.

So, if I multiply this equation throughout by  $u_i$ , I would get again an equation for  $u_i$  square by two which is the mean kinetic energy equation; here is that equation.

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**Mean KE Eqn - 2 - L22( $\frac{4}{20}$ )**

The Eqn for MKE ( $E \equiv u_i u_i / 2$ ) is derived from time-averaged N-S Eqns by first multiplying by  $u_i$  and then adding the three equations.

$$\rho \frac{DE}{Dt} = \underbrace{-\frac{\partial}{\partial x_i}(\rho u_i)}_{(a)} + \underbrace{\frac{\partial}{\partial x_j}(\tau_{ij} u_i)}_{(c)} + \underbrace{\frac{\partial}{\partial x_j}(-\rho \overline{u_i' u_j'} u_i)}_{(d)} - \underbrace{\mu \Phi_v}_{(e)} - \underbrace{(-\rho \overline{u_i' u_j'} \frac{\partial u_i}{\partial x_j})}_{(f)}$$

The total rate of change of mean E ( a ) = the rate of work done by pressure forces ( b ) + by viscous stresses ( c ) + by turbulent stresses ( d ) - the rate of energy dissipated by viscous action ( e ) - the rate of energy transferred to turbulence by the mean motion ( f ).

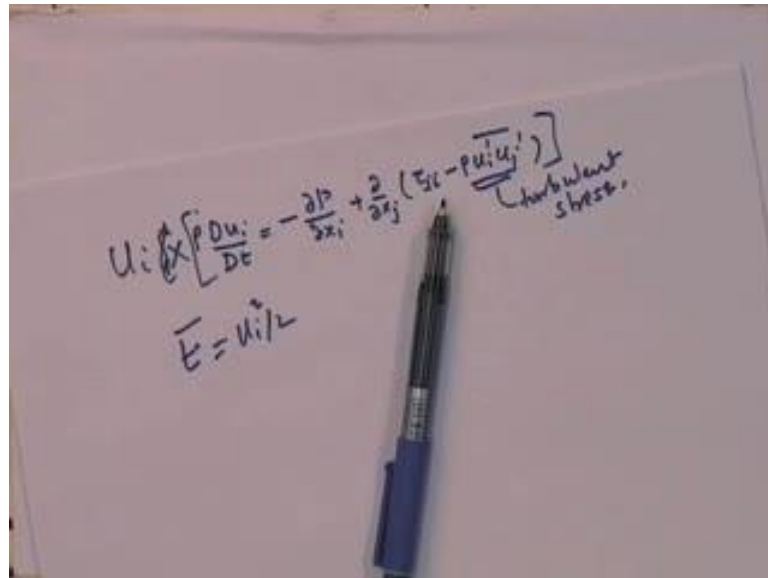
It looks very similar in many terms - this is the pressure work term, this is the work done by laminar stress, this is the work done by turbulence stress, and this would be the viscous dissipation due to mean velocity gradients and minus minus turbulent stress multiplied by  $du_i$  by  $dx_j$  the mean velocity gradient.

The equation essentially says - that the rate of change of mean kinetic energy E is equal to the rate of work done by pressure forces, rate of work done by viscous stresses, rate of work done by turbulence stresses; that is termed a minus the rate of energy dissipated by viscous action and minus this is the most important term f.

That the rate of energy transferred to turbulence by mean motion  $du_i dx_j$ ; now why do I say - rate of energy transferred to turbulence? That you will appreciate from the next slide.



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**Turbulent KE Eqn - 3 - L22( $\frac{5}{20}$ )**  
 The Eqn for TKE ( $e = \overline{u_i' u_i' / 2}$ ) is derived by first time-averaging Eqn for IKE ( $\bar{E}$ ).

$$\rho \frac{D(E + e)}{Dt} + \frac{\partial}{\partial x_j} (u_j \rho \overline{u_i' u_i'}) + \frac{\partial}{\partial x_j} (\rho \overline{u_j' u_i' u_i' / 2}) =$$

$$- \frac{\partial}{\partial x_i} (\rho u_i + \overline{p' u_i'}) + \frac{\partial}{\partial x_j} (\overline{\tau_{ij} u_i} + \overline{\tau_{ij}' u_i'}) - \overline{\tau_{ij} \frac{\partial u_i}{\partial x_j}} - \overline{\tau_{ij}' \frac{\partial u_i'}{\partial x_j}}$$

Then, the Eqn for MKE ( $E$ ) is subtracted

$$\rho \frac{De}{Dt} = \underbrace{- \frac{\partial}{\partial x_j} \overline{u_j' (\rho + \rho u_i' u_i' / 2)}}_{(A)} + \underbrace{(- \overline{\rho u_i' u_j' \frac{\partial u_i}{\partial x_j}})}_{(C)}$$

$$+ \underbrace{\frac{\partial}{\partial x_j} (\overline{u_j' \tau_{ij}})}_{(D)} - \underbrace{\overline{\tau_{ij}' \frac{\partial u_i'}{\partial x_j}}}_{(E)} \text{ (next slide)}$$

Now, I want to derive an equation for the turbulent kinetic energy, which is  $u_i$  dash  $u_i$  dash time average divided by 2; this is the turbulent kinetic energy; it is derived by first time averaging the instantaneous kinetic energy equation; in other words **this equation i time average each term then** time averaging of this term would give me mean E plus turbulent e and so on **and so forth** and the equation would look as I have shown here

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So, from this equation, which is time average form of the instantaneous kinetic energy equation, I now subtract the mean kinetic energy equation which I derived on the previous slide; I subtract this equation from this equation, then you will see that I would get an equation for row D e by d t equal to minus d by d x j u i j dash p dash plus this plus minus rho u i j prime u j prime d u i d x j and then this term and this term.

