

Transport Phenomena
Prof. Sunando Dasgupta
Department of Chemical Engineering
Indian Institute of Technology, Kharagpur
Lecture Number 18
Boundary Layers (Cont.)

(Refer Slide Time 00:18)



So what we have seen in our previous treatment of boundary layers, we were restricting ourselves to a flat flow over a flat plate and when the flow was laminar. What we understood that it's the effect of the flat plate will become less and less at certain point inside the fluid after a certain depth the flow becomes equivalent to that of the freestream flow. So if we have a flat plate and the fluid is approaching it with a constant velocity which is also known as the approach velocity then close to the solid layer the effect, the velocity will vary from the no-slip condition which is zero velocity on the flat plate to asymptotically it will merge smoothly to the flow outside of the thin layer which is known as the boundary layer in which the effect of viscous forces are important.

So beyond the thickness of the boundary layer the velocity will remain constant and for a flat flow over a flat plate laminar flow over a flat plate, this velocity, the constant velocity beyond the boundary layer which is known as the freestream velocity, the velocity which is free from the viscous effects, its known as the freestream velocity and for the special case of flow over the flat plate the approach velocity and the freestream velocity, these two are going to be equal. Inside the thin boundary layer, the effect of viscous forces will be predominant. Now close to the surface the effect of the viscous forces would be more and as we move away from the flat plate, flat solid force the effect of the viscous forces will be progressively

smaller and beyond the boundary layer the flow can be treated as inviscid where there would be no effect of viscosity and therefore the velocity profile in the flow outside of the boundary layer can just resemble, just a flat profile.

So approach velocity and the freestream velocity outside of the boundary layer for flow over a flat plate, they are equal inside the boundary layer the flow is two dimensional, the effect of viscous forces are going to be important, beyond it the effect of viscous forces would not be applicable. So truly speaking Euler's equation which is for an inviscid flow is valid for the region outside of the boundary layer where as the Navier–Stokes equation which is for a viscous fluid, which is for equation of motion of a viscous fluid of constant μ and Newtonian fluid, the Navier–Stokes equation would be valid for flow inside the boundary layer.

And we have already discussed the historical significance of the boundary layer concept and how does that help in correlating the theory and the experiments while designing the motion of ships in sea. The thickness of this boundary layer is arbitrarily defined as the point at which the velocity of the fluid is equal to 99 percent of the freestream velocity. So it is very close to the freestream velocity and the number is defined as the 99 percent of the freestream velocity. So if we call small u as the velocity inside the boundary layer which since the flow is two-dimensional this u is going to be a function both of x where x is action direction or direction of flow and y where y is the distance from the, vertical distance from the top plate.

So u inside the boundary layer is a function both of x and y where as outside of the boundary layer it's a constant, the small u will simply becomes equal to u_{∞} where u_{∞} is the freestream velocity so how does this small u , the velocity inside the boundary layer changes with distance from the solid plate is something which is of importance and you will subsequently see why it is so but by the definition of boundary layer thickness, small u divided by capital U , the local velocity inside the boundary layer and the freestream velocity outside of the boundary layer, the ratio of these is equal to point nine nine which is known where the value of y where this condition is reached is called the boundary layer thickness or the disturbance thickness.

Now we can understand since the velocity near the edge of the boundary is very small so a small change in U mean it is difficult to demarcate the exact location at which the velocity becomes ninety nine percent of freestream velocity so this definition though it gives a pictorial view of the thickness of the boundary layer is difficult to obtain experimentally with sufficient accuracy. This there is definitely, therefore there is a need some thickness which

unlike the previous one which is differential in nature unlike the differential nature of boundary layer thickness, it would be an integral nature and the integrand would be such that the integrand nearly at the, at or near the edge of the boundary layer.

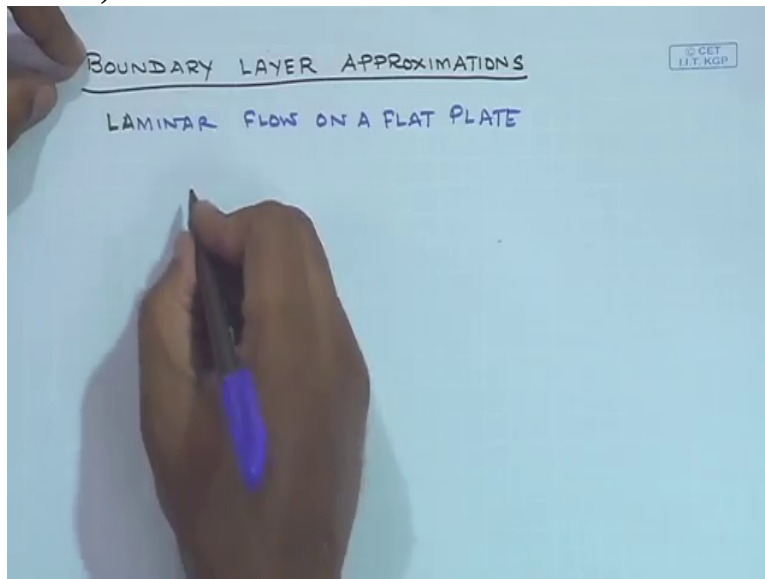
So we have, in the previous class we have also seen two integral thicknesses defined in such a way that when expressed as a series a summation of a series the later terms which are the terms which represent the region close to the edge of the boundary layer, their effect on the total summation is negligible. So these two thicknesses are known as the momentum thickness and the displacement thickness. So displacement thickness when talk in terms of the reduction in mass flow rate because of the presence of the boundary layer and momentum thickness when we talk in terms of the reduction in momentum of the actual mass which is flowing through the boundary layer.

So this is what we have done in our previous class. Now we would like to see if it is possible to obtain an analytic solution or close to an analytic solution for flow inside a boundary layer. We understand that this is a complicated situation because inside this region, the velocity is the function of actual distance, the velocity is the function of distance, the vertical distance from the solid wall, the effect of viscosity is important and therefore the equation we need to start with is the equation of motion or the Navier–Stokes equation for two dimensional flow for two dimensional flow inside the boundary layer and there are various terms which would lead to complicacy whenever we try to analytically obtain a solution for such a case.

So we would see that some of the approximations which are quite common in the treatment of boundary layer, collectively they are called as the boundary layer approximations. So what are those approximations, the logical basis on which these approximations are made and how they can simplify a very complicated problem to something which is so we would start this class with the boundary layer approximations for laminar flow over a flat plate. And whenever there is a flow over a flat plate under laminar flow conditions it's, it's approximated as a zero pressure gradient flow and if we assume the plate to be horizontal there would be no effect of body forces.

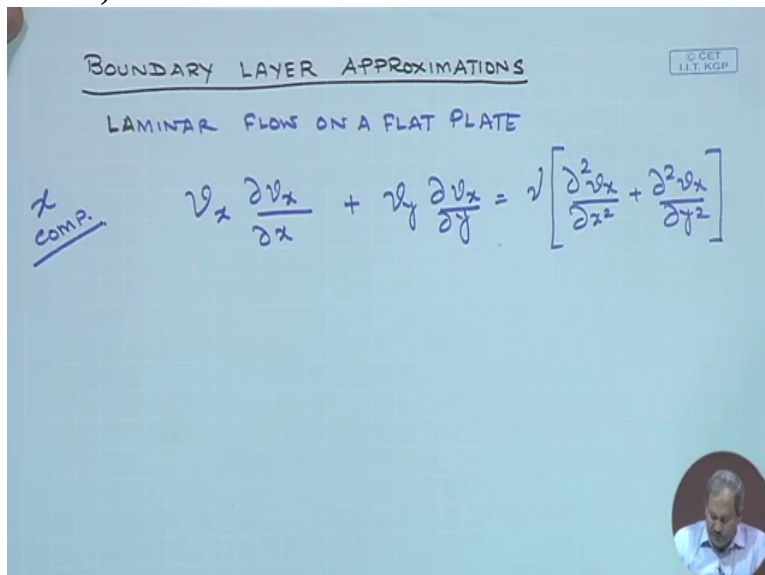
If you consider gravity is the only body force which is present, so the Navier–Stokes equation which we are going to write will, will be for a situation which is zero pressure gradient since it's flow over a flat plate and it's, it's a situation at which the effect of body forces are not present, are negligible. So we are going to write the Navier–Stokes equation for flow inside a boundary layer which would look something like this. We all know that the,

