

Hydraulic Engineering
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Lecture # 57
Computational fluid dynamics (Contd.)

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Problem- 2

- Classify the steady two- dimensional velocity potential equation $(1 - M^2)\phi_{xx} + \phi_{yy} = 0$, when (i) $M < 1$ (ii) $M > 1$ and (iii) $M = 0$.

$M < 1 \rightarrow$ Elliptical PDE
 $M > 1 \rightarrow$ Hyperbolic PDE
 $M = 1 \rightarrow$ Parabolic PDE



Welcome back students. So, in the last lecture we started with a problem and then I went back and showed you what different values of A B and C are. So, solve this problem we will use the whiteboard.

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Soln 2

Given $(1 - M^2)\phi_{xx} + \phi_{yy} = 0$

$A = 1 - M^2$
 $B = 0$
 $C = 1$

(iii) $B^2 - 4AC$ when $M \neq 1$

$= 4M^2 - 4$
 when $M \neq 1$
 $4M^2 - 4 \neq 0$
 \Rightarrow Parabolic PDE

\therefore we have been given $M < 1$
 $\Rightarrow M^2 < 1$
 $\Rightarrow 4M^2 < 4$
 $\Rightarrow 4M^2 - 4 < 0$
 $B^2 - 4AC < 0$
 \therefore Elliptical PDE

(ii) When $M > 1$

$B^2 - 4AC = 4M^2 - 4$
 when $M > 1$
 $4M^2 - 4 > 0 \Rightarrow$ Hyperbolic PDE
 $\Rightarrow B^2 - 4AC > 0$

So, the best way is always to solution to given first we write what the things are given. So equation given $1 - M^2 \phi_{xx} + \phi_{yy}$. So drawing the analogy from the general equation, we write $A = 1 - M^2$, second, B is 0 and C is 1. So the first part, we say when m is less than 1, we have to calculate the value of $b^2 - 4AC$, so B is 0, so $0 - 4$ is $1 - M^2$ into 1. So $-4 + 4m^2$ are $4M^2 - 4$.

We have been given M is less than 1 implies M^2 will also be less than 1 which implies $4M^2$ is less than 4 so if you bring 4 on this side, it will become $4M^2 - 4$ is less than 0. Therefore, this value $4M^2 - 4$ are $B^2 - 4AC$ will be less than 0 which means it is an elliptical PDE so in the second part, when m is greater than 1.

We have found out does not matter what the value but $b^2 - 4AC$ came out to be $4M^2 - 4$, right. So when M is greater than 1, this means $4M^2 - 4$ is going to be greater than 0, which implies $B^2 - 4AC$ is greater than 0, this implies it is hyperbolic PDE. Now the hard part is I will rub this one here $B^2 - 4AC$ when $M = 1$. So $B^2 - 4AC$ came out to be $4M^2 - 4$ right. So when $M = 1$ $4M^2 - 4 = 0$. This means it is parabolic partial differential equation.

So, this is how we have solved the problem. So I will just write the solution here. So, when M is greater than 1 it was elliptical PDE M greater than 1 it was hyperbolic And for $M = 1$ it was parabolic PDE. So, time to move onwards.

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Problem-3

• Consider the function $\phi(x, y) = e^x + e^y$. Consider the point $(x, y) = (1, 1)$.

1. Calculate the exact values of $\frac{\partial \phi}{\partial x}$ and $\frac{\partial \phi}{\partial y}$ at this point.
2. Use first order forward differences with $\Delta x = \Delta y = 0.1$, to calculate the approximate values of $\frac{\partial \phi}{\partial x}$ and $\frac{\partial \phi}{\partial y}$ at $(1, 1)$.

Calculate the percentage difference with

exact values.



Will solve another problem. So, it says that considers the function phi of x y is e to the power x + e to the power y and we have to consider the point x, y as 1, 1 we have to calculate the exact values of del phi del x and del phi del y at this point at point 1, 1. Secondly, use the first order of finite difference with delta x = delta y = 0.1 to calculate the approximate values of delta phi by delta x and delta phi by delta y at 1, 1 and calculate the percentage difference with the exact value. So, this is the application of all the things that we had done in the last lecture and this will be a good way to understand.