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**Mean KE Eqn - 2 - L22( $\frac{4}{20}$ )**  
 The Eqn for MKE ( $E \equiv \overline{u_i u_i} / 2$ ) is derived from time-averaged N-S Eqns by first multiplying by  $u_i$  and then adding the three equations.

$$\rho \frac{DE}{Dt} = -\frac{\partial}{\partial x_i} (\rho u_i) + \frac{\partial}{\partial x_j} (\tau_{ij} u_i) + \frac{\partial}{\partial x_j} (-\rho \overline{u_i' u_j'} u_i) - \mu \Phi_v - (-\rho \overline{u_i' u_j'} \frac{\partial u_i}{\partial x_j})$$

(a) (b) (c) (d) (e) (f)

The total rate of change of mean E ( a ) = the rate of work done by pressure forces ( b ) + by viscous stresses ( c ) + by turbulent stresses ( d ) - the rate of energy dissipated by viscous action ( e ) - the rate of energy transferred to turbulence by the mean motion ( f ).

Notice that the C term here in the turbulent kinetic energy equation has exactly the opposite sign of the f term, they are both identical terms. But in one case you have a negative sign here and this is the positive sign here **you have the positive sign**

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### Comments on TKE - 1 - L22( $\frac{6}{20}$ )

The rate of change of TKE  $e$  ( A ) =

- + the rate of (convective) diffusion of total fluctuating pressure energy  $(\rho' - \rho u_i' u_i' / 2)$  by velocity fluctuation ( B )
- + the rate of energy is transferred from mean motion to turbulence by the turbulent stresses ( C )
- + the rate of work done by viscous turbulent stresses ( D )
- the rate of dissipation of energy by the turbulent motion ( E ).

- 1 Egn of MKE ( E ) shows that E is lost in two ways
  - 1 Firstly, by viscous dissipation ( term e )
  - 2 Secondly, by ( term f ) which appears as a positive contributor to TKE via ( term C ). Hence, term C is called *Production or Generation term*
- 2 In a laminar flow, E is directly dissipated into heat. In a turbulent flow, E is *first transferred to sustain turbulence* before finally *dissipating to heat through ( term E )*

In otherwords, what is a law of kinetic energy? It turns out to be gain of turbulent kinetic energy and what do these terms represent? Well that is what is shown on the left on the next slide.

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### Turbulent KE Egn - 3 - L22( $\frac{5}{20}$ )

The Egn for TKE ( $e = \overline{u_i' u_i' / 2}$ ) is derived by first time-averaging Egn for IKE (  $\dot{E}$  ).

$$\rho \frac{D(E + e)}{Dt} + \frac{\partial}{\partial x_j} (u_j \rho \overline{u_i' u_i'}) + \frac{\partial}{\partial x_j} (\rho \overline{u_j' u_i' u_i' / 2}) =$$

$$- \frac{\partial}{\partial x_i} (\rho u_i + \rho' u_i') + \frac{\partial}{\partial x_j} (\tau_{ij} u_i + \overline{\tau_{ij}' u_i'}) - \tau_{ij} \frac{\partial u_i}{\partial x_j} - \overline{\tau_{ij}' \frac{\partial u_i'}{\partial x_j}}$$

Then, the Egn for MKE ( E ) is subtracted

$$\rho \frac{De}{Dt} = \underbrace{- \frac{\partial}{\partial x_j} \overline{u_j (\rho' + \rho u_i' u_i' / 2)}}_{(B)} + \underbrace{(- \rho \overline{u_i' u_i'} \frac{\partial u_i}{\partial x_j})}_{(C)}$$

$$+ \underbrace{\frac{\partial}{\partial x_j} (\overline{u_j' \tau_{ij}'})}_{(D)} - \underbrace{\overline{\tau_{ij}' \frac{\partial u_i'}{\partial x_j}}}_{(E)} \quad \text{( next slide )}$$

Rate of change of turbulent kinetic energy A which is the left hand side equals the rate of convective diffusion of total fluctuating pressure by velocity fluctuations to go back, this is the term  $\rho$  dash plus  $\rho u_i$  squared by 2 is the total fluctuating pressure, this is the

static pressure, this is the dynamic pressure, and therefore the total term represents total fluctuating pressure and its diffusion due to velocity  $u_j$

plus the rate of energy transferred from mean motion to turbulence by turbulence stresses which is the term C plus by the turbulence stresses; it is the energy transferred to turbulence plus the rate of work done by viscous turbulent stresses this is the  $u_j \tau_{ij}$  and I explain what the definition of  $\tau_{ij}$  is, so that is the diffusion again of the stress tau or the stress work due to turbulent stress.

And finally minus the rate of dissipation of energy by turbulent motion and that is the term E here is a product of fluctuating stress multiplied by fluctuating velocity gradient and therefore this would be very much like the  $\mu \phi_v$  term in which the  $\phi_v$  would now, we form from fluctuating velocity gradients.

