

Advanced Mathematical Techniques in Chemical Engineering

Prof. S. De

Department of Chemical Engineering

Indian Institute of Technology, Kharagpur

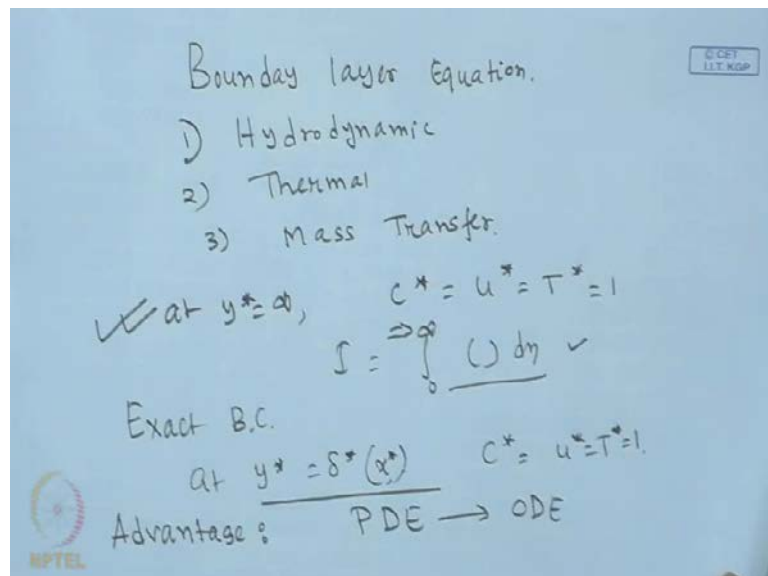
Lecture No. # 39

Integral Method

Welcome to the session of this class. We will be starting with the integral method of solution for solving the partial differential equation. In the last lecture, we have looked into how similarity method of solution can be applied for the solution of partial differential equation.

In this class, we will be looking into the integral method of analysis. Integral method of analysis is quite common, when we are talking about the boundary layer analysis or boundary layer theory.

(Refer Slide Time: 00:48)



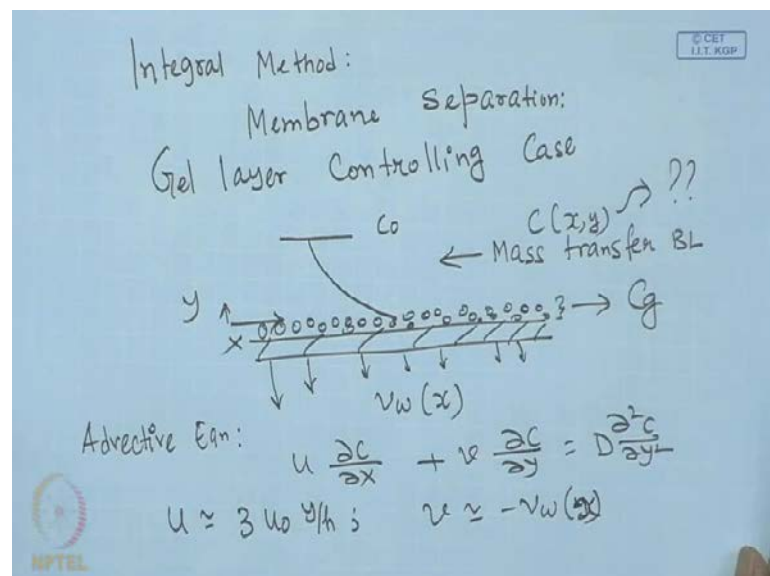
For solution of boundary layer equation, one can use the integral method of solution. In case of three types of boundary layer; hydrodynamic boundary layer, thermal boundary layer and mass transfer boundary layer; one can utilize the integral method of solution. The only difference between this solution and the similarity solution is that, if you

remember at y^* is equal to infinity that was one of the typical boundary condition in similarity solution, where we use to put c^* is equal to u^* is equal to T^* is equal to 1. When **it**, we evaluate the definite integral from 0 to infinity in similarity parameter, we said that we have to carry out this thing numerically but infinity becomes unknown. We have to put an upper limit let us say 5 or 10 then you have to increase the upper limit from 10 to 15 and see whether the result of this integral changes or not. If it does not change over through four decimal places for some value then that will be given by the infinity.

That becomes the problem. In case of integral method analysis, we are substituting this by the exact boundary condition. What is the exact boundary condition? At y^* is equal to δ^* c^* is equal to u^* is equal to T^* is equal to 1. In effect, this δ^* becomes a function of independent variable; either x^* or T in case of transient analysis.

Therefore, this is the only difference between the similarity solution and integral method solution. In case of integral method solution, we are replacing the boundary condition instead of y^* equal to infinity; we are replacing it by the exact boundary condition at δ^* .

(Refer Slide Time: 03:29)



What is the advantage? The advantage is that we will reduce the partial differential equation into an ordinary differential equation that is the advantage of similarity solution.

We will take up an example of the similarity solution, the integral method of solution. The example will be talking about the same problem on membrane based separation process as we have defined earlier; this is a flow through a thin channel. We will be considering a flow through a thin channel and it is a gel layer controlling case.

Here, there is a flow through a thin channel; on this is a membrane surface and these are pores on it. We put lots of you know particles, they form a viscous layer known as the gel layer and over that there is a concentration profile, this is at y is equal to δ .

So, y starts from here and x start from there. The concentration within the gel layer is constant and it is gel layer concentration. Since, the bulk concentration varies from c_{∞} to C_g ; there exists a concentration profile within the concentration boundary layer or this is the mass transfer boundary layer.

Within the mass transfer boundary layer C is a function of x and y . You will be getting the permeate flux which will be a function of x . Therefore, our aim is to find out what is the concentration profile C as a function of x and y in the mass transfer boundary layer; with that we define that aim. We write down the governing equation within the mass transfer boundary layer.

The advective two dimensional equation becomes $u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y}$ is equal to $D \frac{\partial^2 c}{\partial y^2}$. The same that we have done earlier, u becomes $\frac{3}{2} u_0 \left(1 - \frac{y^2}{h^2}\right)$ that is the velocity profile that we have seen earlier in the thin channel and v is equal to minus $\frac{v_0}{h} y$, v_0 as a function of x .

