

Flow Through Porous Media
Prof. Somenath Ganguly
Department of Chemical Engineering
Indian Institute of Technology, Kharagpur

Lecture - 08
Mass Continuity (Non-Uniform Permeability)

I welcome you once again to this lecture of Flow Through Porous Media; what we were discussing in the last lecture was Mass Continuity. What we did so far is we tried to understand the flow through porous media through Darcy's law, through continuum assumptions and through definitions of permeability and porosity. What we did next is we extended it to a mass continuity equation in 3 dimensions.

And then we extended it to cylindrical coordinates because in many cases beyond Cartesian coordinate you can leverage the symmetry in cylindrical geometry to simplify your equations. So, cylindrical geometry we have considered and we have arrived at some equation for the pressure profile and velocity. So, let us just recapitulate quickly the equator equations that we arrived at there. So, we were discussing about Darcy's law, mass continuity in Cartesian and cylindrical coordinates and pressure equations.

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Continuity Equations ... Contd.

$$V_r = -\frac{k}{\mu} \frac{\partial p}{\partial r} = -\frac{k}{\mu r} \frac{(p_e - p_w)}{\ln\left(\frac{r_e}{r_w}\right)}$$

Total flow from sand into the well

$$Q = -h \int_0^{2\pi} v_r (r d\theta) = \frac{2\pi k h (p_e - p_w)}{\mu \ln\left(\frac{r_e}{r_w}\right)}$$

where h is the sand thickness.

$$\Rightarrow p = \frac{Q \mu}{2\pi k h} \ln\left(\frac{r}{r_w}\right) + p_w$$

and $v_r = -\frac{Q}{2\pi r h}$

The slide also features a diagram of a well with flow vectors, a graph showing velocity v_r decreasing as radial distance increases, and a video inset of Prof. Somenath Ganguly.

So, what we did in the last the lecture was we arrived at these, we arrived at this expression for v_r . We arrived at this expression for v_r and we arrived at this expression for v_r , we found that this v_r is inversely proportional to r . That means, we saw that if

this is the x axis is the radial distance from the center of the well. So, if this is radial distance and if y axis is velocity in radial direction; that means, if we are looking at let us say some radial distance r from the center.

And if we are looking at a rate since it is a radial flow if we are looking at this radial flow and if you are trying to find out how v r the radial velocity changes with distance from the center; we found that the absolute value of this velocity would be decreasing with r because, v r is proportional to 1 by r ok. So, depending on what is the; what is the sign on Q if the well is producing; that means, flow is out from the well or if you are injecting something through this well.

So, in that case and this sign of the Q differs and Q is considered positive if radial velocity is negative; that means, Q is positive if something is produced from the well and this radial velocity is negative only if flow is opposite to the directions that are shown here. So, this we discussed in the last lecture and how the pressure profile looks like under such situation. So, what we do next is we have; we have; we have found out the pressure profile in that case.

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Continuity Equations ... Contd.

Non-uniform permeability: Two strata with different permeability
 \Rightarrow Laplace equation for the two strata: $\nabla^2 P^{(1)} = 0$ and $\nabla^2 P^{(2)} = 0$

\Rightarrow Across the surface of discontinuity, pressure and velocity must be continuous \Rightarrow $P^{(1)} = P^{(2)}$
 $k_1 \frac{\partial P^{(1)}}{\partial n} = k_2 \frac{\partial P^{(2)}}{\partial n}$ at all points on the boundary, normal to which is indicated by 'n'.

Reason for such permeability variation (discrete)
 * partial plugging
 * acidizing as in artificial stimulation

$\frac{\partial^2 P}{\partial x^2} + \frac{\partial^2 P}{\partial y^2} = 0$
 $\nabla^2 P = 0$

$P(r) = f(r)$

What we do next is now we look at non-uniform permeability; that means, where we have two strata with different permeability two strata with different permeability; that means, up to certain radial distance we have permeability let us see k 1 and beyond this distance permeability is let us say k 2. So, in one case it is k 1 another case it is k 2. So,

in this case you have this first of all we had this Laplace equation right, when we had uniform permeability we know that we have to solve this equation ok.

