

Computational Fluid Dynamics
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Module No. # 06

Dealing with complexity of physics of the flow domain

Lecture No. # 38

One-equation model for turbulent flow

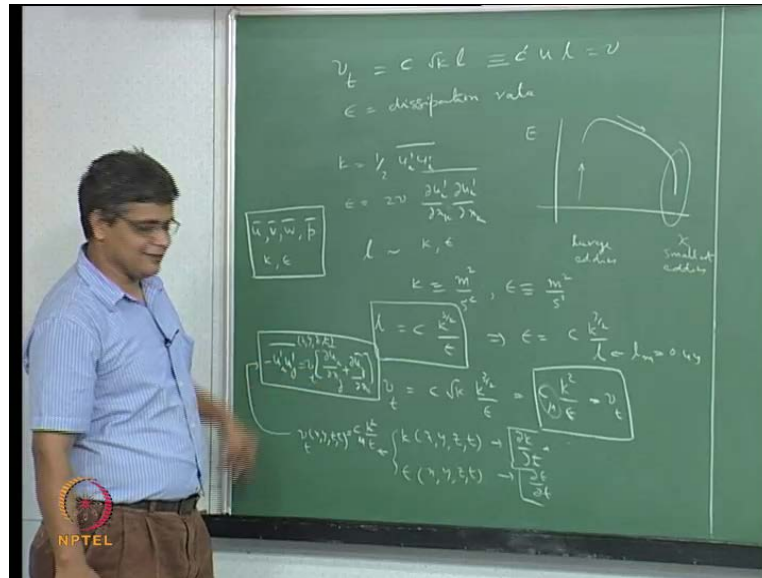
And especially the eddy diffusivity or the extramomentum flux, that is arising out of turbulent fluctuations, and these two parameters are obtained at every point within the flow domain. So, these are two parameters, these will be a function of x , y , z and t , and these are evaluated by their own partial differential equations, which represents the conservation of these quantities, these scalar quantities. We have already seen, one such additional equation for the turbulent kinetic energy, and we look at the similar kind of derivation for the other quantity. Now, what quantities are these that would reflect properly, accurately and well enough the effect of turbulent fluctuations on the overall turbulent flux. It cannot be that everything can, any two parameters will work. It should be that, they have some relevance to the turbulence process that is taking place.

And, in the previous lecture, we have derived the equation for k , the turbulent kinetic energy, and we have seen that the square root of the turbulent kinetic energy can be a measure of the velocity of the eddies, and these could be related, these could be analogous to the velocity of the molecules, gas molecules which interact with each other and produce an enigmatic viscosity.

So, therefore, the turbulent flux is characterized by the effective turbulent viscosity, which has a velocity parameter, which we have derived from the turbulent kinetic energy, and it also requires a length parameter, and it is in the length parameter that we found deficiencies in the one equation module, because we had to resort to the only the length scale that we have, which is the mix in length measure, which is typically taken as y and distance from the wall, and so, that is not a very good prescription for a length scale, in general case, where you may be quite far from the wall or it may be that you have a

significant influence from several walls and so on. So, the idea is to derive a length scale, which is independent of the geometry, and if you were to have that then you could write an expression for the turbulent viscosity.

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Turbulent viscosity has been proportional to constant, times square root of k , times the length scale, which is analogous to u times l times a constant C' , which is a characteristic of the molecular viscosity as per the kinetic fluid gases. Now, what can be the length scale here. The point that, we have to keep in mind is, this is a measure of the turbulent quantities, a measure of the turbulent fluxes, and it should be therefore representing a length scale associated with the turbulent fluctuations, and this is where we also. Notice that, we in the derivation of the equation of k , we have come across the turbulent dissipation rate, and this turbulent dissipation rate, is the rate at which the turbulent energy is getting destroyed, is being taken out of the system and that is a very important quantity in turbulent flow, we have seen a typical spectrum in terms of the wave number k . Let us, not confused this with the turbulent kinetic energy and the energy, and we have seen that typically goes like this. This is where energy is being put into the system, this is the large eddies and this is where we have a smallest eddies.

Turbulent energy is generated by large eddies as a result of destabilization flow, in regions of large velocity gradients, and this is where one can say turbulent energy is produced, and a characteristic of the mean flow parameters, and this energy is cascaded

down, the eddy sizes, as you go from here towards this, the eddy size becomes small and smaller, and this cascading process happens without much of dissipation of turbulence.

So, this is almost like a frictionless transfer of the energy that is created at the large eddy sizes, and this energy is finally dissipated here, at a rate which is given by the turbulent energy dissipation rate, so this dissipation rate is happening, around this smallest eddies and this smallest eddies are so small, that effectively there is no influence of the geometric parameters associated with the system.