We have discussed about this profile of velocity in the earlier class. I am just taking them as they are. We are going to solve this equation by making it non-dimensional.

(Refer Slide Time: 06:23)

Non-dimensionalization:

$$x^* = x/L; \quad y^* = y/h; \quad c^* = c/c_0$$

$$3u_0 \frac{y}{h} \frac{\partial c}{\partial x} - v_w \frac{\partial c}{\partial y} = D \frac{\partial^2 c}{\partial y^2}$$

$$\frac{3u_0}{L} y^* \frac{\partial c^*}{\partial x^*} - \frac{v_w}{h} \frac{\partial c^*}{\partial y^*} = \frac{D}{h^2} \frac{\partial^2 c^*}{\partial y^{*2}}$$

$$\frac{3u_0 h^2}{DL} y^* \frac{\partial c^*}{\partial x^*} - \frac{v_w h}{D} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}$$

$$h \approx \frac{1}{4} d_e$$

$$\Rightarrow \frac{3}{16} \frac{u_0 d_e^2}{DL} y^* \frac{\partial c^*}{\partial x^*} - \frac{1}{4} \frac{v_w d_e}{D} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}$$

Let us make the equation non-dimensional first. We make the equation non-dimensional against these quantities: x^* is equal to x by L , y^* is equal to y by h , c^* is equal to c by c_0 . This becomes $3 u_0 y$ by h , we write down the, you put the velocity profile $\frac{\partial c}{\partial x}$ minus $v_w \frac{\partial c}{\partial y}$ is equal to $D \frac{\partial^2 c}{\partial y^2}$.

Then, we substitute the non-dimensional in terms of non-dimensional variable. This becomes $\frac{3 u_0}{L} y^* \frac{\partial c^*}{\partial x^*}$ minus $\frac{v_w}{h} \frac{\partial c^*}{\partial y^*}$ is equal to $\frac{D}{h^2} \frac{\partial^2 c^*}{\partial y^{*2}}$; multiply both sides by h^2 by D . This becomes $\frac{3 u_0 h^2}{DL} y^* \frac{\partial c^*}{\partial x^*}$ minus $\frac{v_w h}{D} \frac{\partial c^*}{\partial y^*}$ is equal to $\frac{\partial^2 c^*}{\partial y^{*2}}$.

We have already seen that half height can be approximated as one-fourth of equivalent diameter. Therefore, in terms of equivalent diameter we will be having $\frac{3}{16} \frac{u_0 D^2}{DL} y^* \frac{\partial c^*}{\partial x^*}$ minus $\frac{1}{4} \frac{v_w d_e}{D} \frac{\partial c^*}{\partial y^*}$ is equal to $\frac{\partial^2 c^*}{\partial y^{*2}}$.

We have already seen that $\frac{u_0 d^2}{DL}$ is nothing but 3 by Reynold Schmidt D by L and $\frac{1}{4} \frac{v_w d_e}{D}$ is nothing but the non-dimensional $(())$ number at the wall.

(Refer Slide Time: 08:55)

$$\frac{3}{16} \text{Re Sc} \frac{d\delta}{L} y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}$$

$$\boxed{A y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}}$$

at $x^* = 0, c^* = 1 \checkmark$

at $y^* = \delta^*, c^* = 1 \checkmark$

at $y^* = 0, v_w c + D \frac{\partial c}{\partial y} = 0$
 $\Rightarrow \boxed{P_{ew} c_g + \frac{\partial c^*}{\partial y^*} = 0} \checkmark$

We write it down as $\frac{3}{16} \text{Re Sc} \frac{d\delta}{L} y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}$. So, once we get that this is basically nothing but a constant; it depends on the operating condition. Let us write it down as A. This equation becomes $A y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*} = \frac{\partial^2 c^*}{\partial y^{*2}}$. This becomes the governing equation. We have already derived this governing equation earlier.

Let us put the initial and boundary condition; at x^* is equal to 0 we had c^* is equal to 1, at y is equal to 0 y is equal to δ , c^* is equal to c_{naught} , c is equal to c_{naught} , c^* is equal to 1 at y^* equal to δ^* . Let us put, at y^* is equal to 0 $v_w c + D \frac{\partial c}{\partial y}$ is equal to 0. That was the boundary condition at y equal to 0.

Therefore, we make it non-dimensional; $P_{ew} c_g$ at y^* is equal to 0 is c_g , that is constant plus $\frac{\partial c^*}{\partial y^*}$ is equal to 0. So, these three, this is an initial condition at x^* is equal to 0; this is the condition at y^* is equal to δ^* and this is the condition at y^* is equal to 0.

(Refer Slide Time: 11:09)

Assume a concn. profile c^* within MTBL

c^* should satisfy

at $y^* = \delta^* \Rightarrow c^* = 1$ ✓

at $y^* = \delta^*, \frac{\partial c^*}{\partial y^*} = 0$ ✓

at, $y^* = 0, c^* = c_g^*$ ✓

Assume quadratic concentration profile involving three constants:

$$c^* = c_{g0} = a_0 + a_1 \left(\frac{y^*}{\delta^*} \right) + a_2 \left(\frac{y^*}{\delta^*} \right)^2$$

Approximate Analysis

$$\Rightarrow c_g^* = a_0 \mid c^* = c_g^* + a_1 \left(\frac{y^*}{\delta^*} \right) + a_2 \left(\frac{y^*}{\delta^*} \right)^2$$

So, with this we assume a concentration profile of c^* within the mass transfer boundary layer. Next, what we do is we assume a concentration profile within the mass transfer boundary layer; profile c^* within mass transfer boundary layer. The necessary condition of the mass transfer boundary is that the concentration profile c^* should satisfy or at y^* is equal to δ^* , c^* is equal to 1; at y^* is equal to δ^* , $\frac{\partial c^*}{\partial y^*}$ is equal to 0, these are the boundary layer conditions. Any boundary layer must be satisfying these two conditions. For a thermal boundary layer y^* equal to δ^* , T^* should have been one and $\frac{\partial T^*}{\partial y^*}$ should have been 0.