(Refer Slide Time 09:39)



from our statement of Navier–Stokes equation, if we write the x component and we are writing the x component since this is the principle direction of motion, plus $v_y \frac{\partial v_x}{\partial y}$ which is nothing but ν by ρ , the kinematic viscosity, $\frac{\partial^2 v_x}{\partial x^2}$ plus $\frac{\partial^2 v_x}{\partial y^2}$. And there is, as I mentioned before, there would be no effect of, there is no pressure gradient or body force term in this. Now here we are going to make

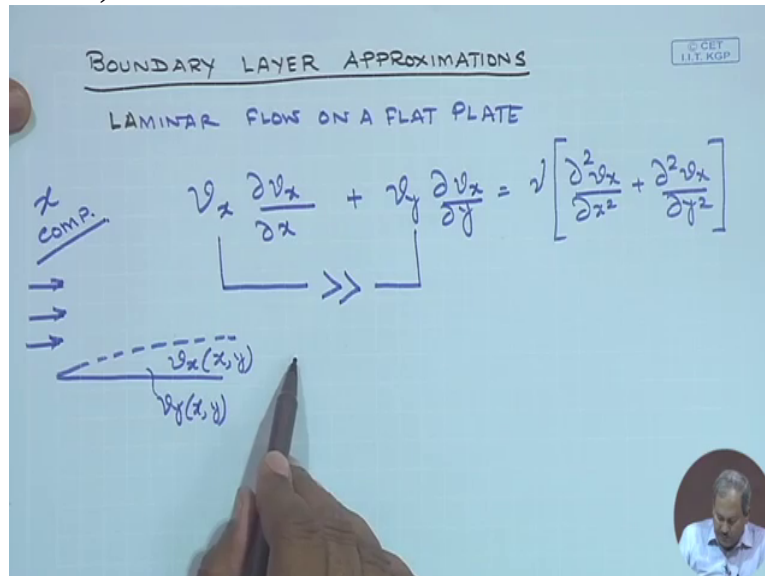
(Refer Slide Time 10:22)



a quick uh mental calculation of the significance of each of these terms Now we are talking about a flow where the flow and this is the boundary layer and here I have v_x which I understand is a function of both x and y . And for this boundary layer to grow I also have a v_y which could also be a function of both x and y . But if we see, if we just analyze this you can

simply see that this v_x is going to be very large as compared to v_y . So v_x , it's the principal direction, the component in the principal direction

(Refer Slide Time 11:11)



of motion must be higher, significantly higher than v_y . But the thickness, the boundary layer thickness at any point is δ and we understand that this δ is a function of x . As x increases, δ keeps on increasing. However the value of δ is quite small. It is the thickness of the boundary layer is generally small, so the variation of v_x with x and variation of v_x with y , if we consider these two terms, v_x varies from zero over here at the solid liquid interface equal to u where u is a freestream velocity. So v_x changes from zero to u over a small distance δ so therefore $\frac{\partial v_x}{\partial y}$ is going to be quite large as compared to $\frac{\partial v_x}{\partial x}$. $\frac{\partial v_x}{\partial x}$ simply tells you the variation in velocity between these two points over a certain distance x so the reason, the analysis, or the understanding here clearly tells us that this $\frac{\partial v_x}{\partial y} \gg \frac{\partial v_x}{\partial x}$

(Refer Slide Time 12:42)

BOUNDARY LAYER APPROXIMATIONS

LAMINAR FLOW ON A FLAT PLATE

x
COMP.

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \left[\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} \right]$$

$\delta(x)$ SMALL

$\frac{\partial v_x}{\partial x} \quad \frac{\partial v_x}{\partial y} \sim \frac{U}{\delta}$

because of the small value of delta is going to be significant larger than $\delta v_x \delta x$ or in the other words, the gradient in velocity in the vertical direction is going to quite large as compared to the axial velocity gradient. So as you see from here, since v_x is large as compared to v_y and $\delta v_x \delta x$ is large in comparison to $\delta v_x \delta x$, the product of these two, we cannot make any

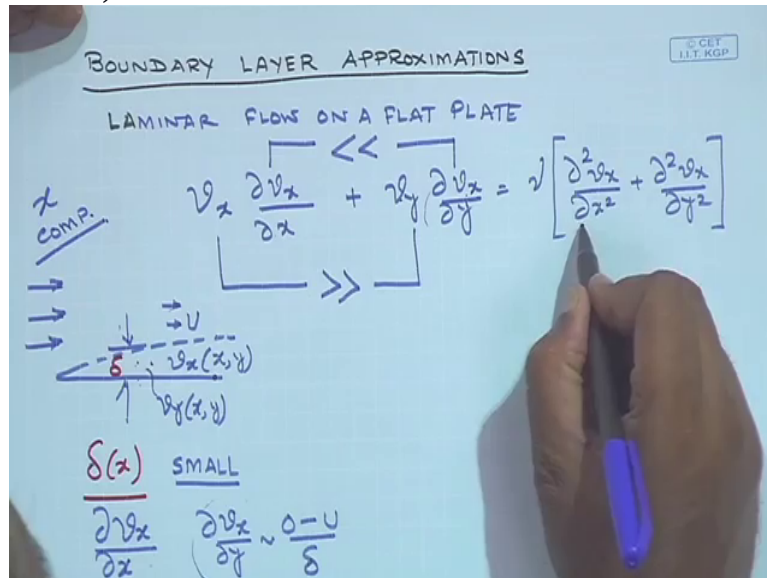
(Refer Slide Time 13:15)



judgment about which one is going to be significant So the each term contains two terms and the nature of the variation or the magnitude of these terms are such that you need to keep both of these terms in the Navier–Stokes equation. There is no way you can say that the, let's say the first term is significant, the second is not and so on. So therefore you cannot make any

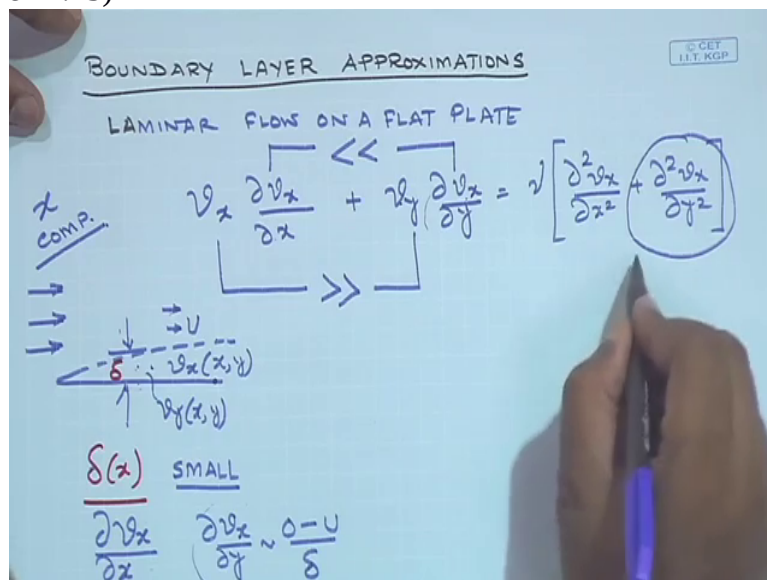
judgment and both the terms are to be kept into this equation. Now when we come to this part over here,

(Refer Slide Time 13:51)