So, this is our key feature of turbulence modeling, especially that the turbulent energy dissipation happens at this smallest eddies of the length scale associated with the turbulence, and these are so small, that they do not know whether the turbulence is created in a flow in a pipe, in a circular pipe or in a boundary layer or in some mixing region or anything like that. So, because those scales associated with the circular pipe or boundary layer or with pressure gradient and all those things, are very large compared to this small eddy scales that are happening, and this is independent to the geometry.

Therefore, the length scale that appears here, characterizing the turbulent viscosity is not dependent on the overall features of the flow, but it depends only purely on the turbulent quantities. And we have seen that we have here, two quantities k , which is defined as $\frac{1}{2} \overline{u'^2 + v'^2 + w'^2}$, sum of all the turbulent velocity fluctuations, and ϵ which is defined as $2 \nu \overline{u' \partial^2 u' / \partial x^2}$. So, this again is a positive quantities square of these things, these are the parameters which depend only on the fluctuating quantities.

These are the quantities which are purely turbulence dependent, and one could therefore, argue that the characteristic length of turbulent flow depends only on k and ϵ , because this is also a turbulent thing, this is also turbulent and this is also turbulent, and over most of the spectrum involving the wave numbers and especially in the regions, where towards a higher scales, these characteristics do not depend on the geometry of this. So, if one were to do like this, based on dimension arguments, because k has dimensions of meter square plus second square, and ϵ has dimensions of meter square and second cube.

One can say that, the length here is in constant times k to the power $3/2$ by ϵ , so this is what we can use in order to get an expression for ϵ , we can write this as

epsilon equal to some constant times, and this is the expression that we use for the turbulent kinetic energy equation, in the one equation model. So, we say that, we replace this with the mixed length model, and therefore, we say that this is for example, equal to point 4 times y, where y is normal distance, and this constant is adjusted for best fit with the data and then we have an overall model, and we know that in this way we have a problem with specification of the mixing length, and we make use of this very factor here. To invert this relation and say that epsilon is given by, not here, it is already inverted here.

We make use of this relation to substitute this into this, and say that ν_t is some constant times square root of k, times k to power 3 by 2 by epsilon, and therefore, constant let's call this as say μ , times k square by epsilon.

Now, the turbulent viscosity is given by in terms of constant to be determined, and k and epsilon which are defined as per, in terms of the turbulent flow fluctuating quantities, velocity fluctuations and their derivatives. So, the idea of coming up with a general model, a generic model which can account for length scale, which is not dependent on 1 dimension prescription, is to express turbulent viscosity in terms of two quantities k and epsilon, for which we can derive the conservation equations, from the fundamental momentum equations and their manipulations, and if you do that then we can evaluate k at every x y z t from its conservation equations like this, and we can evaluate epsilon at every x y z t, using an equation need to be developed like this, and from these things we can define ν_t at x y z t as constant it to be determined, times k square by epsilon.

And from these we can write $u_i' u_j'$ which appears in the momentum equation, as $\nu_t \frac{d u_i}{d x_j} + \frac{d u_j}{d x_i}$. So, in the two equation model, we developed an equation for k, and then an equation for epsilon by solving these in the usual CFD way, we can get the instantaneous and local turbulent kinetic energy and it is dissipation rate

From these we get the turbulent viscosity at a local point and using these, we can evaluate the Reynolds stresses different Reynolds stresses at every x y z t, and this equation here which is in terms of ν_t , which is given by k and epsilon which are being evaluated using these equations, and in terms of the time average velocity gradients, is such that,

there won't be any new terms appearing in the time average momentum equations, then we can write time average equations, in terms of known variables that is \bar{u} , \bar{v} , \bar{w} and \bar{t} , and in terms of two more time average variables k and ϵ , we notice all that we have not put time average here, by definition they are time average quantities.

So, we have 6 equations and 6 unknowns here, and by putting up all these things together, we can get the description for turbulent flow, which enables us to calculate each of these quantities, as a function of x , y , z , t without having to give prescribe any arbitrary values, and in this modeling we still have certain constants we determined, like C_μ and other constants which we will see, and those constants are based found from some experiments and some semi theoretical arguments.