Also, we have a boundary condition that y^* is equal to 0; c^* is equal to c_g^* . Therefore, there are three boundary conditions that the concentration profile must satisfy. **So, at least you should have,** we should assume a quadratic concentration profile involving three constants. We assume a concentration profile c^* is equal to c_g^* plus $a_1 \frac{y^*}{\delta^*}$ plus $a_2 \left(\frac{y^*}{\delta^*} \right)^2$. Since, this concentration profile is assumed within the mass transfer boundary layer, we call the integral method as approximate analysis.

We apply these three boundary conditions and see what we get. At y^* is equal to 0; c^* is equal to c_g^* . Therefore, c_g^* is nothing but a 0; the last two terms will vanish. Therefore, the concentration profile looks something like this, c^* is equal to c_g^* plus $a_1 \frac{y^*}{\delta^*}$ plus $a_2 \left(\frac{y^*}{\delta^*} \right)^2$.

(Refer Slide Time: 14:21)

$$\begin{aligned}
 \text{At } y^* = \delta^*, \quad 1 &= c_g^* + a_1 + a_2 \checkmark \\
 \text{At } y^* = \delta^*, \quad \frac{\partial c^*}{\partial y^*} &= 0 \Rightarrow 0 = \frac{a_1}{\delta^*} + 2a_2 \frac{y^*}{\delta^{*2}} \bigg|_{y^* = \delta^*} \\
 a_1 &= -2a_2 \checkmark \\
 1 &= c_g^* - 2a_2 + a_2 = c_g^* - a_2 \\
 \Rightarrow a_2 &= c_g^* - 1 \quad \& \quad a_1 = -2(c_g^* - 1) \\
 c^* &= c_g^* - 2(c_g^* - 1) \left(\frac{y^*}{\delta^*} \right) + (c_g^* - 1) \left(\frac{y^*}{\delta^*} \right)^2 \\
 \delta^* &= \delta^*(x^*)
 \end{aligned}$$

That gives the concentration profile. We have two constants to be evaluated, a_1 and a_2 . Let us utilize the two boundary conditions that the concentration profile must satisfy. At y^* is equal to δ^* , we had c^* is equal to 1. **So, this**, therefore, 1 is equal to $c_g^* + a_1 + a_2$ and at y^* is equal to δ^* , $\frac{\partial c^*}{\partial y^*}$ is equal to 0. We have 0 is equal to $\frac{a_1}{\delta^*} + 2a_2 \frac{y^*}{\delta^{*2}}$ evaluated at y^* is equal to δ^* .

One δ^* will be cancelling over here and one will be cancelling from there in the denominator. **So, this becomes** a_1 becomes minus $2a_2$. We will combine these two boundary conditions and get a_1 and a_2 . We will be getting 1 is equal to $c_g^* - 2a_2 + a_2$ a_2 plus a_2 is equal to $c_g^* - a_2$. Therefore, a_2 becomes $c_g^* - 1$ and a_1 becomes minus $2(c_g^* - 1)$, we get the concentration profile c^* as $c_g^* - 2(c_g^* - 1) \frac{y^*}{\delta^*} + (c_g^* - 1) \left(\frac{y^*}{\delta^*} \right)^2$.

That gives the concentration profile. In this concentration profile everything is known, except how δ^* varies as a function of x^* , that is left behind. By using the integral method of solution we are exactly going to do that.

(Refer Slide Time: 14:24)

$$\begin{aligned}
 A y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*} &= \frac{\partial^2 c^*}{\partial y^{*2}} \\
 c^* &= c_g^* - 2(c_g^* - 1) \left(\frac{y^*}{\delta^*} \right) + (c_g^* - 1) \left(\frac{y^*}{\delta^*} \right)^2 \\
 \frac{\partial c^*}{\partial x^*} &= 2(c_g^* - 1) \frac{y^*}{\delta^{*2}} \frac{d\delta^*}{dx^*} + (c_g^* - 1) \frac{y^{*2}}{\delta^{*3}} (-2) \frac{d\delta^*}{dx^*} \\
 &= 2(c_g^* - 1) \frac{d\delta^*}{dx^*} \left(\frac{y^*}{\delta^{*2}} - \frac{y^{*2}}{\delta^{*3}} \right) \\
 \frac{\partial c^*}{\partial y^*} &= -2 \frac{(c_g^* - 1)}{\delta^*} + (c_g^* - 1) \frac{2y^*}{\delta^{*2}} \\
 \frac{\partial^2 c^*}{\partial y^{*2}} &= \frac{2(c_g^* - 1)}{\delta^{*2}}
 \end{aligned}$$

Let us look into the governing equation. The governing equation becomes $A y^* \frac{\partial c^*}{\partial x^*} - P_{ew} \frac{\partial c^*}{\partial y^*}$ is equal to $\frac{\partial^2 c^*}{\partial y^{*2}}$. We have the concentration profile as c^* is equal to $c_g^* - 2(c_g^* - 1) \frac{y^*}{\delta^*} + (c_g^* - 1) \left(\frac{y^*}{\delta^*} \right)^2$.

Sodel c star what do we do next? Exactly, like the earlier problem we evaluate different derivatives **that is** $\frac{\partial c^*}{\partial x^*}$, $\frac{\partial c^*}{\partial y^*}$, $\frac{\partial^2 c^*}{\partial y^{*2}}$ of c^* **from this governing**, from this profile and substitute back to the governing equation; $\frac{\partial c^*}{\partial x^*}$ is nothing but $2(c_g^* - 1) \frac{y^*}{\delta^{*2}} \frac{d\delta^*}{dx^*} + (c_g^* - 1) \frac{y^{*2}}{\delta^{*3}} (-2) \frac{d\delta^*}{dx^*}$, it will be $\frac{d\delta^*}{dx^*} \left(\frac{2y^*}{\delta^{*2}} - \frac{2y^{*2}}{\delta^{*3}} \right)$, so minus into minus, plus $\frac{d\delta^*}{dx^*} \left(\frac{2y^*}{\delta^{*2}} - \frac{2y^{*2}}{\delta^{*3}} \right)$, similarly, $\frac{\partial c^*}{\partial y^*} = -2 \frac{(c_g^* - 1)}{\delta^*} + (c_g^* - 1) \frac{2y^*}{\delta^{*2}}$. It takes $2(c_g^* - 1) \frac{d\delta^*}{dx^*}$ common, this becomes $\frac{d\delta^*}{dx^*} \left(\frac{2y^*}{\delta^{*2}} - \frac{2y^{*2}}{\delta^{*3}} \right)$; that goes for $\frac{\partial c^*}{\partial x^*}$.