So, it was in Cartesian coordinate it was $\nabla^2 p = \frac{\partial^2 p}{\partial x^2} + \frac{\partial^2 p}{\partial y^2}$; if you are not considering the z direction and these were supposed to be 0 that was the Laplace equation Now, in case of radial coordinate it was a little different, but we have a very similar equation in terms of $\frac{\partial p}{\partial r}$ and $\frac{\partial p}{\partial \theta}$. And there basically we can call this equation as $\nabla^2 p = 0$ that is basically the governing equation. Now, since you have two different strata so, you have to stop you have to satisfy two different.

So, we will call this part where the inside this cylinder where the permeability is k_1 let us say all these pressures pressure is a function of r, I call this P_1 I call this P_1 this is a function of some function of r ok. Similarly, we have another pressure another definition of a parameter which is P_2 which is applicable for the region outside this inner cylinder. So, that is the region where the pressure we call it P_2 . So, there we so, we instead of one P now we have P_1 and P_2 . They are function of r and they are they have their own ways to you know explain things.

So, basically now we have to satisfy $\nabla^2 p = 0$ then now you have to satisfy Laplace equation for P_1 and Laplace equation for P_2 ; these are to be satisfied separately ok. So, now we have two different equations; one for the inner strata and the other is for the outer strata. And further when you write two equations they are to be coupled in a sense at the surface of discontinuity; that means, this is the surface of discontinuity. That means, this is the surface where you expect the this is the surface where, you this is the surface where you expect that the pressure that is that you are calculating from this side which is P_1 and the pressure that you are calculating from the other side which is P_2 .

These two pressures they have to be equal at this point; that means, when you are calculating from this side continue to finding out pressure as a function of r from this side, solving this. This equation for example, and then when you go to the other from the other side you are having a pressure equation which is a function of r from this side, but here at this point at the point of discontinuity the 2 pressures have to be equal. So, P_1 has to be equal to P_2 that is important and the second thing is that $k_1 \frac{\partial P_1}{\partial r} = k_2 \frac{\partial P_2}{\partial r}$; that means, this is basically negative of v_r at this location.

So, you are what you are what you are doing here is you are at the surface of discontinuity matching pressure and velocity. You are assuming that the pressure and velocity they must be continuous; that means, from inside whatever velocity is there from the outside also if you come at that same point the velocity have to be equal. One has to satisfy this conservation of one of the satisfy the continuity right.

Whatever flow is coming from this side and whatever flow is going into the other side they have to be equal; there is no accumulation here. So, these so, accordingly this $k_1 \frac{\partial P_1}{\partial n}$ has to be equal to $k_2 \frac{\partial P_2}{\partial n}$; n is what? N is normal to which is indicated by n .

So, at this equation is satisfied at all points on the boundary. What is the boundary? Boundary where this strata inside it is k_1 , my permeability is k_1 the outside the permeability is k_2 . So, at that boundary the n is basically normal to this boundary so; that means, normal to this boundary. If I have an area and I if I want to find out what is normal to it then, what we do here is we say that this is normal to it ok. So, similarly here we have this n is normal to this boundary.

So, basically it is $k_1 \frac{\partial P_1}{\partial r}$ ok. So, that this is representing the radial velocity. So, velocity must be continuous and pressure must be continuous. So, this is one condition one has to, these are the two conditions one has to satisfy apart from these two governing equations.

And the reason for such permeability variation it could be this kind of discrete permeability variation is one reason could be partial plugging. Partial plugging means something is being injected for example, during at the time of drilling or at the time of stimuli at the time of fracturing. There are some fluids which contains some suspended matters that fluid is entering into the pore space and plugging the pore space so; obviously, the permeability will decrease at those locations. So, there could be partial plugging or one if one does acidizing as an artificial stimulation then; that means, the inject acid to clean up they debris from the pores.

So, that the pores are more communicable. So, then there that is that also will that will also increase the permeability. In partial plugging the permeability is decreased and here the permeability after stimulation it is increased. So, because of these reasons there could be discrete, there could be discrete change in permeability.