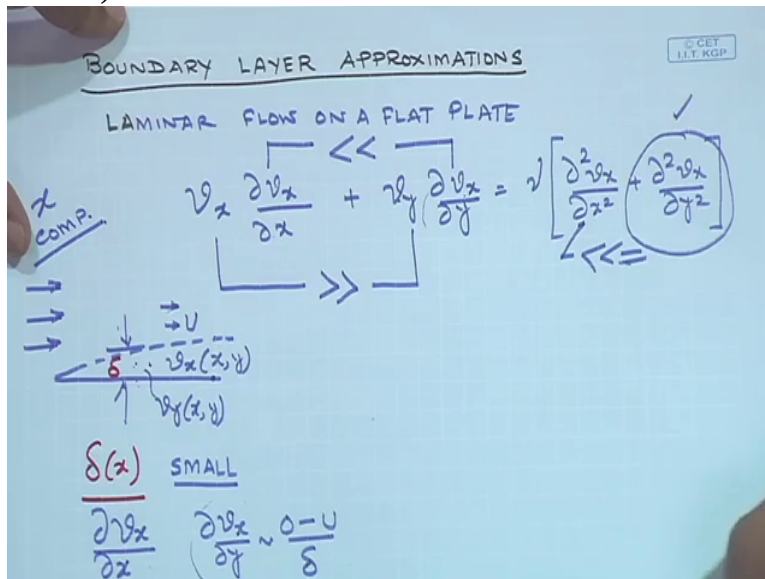
here we see that these are essentially telling me about the viscous transport in the x direction and viscous transport in the y direction, gradient of viscous transport in y direction. And from our discussion over here, we understand that this term is going to predominate and therefore

(Refer Slide Time 14:13)



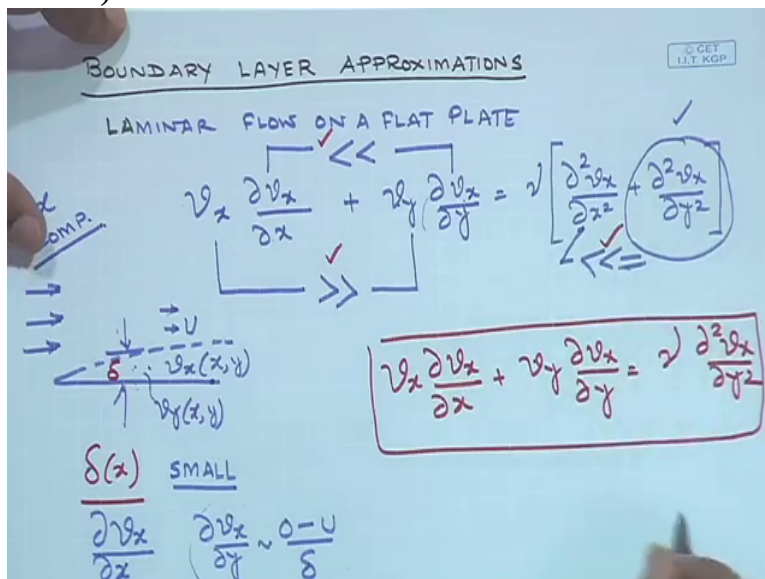
this is going to be quite large as compared to the this term so the second term is going to remain in the Navier–Stokes equation and the first term can simply be neglected.

(Refer Slide Time 14:28)



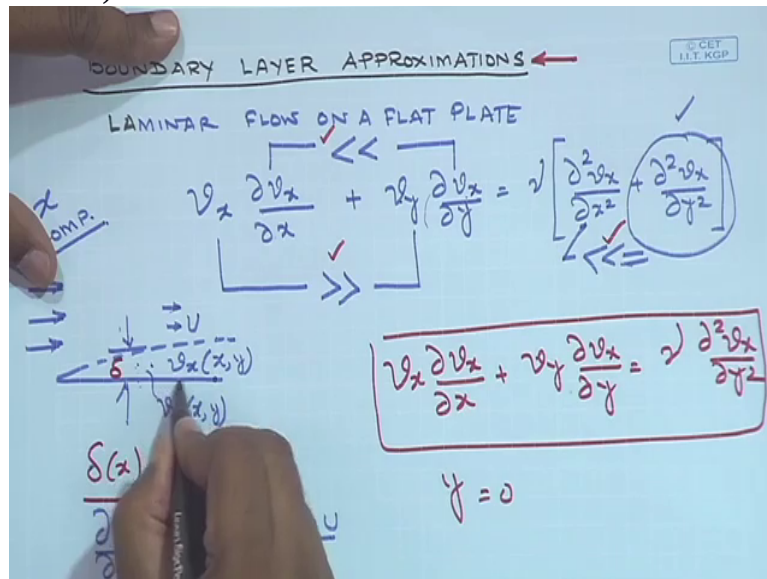
So the final form of Navier–Stokes equation for flow for inside a boundary layer on a flat plate can be written as this. And whatever I have discussed so far in terms of the magnitudes the relative magnitudes of these terms

(Refer Slide Time 14:56)



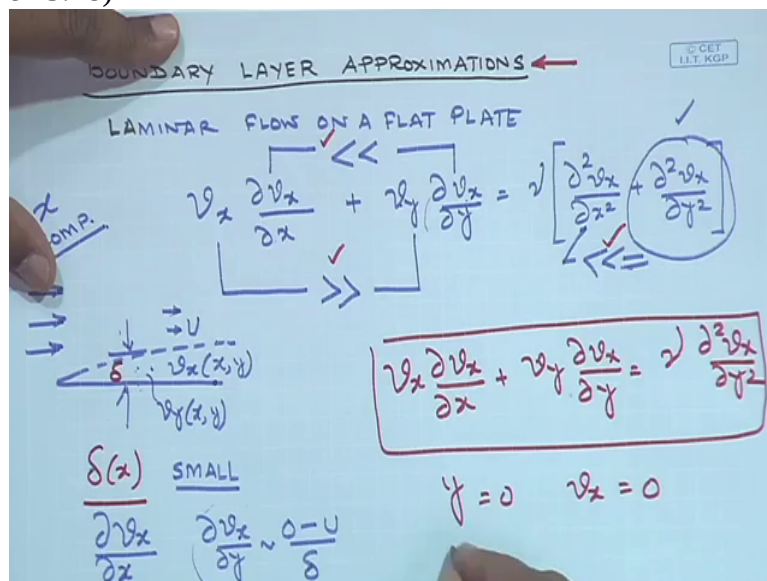
and their inter-relation, they are collectively known as the boundary layer approximations or the boundary layer assumptions so one has to solve this equation for flow inside a boundary layer with appropriate boundary conditions. And what we need is we need two conditions on y and the two conditions on y are at y equal to zero which is at

(Refer Slide Time 15:22)



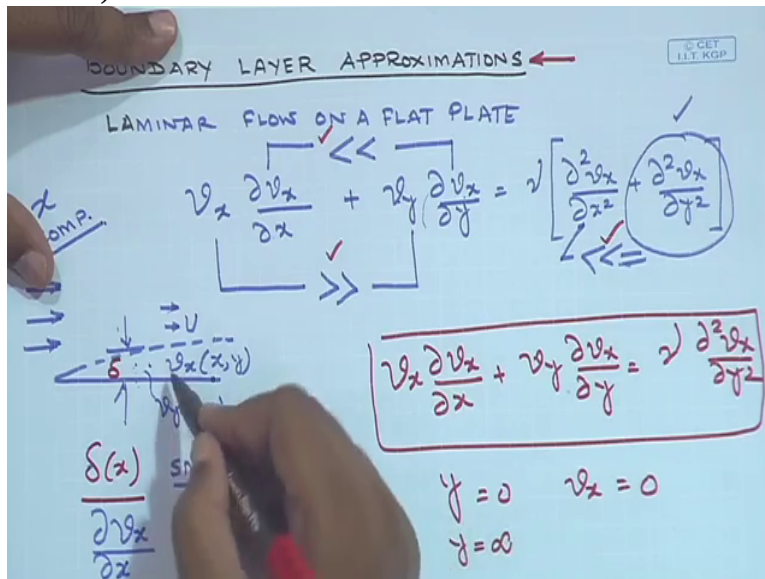
this point your simply v_x at no-slip condition would be zero and at