Then we use derive, we take the derivative, $\frac{\partial c^*}{\partial y^*}$ is equal to $-2 \frac{(c_g^* - 1)}{\delta^*} + (c_g^* - 1) \frac{2y^*}{\delta^{*2}}$ and $\frac{\partial^2 c^*}{\partial y^{*2}}$ will be $\frac{2(c_g^* - 1)}{\delta^{*2}}$. We take the derivative of this equation; this becomes $\frac{d}{dx^*} \left(\frac{2(c_g^* - 1)}{\delta^{*2}} \right)$.

We will write down the governing equation. We just substitute everything there and see what we get.

(Refer Slide Time: 19:15)

$$A y^* \cdot 2(cg^* - 1) \left(\frac{y^*}{\delta^{*2}} - \frac{y^*}{\delta^{*3}} \right) \frac{d\delta^*}{dx^*} - P_{ew} 2(cg^* - 1) \left(-\frac{1}{\delta^*} + \frac{y^*}{\delta^{*2}} \right)$$

$$= \frac{2(cg^* - 1) y^*}{\delta^{*2}}$$

$$A \left(\frac{y^{*2}}{\delta^{*2}} - \frac{y^{*3}}{\delta^{*3}} \right) \frac{d\delta^*}{dx^*} - P_{ew} \left(-\frac{1}{\delta^*} + \frac{y^*}{\delta^{*2}} \right)$$

$$= \frac{1}{\delta^{*2}}$$

Take Zeroth moment
Multiply both sides by $y^0 dy$ & integrate over 0 to δ^*

Before that we utilize the governing equation. At A, we substitute the derivative $A y^*$, $\frac{dc^*}{dx^*}$ is nothing but $2cg^* - 1$ $\frac{y^*}{\delta^{*2}}$ by $\frac{d\delta^*}{dx^*}$ plus P_{ew} and $\frac{dc^*}{dy^*}$ minus $P_{ew} \frac{dc^*}{dy^*}$ is we take $2cg^* - 1$ common, $2cg^* - 1$ common, this becomes -1 by $\frac{d\delta^*}{dx^*}$ plus y^* by $\frac{d\delta^*}{dx^*}$ is equal to $\frac{d\delta^*}{dx^*} \frac{dc^*}{dy^*}$. This becomes $2cg^* - 1$ over $\frac{d\delta^*}{dx^*}$. We cancel both side by $2cg^* - 1$. It goes off and this becomes $A y^{*2}$.

This will be, $\frac{d\delta^*}{dx^*} y^* \frac{d\delta^*}{dx^*}$ minus, we had one more term, y^{*2} by δ^{*3} , this will be in common. So, A What we will be getting is $A y^{*2} \frac{d\delta^*}{dx^*} \frac{d\delta^*}{dx^*} - y^{*3} \frac{d\delta^*}{dx^*} - P_{ew} - 1$ by δ^{*2} plus y^* by δ^{*2} is equal to 1 over δ^{*2} .

What we do is we take zeroth moment of this equation, that means, multiply both sides by y to the power 0 dy and integrate over 0 to δ^* , that is the boundary layer thickness.

(Refer Slide Time: 22:10)

$$A \frac{d\delta^*}{dx^*} \int_0^{\delta^*} \left(\frac{y^{*2}}{\delta^{*2}} - \frac{y^{*3}}{\delta^{*3}} \right) dy^* - P_w \int_0^{\delta^*} \left(-\frac{1}{\delta^*} + \frac{y^*}{\delta^{*2}} \right) dy^*$$

$$= \frac{1}{\delta^{*2}} \int_0^{\delta^*} dy^*$$

$$A \frac{d\delta^*}{dx^*} \left[\frac{\delta^*}{3} - \frac{\delta^*}{4} \right] - P_w \left[-1 + \frac{1}{2} \right] = \frac{\delta^*}{\delta^{*2}}$$

$$\Rightarrow \frac{A\delta^*}{12} \frac{d\delta^*}{dx^*} + \frac{P_w}{2} = \frac{1}{\delta^*}$$

$$\Rightarrow \boxed{\frac{A\delta^{*2}}{12} \frac{d\delta^*}{dx^*} + \frac{P_w\delta^*}{2} = 1.0}$$

We multiply both sides by y to the power 0 dy . $A \frac{d\delta^*}{dx^*}$, this is a sole function of x , it will be taken out of the integral sign 0 to $\delta^* y^*^2$ divided by δ^*^2 minus y^*^3 divided by δ^*^3 dy^* minus P_w , that is a function of x only, it will be minus 1 by δ^* plus y^* by δ^*^2 0 to δ^* dy^* is equal to 1 by δ^*^2 dy^* 0 to δ^* .

We carry out this integration, this becomes $A \frac{d\delta^*}{dx^*}$ and this will be δ^*^3 divided by 3, it will be δ^* by 3 minus δ^* by 4, after integration minus P_w , after integration it will be minus 1 δ^* , δ^* will be cancelled out, it will be plus y^* square by 2, it will be half but δ^*^2 will be cancelled out and you will be having a δ^* over here in the numerator, you will be having δ^*^2 in the denominator, one will be cancelled out. This becomes $A \delta^*$ and this will be δ^* by 12 $A \delta^*$ by 12 $d\delta^* dx^*$, this will be minus half so minus minus plus P_w by 2 is equal to 1 by δ^* . You will be having $A \delta^*$ square by 12 $d\delta^* dx^*$ plus 1 plus $P_w \delta^*$ by 2 is equal to 1; this becomes the governing equation.

(Refer Slide Time: 24:51)

$$\begin{aligned} \text{at } y^* = 0, \quad P_w c_g^* + \frac{\partial c^*}{\partial y^*} &= 0 \\ \left. \frac{\partial c^*}{\partial y^*} \right|_{y^*=0} &= -2 \frac{(c_g^*-1)}{\delta^*} + \frac{(c_g^*-1) 2y^*}{\delta^{*2}} \\ &= -2 \frac{(c_g^*-1)}{\delta^*} \\ P_w c_g &= 2 \frac{(c_g^*-1)}{\delta^*} \quad \boxed{\frac{P_w \delta^*}{2} = \frac{c_g^*-1}{c_g^*}} \\ \frac{A \delta^{*2}}{12} \frac{d \delta^*}{dx^*} + \frac{P_w \delta^*}{2} &= 1 \\ \Rightarrow \frac{A \delta^{*2}}{12} \frac{d \delta^*}{dx^*} &= 1 - \frac{c_g^*-1}{c_g^*} = \frac{1}{c_g^*} \end{aligned}$$

P_w is a function of x and δ^* will also be the function of x . This equation can still be simplified by the boundary condition **at x** , at y is equal to 0. If we look into the boundary condition at y is equal to 0; at y^* is equal 0 $P_w c_g^* + \frac{\partial c^*}{\partial y^*}$ is equal to 0.