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**Mean KE Eqn - 2 - L22( $\frac{4}{20}$ )**  
 The Eqn for MKE ( $E = u_i u_i / 2$ ) is derived from time-averaged N-S Eqns by first multiplying by  $u_i$  and then adding the three equations.

$$\rho \frac{DE}{Dt} = \underbrace{-\frac{\partial}{\partial x_i} (\rho u_i)}_{(a)} + \underbrace{\frac{\partial}{\partial x_j} (\tau_{ij} u_i)}_{(c)} + \underbrace{\frac{\partial}{\partial x_j} (-\rho \overline{u_i u_j} u_i)}_{(d)} - \underbrace{\mu \Phi_v}_{(e)} - \underbrace{(-\rho \overline{u_i u_j} \frac{\partial u_i}{\partial x_j})}_{(f)}$$

The total rate of change of mean E ( a ) = the rate of work done by pressure forces ( b ) + by viscous stresses ( c ) + by turbulent stresses ( d ) - the rate of energy dissipated by viscous action ( e ) - the rate of energy transferred to turbulence by the mean motion ( f ).

Equation for mean kinetic energy shows that E is lost in two ways- firstly by viscous dissipation- term e, the mean energy is lost by viscous dissipation and secondly, by work done by stresses on mean velocity gradients and E is lost in two ways firstly by viscous dissipation term e and secondly by term f which appears as a positive contributor to turbulent kinetic energy C a term C.

Hence term C is called the production or generation term, because it makes a positive contribution to rate of change of E. In laminar flow, the mean energy is directly

dissipated into heat. In turbulent flow we can say that mean energy is first transferred to sustain turbulence before it is finally dissipated to heat through term E.

So, the first mean kinetic energy goes to turbulence through some C which increases that, but turbulent kinetic energy also decreases due to dissipation to heat before finally.

So, this first and before seems to **be there is** have a time lag or a space lag in a fluid flow whichever way we **is to** look at it; so it is not an instance process, it happens perhaps in stages. Now, to explain that we will have to make some further explorations into turbulence which I will take up in the slides to flow as well as the next lecture.

So, remember mean energy is lost in two ways first by viscous dissipation and secondly by transferred to turbulence.

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**Comments on TKE - 2 - L22(7/20)**

- Besides dissipation, MKE (E) and TKE (e) experiences convective-diffusion of energy through terms b, c, d, B and D. These terms merely redistribute ( spatially ) energy but make zero net contribution to the integral energy balance as shown below.
- If the turbulent flow bounded by walls (  $u_i = u_i' = 0$  ) or by a wall and a symmetry plane (  $\tau_{ij} = \tau_{ij}' = 0$  ) is considered and equation for TKE is integrated over flow cross-section

$$\rho \frac{D}{Dt} \int_V e dV = \int_V \left\{ (-\rho \overline{u_i' u_j'}) \frac{\partial u_i}{\partial x_j} - (\tau_{ij}' \frac{\partial u_i'}{\partial x_j}) \right\} dV$$

Net change = Net ( Production - Dissipation )

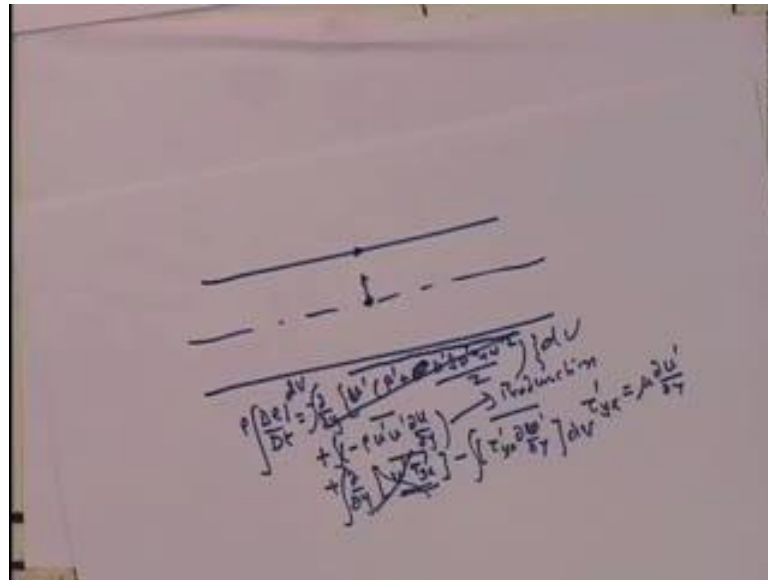
- Net change > 0 when Production > Dissipation and vice-versa. The near-balance represents Transition

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Turbulent kinetic energy on the other hand is sustained because of this transfer from mean energy from the mean energy and secondly it is destroyed by the fluctuating counter part of  $\mu \phi \nu$  which we called turbulent dissipation.

So, beside dissipation, transfer mean kinetic energy and turbulent kinetic energy experience convective-diffusion of energy through terms b, c, d, B and D. These terms simply redistribute energy specially but make no contribution or zero contribution to integral energy balance as we would see now.

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So, for example, consider **let us say** flow between two parallel plates with an access of symmetry and I shall now integrate- I will now consider the kinetic energy equation, so it will look like  $\rho Dk/Dt = \dots$  and assuming that the gradients of all terms are much bigger in y direction then they are in any other direction.

We would write  $d/dy$  minus  $d/dy$  of  $v^2$  into  $p$  plus  $u^2$  plus  $v^2$  plus  $w^2$  by 2, which is nothing but the kinetic energy.

Minus or the plus minus  $\rho u v$  into  $du/dy$  plus  $d/dy$  of  $v$  into  $\tau_{yx}$  minus  $\tau_{yx}$  by  $du/dy$  - let us say where  $\tau_{yx}$  is  $\mu$  times  $du/dy$ .