(Refer Slide Time 15:28)



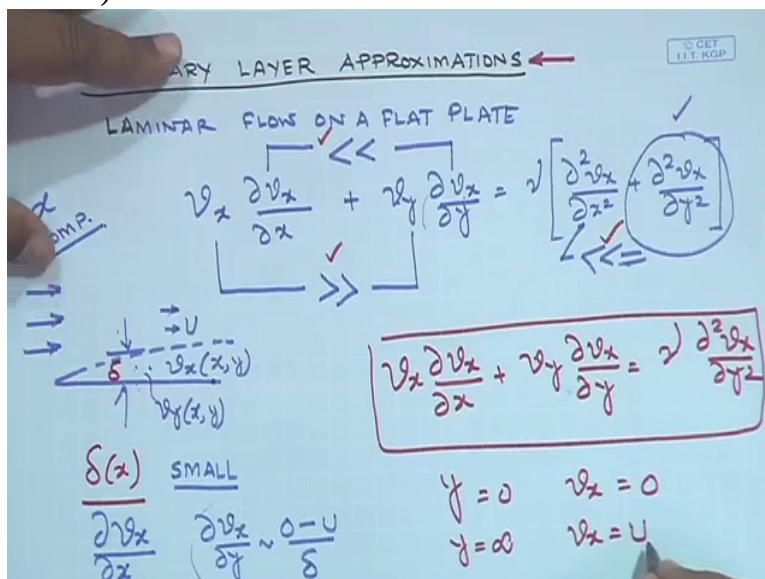
y equals infinity that means at

(Refer Slide Time 15:31)



a distance far from the wall the v_x would simply be equal to u where u is the freestream velocity, Ok.

(Refer Slide Time 15:40)



So these are the two conditions what we can say and the other condition, the initial condition is at x equals zero, v_x would simply be equals capital v where capital v is the velocity, the approach velocity and we understand for special case of flow over a flat plate, this v would simply be equal to u so the three conditions that are needed to solve this equation are at y equal to zero no-slip condition at y equals infinity at far from the flat plate, the velocity is equal to freestream velocity and at the beginning at x equal to zero, the velocity for the flat plate is

(Refer Slide Time 16:25)

BOUNDARY LAYER APPROXIMATIONS ←

LAMINAR FLOW ON A FLAT PLATE

x COMP.

$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \left[\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} \right]$

$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$

$\delta(x)$ SMALL

$\frac{\partial v_x}{\partial x} \left(\frac{\partial v_x}{\partial y} \sim \frac{0-U}{\delta} \right)$

- ✓ $y=0$ $v_x = 0$
- ✓ $y=\infty$ $v_x = U$
- ✓ $x=0$ $v_x = (V=U) = U$

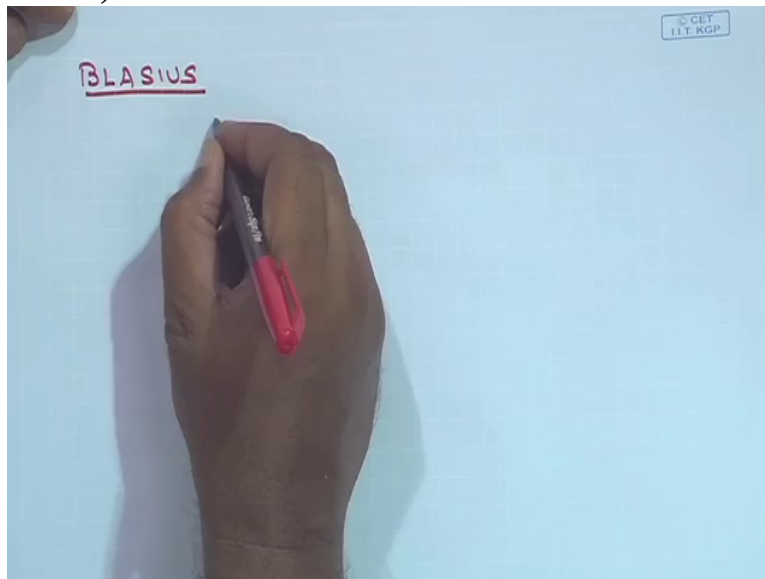
equal to the freestream velocity; so this equation has now to be solved for, for the, using the three boundary conditions Now whenever we come across

(Refer Slide Time 16:39)



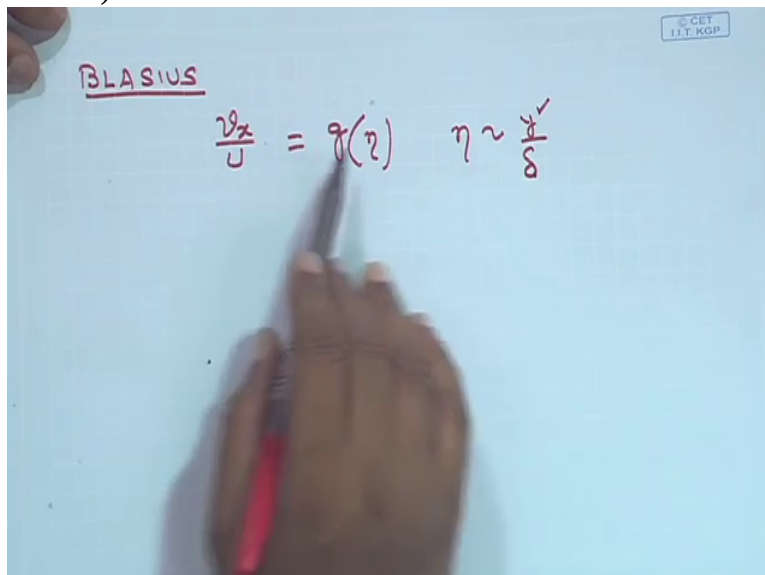
such an equation, the equation was first solved by Blasius and it's also known as the Blasius solution. What Blasius

(Refer Slide Time 16:51)



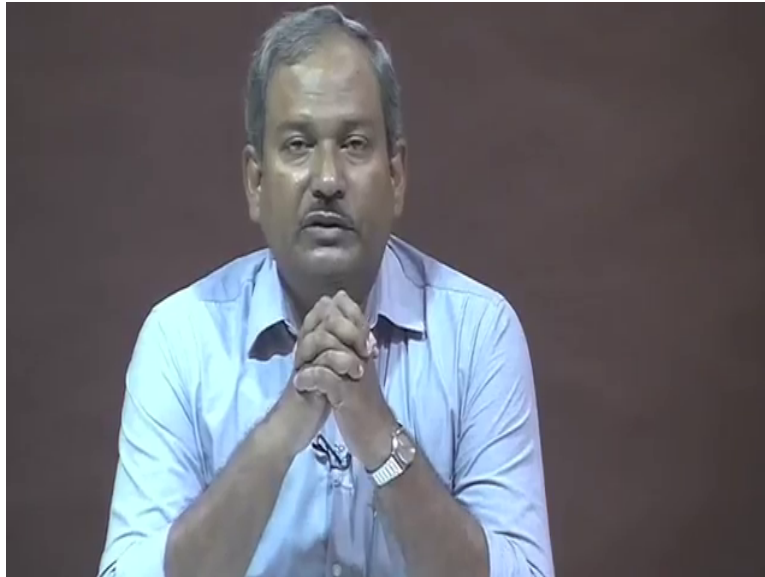
reasoned that the velocity profile, the dimensionless velocity profile should be similar for all values of x when plotted versus non-dimensional distance from the wall. So he has reasoned it's only an assumption that $v \times y / u$ would be a function would be function of η where η is y by δ y is the distance from the wall, δ is the boundary layer thickness at that point. So the dimensionless velocity is going to be a

(Refer Slide Time 17:29)