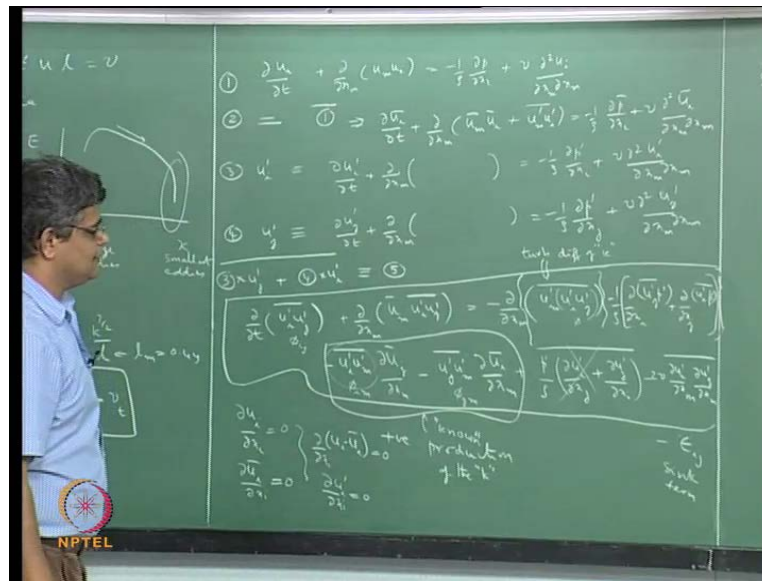
But, essentially people have been able to come up with a set of almost universal constants, which can go into the equations, which describe each of these, so that this model will be a generic model which can be used for 3-dimensional time dependent flows, without having to prescribe ad-hoc kind of coefficient for the quantities which are involved.

So let's just see how we derive these equations, and so that we have a good understanding of the model itself, and when we will discuss some of the limitations of this model and how this can be overcome, how these are overcome in higher level of models.

Now, the essence of the two equation model is to be able to derive a conservation equation for k , and a conservation equation of ϵ , and so that these equations can be solved to get k and ϵ at every x , y , z , t , and we would like these equations to be in the form of the generic scalar transport equation, for which we know how to do the discretization, and then converting them into a finite difference form, and then efficient solutions, all that template is already fixed, and if we like equations which go into the template which describe these turbulent parameters, so that from which we can get k and ϵ and then the turbulent viscosity and then this.

So, how do we derive the equation for k and ϵ , we have already seen the basic idea for the derivation of k , we notice that k consists of the product of u_i' and u_j' , and therefore we have written earlier.

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The instantaneous x momentum equation is the momentum equation like this. Let us call this as equation 1, and then we have derived equation 2, which is the time average of equation 1, and this we can write down as $\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_m} (\bar{u}_m \bar{u}_i + \overline{u'_m u'_i}) = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \nu \frac{\partial^2 \bar{u}_i}{\partial x_m \partial x_m}$.

And by subtracting this from this, we are able to get an equation for u'_i , which was of the form $\frac{\partial u'_i}{\partial t} + \frac{\partial}{\partial x_m} (u'_m \bar{u}_i + \bar{u}_m u'_i) = -\frac{1}{\rho} \frac{\partial p'}{\partial x_i} + \nu \frac{\partial^2 u'_i}{\partial x_m \partial x_m}$, so there are terms that are coming here, and this is for the i th component, and what we need is i th component and i th component, and summed over all the 3. Therefore, the k is to write an equation which is similar for u'_j essentially, wherever you have i here, we place it with j , and then we have an equation for this, in the form of $\frac{\partial u'_j}{\partial t} + \frac{\partial}{\partial x_m} (u'_m \bar{u}_j + \bar{u}_m u'_j) = -\frac{1}{\rho} \frac{\partial p'}{\partial x_j} + \nu \frac{\partial^2 u'_j}{\partial x_m \partial x_m}$, and now what we do is we multiply 3 by u'_i , and add to that the multiplication of every term in the 4th equation by u'_i , and then take the time average, and then we have to do lots and lots of manipulations.

But, this gives us equation 5 which can be written down like this, after doing these things, and then doing the time averaging, we get an equation 5, which is of this form, we can see

that this is the beginning of an equation for the Reynolds stresses by $\overline{u_i u_j}$, that is the mean quantity here, Reynolds stresses, and here we have attempted which looks really humongous, $\overline{u_i u_j}$, it is a simultaneous correlation, time average of the of all the three fluctuating quantities, and terms involving pressure and velocity fluctuations.

So, here we have $\overline{u_i u_j}$ by $\overline{u_i u_j}$, here we have $\overline{u_i u_j}$ by $\overline{u_i u_j}$ of $\overline{u_i u_j}$ correlation like this. And, then we have $\overline{u_i u_j}$, here we have $\overline{u_i u_j}$, so this is $\overline{u_i u_j}$ here and this is $\overline{u_i u_j}$; this is the main quantity and this is a fluctuating quantity, and similarly here we have $\overline{u_i u_j}$ here, and then of course, this is the fluctuating quantity, and here we have mean derivative

So, this mean derivative, mean velocity derivative and this again is the mean velocity derivative, multiply a turbulent stress component here. So, these terms will appear, plus another special term which is returned separately, because this is something that would not finally, appear in the turbulent continuity equation.