So, now if I integrate this from 0 to  $i$  that is over the volume of the channel; then you will notice that this term will have  $v$  dash at the wall and  $v$  dash at the at the access symmetry and therefore both of them would simply vanish.

So, integral of that  $dv$  is simply 0, integral of this term will survive, which we said was production term; this, like this term will also vanish integral whereas this term integral of  $dv$  will survive, because it is a product of velocity gradient and the fluctuating stress.

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**Comments on TKE - 2 - L22( $\frac{7}{20}$ )**

- Besides dissipation, MKE (E) and TKE (e) experiences convective-diffusion of energy through terms b, c, d, B and D. These terms merely redistribute ( spatially ) energy but make zero net contribution to the integral energy balance as shown below.
- If the turbulent flow bounded by walls (  $u_i = u_i' = 0$  ) or by a wall and a symmetry plane (  $\tau_{ij} = \tau_{ij}' = 0$  ) is considered and equation for TKE is integrated over flow cross-section

$$\rho \frac{D}{Dt} \int_V e dV = \int_V \left\{ (-\rho \overline{u_i' u_j'}) \frac{\partial u_i}{\partial x_j} - (\tau_{ij}' \frac{\partial u_i'}{\partial x_j}) \right\} dV$$

Net change = Net ( Production - Dissipation )

- Net change > 0 when Production > Dissipation and vice-versa. The near-balance represents Transition

That is what I show here, so by wall and symmetry plane is considered, so if the turbulent energy is bounded by wall where the velocity fluctuations are 0 because of no slip or by wall and symmetry plane  $\tau_{ij} = \tau_{ij}' = 0$  is considered and equation for turbulent kinetic energy is integrated over the cross section.

Then we would have  $\rho \frac{D}{Dt} \int_V e dV = \text{net production} - \text{net dissipation}$ , what this tells us this following? Is that the net change in kinetic energy over a cross section would be positive when net production exceeds net dissipation.

On the other hand, if the net dissipation exceeded net production, then e will simply die out the kinetic energy will be simply vanish; when there is near equilibrium that is production is very close to dissipation we would have transition.

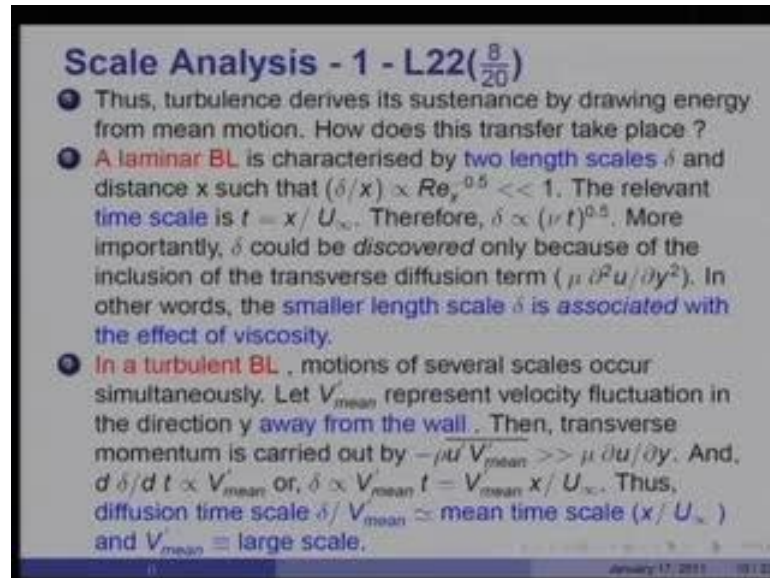
The equation then sets the conditions for sustenance of turbulence, that the net production over a cross section must exceed the net dissipation then the turbulence would be sustained at every cross section downstream.

There are situations in fact, where even in a channel flow, a turbulence when generated can be made to relaminarize, one such possibility is to have a tube which is coiling around a steam with very high turbulent velocity fluctuations,



so that the dissipation term begins to dominate over the production term and the turbulent could then relaminarize inside a pipe, but it is a coiled pipe very very special case not routine encountered in practical engineering.

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When the production and dissipation are near balance, you would expect a kind of flow in which **for a while** the flow is laminar when dissipation over takes production and then the laminar flow will become unstable to produce in which production term it will take over from dissipation and little patches of turbulence and little patches of laminar fluid would appear in a flow and that is precisely what we called the transitional regime.

Thus, the turbulence derives this sustenance by drawing energy from the mean motions. Now, how does this transfer actually take place? That is what we want to ask, how does this transfer take place?

Now, to understand that, we must introduce the ideas of scale; so in a laminar boundary layer, for example, it is characterized by two length scales: one is delta, which is much much smaller, the transverse dimension is much much smaller than the stream wise distance  $x$  and that gives us delta by  $x$  has being proportional to Reynolds  $x$  to the minus 0.5 and this is usually much much smaller than one.