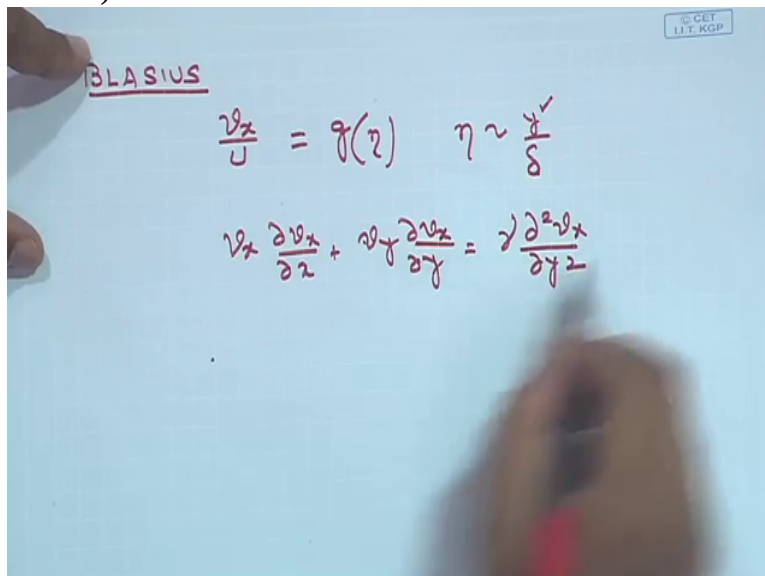
function of dimensionless distance from the solid wall, which, which is logical, because if you,

(Refer Slide Time 17:37)



you think of the velocity, the dimensionless velocity profile it is definitely going to be a function of distance from the solid wall. But since the velocity is non-dimensionalized we need to non-dimensionalize the distance from the solid wall as well. So the, the only dimension which is physically significant in a direction perpendicular to that of the flow has to be, the thickness of the boundary layer. So eta which is the independent variable in this case is defined as some sort of equal to y by δ where δ is the dimensionless thickness. But if you go to the previous slide where I have written down the equation to be solved for the case of flow inside the boundary layer this is not the only

(Refer Slide Time 18:41)



equation, this I call as equation two, this is not the only equation that needs to be solved. Whatever be the solution that must also satisfy the equation of continuity which being the equation of conservation of mass must

(Refer Slide Time 19:01)

BLASIUS

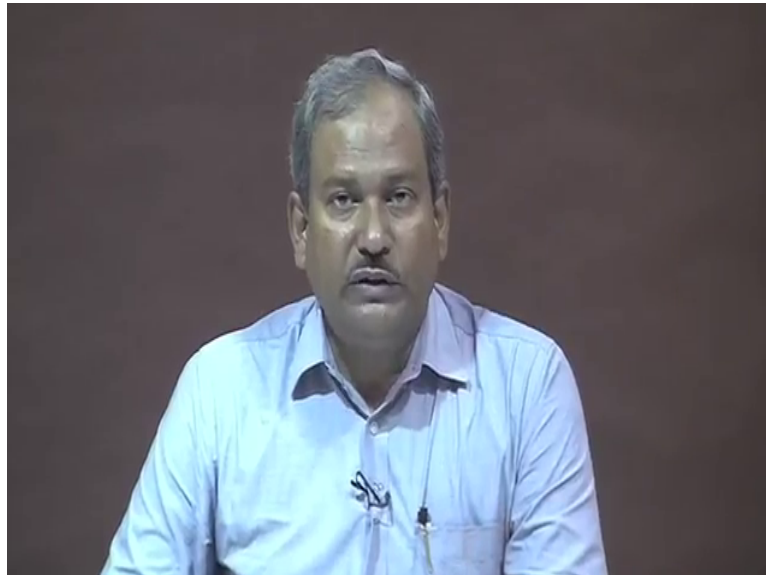
$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y}{\delta}$$

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad \text{--- (2)}$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad \text{--- (1)}$$

always be satisfied. So the two equations which are

(Refer Slide Time 19:06)



to be satisfied for describing flow inside a boundary layer, the first one being equation of continuity, conservation that has to be uh respected at all times and the second one is the equation of motion or the reduced form of equation of motion using the approximations that I have described commonly known as the boundary layer approximations. So I have two equations to deal with. Now it is sometimes advisable that instead of using two equations, if I could reduce it to one equation then it would be probably be, obviously it would be easier to

handle. So I need to do something such that is it possible to do something such that these two equations would reduce to only one equation, such that I need to solve one equation instead of the two equations that I have right now.

And the way to do that is to define something which would automatically ensure that the equation of continuity is satisfied and the way to do that is to do that is to introduce the concept of stream function which from your fluid mechanics you already know that the velocities, in this case the velocities in the x direction and the y direction can be expressed in terms of a stream function which describes the flow and you also probably remember that what are the properties of the stream function like the distance between the stream functions essentially denote what is the volumetric flow rate between, between these two, two stream functions can never cross each other and the tangent to the streamline is, essentially gives you the direction of the velocity at the specific point. But anyway, we have, we know that velocities can be expressed in terms of stream function. So we, we understand that v_x by definition would be $\frac{\partial \psi}{\partial y}$ where ψ is

(Refer Slide Time 21:12)

BLASIUS

$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y}{\delta}$$

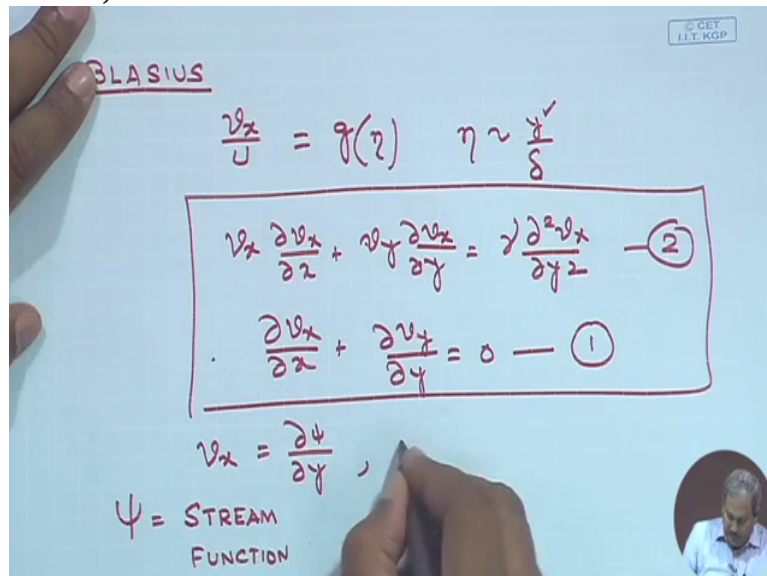
$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad \text{--- (2)}$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad \text{--- (1)}$$

$$v_x = \frac{\partial \psi}{\partial y}$$

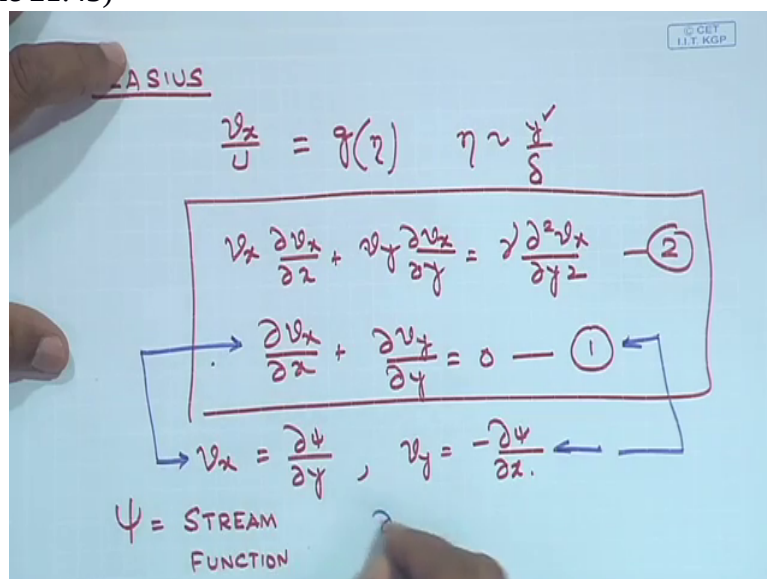
the stream function And v_y

(Refer Slide Time 21:22)



would be minus del chi by del x. So if you look at these two definitions of v_x and v_y and if you plug them into equation 1, what you see is it is going to be