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Solution 3

$$\phi(x, y) = e^x + e^y$$

$$\text{ii) } \frac{\partial \phi}{\partial x} = e^x$$

$$\frac{\partial \phi}{\partial y} = e^y$$

$$\left(\frac{\partial \phi}{\partial x}\right)_{1,1} = e^1 = 2.7183$$

$$\left(\frac{\partial \phi}{\partial y}\right)_{1,1} = e^1 = 2.7183$$

iii) $\Delta x = \Delta y = 0.1$
 let (1,1) be denoted by i, j
 Use first order forward difference

$$\left(\frac{\partial \phi}{\partial x}\right)_{i,j} = \frac{\phi_{i+1,j} - \phi_{i,j}}{\Delta x}$$

$$\left(\frac{\partial \phi}{\partial x}\right)_{1,1} = \frac{\phi_{1.1,1} - \phi_{1,1}}{0.1}$$

$$= \frac{e^{1.1} + e^1 - (e^1 + e^1)}{0.1}$$

$$= 2.8588$$

So, solution number 3. So, what we have been, we know that the function phi x, y has been given as e to the power x + e to the power y. So, for the first part, we should be able to calculate del phi

del x will be e to the power x correct and del phi del y is going to be e to the power y simple partial differential so we have to calculate del phi del x at 1, 1, it is going to be e to the power 1 are 2.7183. Similarly, del phi by del y at 1, 1 e to the power y that is e to the power 1 2.7183.

So, that was a first question that we have solved the values of del phi del x at 1, 1 del phi del y at 1, 1. In the second part we have been given that delta x = delta y = 0.1 this is what we have to assume let 1, 1 be denoted by i, j. And if we use first order forward difference del phi del x at i, j can be written as phi of i, j + 1, j - phi i, j divided by delta x del phi del x i, j can be written as phi of phi at what .1 because delta x is .1, so 1 + delta x so that is 1.1, 1 - phi at 1, 1 divided by 0.1.

This will be e to the power 1.1 + e to the power 1 - e to the power 1 + e to the power 1 we just putting in the values and if you use your calculator, it is going to be 2.8588. That is del phi del x at 1, 1. So, we are going to it is everything here and proceed.

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Similarly

$$\left(\frac{\partial \phi}{\partial x}\right)_{i,j} = \frac{\phi_{i,j+1} - \phi_{i,j}}{\Delta x}$$