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Continuity Equations Contd.

Discontinuous radial variation

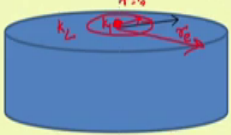
For Region 1, $P_1 = a_1 \ln r + b_1$ k_1
 For Region 2, $P_2 = a_2 \ln r + b_2$ k_2

Boundary conditions:
 @ $r = r_w$, $P = P_w$ $\Rightarrow P_w = a_1 \ln r_w + b_1$... (1)
 @ $r = r_e$, $P = P_e$ $\Rightarrow P_e = a_2 \ln r_e + b_2$... (2)

And at the interface ($r = r_0$), pressure from both sides are equal.
 P_1 from Region 1 at $r = r_0 = a_1 \ln r_0 + b_1$
 P_2 from Region 2 at $r = r_0 = a_2 \ln r_0 + b_2$... (3)

And at the interface, velocities are equal
 $\Rightarrow -\frac{h}{\mu} \left[\frac{\partial}{\partial r} [a_1 \ln r] \right]_{r=r_0} = -\frac{k_2}{\mu} \left[\frac{\partial}{\partial r} [a_2 \ln r] \right]_{r=r_0}$... (4)

$-\frac{k_1}{\mu} \frac{\partial P_1}{\partial r} \Big|_{r=r_0} = -\frac{k_2}{\mu} \frac{\partial P_2}{\partial r} \Big|_{r=r_0}$



So, now if we try to solve this equation what we see here is I have mentioned region 1 and region 2. So, we had a region 1 and we have a region 2, region 1 has permeability k_1 and region 2 has permeability k_2 . So, region 1 we have that is in a general equation that is valid there P_1 is equal to $a_1 \ln r + b_1$ because, you remember we had the original equation that we derived there is P is equal to $c_1 \ln r + c_2$ right.

So, that is the pressure profile. So, here in this case instead of c_1 and c_2 we are putting these constants as a_1 and b_1 for region 1 with permeability k_1 and for region 2 with permeability k_2 we are writing it as $a_2 \ln r + b_2$. So, in this case the constants are different, but finally this if you solve $\nabla^2 P = 0$ you will end up with this form of equation; P is equal to some constant multiplied by $\ln r$ plus some other constant.

So, automatically you will have this equation there even, I mean if you solve a solve this Laplace equation you will end up with these two solutions. For they this solution were applicable to P_1 and P_2 for the two regions. Now, boundary condition we have imposed is at $r = r_w$; that means, $r = r_w$ means at the well.

So, this is the well right. So, at $r = r_w$; r_w is the radius of the well so, there the pressure is P_w . So, that has to be satisfied P_w is equal to $a_1 \ln r_w + b_1$ and at $r = r_e$, r_e is far away from this. So, let us say this radius is r_e . So, at far away it is and $r = r_e$ P is equal to P_e . So, P_w is coming in within the region of permeability

k_1 . So, it is $a_1 \ln r + b_1$ whereas, P_e is in the region of permeability k_2 . So, that is why it is $a_2 \ln r + b_2$ and at the interface let us say r is equal to r_0 . So, you are calling this interface as r is equal to r_0 . So, r_0 is where this transition from permeability k_1 to permeability k_2 takes place.

So, and so, at that interface r equal to r_0 pressure from both sides have to be equal we said and the flow volumetric flux that is the velocity that has to be equal. So, when we apply that we see here if pressure has to be equal then $a_1 \ln r_0$. So, simply P_1 we are measuring now within instead of r we are writing it as r_0 . So, this is the pressure at r is equal to r_0 from inside, so, from the inner region for from region 1. So, this is pressure applicable from pressure from region 1 at r is equal to r_0 ; at r is equal to r_0 and this is pressure from region 2, this is pressure from region 2 at r is equal to r_0 .

So, these two they have to be equal the pressure, the two pressures have to be equal and at the interface the velocities are equal. So, what would be the velocity? It is $-\frac{k_1}{\mu} \frac{dP}{dr}$. So, when I take $\frac{dP_1}{dr}$; obviously, b_1 is constant. So, this is only a function of r . So, that is what is written. So, $-\frac{k_1}{\mu} \frac{d}{dr} (a_1 \ln r)$ at r is equal to r_0 and from this side the velocity would be $-\frac{k_2}{\mu} \frac{dP_2}{dr}$ that is same thing.