(Refer Slide Time 21:43)



del chi del x del y and this one is going to be del chi del y del x. And chi being an exact differential, the order of the, order of the derivative is unimportant so therefore the result of this would be equal to zero,

(Refer Slide Time 22:15)

BLASIUS

$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y}{\delta} \sqrt{x}$$

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad \text{--- (2)}$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad \text{--- (1)}$$

$$v_x = \frac{\partial \psi}{\partial y}, \quad v_y = -\frac{\partial \psi}{\partial x}$$

$\psi =$ STREAM FUNCTION

$$\frac{\partial^2 \psi}{\partial x^2} - \frac{\partial^2 \psi}{\partial y^2} = 0$$

ψ EXACT DIFFERENTIAL

so since the order of differentiation is unimportant, irrelevant for the case of exact differential, so del chi by del x del y and del chi by del y del x are essentially equal and since we have a minus n here, the equation of continuity automatically gets satisfied the moment we start to express v x in terms of

(Refer Slide Time 22:41)

BLASIUS

$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y}{\delta} \sqrt{x}$$

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad \text{--- (2)}$$
~~$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad \text{--- (1)}$$~~

$$v_x = \frac{\partial \psi}{\partial y}, \quad v_y = -\frac{\partial \psi}{\partial x}$$

$\psi =$ STREAM FUNCTION

$$\frac{\partial^2 \psi}{\partial x^2} - \frac{\partial^2 \psi}{\partial y^2} = 0$$

ψ EXACT DIFFERENTIAL

a stream function, v x and v y in terms of stream functions So now we do not have

(Refer Slide Time 22:47)

BLASIUS

$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y\sqrt{x}}{\delta}$$

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad (2)$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad (1)$$

$v_x = \frac{\partial \psi}{\partial y}$, $v_y = -\frac{\partial \psi}{\partial x}$

$\psi = \text{STREAM FUNCTION}$

the equation of continuity any more It's automatically satisfied so we just have one equation

(Refer Slide Time 22:54)

BLASIUS

$$\frac{v_x}{U} = f(\eta) \quad \eta \sim \frac{y\sqrt{x}}{\delta}$$

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2} \quad (2)$$

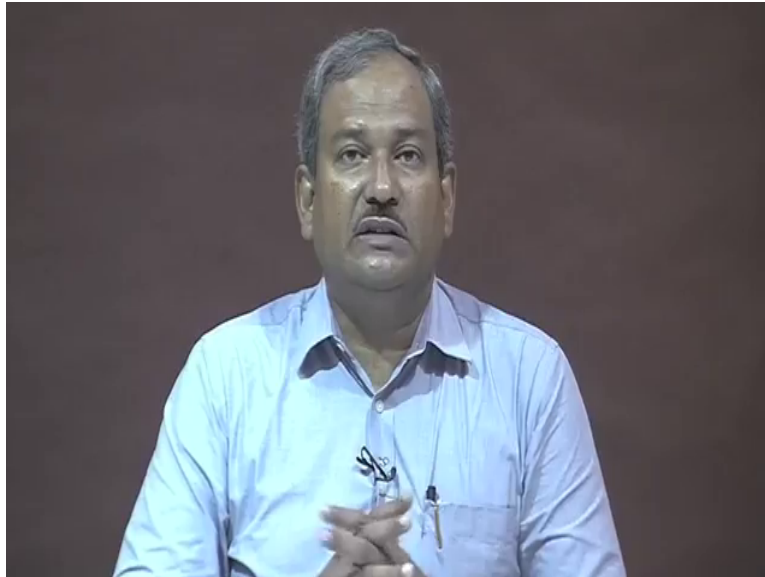
$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \quad (1)$$

$v_x = \frac{\partial \psi}{\partial y}$, $v_y = -\frac{\partial \psi}{\partial x}$

$\psi = \text{STREAM FUNCTION}$

to deal with which is the

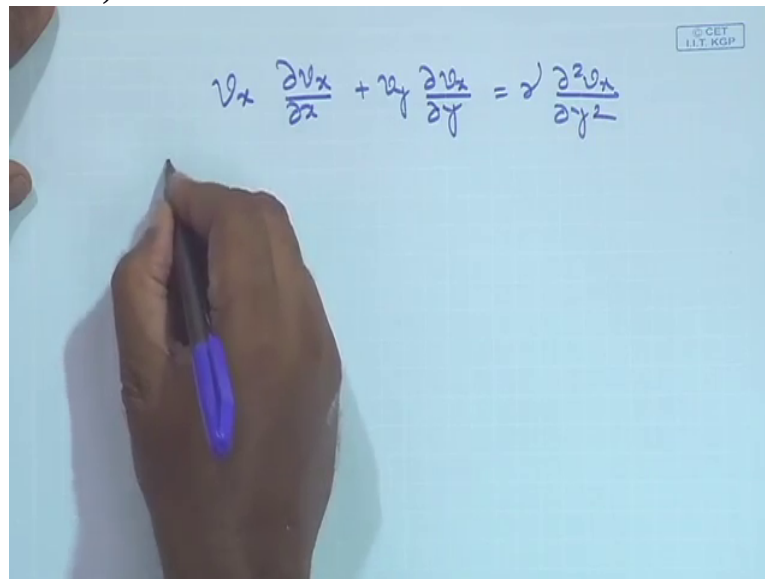
(Refer Slide Time 22:56)



equation of continuity, which is the equation of motion So bringing in the concept of stream function allows me to substantially reduce the complexity of the problem. The next, it is still a partial differential equation, v_x and v_y are functions of both x and y . x and y are both independent variables. So is it possible somehow to club these two independent variables and define a new independent variable which is, which is a result of x and y in a certain form related to the new dimensionless variable and then express v_x , v_y and χ in terms of the new variable. I will repeat this once again. What we see here is we are dealing with the partial differential equation in the form of equation of motion. It would be even simpler if we can revert this partial differential equation to an ordinary differential equation.

And since v_x and v_y are functions of x and y , two independent variables, if I can club two independent variables in a specific way such that I end up with only one independent variable and v_x and v_y are now not functions of x and y but functions of the new independent variable. Now in that case, I then have, instead of a partial differential equation I have an ordinary differential equation where v_x and v_y are functions of only one variable which is some sort of the combination of the two independent variables x and y . So the method of converting a partial differential equation to an ordinary differential equation by combining the independent variables in a specific way is known as the method of combination of variables. So we will see how the method of combination of variables can give a solution to this specific problem. And we would first, our aim is to obtain an expression, a relation between x and y . So I start with this equation again and try to see what is going to happen if I do an order of magnitude analysis of this equation near the boundary layer.