$$= \frac{\phi_{1,1.1} - \phi_{1,1.0}}{0.1}$$

$$= \frac{e^1 + e^{1.1} - (e^1 + e^1)}{0.1}$$

$$= 2.8588$$

% difference for both cases

$$\% \text{ diffn} = \frac{2.8588 - 2.7183}{2.7183}$$

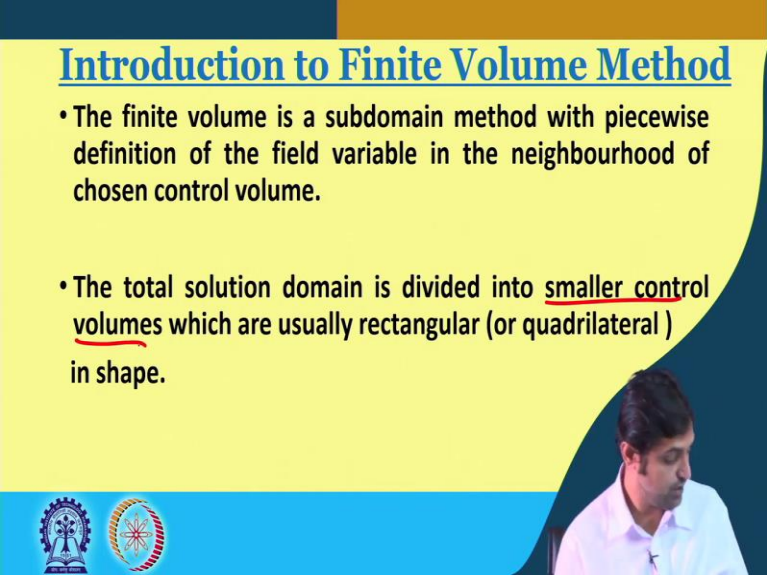
$$\% \text{ diffn} = 5.2\%$$

Answer

So, similarly del phi by del y i, j will be phi of i, j + 1 - phi of i, j divided by delta y are the value of the function at 1, 1 .1 - phi at 1, 1 divided by delta y 0.1 are e to the power 1 + e to the power 1 + 1 - e to the power 1 + e to the power 1 divided by 0.1. This is 2.8588. So, percentage difference for both cases is 2.8588 - 2.7183 divided by 2.7183 and this percentage difference come out to be if this 5.2%.

So, this is the answer. So, this was the simple most question and the solution for demonstrating the percentage difference and the concepts that we have learned in the last lecture. So, we proceed from this point now.

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Introduction to Finite Volume Method

- The finite volume is a subdomain method with piecewise definition of the field variable in the neighbourhood of chosen control volume.
- The total solution domain is divided into smaller control volumes which are usually rectangular (or quadrilateral) in shape.

To we mentioned about other schemes of may be machine that is the introduction to finite volume method, what is finite volume method. So, the finite volume is the sub domain method with piecewise definition of field variable in the neighborhood of chosen control volume, so, the total solution domain in the Finite volume is divided into smaller control volume. So, the total solution to the total domain is divided into smaller control volumes. Normally they are rectangular in shape or quadrilateral inch.

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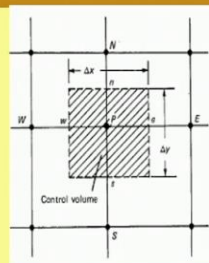
- Nodal points are used within these control volumes for interpolating the field variable and usually, a single node at the centre of control volume is used for each control volume.
- It is based on cell balance equation.
- Solved by integral approach which is more accurate than finite difference method because it is free from truncation errors.



So, nodal points are used with these control volumes for interpolating the field variable and usually a single node at the center of the control volume is used for each control volume. So, this is the 1 single point in that control volume that is used and this is based on the cell balance equation. It is solved by the integral approach which is more accurate than the finite difference method because it is free from truncation error. So, one thing about the integral approach is that it is free from the truncation errors.

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- Cell structure is shown in the figure.
- SIMPLE [Semi implicit Method for Pressure Linked Equation] algorithm is based on Finite Volume Method.



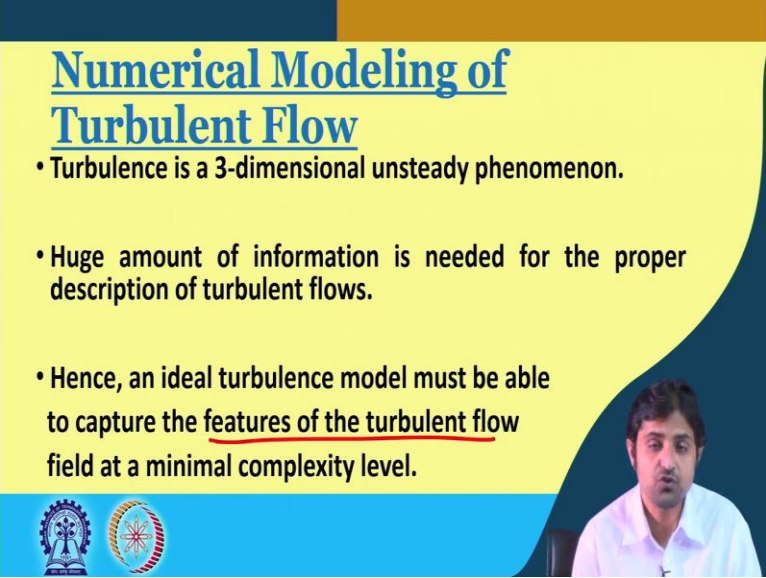
Cell structure



Cell structure is shown in this figure here, you see, this is the control volume the dashed no zone and this at the center point you know, we calculate the things simple is one method which is called semi implicit method for pressure linked equations. So, simple algorithm is based on finite

volume method this is just one example of finite this was just something about the finite volume method.