If you look into the derivative of $\frac{\partial c^*}{\partial y^*}$, it becomes $\frac{-2(c_g^*-1)}{\delta^*} + \frac{(c_g^*-1) 2y^*}{\delta^{*2}}$. Evaluated at y^* is equal to 0, this term will go and you will be simply having $\frac{-2(c_g^*-1)}{\delta^*}$.

So, P_w so substituted over here, so $P_w c_g$ is equal to $2 \frac{(c_g^*-1)}{\delta^*}$. We will be having $\frac{P_w \delta^*}{2}$ is nothing but $\frac{c_g^*-1}{c_g^*}$.

Therefore, we substitute this in the governing equation; $\frac{A \delta^{*2}}{12} \frac{d \delta^*}{dx^*} + \frac{P_w \delta^*}{2}$ is equal to 1.

You substitute this here, what we get is $\frac{A \delta^{*2}}{12} \frac{d \delta^*}{dx^*}$ is equal to $1 - \frac{c_g^*-1}{c_g^*}$. **So, it will be getting** c will be cancelled out in the numerator; it will be simply c_g^* .

(Refer Slide Time: 26:52)

$$\delta^{*2} \frac{d\delta^*}{dx^*} = \frac{12}{A c g^*}$$

At $x^* = 0$, $\delta^* = 0$

$$\Rightarrow \int_0^{x^*} \delta^{*2} d\delta^* = \frac{12}{A c g^*} \int_0^{x^*} dx^*$$

$$\Rightarrow \frac{\delta^{*3}}{3} = \frac{12}{A c g^*} x^*$$

$$\Rightarrow \delta^{*3} = \frac{12 \times 3}{A c g^*} x^* = \left(\frac{36}{A c g^*} \right) x^*$$

$$\Rightarrow \boxed{\delta^* = \left(\frac{36}{A c g^*} \right)^{1/3} x^{*1/3}}$$

The governing equation of del star square will be nothing but del star square d del star d x star is equal to 12 A c g star. You carry out the integration and integration will be from 0 to **let us say**, x star in this and delta star will be here. At x is equal to 0 my delta star is equal to 0; with this we evaluate the boundary condition. We will be getting that delta square d delta star is equal to 12 by A c g star d x star.

Once we get that we carry out this integration from 0 to del star from 0 to x star delta star cube by 3 is equal to 12 A c g star x star; delta star now becomes 12 by 12 into 3 A c g star x star; this becomes 36 A c g star x star and this is delta star cube. Therefore, delta star becomes 36 by A c g star to the power 1 upon 3 and x star to the power 1 power upon 3.

If you now recall that this is the functional form that how del star is varying as a function of x star in case of similarity solution. In case of some a similarity solution delta star was a function of x star and the functional variation was x star to the power 1 upon 3. In integral method of solution also, we have found out that delta star is varying as a function of x star to the power of 1 upon 3 with the coefficient 36 A c g star rest to the power 1 upon 3.

(Refer Slide Time: 29:20)

$$C^*(x^*, y^*) = C_{g^*} - 2(C_{g^*} - 1) \left(\frac{y^*}{\delta^*} \right) + (C_{g^*} - 1) \left(\frac{y^*}{\delta^*} \right)^2$$
$$\text{Where, } \delta^* = \left(\frac{36}{A C_{g^*}} \right)^{1/3} x^{*1/3}$$
$$C^* = C^*(x^*, y^*) \rightarrow \text{Concn. Profile within BL.}$$

Summarize :

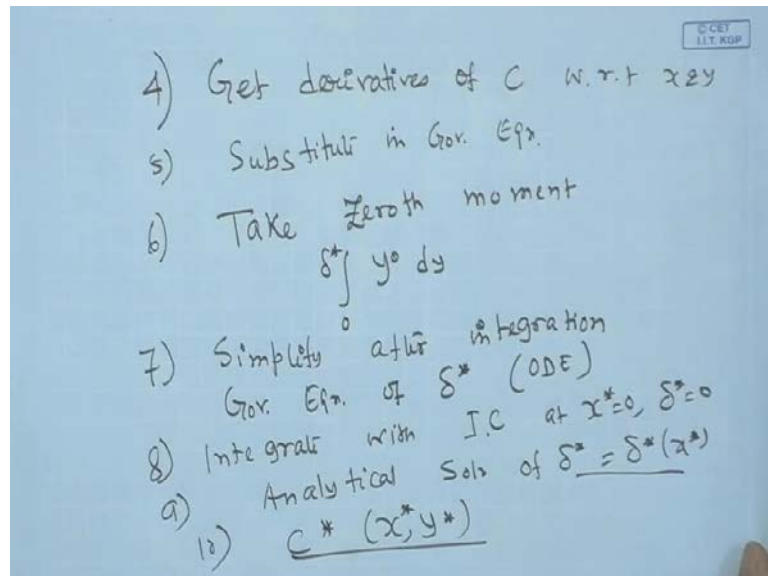
- 1) Write Gov. Eq. & BCs
- 2) Assume a concn. Profile
- 3) Evaluate constants in concn. profile from suitable BCs.

That completes the solution. If you look into the concentration profile which is a function of x^* and y^* ; this becomes c_{g^*} minus $2(c_{g^*} - 1) y^* \text{ by } \delta^*$ plus $(c_{g^*} - 1) y^* \text{ by } \delta^* \text{ square}$.

Where, δ^* can be explicitly written as $36 \text{ divided by } A c_{g^*} \text{ rest to the power } 1 \text{ upon } 3 \times x^* \text{ to the power } 1 \text{ upon } 3$. We substitute δ^* as a function of x^* over here, you will be getting completely c^* as a function of x^* and y^* . We get the concentration profile within the boundary layer.