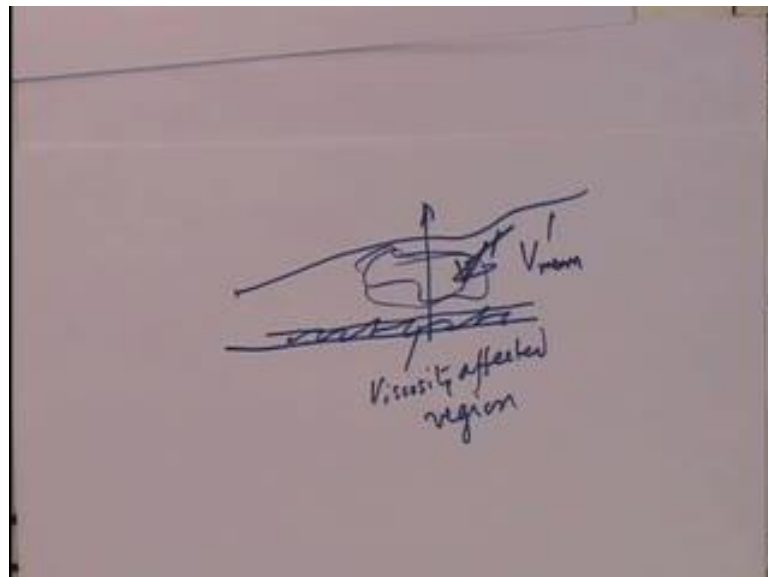
So, the relevant time scale however is  $t$  equal to  $x$  divided by  $U_\infty$  and therefore, if I substitute that in here I would say delta is proportional to  $\nu t$  raise to minus 0.5, where

$\nu$  is a small number. Therefore,  $\delta$  would be a very very small quantity again as shown earlier.

More importantly, if you remember  $\delta$  could be discovered only because of the inclusion of the transverse diffusion term  $\mu \frac{d^2 u}{dy^2}$  in the laminar boundary layer equation.

One way to interpret this fact is to say the smaller length scale  $\delta$  is associated with the effect of viscosity as shown here.

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What about turbulent flow? Now, in a turbulent flow- turbulent boundary layer very close to the wall of course you have viscosity dominates- viscosity affected region, but the outer parts are certainly almost independent of the effects of viscosity, the laminar fluid viscosity.

So, in this region, if I were to say- what brings about transverse of momentum? Well, let us say- it is a representative velocity fluctuation  $V'$ ; mean, let us say- I call it  $V'$  mean as the representative fluctuation which brings about transverse momentum.

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**Scale Analysis - 1 - L22( $\frac{8}{20}$ )**

- Thus, turbulence derives its sustenance by drawing energy from mean motion. How does this transfer take place?
- A laminar BL is characterised by two length scales  $\delta$  and distance  $x$  such that  $(\delta/x) \propto Re_x^{-0.5} \ll 1$ . The relevant time scale is  $t = x/U_\infty$ . Therefore,  $\delta \propto (\nu t)^{0.5}$ . More importantly,  $\delta$  could be discovered only because of the inclusion of the transverse diffusion term ( $\mu \partial^2 u / \partial y^2$ ). In other words, the smaller length scale  $\delta$  is associated with the effect of viscosity.
- In a turbulent BL, motions of several scales occur simultaneously. Let  $V_{mean}$  represent velocity fluctuation in the direction  $y$  away from the wall. Then, transverse momentum is carried out by  $-\rho \overline{u' V_{mean}'} \gg \mu \partial u / \partial y$ . And,  $d\delta/dt \propto V_{mean}$  or,  $\delta \propto V_{mean} t = V_{mean} x / U_\infty$ . Thus, diffusion time scale  $\delta / V_{mean} \approx$  mean time scale  $(x / U_\infty)$  and  $V_{mean} =$  large scale.

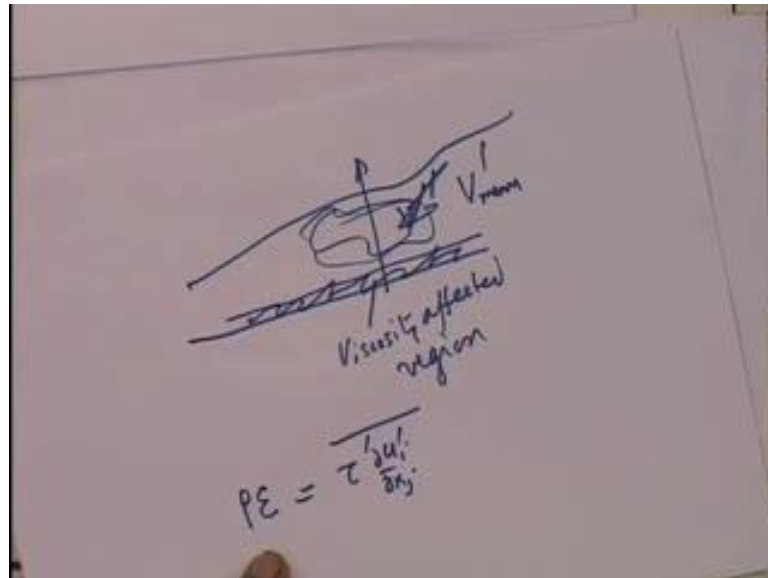
Then, you will see in turbulent boundary layer, motions of several scales occur simultaneously and we are going to choose  $V$  dash mean as the representative velocity fluctuation in the direction of  $y$  away from the wall.

Then, the transverse momentum is carried out by minus rho  $u$  dash  $V$  dash time average which would be much much greater than  $\mu \partial u / \partial y$  and,  $d\delta/dt$ , that is the rate of growth of turbulent boundary layer thickness would be proportional to  $V$  dash mean essentially and therefore  $\delta$  would be proportional to  $V$  dash mean by  $t$  in multiplied by  $t$  but  $t$  as we observed would be  $x$  divided by  $U$  infinity even in a turbulent flow and therefore  $V$  dash  $x$  by  $U$  infinity, this would be  $V$  dash mean into  $x$  multiplied by  $(\ )$

Thus, the diffusion time scale,  $\delta$  by  $V$  dash mean would be approximately equal to mean time scale  $x$  by  $U$  infinity; this is very interesting, the  $\delta$  is a small length scale;  $V$  dash mean is the representative fluctuating velocity in the turbulent core or the fully turbulent path of the boundary layer

and the time scale associated with it is exactly same as the mean time scale and therefore, we shall regard  $V$  dash mean as a representative of the large scale motion; this is a very important idea that  $V$  dash mean would be taken as the representative of the large scale motion.