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Numerical Modeling of Turbulent Flow

- Turbulence is a 3-dimensional unsteady phenomenon.
- Huge amount of information is needed for the proper description of turbulent flows.
- Hence, an ideal turbulence model must be able to capture the features of the turbulent flow field at a minimal complexity level.

The slide features a yellow background with a blue header and footer. In the bottom right corner, there is a small video inset showing a man in a white shirt. The footer contains two circular logos on the left.

So, now going to the things that are very much relevant to our hydraulic engineering course that how do we model or do the numerical modeling of the turbulent flows because most of the flows in real nature at turbulent for turbulence is a 3 dimensional unsteady phenomenon. So, it is a function of time and it also function of a space. So, a huge amount of information is needed for the proper description of the turbulent flows that is a very well established fact.

Hence, an ideal turbulence method must be able to capture the features of the turbulent flow field at a minimum complexity level. So, ideally the best of the numerical model that can do this type of turbulent flow modeling should be able to capture the features of the turbulent flow with least complexity level. So, the model should be least complex as well.

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- Turbulent flows can be modeled numerically to capture:
 - The temporal fluctuations.
 - Time-averaged features of the flow-field.
- Averaged flow properties and the turbulent fluctuations are coupled. We cannot ignore the fluctuations under any circumstances.
 Due to the non-linear nature of the turbulence.

Turbulent flows can be modeled numerically to capture the temporal fluctuations the time average features of the flow field. So, in the real velocity you know I mean the fluctuations mean the deviation from the average velocity and the time average features of the flow field. So, these because these 2 effect the turbulence in terms of turbulent stresses these 2 quantities, you remember we mentioned about you prime and you bar in our laminar and turbulent force flows.

So, average flow properties in the turbulent fluctuations are actually coupled and why are the coupled due to nonlinear nature of the turbulence, this is all the information that we know from before. And for this particular reason, we cannot ignore the fluctuations under any circumstances. So, an ideal turbulent model should be able to capture all these fluctuations too.



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• Turbulent flow is comprised of vortices with a range of different sizes.

• Simulations of all the scales of the vortices is not possible.

Limitations of the available computational facilities.

• Further, a universal turbulence model which is valid for all turbulent flows is not yet available.



This turbulent flow is comprised of vortices with a range of different sizes. Simulations of all scales of the vortices is not possible, I mean, the vortices could be very, small as well. So, the modeling of the smallest of these vortices might not be possible, because the reason is we have limitations on the available computational facilities. The time and the quantum computing is the reality this might be an easier thing to do.

But for now, until that point, we still consider that our computational facilities where we are able to capture all the scales of what it says is not yet possible. Further a universal turbulence model which is valid for all the turbulence flows is not yet available as well.



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Reynolds- Averaged Navier-Stokes Equations