This is this time it is $\frac{d}{dr} (a_2 \ln r)$ so; that means, this is essentially saying $-\frac{k_2}{\mu} \frac{dP_2}{dr}$, now $\frac{dP_1}{dr}$ at r is equal to r_0 is equal to $-\frac{k_2}{\mu} \frac{dP_2}{dr}$ at r is equal to r_0 . So, that is so, instead of $\frac{dP_1}{dr}$ when we take a derivative of these $\frac{dP_1}{dr}$ then; obviously, $\frac{dv_1}{dr}$ is 0 and these we have to take the derivative of this. So, that is exactly what has been done here. So now, if we now try to see what kind of solution one gets.

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Continuity Equations ... Contd.

Solution for discontinuous radial variation
 (4 Eqs., Unknowns: q_1, q_2, r_0, r_w)

$$P_1 = \frac{P_e - P_w}{\ln\left(\frac{r_0}{r_w}\right) + \frac{k_1}{k_2} \ln\left(\frac{r_e}{r_0}\right)} \ln\left(\frac{r}{r_w}\right) + P_w \quad \text{for } r_w \leq r \leq r_0$$

$$P_2 = \frac{k_1 (P_e - P_w) \ln\left(\frac{r}{r_0}\right)}{\ln\left(\frac{r_0}{r_w}\right) + \frac{k_1}{k_2} \ln\left(\frac{r_e}{r_0}\right)} + P_e \quad \text{for } r_0 \leq r \leq r_e$$

The rate of fluid flow from the reservoir to the well per unit length is given by

$$Q = \frac{2\pi h (P_e - P_w)}{\ln\left(\frac{r_0}{r_w}\right) + \frac{k_1}{k_2} \ln\left(\frac{r_e}{r_0}\right)}$$

So, we had basically solution for this continuous radial variation we are looking at. So, we have seen 4 equations. What are those 4 equations? We had seen; we had seen a 4 equations and those 4 equations, where one is this equation 1, equation 2, equation 3 and equation 4. We have these 4 equations and we have 4 unknowns. What are those? A 1 b 1 a 2 b 2 so, these are the 4 unknowns and these are the 4 equations. So now, if we now look at the solution of these 4.

So, we have solutions for discontinuous radial variation 4 equations and 4 unknowns. So, we get P 1 is equal to this is the solution I mean I have I am not provide I am not putting the providing the steps here, that are; that are; that are required to arrive at this equation. But, these are the two P 1 and P 2 that we have. So now, if you try to plot these; plot these equation P as a function of r and if this is the point where r is equal to r 0. So, one can see that we said that from between r w actually this must be r is equal to r w and this must be r is equal to r e.

So, the between r w and r 0 you have one equation. So, you have one curve, between r 0 and r e you have another curve. So, these two curves are different ok. There is a discontinuity I can see, but the pressure coming from this side and pressure coming from that side they are meeting at the same place. Now, if we did not have a variation if we remember what did we see that time. We have seen this kind of a profile, when the

permeability was uniform, but now we have what? Now, we have; now we have a discontinuity that is what you are seeing that this is the r is equal to r_0 .

So, there would be a discontinuity of course, this point starts at r equal to r_w . So, essentially the right thing to do here would be to start from r is equal to r_w below r_w we are not talking about it. And the pressure at r equal to r_w would be not 0; it would start from some finite point here. So, this curve should be this and followed by this and if you have a uniform permeability then it would be a continuous line.

But, if you have different permeability k_1 and k_2 then in that case there will be a discontinuity, but the pressure has to be equal at this point the velocity has to be equal at this point ok; velocity has to be equal at this point means the $k_1 \mu$ is constant.