So, this is the resulting equation upon manipulation, which we can get, and it looks permeable, it has been derived by many of graduate students all over the world. So, this has the assurance that it can be derived, but one has to be patient, it has been put together in this form.

So as to give some specific meaning here, so we can see that this is of form similar to the standard generic scalar transport equation, and the scalar that we are referring to here, is this ϕ , and of course this has an index ϕ_j , this is a stress here, and this is the advection term, this is being advected by the mean flow, that is the mean velocity here, and gradient that is coming here, so the divergence operator.

And we are missing, I think we are missing this, so if missing a term which is in the generic scalar transport equation we have an advection term, and diffusion term and then we have a source term here, and so we have all these rest of the terms here, which constitute all the unknown kind of things, these are in a way, there are some terms which are known, but this does not fit into the standard diffusion term.

For example, here this is another scalar ϕ_i , and this is another component of this particular scalar, so in that sense one could say that if there are 6 such scalars,

these are known terms and this is also known. So, from that point of view, these two terms here, or in a way one can say these are known or movable, when we write all these terms together, but these are triple correlations of 3 different velocity components, and these are not to be known, within context of solution of these equations, these 6 equations along with momentum equations and the continuity equations.

Again, the simultaneous fluctuation of p and u' again is not known, this term here is the simultaneous fluctuation of the pressure fluctuation and the velocity gradient fluctuations is not known, and this is also not known. So, there are so many terms that are not known here, and these have been given an interpretation. Now, we have said in the previous lecture, and also right in the beginning, that turbulence is produced in the region where you have large mean velocity gradients, and the mean velocity gradients are coming in this overall equations right here, so this is a mean velocity gradient and this is another mean velocity gradient, and this is like a Reynolds stress term, and we have put it here in this particular way.

So, and we have put it in the way that $-\overline{u'_i u'_j}$ here is ν times $d u / dy$ like this, and in the specific case of 1 dimensional flow this thing will become $\nu d u / dy$, and that is equal to $-\overline{u' v'}$, and so $-\overline{u' v'}$ is the positive quantity here. So, one could say that, this along with the minus is a positive quantity, and also this along with a minus is typically a positive quantity, and when this is positive, this is positive and soon. So, this whole thing is a positive quantity, and this is a positive quantity, in which the mean velocity gradients are coming into picture, and this is therefore, treated as a term production of the turbulent kinetic energy.

And similarly, this term here is when we put $i = j$, this becomes a positive quantity, so this becomes a negative term, so together one calls this as ϵ , and in the present format it will be ϵ_{ij} , but once we intend to derive from this, the expression for k we have to put $i = 1$ and $j = 1$ here, and then write in equation for the u' square, and then you put $i = 2$ and $j = 2$ here, and then to the corresponding thing, so essentially when we put $i = j = 1, 2, 3$ we get the three normal spaces, and we add together to get the overall k equation.

So, essentially as far as, the turbulent kinetic energy equation is concerned, i is equal to j , so in that sense we go away, and then we have a ϵ here, and at that point this is a positive quantity, this is the rate of dissipations of turbulent kinetic energy.

So, this is simply like a sink term, so this is a source term, and this is a sink term for this. This term is such that, although this is not known, once you put i equal to j and this thing goes to 0, because this becomes, we get $\frac{\partial u_i}{\partial x_i}$ by $\frac{\partial u_i}{\partial x_i}$ by $\frac{\partial u_i}{\partial x_i}$ by $\frac{\partial u_i}{\partial x_i}$, and that becomes equal to 0, because are instantaneous continuity equation is $\frac{\partial u_i}{\partial x_i} = 0$, that time average form of the continuity equation is $\frac{\partial \bar{u}_i}{\partial x_i} = 0$.

So, if you subtract this from this, you get $\frac{\partial u_i}{\partial x_i}$ of u_i minus \bar{u}_i equal to 0 and this is nothing, but, $\frac{\partial u_i}{\partial x_i}$ by $\frac{\partial u_i}{\partial x_i}$ is equal to 0. So, that means that value put i equal to j here, in order to get the normal stresses, and then this term is identically 0, this is identically 0, so this would not come in to picture, that is why we want to decompose this in to this form.