• We have already discussed

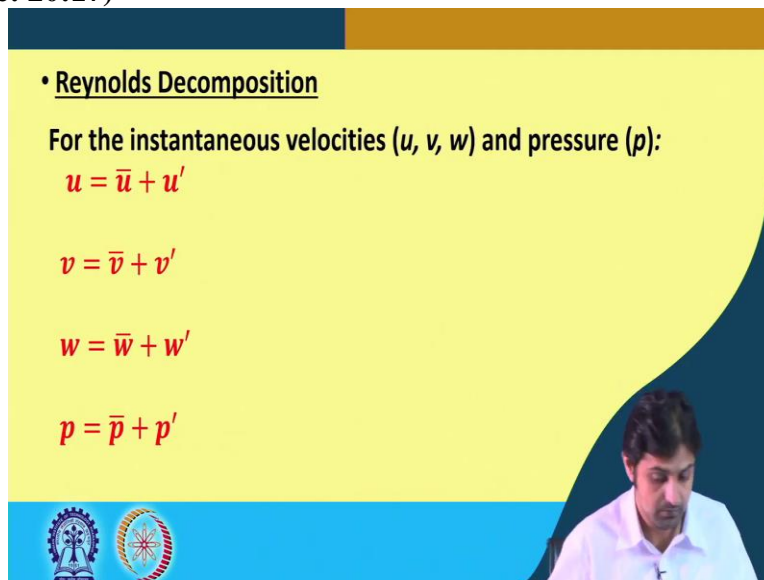
- Reynolds Decomposition ✓
- Reynolds Condition ✓

CAN YOU RECALL ???



So, with this background, we come to one of the most important techniques to solve these Navier-Stokes equation and this is called Reynolds average Navier-Stokes equation as the name indicates, what we do is, we do the averaging of the Navier-Stokes equation Reynolds because Reynolds was the first scientist to do it. So, we have already discussed this term called Reynolds decomposition we have discussed this and laminar and turbulent flow module and the Reynolds condition. If you are able to recall just in just in a case where you are not I have included that again as a quick repetition.

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• Reynolds Decomposition

For the instantaneous velocities (u, v, w) and pressure (p):

$$u = \bar{u} + u'$$
$$v = \bar{v} + v'$$
$$w = \bar{w} + w'$$
$$p = \bar{p} + p'$$



So, what is Reynolds decomposition for the instantaneous velocity is u, v, w and the pressure p can be written as $\bar{u} + u'$. And v is written as $\bar{v} + v'$ this is the bar whatever is in the bar denotes the average value and whatever is with the prime it indicates the fluctuations. Similarly, w is written as $\bar{w} + w'$ and pressure is written as $\bar{p} + p'$.

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• If f' and g' are any two general fluctuating parameters, then the following results hold true

- $\overline{f'} = \overline{g'} = 0$
- $\overline{f'g'} \neq 0$
- $\overline{\frac{\partial f'}{\partial s}} = \overline{\frac{\partial^2 f'}{\partial s^2}} = 0$
- $\overline{\frac{\partial f'g'}{\partial s}} \neq 0$

Reynolds Conditions

So, if we say that f' and g' are any two general fluctuating parameters, we also have dealt this in our previous slide, then the average of $\overline{f'}$ and $\overline{g'}$ is going to be 0 so, $\overline{f'}$ and $\overline{g'}$ is 0. Also we know that $\overline{f'g'} \neq 0$. If you recall we had Reynold shear stress in u' . If this was 0 then there would be no shear stress but this is not equal to 0 there is a finite shear stress.

The third is the $\frac{\partial f'}{\partial s}$. So, the $\frac{\partial}{\partial s}$ of the fluctuation the first differential and also the second differential and if we take the whole bar = 0 also if we multiply both the fluctuations f' and g' take the differential and average it will not be equal to 0. So these are called the Reynolds condition. So, this we have already seen before.

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- For a velocity field u_i , we can write

$$\overline{u_i' u_j'} = 0$$

$$\overline{\overline{u_i}} = \overline{u_i}$$

$$\overline{u_i'} = 0$$

So, for a velocity field u_i we can write u_i prime into u_j bar to the whole bar = 0. Also u_i double bar = u_i bar. If you take the average of the average it is the average itself and the fluctuation if it is average it is 0, this is Reynolds averaging.