So, $k_1 \frac{dP}{dr}$ and $k_2 \frac{dP}{dr}$ they have to be same. So, you can see very well that if k_1 is equal to k_2 then $\frac{dP}{dr}$ has to be equal to $\frac{dP}{dr}$. So, in that case there would be this there would be no that the slope of this line at this point and the slope at this line of this line at this point they would be equal.

So that means, you will have a continuous line which you have shown here. Whereas, since the permeability is they are different, so, that is why we have a discontinuity and this discontinuity will be more pronounced the more there is a this $k_1 k_2$; if their orders of magnitude different you will see they see this discontinuity more pronounced.

Anyway, if when this when you have these pressure profiles in place then one can write the equation here. Once again we are familiar with first of all minus k by $\mu \frac{dP}{dr}$, but since Q is rate of fluid flow from the reservoir to the well and v_r is from the well to the reservoir so; that means, with the sign is inverse.

So, that is why this minus sign is drawn because, Q is defined that way and Q is this essentially flow rate whereas, the v_r that we talked about that is the volumetric flux right. The superficial velocity same as volumetric flux and volumetric flux means volumetric flow rate divided by area. So, if you want to convert that to the volumetric flow rate then you have to multiply this by the area. Now, area is what? Area is $2 \pi r h$ right, this height is h and $2 \pi r$.

So, in the area of the cylinder is $2\pi rh$, but we are they are not writing h here because, they have written reservoir to the well per units and thickness; per units and thickness that is important. So, per units and thickness means h is equal to 1. So, if you consider h to be 1 if you consider h to be not 1 h to have a finite value put that put the h here there will be a h continued ok. So, Q is equal to this quantity and then now if you take this $\frac{d}{dr}$ within this pressure profile and take the derivative of it you end up with an expression of flow rate which is given by this. So, if there is a break in permeability one can have a way to solve this.

I mean this Laplace equation that we have discussed earlier for a single permeability set up that Laplace equation has to be solved now. In this case we have last time we had only one equation P is equal to $c_1 \ln r$ plus c_2 . And our job was to find out what is c_1 and what is c_2 and plug them and then write $k_1 - k_2$ by $\nu \frac{dP}{dr}$ and be happy with that as an expression for v_r .

But, now since we have two different permeabilities so, we have to solve this Laplace equation for the two domains. One with permeability k_1 another if for permeability k_2 and they have to be coupled at the interface. At r is equal to r_0 you have to assume the continuity, continuity in terms of pressure; the pressure from this side and pressure from that side has to be equal and the velocity from this side and velocity from that side this has to be equal.

So, this these velocities are equal and pressure are equal they are putting these two conditions you can get this flow rate ok. So, this is how the permeable discontinuous radial variation this is how this discontinuous radial variation is handled.

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Continuity Equations ... Contd.

Permeability variation in linear system

k_1, k_2 in series $\Rightarrow \frac{l_1 + l_2}{k_{eff}} = \frac{l_1}{k_1} + \frac{l_2}{k_2}$

$\Rightarrow \frac{\sum l_i}{k_{eff}} = \sum \frac{l_i}{k_i}$

k_1, k_2 in parallel $\Rightarrow k_{eff}(A_1 + A_2) = k_1 A_1 + k_2 A_2$

$\Rightarrow k_{eff} \cong A_i = \sum k_i A_i$

The image contains a slide titled 'Continuity Equations ... Contd.' with handwritten mathematical derivations and diagrams. The derivations show the relationship between permeability, length, and effective permeability for series and parallel configurations. The diagrams illustrate a cylindrical pipe with two sections of different permeabilities and a rectangular block with two parallel paths of different permeabilities, showing flow directions and pressure drops.

Now, you let us look at the situation where, you have permeability if a permeability variation is in a linear system because, we have been talking about cylindrical coordinate. Of course, cylindrical coordinate has a net I mean is more important when somebody is working with a reservoir or working with an electrode where, some fluid is injected. Or fluid is collected many a times you will find in an electrode the fluid is collected from a particular location and so, that would be acting as a point sink that would be acting as a sink. So, it is a flow would be radially moving towards the sink.