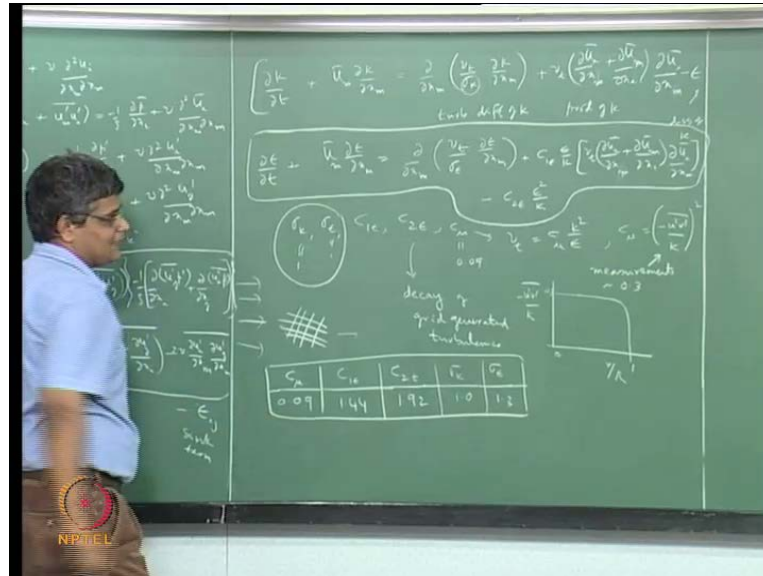
So, of all the terms that are referring here, these two terms together, cross should be the production term, as of source positive source term, and this term here, cross words a sink term which is trying to reduce the amount of turbulent kinetic energy, and this is the term these two terms are essentially not known very well, and what people have try to show is that, this term is being neglected in the case of, is canceling of in the case of k term, this is very important in the relative magnitude of the various normal stresses, so in that sense very important term, and because of the ϵ between this u_i' and fluctuation and $\frac{\partial u_i}{\partial x_i}$ gradient, that is coming here in this, and if one worth treat this has a scalar that were the dealing with, the scalar is the time average quantity of this, where as this is the instantaneous that quantity of that kind of thing.

So, it is not exact, but in one word to say that, this is ϕ here and this is $\frac{\partial u_i}{\partial x_i}$ of u_i minus \bar{u}_i , then it become very similar to this, and this represents the turbulent diffusion of x momentum, so, by the same token, this we considered as turbulent diffusion of this quantity, which is the k like whom quantity here.

So, this time is not very easy to deal with, so together these terms are brought under the umbrella of turbulent diffusion of k . So, this equation of the Reynolds stress when we

contract the enosis, that is when you make i equals j here, and then right in a equation for dau by daut of half of u i prime u i prime, which is nothing but k here.

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Finally, takes a form like this, this is the turbulent diffusion, and we have turbulent diffusion of momentum, and this can be considered as an equivalent of the Prandtl number of the k, so Prandtl number is the ratio of momentum diffusivity to thermal diffusivity, and that comes into picture when we are looking at temperature gradient in the corresponding thermal diffusivity. Here we are looking at diffusion of k, so this sigma k can be called as the equivalent of Prandtl number or the Schmidt number for k, and this is essentially by the turbulent mechanism, so we can put it like this.

So, this is overall effective diffusivity of k, and then we have the production term when you put i equal to j here, then this becomes 2 times this and 2 times u i prime here, and we have to divide by half throughout, so ultimately we can get, and this quantity is expressed using this expression here, so that once you put this into here, and then you do this, we get the overall production term $\frac{1}{2} \frac{\partial}{\partial x_i} \left(\bar{u}_i \frac{\partial \bar{u}_j}{\partial x_j} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_i} \right)$. We are using m here throughout, so we can use m without any loss of generality, so that is the production term which takes account to this, and this term is 0, and then we have minus epsilon, so this is overall equation for the for k which is derived from some kind of hand waving argument, with respect to the diffusion term, and especially with the triple correlation, but otherwise one can derive this exactly.

And in the process, we have introduced only one constant σ_k , and we have made use of the $\langle \langle \rangle \rangle$ type of hypothesis to represent these things as ν_t times $\overline{d u_i}$ and $\overline{d x_j}$ and all these, when we are dealing with production term. So, in this way we can derive equation for k , and the derivation of the epsilon is also similar, in the case of k equation we wrote an equation for u_i' , and then we wrote an equation for u_j' , and then we multiplied by u_j' here, and then u_i' here, and then added them, and then took time average to get an equation for this, and then we contracted the indices. Epsilon here has $\overline{d u_i'}$ by the $\overline{d u_i'}$ by $\overline{d x_k}$ time average.