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- The continuity equation for the incompressible flow is

$$\frac{\partial u_k}{\partial x_k} = 0 \quad (\text{Eq. 1})$$

- Performing Reynolds averaging on the above equation yields

$$\frac{\partial \overline{u_k}}{\partial x_k} = 0 \quad (\text{Eq. 2})$$

So the continuity equation for the incompressible flow is this $\text{Del } u_k \text{ by } \text{del } x_k = 0$, right. And if we do the we perform the Reynolds averaging on the above equation, it is going to yield one equation that is $\text{del } u_k \text{ bar by } \text{del } x_k \text{ bar} = 0$, right? You do not have just u_k you can write u_k bar + u_k Prime. And so $\text{Del}, u_k \text{ by } \text{del } x_k$ will be $\text{del } u_k \text{ bar by } \text{del } x_k + \text{del } x_k u_k \text{ bar}$ and this will go to 0 So, this will can be represented as this.

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- The Navier- Stokes equation for an incompressible flow can be written as:

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} (2\nu D_{ij})$$

Standard form of
Navier-Stokes
Equation
(Eq. 3)

Strain-rate tensor

$$D_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$



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The Navier stokes equation for incompressible flow can be written as $\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} (2\nu D_{ij})$ this is a standard form of. So, D_{ij} here is a strain rate tensor which we have seen in the last lecture in our viscous fluid flow that D_{ij} returns half of $\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}$. I think this is not a problem because we have derived it.

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- Averaging of the Navier- Stokes equation leads to:

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} (-\tau_{ij} + 2\nu \bar{D}_{ij}) \quad (\text{Eq. 4})$$

- Using Eq. 2, the above equation can be expressed as:

$$\frac{\partial \bar{u}_i}{\partial t} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} (-\tau_{ij} + 2\nu \bar{D}_{ij}) \quad (\text{Eq. 5})$$

RANS: Reynolds Averaged
Navier- Stokes Equation

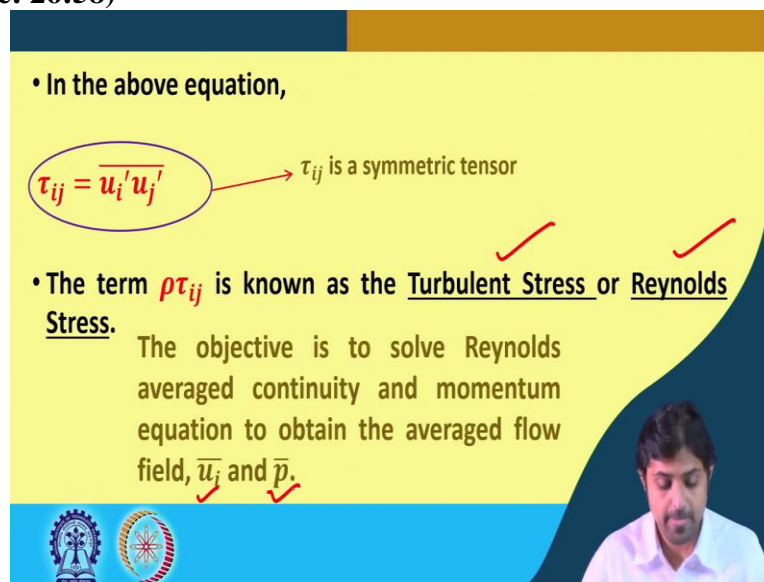


So, if we do the averaging of navier stokes equation, if we put $u = \bar{u} + u'$ and take the whole average of the equation so, $u = \bar{u} + u'$ and $v = \bar{v} + v'$ and $w = \bar{w} + w'$ and $p = \bar{p} + p'$ and put it into Reynolds equation and do the whole average of the

equation. We are going to get equation like $\frac{d}{dt} \overline{u_i}$, $\frac{d}{dt} \overline{u_j}$ So, if you see this is average term, this is also average term and this is also average term right.

So, if we use equation to the above equation, you see you remember that equation to this one here $\nabla \cdot \mathbf{u} = 0$ using the continuity equation it can be written as $\frac{d}{dt} \overline{u_i} = -\frac{1}{\rho} \nabla \cdot \overline{\mathbf{p}} + \nabla \cdot \overline{\boldsymbol{\tau}}$. As if this is equation number 5. So, this actually is nothing but Reynolds average Navier stokes equation. There is some things that we need to find out what is τ_{ij} we already know.

