

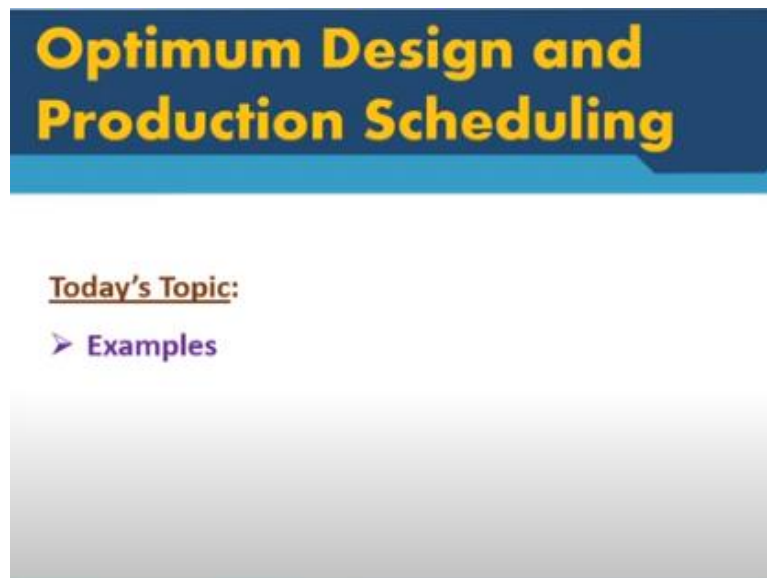
Plant Design and Economics
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Lecture - 57
Examples

Welcome to lecture 57 of Plant Design and Economics. In this module, we are talking about optimum design and production scheduling. In our previous lecture, we have talked about the optimality criteria for unconstrained single variable function as well as unconstrained multivariable functions.

In this lecture, we will go through several examples, and we will see the applications of those optimality criteria for solving problems related to plant design and economics for chemical engineers.

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Example-1: Optimum Diameter of A Vessel

Obtain the optimal diameter of a cylindrical storage vessel of volume V . The curved shell costs C_s (in $\$/m^2$), and the flat top and bottom plates cost C_p (in $\$/m^2$).

GATE 2006

Solution:

Let Diameter = D , Height = h

Convert:

$$f(D, h) \rightarrow f(D)$$

Substitute:

$$V = \frac{\pi D^2}{4} h \Rightarrow h = \frac{4V}{\pi D^2}$$

Cost function (total cost):

$$f(D, h) = C_s (\underbrace{\pi D h}_{\text{curved shell}}) + C_p \left(\underbrace{2 \frac{\pi D^2}{4}}_{\text{Top/Bottom}} \right)$$

$$f(D) = C_s \left(\pi D \frac{4V}{\pi D^2} \right) + C_p \left(\frac{\pi D^2}{2} \right)$$

$$\Rightarrow f(D) = C_s \left(\frac{4V}{D} \right) + C_p \left(\frac{\pi D^2}{2} \right)$$

So let us take the first example, which is the determination of optimum diameter for a vessel. Obtain the optimal diameter of a cylindrical storage vessel of volume V . The current shell cost C_s in dollar per meter square and the flat top and bottom plates cost C_p in dollar per meter square. So you have to find out the optimal diameter of the cylindrical storage vessel of specified volume V .

So what we will do is let us assume the diameter to be D and the height be h . Note that since no numbers are given, for example say $V = 1000$ liter or so here the expression will be in terms of this V , C_s , C_p etc. So we define the diameter of the cylindrical can as D and the height of the cylindrical can as h . So now we can find out the total cost of fabrication.

That you can find out by finding out the area of the curved shell as well as the area of the flat top part and the flat bottom part. So you know that the area of the curved shell is π into D into h . So that multiplied by C_s will give me the cost in terms of dollar for the curved shell portion of the cylindrical storage vessel. Similarly, we have one flat top and one flat bottom. So those plates right will have area πD^2 by 4 each.

So 2 into πD^2 by 4 represents the area of the top part and the bottom part combined. So that multiplied by C_p gives me the cost of top plate and the bottom plate combined together in the units of dollar. So this gives me the objective function, the economic criteria to be minimized. Note that this is a function of two variables diameter D and height h .