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Recall that the dissipation process,  $\mu \tau \frac{\partial u_i}{\partial x_j}$  - this was the dissipation process; this I will represent as a  $\rho$  times  $\epsilon$ , where  $\epsilon$  is called the dissipation rate of kinetic energy.

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**Scale Analysis - 2 - L22 ( $\frac{9}{20}$ )**

- Recall that the dissipation process ( $\rho \epsilon = \tau \frac{\partial u_i}{\partial x_j}$ ) essentially *kills or smoothens out* velocity fluctuations due to action of viscosity and  $l_v \ll l_{mean}$  and  $t_v \ll t_{mean}$ .
- At such very small scales, turbulent fluctuations in all three directions could be considered **statistically equal**. That is,  $\overline{u'^2} = \overline{v'^2} = \overline{w'^2}$  and their spatial variations are also small.
- Such a small scale turbulence structure is called **homogeneous and isotropic**. It is characterised in association with  $\epsilon$  by **Kolmogorov Scales**.

$$u'_i = v'_i = w'_i = (\nu \epsilon)^{0.25} \text{ (velocity scale)}$$

$$t_v = \left(\frac{\nu}{\epsilon}\right)^{0.50} \text{ (time scale)} \quad l_v = \left(\frac{\nu^3}{\epsilon}\right)^{0.25} \text{ (length scale)}$$

$$Re_{t,v} = \frac{(l_v)_{t,v}}{\nu} = 1 \ll Re_{t,mean} = \frac{(l_v)_{mean}}{\nu} \approx O(100)$$

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Now, this actually kills turbulence-  $\rho$  into  $\epsilon$  actually kills turbulence and smoothens out velocity fluctuations due to action of viscosity and therefore, the length scales associated with it would be much much smaller than the mean length scales and

the time scales associated with it will also be much much smaller than the mean time scales.

At such very small scales of motion, turbulent fluctuations in all 3 dimensions- directions can be taken to be essentially statistically equal that is  $u' \text{ square}$  is equal to  $v' \text{ square}$  is equal to  $w' \text{ square}$ ,

as well as the gradients will be 0. In another word, the spatial variations will also be very small; when special variations of fluctuating a time average quantities are 0 or **this** when the spatial gradients of the fluctuating quantities time average fluctuating quantities are 0, we say the structure is homogeneous and when the components of the velocity fluctuations are equal, we say it is isotropic and then therefore, we would essentially have where the viscosity plays its dominant role we would have essentially a homogeneous and isotropic turbulence structure.

It is characterized in association with epsilon by what are called Kolmogorov scales; so Kolmogorov use the idea, that is very small scale motions are essentially characterized by the effect of viscosity and by the effect of a turbulent dissipation and he brought in the quantity epsilon to represent the velocity scales of the associated with dissipation process as new epsilon raise to 0.25- this is dimensionally correct.

Similarly, the time scale  $t \text{ epsilon}$  was taken as  $\nu \text{ by epsilon raise to } 0.5$  and  $l \text{ by } l \text{ sub epsilon}$  was taken as  $\nu \text{ cube by epsilon raise to } 0.25$  as the length scale.

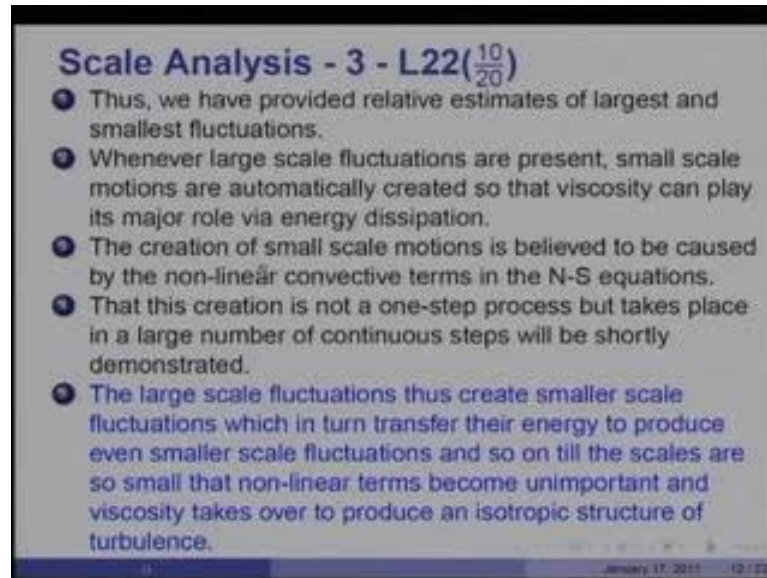
So, if I form Reynolds number based on length scale, velocity scale- I will get  $l \text{ v dash}$  epsilon divided by  $\nu$  and let us say- it is of the order of 1.

Then it follows that it would be much much smaller than  $l \text{ V dash}$  mean by  $\nu$ , which is the large scale motion and large scale length scale and that would be of the order of 100 or even more.