So, once we do this we have to take $\overline{d u_i'}$ by $\overline{d x_k}$, we need to take the divergence of this and that will give us the equation for $\overline{d u_i'}$ by $\overline{d x_k}$, and then we have to take again the divergence of this whole equation to get $\overline{d u_j'}$ by $\overline{d x_k}$, and then we need to multiply this by this, and this by this, and then add them together and then take the time average, and then we get horrendous expression involving many more correlations and many more unknowns, plus some term which we can readily identify. So, just as in this equation, in this exact equation without any assumptions here, this is derived wholly from the Navier-Stokes equations and continuity equations, and in this we can identify this term and this term readily, and we can identify some elements of these terms, but there are number of terms which are not identified.

The number of terms which are not identified by the epsilon equation is much more, and all of them are swept under these generic terms, this will be exact, we have diffusion so one can say this is turbulent diffusion of k , production of k , and this is the dissipation of k . So, a very analogous relation is finally derived from the mess, that comes out of all these operations here, and then the final equation will be of this form, again a diffusive term, which is very loosely written and analogously written as ν_t by epsilon, σ_ϵ epsilon, plus a production of epsilon, which is essentially this term multiplied by epsilon by k .

So, C_1 epsilon, epsilon by k , times this term, and this term is also multiplied by another constant C_2 epsilon, epsilon by k multiplied with the epsilon by epsilon square by k . So, this is the module equation for epsilon and that is the epsilon equation that we talking about.

So this is only loosely and roughly derived from the exact Navier-Stokes equations with a lot of approximations and simplifications, and when you look at the equations, the additional equations that we have to solve, you see that these are of the standard form generic scalar transport form with an accumulation term, advection term, a diffusion term, and production plus, source and sinks put together. The only difficulty from a mathematical point of view is some of these terms are non-linear, and this term involves ϵ is a function of ϵ , this term is also function of ϵ , and in this, this is an unknown, so there is coupling into just between this and this, and coupling introduced between these and these together to the k term, which is appearing here, and there is coupling introduced between these two and the momentum equations, in the form of the expression for $u_i' u_j'$ here, which is expressed in this way, where ν_t itself is expressed in the form k and ϵ .

So, we have the overall set of equations, the 6 equations that we have for \bar{u} , \bar{v} , \bar{w} , \bar{p} , k and ϵ are very strongly coupled among each other, through these algebraic expressions, and through these expressions for k and ϵ , which not only are inter-coupled through the dissipation rate and then the production rate, but also with the mean velocity gradients which are coming in the production term.

So, the source term linearization and their treatment of the source term is very important, especially when we talk about the turbulence model, but other than that the equations look very similar to what we have, and the things that are yet to be determined are the constants σ_k , σ_ϵ , $C_1 \epsilon$, $C_2 \epsilon$, and the constant which is coming here we have written it as C_μ , which is appearing in $\nu_t = C_\mu k^2 / \epsilon$, these constants are determined partly from some estimates of what is expected, these are effectively Prandtl number for diffusivity of k and ϵ , and in real case, when we talk about fluids, the Prandtl number of a fluid can be very different from 1, for example the Prandtl number for gases typically, so the order of point 7, but for water, it is the order of 7, and for some organic liquids it can be very large, going into thousands, and for liquid metals Prandtl number is very low of the order point 0.1, so they can be quite a lot of variations for real fluids.

Similarly, for the diffusivity, are the Schmidt number which represents the ratio of the kinematic viscosity, and the diffusivity, the mass diffusivity, so that can also vary

over a very wide range, when you look at the typical fluids, and in those cases, the mechanism is by molecular interaction.

But, in these cases, the diffusion that is coming here, and the diffusivity that is causing the diffusion of k , and ϵ is essentially by the same mechanism which is also the causing the turbulent diffusion of momentum, and that is arising out of mixing of different fluid molecules, by the fact that we have turbulent fluctuations, and by the fact that we have these eddy structures.

So, the rate of this mixing, and the rate of this effective flux that is generated is determined essentially by the intensity of turbulence, which is causing the eddies to be present, and also the size range of eddies that are presented.

So, in that sense, the mixing of k and ϵ , these are different scalar quantities is not governed by the intensive property of the k and ϵ , but it is governed by the rate of mixing, and it is the size of the eddies that represent. So, whether we talk about the momentum diffusivity, the turbulent momentum diffusivity, or the turbulent viscosity or the turbulent Prandtl number, or the turbulent Prandtl number for k , that is the σ_k and σ_ϵ , all these are dependent on the same quantity.

Therefore the ratios of the turbulent momentum diffusivity to turbulent k diffusivity, which is what is represented by the σ_k , these should be of the order of one, and this is also of the order of one, and the precise values of these are adjusted by comparing the overall results for velocity profiles in turbulence levels in experiments, but these two are expected to be of the order of one.