But I can convert it to a single variable function by making use of the relationship V equal to $\pi D^2 h / 4$. Because we have to find out the optimum diameter so the two variable objective function is being converted to a single variable objective function by making use of this relationship that relates D and h to volume. So if you substitute h equal to $4V / \pi D^2$ in this expression, I will get this.

Note that now I have my objective function which is a single variable function and the decision variable is D .

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Example-1: Optimum Diameter of A Vessel

Solution (Cont'd):

$$f(D, h) = \underbrace{C_s(\pi Dh)}_{\text{curved shell}} + \underbrace{C_p \left(2 \frac{\pi D^2}{4} \right)}_{\text{Top Bottom}} \Rightarrow f(D) = C_s \left(\frac{4V}{D} \right) + C_p \left(\frac{\pi D^2}{2} \right)$$

(Original cost function) (Transformed cost function)

Set: $\frac{df(D)}{dD} = -C_s \left(\frac{4V}{D^2} \right) + \pi C_p D = 0$

$$\Rightarrow D^3 = C_s \left(\frac{4V}{\pi C_p} \right) = C_s \left(\frac{4V}{\pi C_p} \right) \Rightarrow D_{\text{opt}} = \left(\frac{2VC_s}{\pi C_p} \right)^{1/3}$$

So regional cost function, which is function of D and h is now converted to a transformed cost function which is function of the diameter of the vessel D alone. So now set the first order necessary condition. That means, the derivative of this objective function with respect to diameter D , evaluate that, set that equal to zero and then solve that. That will give me the optimum value of diameter D .

So I obtain the optimum value of the diameter D . So note that since, we have been given the volume as V the cost as C_s or C_p , so I obtain the diameter also as a function of this V , C_s and C_p only.

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Example-2A: Optimal Plant capacity

A plant produces phenol. The variable cost in Rs/ton of phenol is related to the plant capacity P (in ton/day) as $45,000 + 5P$. The fixed charge are Rs. 1,00,000 per day. The selling price of phenol is Rs. 50,000 per ton.

Find the optimal plant capacity (in ton/day) for minimum cost per ton of phenol.

Solution:

GATE 2010

Let, f = the cost of phenol per ton (Rs/ton)

$$\begin{aligned} f \text{ (Rs/ton)} &= \text{Fixed cost} + \text{Variable cost} \\ &= (1,00,000 \text{ Rs/day}) \times [(1/P) \text{ day/ton}] + (45,000 + 5P) \end{aligned}$$

$$f = 1,00,000/P + 45,000 + 5P$$

Now let us consider problem number two. So this has actually two parts. So let us talk about the first part. It is about determination of optimal plant capacity. And then the next part is about the breakeven point. A plant produces phenol. The variable cost in rupees per ton of phenol is related to the plant capacity P in ton per day as 45,000 plus $5P$. The fixed charges are rupees one lakh per day.

The selling price of phenol is Rs. 50,000 per ton. Find the optimal plant capacity in ton per day for minimum cost per ton of phenol. So what is given as the plant capacity is P and expressed as ton per day. Variable cost is a function of the plant capacity and given as $45,000 + 5P$. So variable cost is given as rupees per ton. The fixed charges are given and the selling price of phenol is also given.

So you have to find out the optimal plant capacity in ton per day for minimum cost per ton of phenol. So let us first frame the objective function. We consider f the cost of phenol per ton, so rupees per ton. So the objective function will be sum of two cost components, fixed cost and the variable cost. Now we are talking about f the cost of phenol as rupees per ton.

The variable cost is already expressed as rupees per ton $45,000 + 5P$. Now fixed cost is expressed as rupees one lakh per day. So the fixed cost for the problem which is one lakh rupees per day, divide that quantity by the plant capacity P which is expressed as ton per day. So then it becomes rupees per ton. So f will be equal to some variable cost, which is $45,000 + 5P$ already in terms of rupees per ton.

And then fixed cost is one lakh rupees per day divided by P ton per day. So that becomes rupees per ton. So this will give me my objective function f equal to one lakh by P + 45,000 + 5P.

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Example-2A: Optimal Plant capacity

Solution (Cont'd): $f = 1,00,000/P + 45,000 + 5P$

For optimal plant capacity (P ton/day): $\frac{df}{dP} = -\frac{1,00,000}{P^2} + 5 = 0$

$\Rightarrow 5P^2 = 1,00,000$

$\Rightarrow P_{opt} = \sqrt{20,000} = 141.42 \text{ ton/day}$

Optimal plant capacity for minimum cost per ton of phenol.