This example clearly demonstrates that how integral method of solution can be applied to boundary layer analysis in chemical engineering applications. Let us summarize the different steps. First, you write down the governing equation and boundary conditions. Next, we assume a concentration profile that is why it is known as approximate integral method. Once you assume a concentration profile then third step is to evaluate constants in concentration profile from suitable boundary conditions.

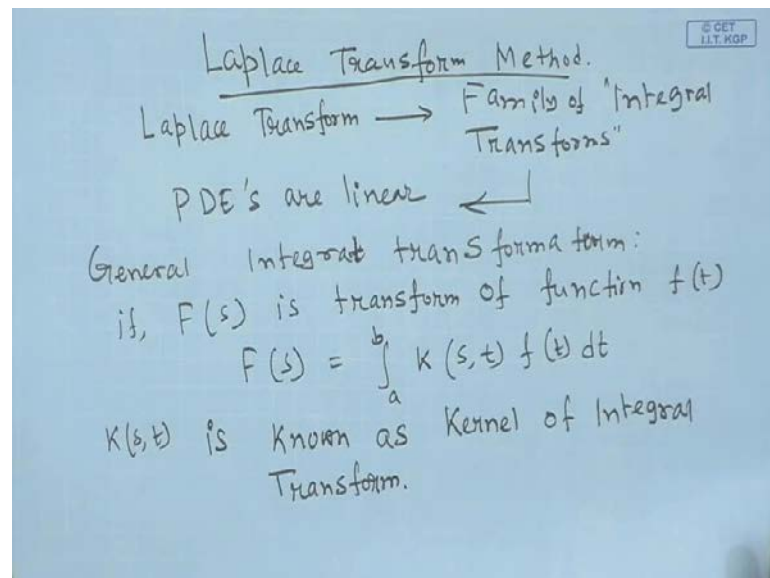
(Refer Slide Time: 31:38)



Among the suitable boundary condition, the boundary layer conditions must be satisfied that at y^* is equal to δ^* , C^* is equal to 1 and $\frac{\partial C^*}{\partial y^*}$ is equal to 0. Corresponding to velocity on thermal boundary layer you will be having the corresponding conditions, get the derivatives of concentration with respect to x and y ; substitute them in the governing equation; after that take the zeroth moment, that means, you multiply both sides by y to the power 0 dy and then integrate across the boundary layer thickness 0 to δ^* .

Simplify after integration in y , what you will be getting? You will be getting the governing equation of δ^* which is nothing but an ordinary differential equation, then integrate it out with initial condition at x^* is equal to 0 δ^* is equal to 0, then what we will be getting is that you will be getting an analytical solution of δ^* as a function of x^* . The final step is that once you know the δ^* as a function of x^* analytically, then you substitute that in the concentration profile and from the concentration profile you will be getting concentration within the mass transfer boundary layer as a function of x^* and y^* . In fact, this is the similar type of approach which should be taken for calculation of temperature profile within the thermal boundary layer and velocity profile within the hydrodynamic boundary layer. We can successfully utilize the integral method of solution for the solution of boundary analysis in chemical engineering problem.

(Refer Slide Time: 34:11)



We complete the integral method of solution. Next, we will look into the Laplace transform method. This method belongs to the family of integral transform, Laplace transform belongs to family of integral transform.

Integral transforms can be applied if and only if your governing partial differential equation or ordinary differential equations are linear for linear governing equations only, the integral method of solution can be, **can be** integral method of integral transform methods can be applicable.

General integral transformation can be written in this form, $F(s)$ is the transform of function $f(t)$, then $F(s)$ can be written as $\int_a^b k(s,t) f(t) dt$ this $k(s,t)$ is known as Kernel of integral transform.

(Refer Slide Time: 36:48)

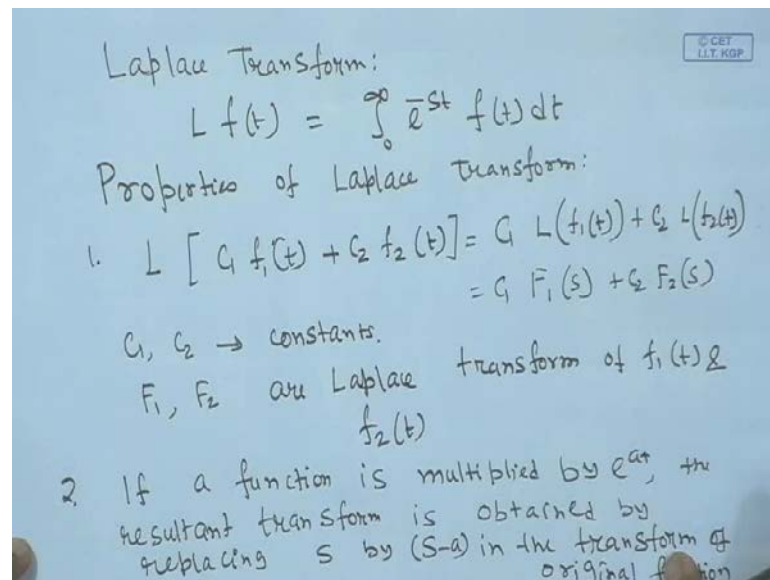
© CET
I.I.T. KGP

Kernels & limits of various transform.

Transform	$K(s,t)$	a	b
Laplace	e^{-st}	0	∞
Fourier	$\frac{1}{\sqrt{2\pi}} e^{ist}$	$-\infty$	∞
Fourier Sine Transform	$\sqrt{\frac{2}{\pi}} \sin st$	0	∞
Fourier Cosine Transform	$\sqrt{\frac{2}{\pi}} \cos(st)$	0	∞
Hankel Transform	$t J_n(st)$	0	∞
Mellin transform	t^{s-1}	0	∞

And this kernels and limits of various transforms are given below. Now we just put transform in a tabular form then k of s t that is the Kernel lower limit a **the** upper limit b . So, if it is a Laplace transform then Kernel is e to the power minus s t this from 0 to infinity. Fourier is 1 over root over 2 π e to the power i s t minus infinity to plus infinity, then Fourier trans sin transform, this is becomes root over 2 over π \sin s t 0 to infinity. Fourier cosine transform, this becomes root over 2 over π cosine s t 0 to infinity. Hankel transform, t n th order Bessel function s t 0 to infinity. Mellin transform, t to the power s minus 1 0 to infinity. So, these are the various kernels lower limit and upper limit of the of the transform for various types of transform.