Now, this quantity here is determined under conditions, where the k equation, the k evaluation and ϵ evaluation are determined wholly by the source terms. For example, when you are looking at cases very close to the wall, where under the study conditions, where u_m is very close to 0, and the diffusion term can be neglected, and it is the rate of production of k and the rate of local dissipation of ϵ , these two factors dominate, so under those conditions one can show that $C_\mu \bar{u'v'}$ by k , whole square, and measurements show that very close to the wall at which point these equilibrium between the rate of production of k and the rate of dissipation, under those conditions, measurements show that, this ratio is of the order of

point 3, and so if you were to plot along the radial distance r by R , and these quantity minus $u'v'$ by k , we note that k is also a turbulence quantity.

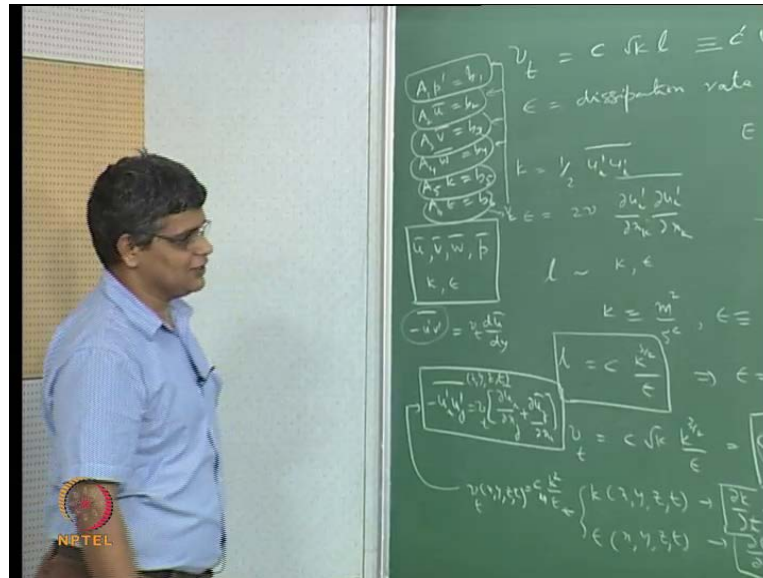
So, we find typically, it is like this around point 3, and close to the wall, it goes down like this, over a large portion of this r by R is equal to 0 and 1, so over a large portion this has a value of point 3, based on that you put these here, you get C_μ equal to point 0.9.

Now, under the conditions of decay of grid generated turbulence that is you have a grid, you have a mesh, and you have flow going over it, and you have essentially uniform flow going over it without any significant velocity gradient. The fact that is flowing over the wires will produce some velocity gradients and turbulence, and some fluctuations of k and ϵ and as you go past these grid, there is no more generation of turbulence, because at this point $d\bar{u}/dx$ is going to be 0, because there is no mean velocity gradient, so this term will be 0.

So, this is 0, this term is there, and so this term is usually a negligible, you have set in rate of decay of k with respect to distance, and based on that and we can get this value here, and so based on these considerations, you can fix the overall values for the constants these are vary from person to person C_μ is point 0.9, $C_1\epsilon$ is 1 point 4 4, $C_2\epsilon$ is 1.92, σ_k is 1.0 and σ_ϵ is 1.3. So, these are the typical values and one can see that these two are of the order of one here, and these are fix by the grid turbulence, and other measurements, and this is based on the velocity measurements close to the wall here.

So, once these values are specified, then in this equation we have only ϵ , which is the parameter of importance here, and this equation determines the value of ϵ at every x, y, z, t , and similarly in this equation this value is known, and everything else is in terms of known variables, and therefore this can be used to calculate k . So, in the two equation model, of which this is one particular form, in the two equation model, we are solving two equations, that turbulent kinetic energy conservation equation, the conservation equation for the rate of dissipation of turbulent kinetic energy, so big quantity, and these two equations are solved for the instantaneous local values of k and the ϵ .

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And from these things we evaluate the instantaneous local value of the turbulent viscosity, using the constant of point 0.9 and k square by epsilon. And, using this instantaneous local value of the turbulent viscosity, we evaluate the Reynolds stress component in terms of $(\overline{u_i' u_j'})$, where you have the mean velocity gradients that are coming here.

So, this value, in each of the momentum equations there will be gradients, appropriate gradients of 3 of these fluxes, and these fluxes reevaluated, and these come into as source terms, in the source terms or effective diffusion term in the momentum equation. Therefore, in the momentum equation we no longer have to write these u_i' or u_j' , we need to only this, but in order to evaluate this term we need to know this, and in order to evaluate this, we need to know these two, and these two are obtained only from these equations.