Check for optimality:

$\frac{d^2f}{dP^2} = \frac{2(1,00,000)}{P^3} > 0$ Sufficient condition for minimization

So to find out the optimal plant capacity we take the derivative of this expression, which is a function of plant capacity alone, set that equal to zero and we get the optimum plant capacity as 141.42 ton per day. So this is the optimal plant capacity for minimum cost per ton of phenol. Now is this really optimal for that, you have to find out the second order condition.

So check optimality by evaluating d^2f/dP^2 , second order derivative. Note that the first order derivative is this. So the second order derivative becomes 2 into 1,00,000 by P cube which is definitely greater than zero because P is greater than zero. So the second derivative greater than zero you remember that that is a sufficient condition for local minimum. So $P = 141.42$ ton per day minimize the objective function.

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Example-2B: Breakeven Capacity

A plant produces phenol. The variable cost in Rs/ton of phenol is related to the plant capacity P (in ton /day) as $45,000 + 5P$. The fixed charge are Rs. 1,00,000 per day. The selling price of phenol is Rs. 50,000 per ton.

GATE 2010

Find the break-even capacity in ton/day.

Solution:

$$\checkmark \text{ SP (selling price, Rs/day)} = (50,000 \text{ Rs/ton}) \times (P \text{ ton /day})$$

$$\begin{aligned} \checkmark \text{ CP (production cost, Rs/day)} &= \text{Fixed charge} + [(45,000 + 5P \text{ Rs/ton}) \times (P \text{ ton/day})] \\ &= 1,00,000 + (45,000 + 5P)P \end{aligned}$$

At break-even point (there is no gain or no loss): $CP = SP$

So now let us take a look at the second part of the problem which is about breakeven capacity. Same problem, a plant produces phenol. The variable cost in rupees per ton of phenol is related to the plant capacity P in ton per day as $45,000 + 5P$. The fixed charge are rupees one lakh per day. The selling price of phenol is Rs. 50,000 per ton. Find the breakeven capacity in ton per day.

So what is breakeven capacity? Where selling price is equal to cost price. So let us find out selling price as in the unit rupees per day. The plant capacity is P ton per day multiplied by the selling price of the phenol which is Rs. 50,000 per ton. So that gives me selling price in rupees per day. Now let us find out the cost price in rupees per day. So cost price will have again two components, fixed charges and the variable charges.

So fixed charge is already given as rupees per day, rupees one lakh per day and the variable cost is given as $45,000 + 5P$ in rupees per ton. So that should be multiplied by the plant capacity P ton per day to obtain the variable cost component in rupees per day. So that is what we obtain $45,000 + 5P$ into P .

So this gives me an expression for production cost CP . So at breakeven point there will be no gain no loss and the selling price will be equal to production of cost. So we will equate these two quantities and solve for P .

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Example-2B: Breakeven Capacity

Solution (Cont'd):

At break-even point (there is no gain or no loss): $CP = SP$

$$50,000P = 1,00,000 + 45,000P + 5P^2$$

$$P = 979.58 \text{ and } 20.41$$

The break-even capacity is 20.41 ton/day

So the breakeven capacity obtained as 20.41 ton per day. This being an equation a quadratic equations, we obtained two solutions, but at 20.41 you get the breakeven.

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Example-3: Optimum Batch Size

A batch reactor produces 1×10^5 kg of a product per year. The total batch time in hours of the reactor is $\sqrt[3]{P_B}$, where P_B is the product per batch in kg and $k = 1.0 \text{ h}/\sqrt{\text{kg}}$. The operating cost of the reactor is Rs 200/h. The total annual fixed charges are Rs. $340 \times P_B$ and the annual raw material cost is Rs 2×10^6 . Find the optimum size (in kg) of each batch. GATE 2012

Solution:

Basis = 1 year

Production capacity = 1×10^5 kg

Number of batches produced

$$= (1 \times 10^5 \text{ kg product}) \times (1/P_B \text{ batch/kg product})$$

$$= 10^5/P_B$$

Batch time (time required to process 1 batch) = $\sqrt[3]{P_B} + \sqrt{P_B}$ ($k = 1.0$)

So now let us take the example three, which is about determination of optimum batch size of a reactor. So the problem goes as follows. A batch reactor produces 10^5 kg of a product per year. The total batch time in hours of the reactor is $k \sqrt[3]{P_B}$ where P_B is the product per batch in kg. So P_B represents product per batch in kg, kg product per batch, so batch size where k the numerical value is equal to 1 in appropriate unit.