(Refer Slide Time: 39:01)



Laplace Transform:
$$L f(t) = \int_0^{\infty} e^{-st} f(t) dt$$

Properties of Laplace transform:

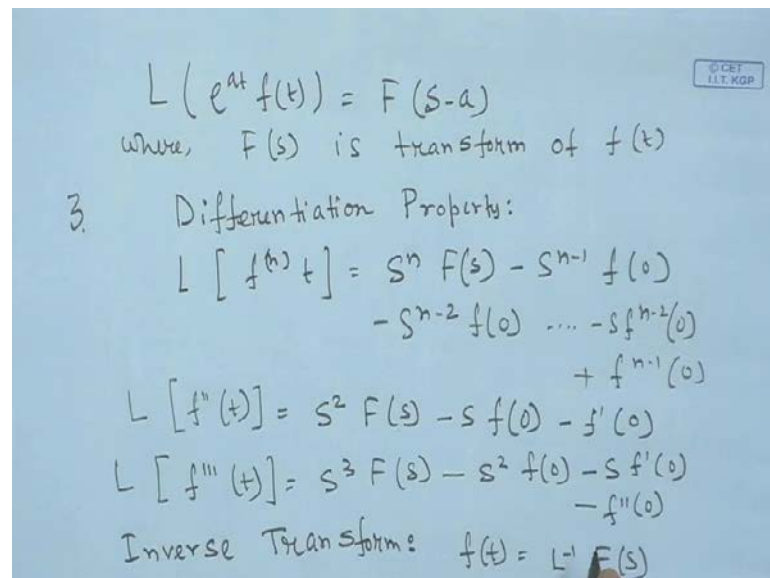
- $$L [C_1 f_1(t) + C_2 f_2(t)] = C_1 L(f_1(t)) + C_2 L(f_2(t))$$
$$= C_1 F_1(s) + C_2 F_2(s)$$

$C_1, C_2 \rightarrow$ constants.
 F_1, F_2 are Laplace transform of $f_1(t)$ & $f_2(t)$
- If a function is multiplied by e^{at} , the resultant transform is obtained by replacing s by $(s-a)$ in the transform of original function

And then let us concentrated on Laplace transform and how this transform can be utilized for the solution of linear partial differential equation. L is called the Laplace operator L of $f(t)$ is nothing but $\int_0^{\infty} e^{-st} f(t) dt$ so e^{-st} is the kernel. Now, let us look into the various properties of Laplace transform the first property is Laplace of $C_1 f_1(t) + C_2 f_2(t)$ should be is equal to $C_1 L f_1(t) + C_2 L f_2(t)$. So, this is nothing but $C_1 F_1(s) + C_2 F_2(s)$, where C_1, C_2 are constants F_1, F_2 which are the function of s are Laplace transform of $f_1(t)$ and $f_2(t)$.

The second property is that, if a function $f(t)$ is multiplied by e^{at} , the resultant transform is obtained by replacing s by $s - a$ in the transform of original function. That is the second property, it should satisfy. Therefore, we just write it down in a neat form compact form.

(Refer Slide Time: 41:54)



$$L(e^{at} f(t)) = F(s-a)$$
 where, $F(s)$ is transform of $f(t)$

3. Differentiation Property:

$$L[f^{(n)}(t)] = s^n F(s) - s^{n-1} f(0) - s^{n-2} f'(0) - \dots - s f^{(n-2)}(0) + f^{(n-1)}(0)$$

$$L[f''(t)] = s^2 F(s) - s f(0) - f'(0)$$

$$L[f'''(t)] = s^3 F(s) - s^2 f(0) - s f'(0) - f''(0)$$

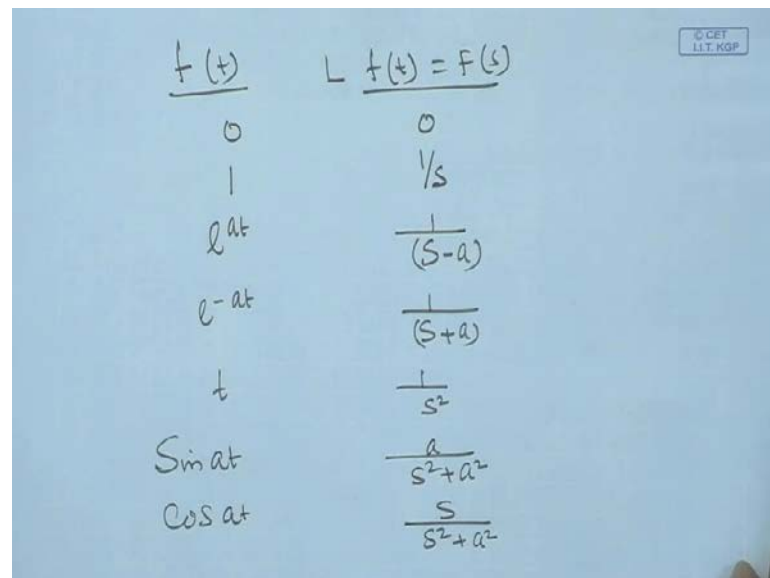
Inverse Transform: $f(t) = L^{-1} F(s)$

L of $e^{at} f(t)$ should be equal to $F(s-a)$, that means, if $F(s)$ is the Laplace transform of $f(t)$, then Laplace transform of $e^{at} f(t)$ is nothing but I just replace s by $s-a$ in the transform, where, so in this equation where $F(s)$ is transform of $f(t)$.

Third important property is the differentiation property. Laplace of $f^{(n)}(t)$ means n th order of differentiation is nothing but, $s^n F(s) - s^{n-1} f(0) - s^{n-2} f'(0) - \dots - s f^{(n-2)}(0) + f^{(n-1)}(0)$. So, Laplace transform of $f''(t)$ is nothing but $s^2 F(s) - s f(0) - f'(0)$. Laplace of $f'''(t)$ is nothing but $s^3 F(s) - s^2 f(0) - s f'(0) - f''(0)$.