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- In the above equation,

$\tau_{ij} = \overline{u_i' u_j'}$ $\rightarrow \tau_{ij}$ is a symmetric tensor

- The term $\rho \tau_{ij}$ is known as the Turbulent Stress or Reynolds Stress.

The objective is to solve Reynolds averaged continuity and momentum equation to obtain the averaged flow field, $\overline{u_i}$ and \overline{p} .

So, in the above equation τ_{ij} is u_i' multiplied by u_j' this is generally called Reynolds shear stress and as we have read about it, is much more than the kinematic stress and τ_{ij} here is a symmetric tensor symmetric means, $u_i' u_j' = u_j' u_i'$. So, the term ρ into when ρ multiplied by τ_{ij} is known as turbulence stress or Reynolds stress. The objective is to solve the Reynolds average continuity and momentum equation to obtain the average flow field $\overline{u_i}$ and ρ .

So the objective of this thing is to solve the flow for $\overline{u_i}$ and \overline{p} we want to find out the average quantities that is so that is why we do some turbulence modeling.

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Reynolds Stress Equation

- Subtracting Eq. 2 from Eq. 1, we get

$$\frac{\partial u_k'}{\partial x_k} = 0 \quad (\text{Eq. 6})$$

- Similarly, subtracting Eq. 4 from Eq. 3

$$\begin{aligned} \frac{\partial u_i'}{\partial t} + \overline{u_j} \frac{\partial u_i'}{\partial x_j} \\ = -\frac{1}{\rho} \frac{\partial p'}{\partial x_i} + \frac{\partial}{\partial x_j} (-u_i' u_j' - \overline{u_i} u_j' + \tau_{ij} + 2\nu D_{ij}') \end{aligned} \quad (\text{Eq. 7})$$



So how do we do it we solve the Reynolds stress equation if we subtract equation to the beginning equation, second equation from equation 1 we can get $\frac{\partial u_k'}{\partial x_k} = 0$. Similarly, if you subtract equation 4 from equation 3 you see question number 4, this 1 is 4 and this 1 is 3. So, what we are doing is we are subtracting the average to a general equation in both the cases.

We are going to get $\frac{\partial u_i'}{\partial t} + \overline{u_j} \frac{\partial u_i'}{\partial x_j}$ original equation - averaged equation same is here original equation - average equation and why do we do this to obtain fluctuation equations. So, with that this is how we are we obtain the equations with fluctuation terms in terms of differential equations.

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• Expressing $u_j' \left(\frac{\partial u_i'}{\partial t} \right) + u_i' \left(\frac{\partial u_j'}{\partial t} \right)$ in terms of Eq. 7 and taking the Reynolds average yields

$$\frac{\overline{D}\tau_{ij}}{Dt} = P_{ij} + \Pi_{ij} - \varepsilon_{ij} + \frac{\partial J_{ijk}}{\partial x_k}$$

↓

Reynolds Stress Equation


- P_{ij} - Production of Reynolds Stress
- Π_{ij} - Pressure- Strain Correlation Tensor
- ε_{ij} - Dissipation
- J_{ijk} - Diffusive Flux



If expressing $\overline{u_j}$ into $\overline{D u_i} / Dt$ $\overline{D u_j} / Dt$ into $\overline{D u_i} / Dt + u_i'$ in terms of equation 7. So, if we express that in terms of equation 7 here, you know and this is called the Reynolds stress equation where this $\overline{D \tau_{ij}} / Dt$ is called the production of Reynolds stress, this Π_{ij} is the pressure strain correlation tensor and ε_{ij} is a dissipation where J_{ijk} is diffusive flux you can try to do this at your own, but the derivation of this is outside the scope of the current course, I have shown you the methods how to get 1 equation from the other but the details is not in your course curriculum.