The operating cost of the reactor is Rs. 200 per hour. The total annual fixed charges are 340 multiplied by P_B the batch size. And the annual raw material cost is rupees 2

into 10 to the power 6. Find the optimum size that is optimum batch size in kg. So find the optimum size of each batch in kg. So let us summarize again. We have a batch reactor which produces 10 to the power 5 kg of product per year.

The total batch time in hours of the reactor is given which is a function of batch size. The operating cost of the reactor is given as Rs. 200 per hour. Total annual fixed charges are given as a function of batch size. And the annual raw material cost is fixed at 2 into 10 to the power 6. We have to find out the optimum batch size. So what we have to do first is we have to formulate the objective function.

And we have to formulate the objective function as a function of batch size $P B$. So the objective function will be an economic criteria which reflects the cost, the total cost. So what will be the components of that? Operating cost, the fixed charges, and the annual raw material cost. Annual raw material cost is a constant term which is specified. The fixed charges are already expressed as a function of batch size $P B$.

So what we have to do is basically we have to find out the operating cost as a function of batch size $P B$. Then we can take the derivative of that expression, set that equal to zero and we will be able to obtain the optimum batch size. So let us consider the basis as one year. Production capacity is given as 10 to the power 5 kg. Now let us find out the number of batches produced in a year.

If the total production capacity is 10 to the power 5 and the batch size is $P B$ kg, then the number of batches produced in a year will be 10 to the power 5 by $P B$. So what will be the batch time that is the time required to process one batch? That is given us k root $P B$. Note that the numerical value of k equal to 1. So this is same as square root of $P B$. So batch time or the time required to process one batch is square root of $P B$.

So the total number of batch in a year is 10 to the power 5 by $P B$ and the time required to process one batch is square root of $P B$.

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Example-3: Optimum Batch Size

A batch reactor produces 1×10^5 kg of a product per year. The total batch time in hours of the reactor is $\frac{10^5}{\sqrt{P_B}}$, where P_B is the product per batch in kg and $k = 1.0 \text{ h}/\sqrt{\text{kg}}$. The operating cost of the reactor is Rs 200/h. The total annual fixed charges are Rs. $340 \times P_B$ and the annual raw material cost is Rs 2×10^6 . Find the optimum size (in kg) of each batch.

GATE 2012

Solution (Cont'd):

$$\text{Total time of production} = \frac{10^5}{P_B} \sqrt{P_B} = \frac{10^5}{\sqrt{P_B}} \text{ hour}$$

$$\text{Total production cost, } f = 200 \left(\frac{10^5}{\sqrt{P_B}} \right) + 340P_B + 2 \times 10^6$$

Operating cost	Fixed charges	Raw material cost
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So we will obtain the total time of production as 10^5 divided by $\sqrt{P_B}$ multiplied by square root of P_B . So these many hours is the total time of production. Note that this is in a year. So now I am able to write my objective function which reflects the total production cost, which is sum of operating cost, fixed charges as well as raw material cost. Now operating cost, how to find out?

The total time of production in a year is 10^5 divided by square root of P_B and we know that the operating cost of the reactor is Rs. 200 per hour. So 200 multiplied by 10^5 by square root of P_B gives me the operating cost. The fixed charge is already expressed as a function of P_B $340 P_B$.

And then the raw material cost is fixed at 2×10^6 . So this gives me total production cost. So I have an objective function which is a function of the batch size P_B alone.

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Example-3: Optimum Batch Size

A batch reactor produces 1×10^5 kg of a product per year. The total batch time in hours of the reactor is $\sqrt[3]{P_B}$, where P_B is the product per batch in kg and $k = 1.0 \text{ h}/\sqrt[3]{\text{kg}}$. The operating cost of the reactor is Rs 200/h. The total annual fixed charges are Rs. $340 \times P_B$ and the annual raw material cost is Rs 2×10^6 . Find the optimum size (in kg) of each batch.