(Refer Slide Time 25:40)

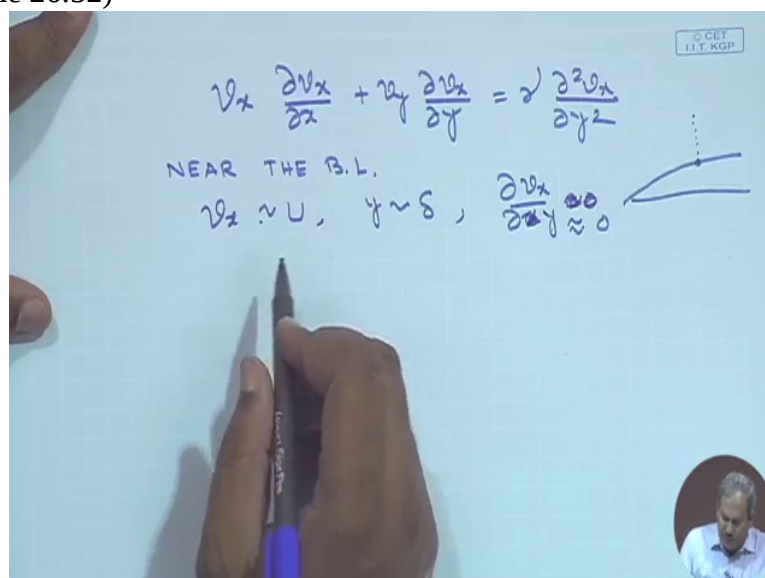


A hand is writing the following partial differential equation on a whiteboard:

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$$

So what is going to happen near the boundary layer, I am going to make a judgment on that. Near the boundary layer, v_x is approximately going to be equal to u , y is essentially equal to δ and since the velocity does not change, v_x does not change beyond the boundary layer, $\frac{\partial v_x}{\partial x}$ sorry $\frac{\partial v_x}{\partial y}$ is going to be equal to zero. So if this is the boundary layer, v_x does not vary with y beyond the boundary layer. So at the edge of the boundary layer the variation in axial component of velocity with y is approximately equal to zero. So if we, if we see this then what we, what we are going to do is

(Refer Slide Time 26:32)



A hand is writing the following text and diagram on a whiteboard:

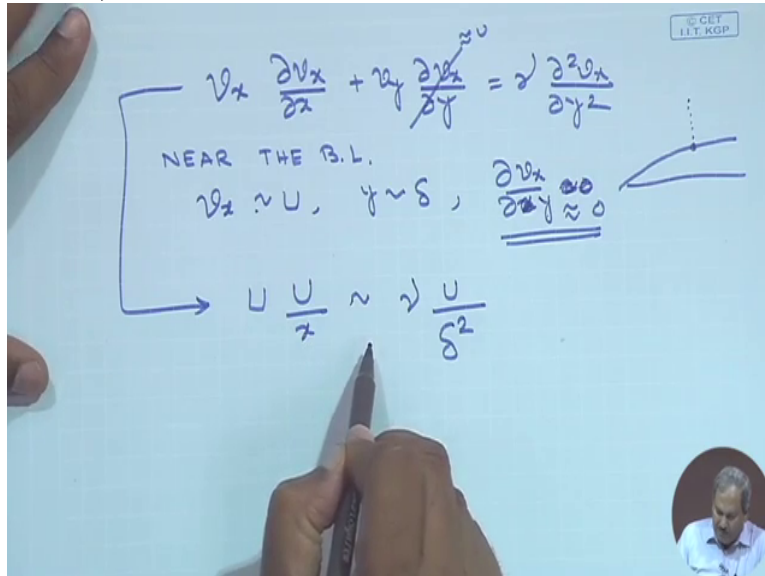
NEAR THE B.L.
 $v_x \sim U, \quad y \sim \delta, \quad \frac{\partial v_x}{\partial y} \approx 0$

The diagram shows a boundary layer profile with a dashed vertical line indicating the boundary layer thickness δ .

I am going to write this equation, the approximate form of this equation is as u instead of v_x u by x which would be equal to this this part is going to be approximately equal to zero since I have written over here and this is going to be equals ν and then what I have u and the value

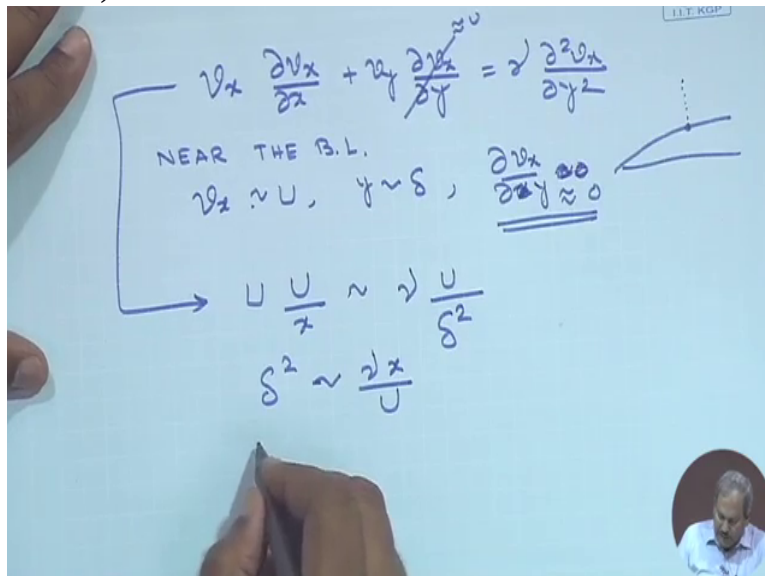
of y is going to be equal to delta; so the relation that you get over here, the approximate relation that you are going to get based on an approximation,

(Refer Slide Time 27:09)



based on order of magnitude analysis, as scaling parameter what you would see is that delta square is going to be equal to nu times x by u. And your delta

(Refer Slide Time 27:24)



is simply going to be equal to or approximately equal to nu x by u; so if I define my new dimensionless variable eta to be y by delta as we have done before, this would simply be equal to y u by nu x. So this is the combination variable that

(Refer Slide Time 27:52)

Handwritten derivation on a whiteboard:

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$$

NEAR THE B.L.
 $v_x \sim U, \quad y \sim \delta, \quad \frac{\partial v_x}{\partial y} \approx 0$

$$U \frac{U}{x} \sim \nu \frac{U}{\delta^2}$$

$$\delta^2 \sim \frac{\nu x}{U}$$

$$\delta \sim \sqrt{\frac{\nu x}{U}}$$

$$\eta = \frac{y}{\delta} = y \sqrt{\frac{U}{\nu x}}$$

A small diagram on the right shows a boundary layer profile over a flat surface, with a vertical dashed line indicating the boundary layer thickness δ .

contains both y and x in a specific functional form and the functional form is essentially y by root over x and we have these two terms which come from an order of magnitude analysis of the equation near the boundary layer at the edge of the boundary layer. So approximately it gives me a form of δ in terms of x ,

(Refer Slide Time 28:20)

Handwritten derivation on a whiteboard, identical to the previous slide:

$$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$$

NEAR THE B.L.
 $v_x \sim U, \quad y \sim \delta, \quad \frac{\partial v_x}{\partial y} \approx 0$

$$U \frac{U}{x} \sim \nu \frac{U}{\delta^2}$$

$$\delta^2 \sim \frac{\nu x}{U}$$

$$\delta \sim \sqrt{\frac{\nu x}{U}}$$

$$\eta = \frac{y}{\delta} = y \sqrt{\frac{U}{\nu x}}$$

The final result $\delta \sim \sqrt{\frac{\nu x}{U}}$ is enclosed in a red rectangular box.