So, when we talk about a turbulent flow calculation, using the two equation model, we have the continuity equations, which will be put in the form of $\nabla \cdot \mathbf{u} = 0$ in its discretized form, together pressure fluctuation, and pressure correction and from this we get the mean value of pressure. Please note that, this is not pressure fluctuation, this is a pressure correction, and then we have the discretization of the time average x momentum equation will give us $\nabla_x \overline{u} = \dots$, and the discretization of the time average form of the y equation, will give us $\nabla_y \overline{v} = \dots$, and similarly, the time average z momentum equation, it will give us $\nabla_z \overline{w} = \dots$, and the

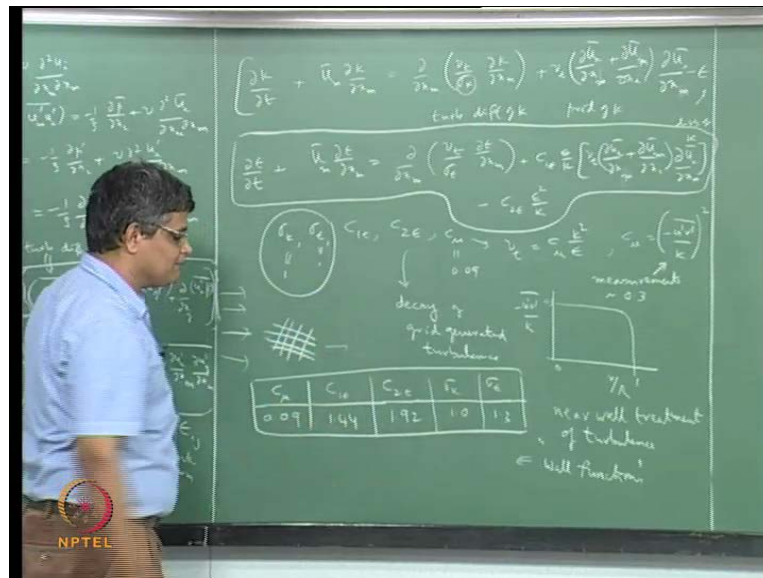
discretization of the k equation, right here, will give us A 5 k equal to b 5, and the discretization of the epsilon equation will give us A 6 epsilon equal to b 6.

So, we have a big loop in which; we evaluate this, and then we evaluate this, and then we evaluate this, and then we evaluate this, and then we can evaluate this, evaluate this. We get nu t, and using nu t and available estimate, we can evaluate the u i term and u j term which will fill into these things, and then once we update all these things, along with the updates which is going into this, we come back and do one more iteration.

So, we can do each of these things sequentially, that is one after the other, and update the values frequently with an under relaxation, and get an overall evaluation of the time average velocity, components and the pressure, and the local time average quantities represent in turbulence k and epsilon, from which we can determine the diffusivities and so on.

So these is how two equation model of turbulence works, and what we notice is, that these conservation equations do not require specification of the mixing length or turbulent viscosity or anything like that these are self consistent contained equations.

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And there is no more, need to say anything other than the fluid properties, the flow domain, and these constants. The only thing that remains is the boundary conditions, there are certain boundary conditions very close to the wall, specifically for k and

epsilon, and we have to give some special treatment at the wall, and that forms a subject of a large variety of turbulent models, the near wall turbulence thing, we don't have that much time in this course to deal with the turbulence modeling approaches, but we need to do something close to the wall, near wall treatment of the turbulence, I would refer you to standard books on turbulence modeling and advanced fluid mechanics, but one approach, one simplistic approach is to use some kind of wall functions, which roughly capture the variation of k and ϵ and the velocities very close to the wall, and they give rise to algebraic prescriptions for what the u , v , w and k and ϵ would be close to the wall, and that way we can overcome the special effects associated with near the wall, there are much more advanced models like that.

So, along with these, wall functions, wall prescriptions for this, we have a complete description of all the parameters that describe fairly additively and in a fairly general way a turbulent flow, and one would have to solve these extra equations, in order to come up with the calculations for turbulent flows.

So, in the next lecture, we will see how we can extend this, when we have, for example, the calculation of the non-isothermal flows, that is what we can do for the energy equation, and also for the typical scalar transport equation, where we are looking at mass transfer or flows with chemical reactions and so on, with that we will be able to say that, we would now have equations, which describe turbulent reacting non-thermal flows, and all of these are put together in the standard form, and they can be readily appended to the method that already developed for a typical CFD calculation.