GATE 2012

Solution (Cont'd):

$$\text{Total production cost: } f = 200 \left(\frac{10^5}{\sqrt[3]{P_B}} \right) + 340P_B + 2 \times 10^6$$

$$\text{For optimal batch size, set } \frac{df}{dP_B} = 0 = \frac{-200 \times 10^5}{2 \times (P_B)^{3/2}} + 340$$

$$\Rightarrow (P_B)^{3/2} = \frac{-200 \times 10^5}{2 \times 340} = 29411.76 \Rightarrow P_{B,\text{opt}} = (29411.76)^{2/3} = 952.82 \text{ kg}$$

So I have a single variable unconstrained function. So for optimal batch size, set the derivative of the total production cost with respect to batch size $P_B = 0$. Solve this and you obtain the batch size as, optimal batch size as 952.82 kg. So this is how we can obtain the optimum batch size for this process.

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Example-4: Multivariable Optimization

The cost of two independent process variables f_1 and f_2 affects the total cost C_T (in lakhs of rupees) of the process as per the following function:

$$C_T = 100f_1 + \frac{1000}{f_1f_2} + 20f_2^2 + 50$$

Find the lowest total cost C_T in lakhs of rupees.

GATE 2015

Solution:

$$C_T = 100f_1 + \frac{1000}{f_1f_2} + 20f_2^2 + 50 \quad \text{For lowest cost: } \nabla C_T = \begin{bmatrix} \frac{\partial C_T}{\partial f_1} \\ \frac{\partial C_T}{\partial f_2} \end{bmatrix} = 0 \Rightarrow \frac{\partial C_T}{\partial f_1} = 0, \quad \frac{\partial C_T}{\partial f_2} = 0$$

$$\frac{\partial C_T}{\partial f_1} = 0 = 100 - \frac{1000}{f_1^2 f_2} \Rightarrow f_1^2 f_2 = 10$$

$$\frac{\partial C_T}{\partial f_2} = 0 = -\frac{1000}{f_1 f_2^2} + 40f_2 \Rightarrow f_1 f_2^3 = 25$$

Now let us look at another problem. This is a multivariable optimization problem, a two variable optimization problem to be more specific. The cost of two independent process variables f_1 and f_2 affects the total cost C_T in lakhs of rupees of the process as per the following expression or the following function which is given us $C_T = 100$ into $f_1 + 1000$ divided by f_1 into $f_2 + 20 f_2$ square + 50.

Find the lowest total cost C_T in lakhs of rupees. So basically, we have been given a function in two variables. Those variables are process variables f_1 and process variable f_2 . So the objective function which is the total cost in lakhs of rupees is a function of f_1 and f_2 as given. So you have to find out the lowest total cost C_T in lakhs of rupees. So you have to find out that value of f_1 and f_2 which minimizes the C_T

So basically this is same as saying you minimize the unconstrained objective function C_T as given. So find out the value of f_1 and f_2 which minimizes C_T . So it is an multivariable unconstrained problem. So for lowest cost, the first order necessary condition will be set the gradient equal to zero. So what will be gradient? The gradient will be $\frac{\partial C_T}{\partial f_1} = 0$, $\frac{\partial C_T}{\partial f_2} = 0$.

So the gradient of C_T will be a vector with elements $\frac{\partial C_T}{\partial f_1}$ and $\frac{\partial C_T}{\partial f_2}$. This will be equal to zero. Note that this is same as saying $\frac{\partial C_T}{\partial f_1} = 0$ and $\frac{\partial C_T}{\partial f_2} = 0$. So now you take the derivative of C_T with respect to f_1 , set that equal to zero and also you get an expression and then take $\frac{\partial C_T}{\partial f_2}$. So the derivative of C_T with respect to f_2 you take, set that equal to zero and obtain an expression.

So you will have two expressions in two variables, two equations in two variables. You can solve f_1 and f_2 then. So I take $\frac{\partial C_T}{\partial f_1} = 0$ and I obtain f_1^2 into f_2 equal to 10 from this. Similarly, I now take $\frac{\partial C_T}{\partial f_2} = 0$ and then obtain $f_1 f_2^3$ equal to 25. So you have these two equations in two variables. We can solve simultaneously and find out the value of f_1 and f_2 .

So those will be the candidate optimal points. That means, points which are likely to be minimum points, whether minimum or not we have to make use of higher order conditions or sufficient conditions.