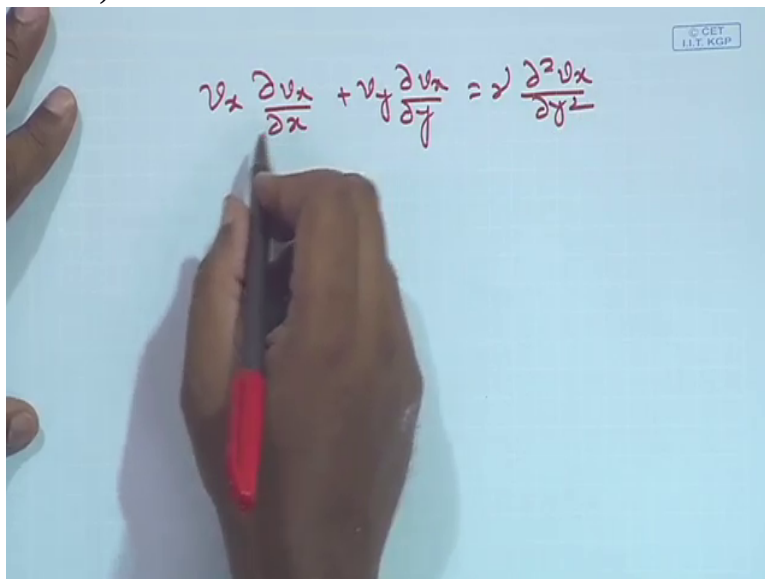
δ is the film thickness which is only a function of x ; δ is the boundary layer thickness which is only a function of x . So it gives me δ as a function of x and since the dimensionless distance is defined as y by δ , so it is of the form of this only. So therefore my equation, the equation that I have over here, the equation of motion

(Refer Slide Time 28:49)



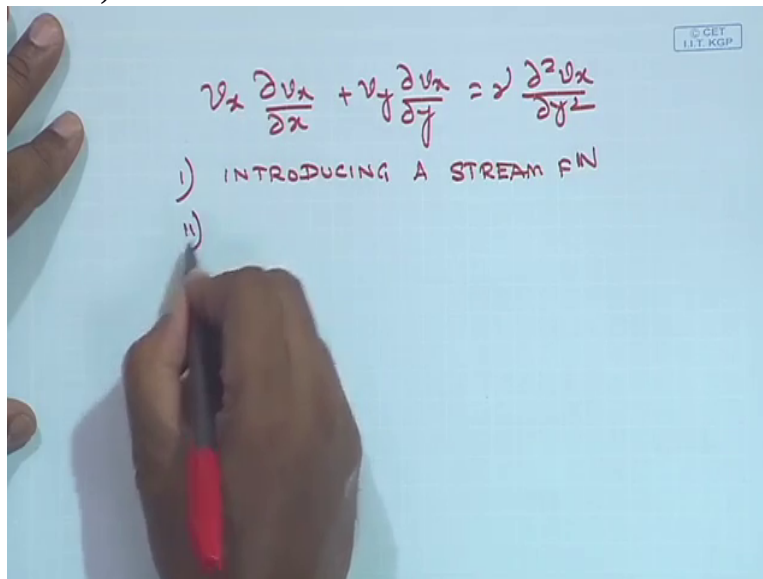
which is $v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y}$ is equal to $\nu \nabla^2 v_x$. This can

(Refer Slide Time 29:03)



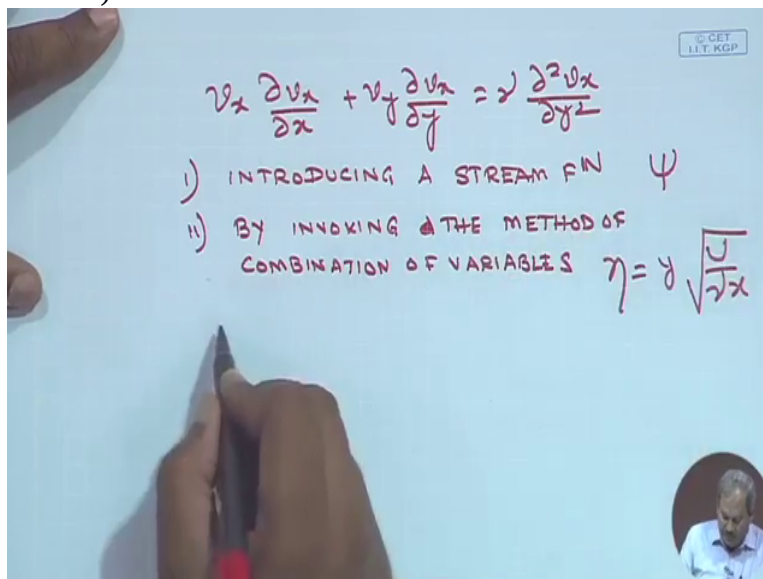
now be, now be handled first by introducing a stream function and second is by

(Refer Slide Time 29:20)



invoking the method of combination of variables And the stream function that we have defined is chi and the, combination variable that we have defined is eta equals y root over u by nu x. And since stream function, since I am going to make everything dimensionless,

(Refer Slide Time 30:07)



I am defining a dimensionless stream function which is f equals chi by root over nu x u. This dimensionless stream function is a function only of eta;

(Refer Slide Time 30:29)

$v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$

i) INTRODUCING A STREAM FN ψ

ii) BY INVOKING THE METHOD OF COMBINATION OF VARIABLES $\eta = y \sqrt{\frac{U}{\nu x}}$

DIMENSIONLESS STR. FN

$$f(\eta) = \frac{\psi}{\sqrt{\nu x U}}$$

so next what is remaining is to convert the equation, the governing equation in terms of the stream function and in terms of the new independent variable eta; so instead of

(Refer Slide Time 30:45)

$\rightarrow v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$

i) INTRODUCING A STREAM FN ψ

ii) BY INVOKING THE METHOD OF COMBINATION OF VARIABLES $\eta = y \sqrt{\frac{U}{\nu x}}$

DIMENSIONLESS STR. FN

$$\underline{f(\eta) = \frac{\psi}{\sqrt{\nu x U}}}$$

v_x, v_y as a function of x and y , I need to have $f(\eta)$ as a function only of η . If I can do that, this gives rise to a p d e but since $f(\eta)$ is a function

(Refer Slide Time 31:02)

$$\rightarrow v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$$

1) INTRODUCING A STREAM FN ψ
2) BY INVOKING THE METHOD OF COMBINATION OF VARIABLES

$$\eta = y \sqrt{\frac{U}{\nu x}}$$

DIMENSIONLESS STR. FN

$$f(\eta) = \frac{\psi}{\sqrt{\nu x U}}$$

$f(\eta) \rightarrow \eta$

v_x, v_y
 x, y
PDE

only of eta this will give rise to an o d e. So in the next class I am going to just see how this transformation

(Refer Slide Time 31:12)

$$\rightarrow v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} = \nu \frac{\partial^2 v_x}{\partial y^2}$$

1) INTRODUCING A STREAM FN ψ
2) BY INVOKING THE METHOD OF COMBINATION OF VARIABLES

$$\eta = y \sqrt{\frac{U}{\nu x}}$$

DIMENSIONLESS STR. FN

$$f(\eta) = \frac{\psi}{\sqrt{\nu x U}}$$

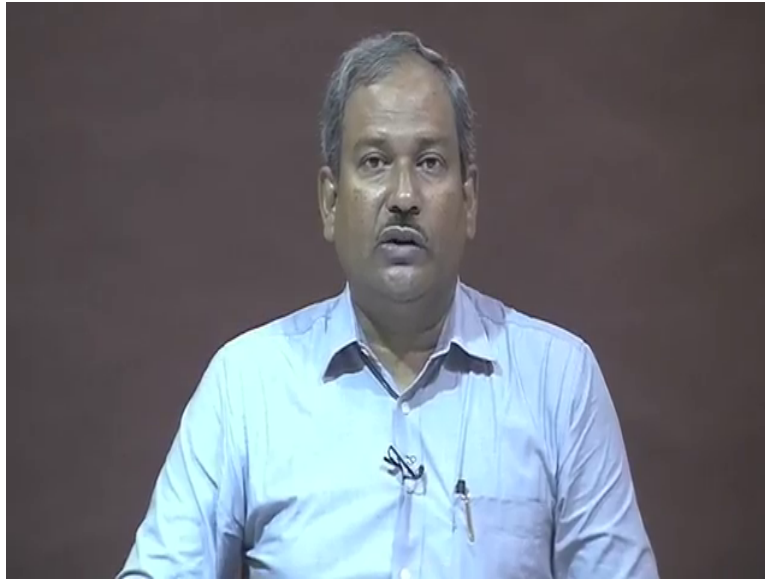
$f(\eta) \rightarrow \eta$

v_x, v_y
 x, y
PDE

ODE \leftrightarrow PDE

from p d e to o d e takes place and that would allow us to solve this

(Refer Slide Time 31:17)



equation in a more meaningful way, in a more easy manner also eliciting fundamental information about what happens at the edge and on the solid surface for flow inside a boundary layer