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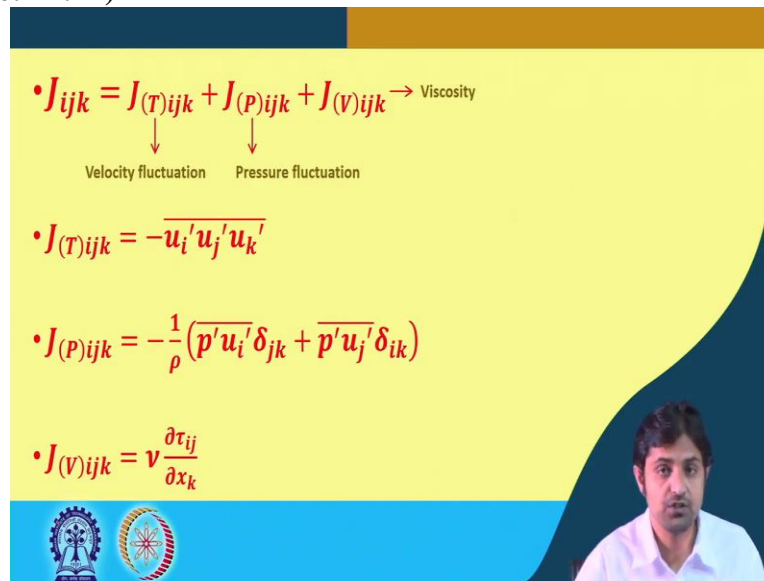
- $P_{ij} = -\overline{\tau_{ik} \frac{\partial \overline{u_j}}{\partial x_k}} - \overline{\tau_{jk} \frac{\partial \overline{u_i}}{\partial x_k}}$
- $\Pi_{ij} = \overline{\frac{p'}{\rho} \left(\frac{\partial u_i'}{\partial x_j} + \frac{\partial u_j'}{\partial x_i} \right)}$
- $\varepsilon_{ij} = 2\nu \overline{\frac{\partial u_i'}{\partial x_k} \frac{\partial u_j'}{\partial x_k}}$ ✓



And this is Reynolds stress equation, equation number P_{ij} is given as $-\tau_{ik} \frac{\partial \overline{u_j}}{\partial x_k} - \tau_{jk} \frac{\partial \overline{u_i}}{\partial x_k}$ this is the expression of the dissipation production and pressure strain

correlation factor epsilon ij is the dissipation it is expressed like this to nu del ui prime del xk del uj prime del xk whole bar.

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$$\bullet J_{ijk} = J_{(T)ijk} + J_{(P)ijk} + J_{(V)ijk} \rightarrow \text{Viscosity}$$

Velocity fluctuation Pressure fluctuation

$$\bullet J_{(T)ijk} = -\overline{u_i' u_j' u_k'}$$

$$\bullet J_{(P)ijk} = -\frac{1}{\rho} (\overline{p' u_i'} \delta_{jk} + \overline{p' u_j'} \delta_{ik})$$

$$\bullet J_{(V)ijk} = \nu \frac{\partial \tau_{ij}}{\partial x_k}$$

Where J_{ijk} is given in this for this is velocity fluctuation, this is pressure fluctuation and this is fluctuation due to the viscosity. Therefore, J_{Tijk} can also be written as $\overline{u_i' u_j' u_k'}$ and u_k' Prime are you see, this velocity fluctuations is written like this the pressure fluctuation is written like this and viscosity fluctuations is written like this. So, we have seen what all these terms of we have seen that all what all these term means, for this Reynolds stress equation.

You see this one here, $\overline{p_i' p_j'}$ a production of Reynolds stress diffusive flux and pressure strain correlation factor. So, you do not need to remember all the details here, but the way of doing it is quite an important and somebody who would be interested in doing further research or further studies in M.Tech this will be a complete course in itself. So, now, how to close this problem is the important question and that will be the topic of our next lecture.

And we will also proceed with techniques like direct numerical simulation and large at simulation for the modeling of computational fluid dynamics. So, this will be all for today. Thank you so much for listening and I will see you in the next lecture.