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Example-4: Multivariable Optimization

The cost of two independent process variables f_1 and f_2 affects the total cost C_T (in lakhs of rupees) of the process as per the following function:

$$C_T = 100f_1 + \frac{1000}{f_1f_2} + 20f_2^2 + 50$$

Find the lowest total cost C_T in lakhs of rupees.

Solution (Cont'd):

$$f_1^2 f_2 = 10$$

$$f_1 f_2^3 = 25$$

$$f_1 = 2.090$$
$$f_2 = 2.286$$

$$C_T = 100f_1 + \frac{1000}{f_1f_2} + 20f_2^2 + 50$$

$$C_T = 572.82$$

lakhs of rupees

So solve these two simultaneously and we obtain $f_1 = 2.090$ and $f_2 = 2.286$. So the lowest total cost C_T in lakhs of rupees will be obtained from this expression by putting the value of f_1 and f_2 . So we can obtain this. Now to really check for optimality we can evaluate the Hessian at these points and see whether that is positive definite or not. Note that we are finding out f_1 and f_2 such that the cost function is minimum.

So the Hessian matrix of this cost function evaluated at these two stationary points at this stationary point rather, f_1 and f_2 together represents one point here, because it is a multivariable function. So the Hessian matrix evaluated at f_1 and f_2 as given will be positive definite. So that is the sufficient condition for the local minimum for a multivariable function. So let us see that.

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Example-4: Multivariable Optimization

Check for optimality:

$$C_T = 100f_1 + \frac{1000}{f_1f_2} + 20f_2^2 + 50^3$$

$$\frac{\partial C_T}{\partial f_1} = 100 - \frac{1000}{f_1^2 f_2}$$

$$\frac{\partial C_T}{\partial f_2} = -\frac{1000}{f_1 f_2^2} + 40f_2$$

$$\frac{\partial^2 C_T}{\partial f_1^2} = \frac{2000}{f_1^3 f_2}$$

$$\frac{\partial^2 C_T}{\partial f_1 \partial f_2} = \frac{\partial^2 C_T}{\partial f_2 \partial f_1} = \frac{2000}{f_1^2 f_2^2}$$

$$\frac{\partial^2 C_T}{\partial f_2^2} = \frac{2000}{f_1 f_2^3} + 40$$

Stationary Points:

$$f_1^* = 2.090$$

$$f_2^* = 2.286$$

$$\left. \frac{\partial^2 C_T}{\partial f_1^2} \right|_{f_1^*, f_2^*} = \frac{2000}{(2.090)^3 (2.286)} = 95.833$$

Hessian Matrix:

$$H = \begin{bmatrix} 95.833 & 87.616 \\ 87.616 & 80.104 \end{bmatrix}$$

$$|D_1| = 95.833 > 0, \quad |D_2| = 0.0431 > 0$$

H is positive definite.

(f_1^*, f_2^*) is Minimum.

$$\left. \frac{\partial^2 C_T}{\partial f_2^2} \right|_{f_1^*, f_2^*} = \frac{2000}{(2.090)(2.286)^3} = 80.104$$

$$\frac{\partial^2 C_T}{\partial f_1 \partial f_2} = \frac{\partial^2 C_T}{\partial f_2 \partial f_1} = \frac{2000}{(2.090)^2 (2.286)^2} = 87.616$$

So find out del C T del f, del C T del f 1, del C T del f 2 we have already found out. So find out all the second order partial derivatives. Del square C T del f 1 square, del square C T del f 2 square and del square C T del f 1 f 2 which will be same as del square C T del f 2 del f 1. So all these are expressions for f 1 and f 2. So set the values of f 1 and f 2. As we have obtained f 1 equal to 2.090, f 2 equal to 2.286.

So find out all the elements of the Hessian matrix and we obtain this Hessian matrix as this. Find out the leading principal sub-matrices. First is 95.833 which is greater than zero and next is the determinant of the matrix itself which is also positive. So Hessian matrix is positive definite. So the obtained f 1 and f 2 really minimizes the given cost function. So that is how we could satisfy the sufficient condition.