So, in those cases this kind of cylindrical geometry is perfectly is a perfect way of doing things. Now, it may so, happen that you are simply working with a linear system in a particular setup you are working with linear system. So, how these permeabilities they play out? So, linear system means that suppose I have a core we have been talking about this core right. So, suppose we have a core and we have let us say I am having a flow rate here. And I have a permeability up to this point is the permeability is let us say k_1 and permeability beyond is k_2 . It is a linear system, not a cylindrical system just a 1 dimensional problem right.

I mean it could be we just used a cylindrical cross section, but we could have; we could have used a square cross section that is fine. You can even use a square cross section it does not matter and you could we could have used a square cross section as well. So now, this is suppose let us say I have a permeability k_1 and permeability k_2 and they

are in series. So now, if somebody wants to know what is the effective permeability of this; that means, why do I need to know effective permeability? Suppose I am having a flow rate Q and I want to know what would be the pressure drop in this case. So, how would I find out the pressure drop? I will use Darcy's law.

So, Darcy's law means I need; so, say for example, you can say that the let us say this length is L , this length is L and let us say the pressure drop across this is ΔP I write it ok. So, we would write then Q is equal to; Q is equal to or Q divided by area let us say that, let us say the cross sectional area is A . So, Q divided by A is equal to then we have to write some permeability k divided by viscosity this and ΔP let us say I write this ΔP as $P_{\text{inlet}} - P_{\text{outlet}}$. So, ΔP is defined let us say as $P_{\text{inlet}} - P_{\text{outlet}}$ to avoid any confusion about whether you have ΔP should be taken as minus or plus let us say this is what is ΔP .

So, ΔP divided by L so, I can find out what is ΔP ; I mean if I do not want to run this experiment as such I may like to find out what would be the ΔP . I can expect if I inject certain flow rate of some say millilitre per minute or something. So, this so, for this purpose you need a permeability, had it been a single permeability set up we could have used this \times the use this equation Darcy's law. We can use it to find out what is the; what is the ΔP , but provided I am giving you a permeability let us say of 500 milli Darcy. That means, 500 into 10 to the power minus 3 Darcy 500 into 500 into 10 to the power minus 3 Darcy.

So, this is 500 into minus 3 Darcy let us say I give you this k . So, you can find out immediately what is the; what is the corresponding ΔP flow rate being known. Now, if you have a situation where you have k_1 and k_2 , so, should you be writing k as $k_1 + k_2$ or how what would be the; what would be the right way of expressing k in terms of k_1 and k_2 .

So, we can think of this situation also there could be a parallel situation where, you have let us say a block. You have a block like this and let us say I have a permeability which is existing here as the upper one has k_1 and the lower one has k_2 . So that means, I have permeability of k_1 and k_2 which are running in parallel. One thing I must point out at this time is that running these two permeabilities parallelly and still expecting the flow to be unidirectional, that may not be that easy.

Because, suppose there is a flow taking place and I am expecting that the flow will take place in parallel; that means, here I am having some velocity which depends on k_1 , here I am having a some velocity which is which depends on k_2 ok. So, then one must ensure that there is no cross flow happening. So, one must ensure that these two permeabilities they are somehow separated ok. This particularly if the k_1 and k_2 they are varying by a large magnitude by orders of magnitude in that case you can expect that fluid will tend to channel through higher permeability region. So, one must have this separation in place which may not be the case over which is not the case for permeabilities in series.

So, if you have such kind of sequence then how do you find out what is the effective permeability? In this regard I would in fact, I am going to close this discussion at this time. But, before you come for the next lecture, before you attend the next lecture I would suggest you review this your theories of resistances in series. That means, you have two resistances in series, how do you; how do you find the effective or equivalent resistance in this case. And if you have the resistances in parallel which is R_1 and R_2 and how do you; how do you find the equivalent resistance where the resistance is two resistances R_1 and R_2 are in parallel.

So, let us just before these are some fundamental concepts of electrical resistances. So, please review this particular part before we start and before we proceed further with this discussion. I that is all I have as far as this lecture module this part of the module is concerned. So, I will continue this discussion again in the next class where, we will talk about how to incorporate these understanding into the two permeabilities in series and two permeabilities in parallel, that is all I have for this particular module.

Thank you.