The Reynolds number associated with dissipative length scales and velocity fluctuation scales is much much smaller than the mean Reynolds number form from mean length scale and fluctuating velocity scales, which would be of the order of 100 or more.

Thus, we have provided relative estimates of the largest and the smallest scales; so largest scales belong to the mean dimensions, mean motion, where is the smallest one belonging to the dissipation scales.

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**Scale Analysis - 3 - L22( $\frac{10}{20}$ )**

- Thus, we have provided relative estimates of largest and smallest fluctuations.
- Whenever large scale fluctuations are present, small scale motions are automatically created so that viscosity can play its major role via energy dissipation.
- The creation of small scale motions is believed to be caused by the non-linear convective terms in the N-S equations.
- That this creation is not a one-step process but takes place in a large number of continuous steps will be shortly demonstrated.
- The large scale fluctuations thus create smaller scale fluctuations which in turn transfer their energy to produce even smaller scale fluctuations and so on till the scales are so small that non-linear terms become unimportant and viscosity takes over to produce an isotropic structure of turbulence.

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The most important to cut the story short, the most important aspect of it is that whenever large scale fluctuations are presents small scale motions are automatically created so that viscosity can play its major role via energy dissipation.

The creation of this small scale motions is believed to be cause by the non-linear convective terms in the Navier-Stokes equations. That this creation of smaller and smaller scales motion is not a one-step process but takes place in a large number of continuous steps will be demonstrated shortly- it can be done in more than one ways and I will try to do it in as simpler manner as possible.

The large scale fluctuations thus creates smaller scale fluctuations, which in turn transfer their energy to produce even smaller scale fluctuations and so on till the scales are so small that non-linear terms become unimportant and viscosity takes over to produce an isotropic structure of turbulence I mean that is the story that is the story of sustains of turbulence.

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**Spatial Correlation - 1 - L22(<sup>11</sup>/<sub>20</sub>)**

In turbulence literature, the idea of scales is often expressed through the notion of an *eddy*. Whenever a fluctuation occurs, it can be expected to influence events over a zone that extends both *spatially* and *in time*. The *eddy*, notionally represents the *size of this zone*.




Figure: Here  $\lambda_x = l_x$  and  $\lambda_y = l_y$

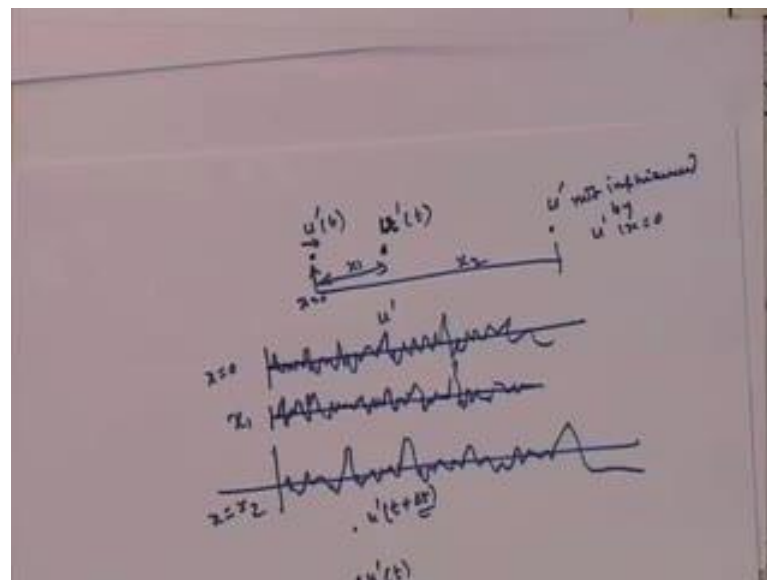
Consider two points at positions  $r_1$  and  $r_2$  with  $\vec{r} = r_2 - r_1$ . Then, let  $u_i$  at  $r_1(x_1, x_2, x_3)$  and  $u_j$  at  $r_2(x_1 + r, x_2, x_3)$  be the velocity fluctuations at the *same time instant*.

Define Spatial correlation coefficient

$$R_{ij} = \frac{B_{ij}}{\sqrt{B_{ii}} \sqrt{B_{jj}}} \quad \text{---} \quad B_{ij} = \overline{u_i u_j}$$

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Now, in order to explain these ideas little further, it is customary to introduce the idea of a turbulence eddy; now you can imagine that- let us say I have 2 points in the flow and I consider- let us say,  $u'$  dash here and  $v'$  dash here at the same time  $t$  or let us say to begin with  $u'$  dash and  $u'$  dash itself, I consider the fluctuation in the  $x$  direction at the same time instant at two different points separated by a distance.

Now, we all know that if I a fluctuation at this point will influence this point if they were close to each other, so the fluctuation here would be influenced by fluctuation here.

However if this point was sufficiently far away, say here, then the  $u'$  here will not be influenced by  $u'$  at  $x$  equal to 0- let us say this is at  $x$  equal to 0 and this is the separation distance  $x_1$  and this is definition distance  $x_2$  let us say.

So, at this point, it is unlikely that  $u'$  will sense what  $u'$  at  $x$  equal to 0 is doing; in effect if I have to look at them in time at  $x$  equal to 0 then the fluctuations  $u'$  would at  $x$  equal to 0 will look like that.

At  $x$  equal to  $x_2$  let us say, they would look absolutely different and you can say that this form of  $u'$  at  $x$  equal to 0 which is completely uncorrelated with what is happening at large distance.