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Example-5: Optimum Tank Diameter

A vertical cylindrical tank with a flat roof and a bottom is to be constructed for storing 150 m³ of ethylene glycol. The cost of material and fabrication for the tank wall is Rs. 6000 per m² and the same for the roof and the tank bottom are Rs 2000 and Rs 4000 per m², respectively. The cost of accessories, piping and instruments can be taken as 10% of the cost of the wall. 10% of the volume of the tank needs to be kept free as vapour space above the liquid storage. What is the optimum diameter (in m) for the tank?

GATE 2016

Solution:

Let V be the total volume of tank

$$V = 150 + 0.1V$$

$$\Rightarrow 0.9V = 150 \text{ m}^3$$

$$\Rightarrow V = 166.67 \text{ m}^3$$

Let, H = the height of tank

D = the diameter of tank

C_T = the total cost of fabrication

Next, let us take another problem, which is about optimum diameter of a tank. A vertical cylindrical tank with a flat roof and a bottom is to be constructed for storing 150 meter cube of ethylene glycol. The cost of material and fabrication for the tank wall is Rs. 6000 per meter square and the same for the roof and the tank bottom are Rs. 2000 and Rs. 4000 per meter square.

So fabrication of all the walls tank wall as well as roof and bottom are all given in units of per meter square. The cost of accessories, piping and instruments can be taken as 10% of cost of the wall. And 10% of the volume of the tank needs to be kept free as vapor space above the liquid storage. What is the optimum diameter in meter for the tank? So we have to find out the optimum diameter of the tank here.

Again, so this problem is similar to one of the problems that we have solved before. Note that the diameter, okay before that let us find out the volume of the tank. So we are constructing a cylindrical, vertical cylindrical tank with flat roof and flat bottom for storing 150 meter cube of ethylene glycol. And then at least 10% of the volume of the tank needs to be kept free as vapor space above the liquid storage.

So the V then will be equal to $150 + 10\%$ of V . So that gives me the volume of the tank as 166.67 meter cube. Now if we considered H equal to height of the tank and D equal to diameter of the tank and $C T$ equal to cost of the total fabrication, I will be able to express the cost of fabrication $C T$ as a function of height and diameter. What will be the total cost?

The total cost will be the cost of the tank wall, cost for fabricating the tank wall plus cost of fabricating the roof as well as bottom and then the 10% of the tank wall as accessories. The cost of accessories, piping and instruments can be taken as 10% of the cost of the wall. So all these three will be functions of D and H and then I can obtain the $C T$ as a function of D and H . So that will be a function in two variables.

But I can always make use of the relationship between volume, diameter and height of the tank to convert the two variable objective function to a single variable objective function. So let us do that.

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Example-5: Optimum Tank Diameter

A vertical cylindrical tank with a flat roof and a bottom is to be constructed for storing 150 m³ of ethylene glycol. The cost of material and fabrication for the tank wall is Rs. 6000 per m² and the same for the roof and the tank bottom are Rs 2000 and Rs 4000 per m², respectively. The cost of accessories, piping and instruments can be taken as 10% of the cost of the wall. 10% of the volume of the tank needs to be kept free as vapour space above the liquid storage. What is the optimum diameter (in m) for the tank?

Solution (Cont'd): The total volume of tank = $\frac{\pi D^2}{4} H = 166.67 \text{ m}^3$

$$C_T = \text{cost of (roof + bottom + wall + piping)} \Rightarrow H = \frac{4 \times 166.67}{\pi D^2}$$

$$C_T = \underbrace{\left(\frac{\pi D^2}{4}\right)(2000)}_{\text{Roof}} + \underbrace{\left(\frac{\pi D^2}{4}\right)(4000)}_{\text{Bottom}} + \underbrace{(\pi DH)(6000)}_{\text{Wall}} + \underbrace{(\pi DH)(6000)(0.10)}_{\text{Accessories}}$$

So a cylindrical tank. So pi D square by 4 into H is the volume which is set equal to 166.67 meter cube that we have obtained previously. So the height of the tank is obtained as a function of diameter. Now note the objective function which is the total cost. So pi D square by 4 multiplied by Rs. 2000 is the cost of fabricating the roof. Then pi D square by 4 into Rs. 4000 is the fabrication cost of material as well as fabrication combined is for bottom.

And then wall will be the curved wall right? The pi DH multiplied by Rs. 6000. And then 10% of these as accessories. So this is a function of D and H. Now I can make use of this relationship to convert it to a function of D only.