What about intermediate distances? Here we can expect supposing  $x_1$ , which is very close to  $x$  equal to 0- I can explain something like that; marginally, good correlation at least it will look somewhat similar, but at very large distance it could be absolutely very different,

I can say therefore **and of course** if I took this second point to merge with this, of course I will reproduce the same pattern, which means a complete correlation exist between the two points when they collapse on one another; a complete correlation exist when they are very very far, but a moderate correlation can exist for in between distances

and of course we do not know what that distance  $x_2$  will be in real turbulent flow and that is what we wish to find out; this is spatial influence. but now if I take for example,  $u'$  at time  $t$  and  $u'$  at say another time  $t$  equal to  $t$  plus  $\Delta t$  separated by a distance  $\Delta t$  **time distant  $\Delta t$**  then a similar situation will arise.



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**Spatial Correlation - 1 - L22(<sup>11</sup>/<sub>20</sub>)**

In turbulence literature, the idea of scales is often expressed through the notion of an *eddy*. Whenever a fluctuation occurs, it can be expected to influence events over a zone that extends both *spatially* and *in time*. The *eddy*, notionally represents the *size of this zone*.




Figure: Here  $\lambda_y = l_y$  and  $\lambda_z = l_z$

Consider two points at positions  $r_1$  and  $r_2$  with  $r = r_2 - r_1$ . Then, let  $u_i$  at  $r_1(x_1, x_2, x_3)$  and  $u_j$  at  $r_2(x_1 + r, x_2, x_3)$  be the velocity fluctuations at the *same time instant*

Define **Spatial correlation coefficient**

$$R_{ij} = \frac{B_{ij}}{\sqrt{B_{ii}}\sqrt{B_{jj}}} \quad \text{---} \quad B_{ij} = \overline{u_i' u_j'}$$

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If delta t was small- I would expect reasonably good correlation between the two; but if it was very very large, then of course they would be completely uncorrelated.

These ideas are expressed here in this figure, where I show two points  $u_1$  and  $u_1$  at two point separated in  $x_1$  direction and is define a spatial correlation coefficient as  $B_{ij}$  under root  $B_{ii}$  under root  $B_{jj}$ , where  $B_{ij}$  is the  $u_i$  prime  $u_j$  prime at two different points but at the same time instant.

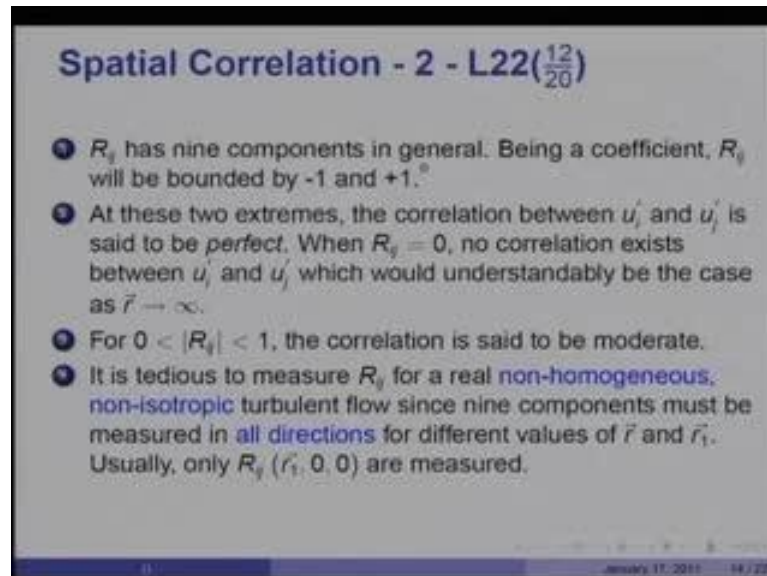
I do the same thing here for  $u_2$  dash and  $u_2$  dash separated in  $x_1$  direction and then if I plot  $R_{ij}$  from measurements of these quantities, then it would **be it will** look like perfect correlation of 1 at separation distance equal to 0 and the correlation would die out 0, that means there is no correlation beyond some long distance.

Similar thing would happen with respect to  $u_2$  dash at the same time all though it will go through a negative before going to 0 at infinity, this is called the longitudinal time scale **ah** correlation;this is called the transverse correlation.

And for example, if I were to integrate this over a long time of infinity, then this would give me a length dimension which would be representative the average dimension over which a fluctuation at a point is going to influensive hence.

That I would call as the integral length scale of the fluctuation or the spatial size of the eddy in longitudinal direction- I can do the same thing for with respect to  $u_2$  velocity and I would get a similar dimension in the transverse direction I can say; so I have estimated the size of the eddy physical size of or the zone over which turbulence is going to influence hence.

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Spatial correlation has nine components,  $R_{ij}$  as defined has nine components in general and being a coefficient it would vary between minus 1 and plus 1. At these two extremes, we say the correlation is perfect, absolutely perfect because its magnitude is 1.

When  $R_{ij}$  is equal to 0, of course no correlation exist between  $u_i'$  and  $u_j'$  which would understandably be the case when the separation distances  $r$  tends to infinity; between 0 and 1 we say the correlation is moderate.

It is tedious to measure  $R_{ij}$  in a real non homogenous isotropic turbulent flow, because nine components must be measured in all directions for different values of separation distance  $r$  and the direction  $r_1, r_2$  and  $r_3$  and therefore usually only in the direction  $r_1$  or  $x_1$  is the only direction which is taken to measure

Whenever measured by enlarge correlation coefficients are extremely difficult to measure the spatial correlations are extremely difficult.

I will stop here and continue with this lecture next class.