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Example-5: Optimum Tank Diameter

A vertical cylindrical tank with a flat roof and a bottom is to be constructed for storing 150 m³ of ethylene glycol. The cost of material and fabrication for the tank wall is Rs. 6000 per m² and the same for the roof and the tank bottom are Rs 2000 and Rs 4000 per m², respectively. The cost of accessories, piping and instruments can be taken as 10% of the cost of the wall. 10% of the volume of the tank needs to be kept free as vapour space above the liquid storage. What is the optimum diameter (in m) for the tank?

Solution (Cont'd): $C_T = \left(\frac{\pi D^2}{4}\right)(2000) + \left(\frac{\pi D^2}{4}\right)(4000) + (\pi DH)(6000) + (\pi DH)(6000)(0.10)$

Substitute: $H = \frac{4 \times 166.67}{\pi D^2} \Rightarrow C_T = \left(4.712D^2 + \frac{4400.09}{D}\right)(1000)$

For optimum diameter: $\frac{dC_T}{dD} = 0 \Rightarrow D_{\text{opt}} = 7.757 \approx 7.8 \text{ m}$

So this is what we do here. So if you do this algebra you will get C T as function of D alone. So for optimum diameter, you take the derivative of this function with respect to D, set that equal to zero and solve it for optimum diameter of the tank as about 7.8 meter.

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Example-5: Optimum Tank Diameter

Check for optimality: $C_T = \left(4.712D^2 + \frac{4400.09}{D} \right) (1000)$

$$\frac{dC_T}{dD} = \left(9.424D - \frac{4400.09}{D^2} \right) (1000) \quad \frac{dC_T}{dD} = 0 \Rightarrow D_{opt} = \left(\frac{4400.09}{9.424} \right)^{1/3} = 7.757 \approx 7.8 \text{ m}$$

$$\frac{d^2C_T}{dD^2} = \left(9.424 + \frac{2(4400.09)}{D^3} \right) (1000) > 0$$

Optimum diameter $D_{opt} = 7.757 \text{ m}$ corresponds to the minimum cost of the tank.

Is it really optimum, let us check for optimality. So this was the expression for the cost function. And we took first the derivative of this with respect to diameter, set that equal to zero and I obtain this as optimum value of the diameter 7.8 meter. Now take second order derivative. Note the second order derivative is always greater than zero. D is positive and there is no negative term over here.

So second order derivative is always greater than zero, which means that this fulfills the sufficient condition for local minimum. So the optimum diameter D equal to 7.757 minimizes this cost function for the construction and fabrication of the tank.

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Example-6: Multivariable Optimization

The total cost (C_T) of an equipment in terms of the operating variables x and y is: $C_T = 2x + \frac{12000}{xy} + y + 5$
Find the optimal value of C_T .

Solution:

For optimal cost:

$$\nabla C_T = \begin{bmatrix} \frac{\partial C_T}{\partial x} \\ \frac{\partial C_T}{\partial y} \end{bmatrix} = 0 \Rightarrow \frac{\partial C_T}{\partial x} = 0, \frac{\partial C_T}{\partial y} = 0$$

$$\frac{\partial C_T}{\partial x} = 0 = 2 - \frac{12000}{x^2 y} \Rightarrow x^2 y = 6000$$

$$\frac{\partial C_T}{\partial y} = 0 = -\frac{12000}{xy^2} + 1 \Rightarrow xy^2 = 12000$$

$$x = 14.42, y = 28.84$$

Putting the value of x and y in the expression of C_T we get, $C_T = 91.53$

Now let us take another multivariable optimization problem. The total cost, total cost C_T of an equipment in terms of the operating variables x and y is C_T equal to $2x$ plus $12,000$ divided by xy plus y plus 5 . Find the optimal value of C_T . So this is very much similar to another problem that we just solved. Again for optimal cost, set the gradient of C_T equal to zero. So $\frac{\partial C_T}{\partial x} = 0, \frac{\partial C_T}{\partial y} = 0$.

Solve these two equations simultaneously. $x^2 y = 6000$. $xy^2 = 12000$. You solve these two equations simultaneously and we obtain $x = 14.42$ and $y = 28.84$. So these are the candidate optimal points. So you can put these values of x and y in the expression of C_T to obtain the value of C_T as 91.53 . So that is the optimal value of C_T . So with this we stop our discussion here.