Next, we get the once we get the transform, then we get an inverse transform what is inverse transform $f(t)$? Can be obtained by taking the Laplace inverse of $F(s)$.

(Refer Slide Time: 44:27)

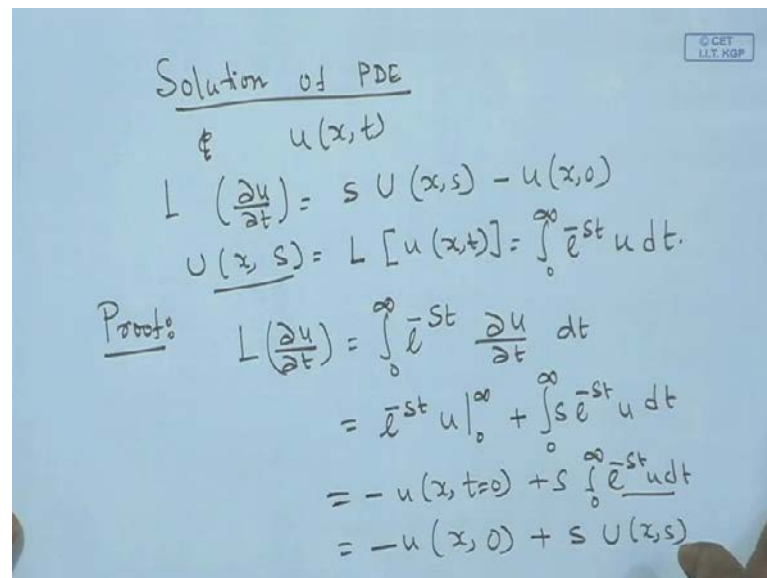


$f(t)$	$L f(t) = F(s)$
0	0
1	$1/s$
e^{at}	$\frac{1}{(s-a)}$
e^{-at}	$\frac{1}{(s+a)}$
t	$\frac{1}{s^2}$
$\sin at$	$\frac{a}{s^2+a^2}$
$\cos at$	$\frac{s}{s^2+a^2}$

So, we can get from s to t domain; now, let us get some of the f of t and what are the corresponding Laplace transform in s domain? So, for 0 this is 0, for 1 this is 1 over s, for e to the power a t this will be 1 over s minus a, for e to the power minus a t this will be 1 over s plus a, for t it will be nothing but 1 over s square, for sin a t this will be a divided by s square plus a square, for cosine a t this will be s divided by s square plus a square.

So, these are some of the typical you know Laplace transform of some simple function in s domain from t domain. So, these functions are quite common, in fact in the book of Carsick or any such you know fundamental books, which are applicable for first year all courses, under graduate courses. There are (()) of some functions are available in the tabular form where the Laplace transform are given.

(Refer Slide Time: 45:58)



© CET
I.I.T. KGP

Solution of PDE

$u(x, t)$

$$L\left(\frac{\partial u}{\partial t}\right) = sU(x, s) - u(x, 0)$$

$$U(x, s) = L[u(x, t)] = \int_0^{\infty} e^{-st} u \, dt.$$

Proof:

$$L\left(\frac{\partial u}{\partial t}\right) = \int_0^{\infty} e^{-st} \frac{\partial u}{\partial t} \, dt$$

$$= e^{-st} u \Big|_0^{\infty} + \int_0^{\infty} s e^{-st} u \, dt$$

$$= -u(x, t=0) + s \int_0^{\infty} e^{-st} u \, dt$$

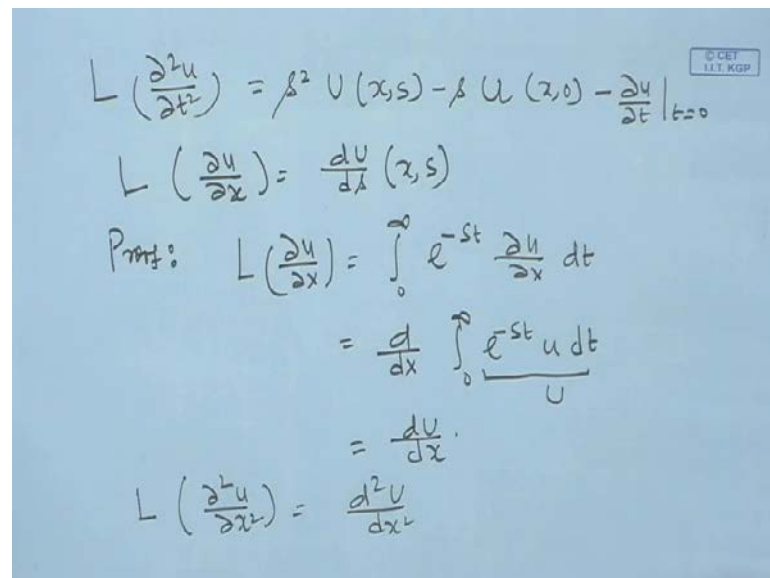
$$= -u(x, 0) + sU(x, s)$$

Now, let us with this background of Laplace transform, let us see, how this Laplace transform can be utilized for the solution of partial differential equation. Now, Laplace of if u is function of x and t then Laplace of $\frac{\partial u}{\partial t}$ is written as $sU(x, s) - u(x, 0)$, where capital u is basically the transform function where we have transform t into s domain. So, $U(x, s)$ is nothing but Laplace of $u(x, t)$, so this will be nothing but 0 to infinity $e^{-st} u \, dt$.

So, we can proof this thing and the proof goes like this Laplace of $\frac{\partial u}{\partial t}$ is nothing but 0 to infinity $e^{-st} \frac{\partial u}{\partial t} \, dt$. So, this becomes $e^{-st} u$ from 0 to infinity, first function, this is the first function integral of second function minus differentiation of the first function 0 to infinity, minus **into** minus, plus e^{-st} integration of the second function $u \, dt$.

So, I take e^{-st} at infinity is 0 and at time t is equal to 0 , so this becomes minus, so first term will be 0 , minus e^{-st} at $t=0$ is 1 , so $u(x, 0)$ plus $s \int_0^{\infty} e^{-st} u \, dt$, so what is this, this is nothing but capital U as a function of x and s . So, this will be nothing but $u(x, 0)$ plus $sU(x, s)$ so that is the Laplace of $\frac{\partial u}{\partial t}$.

(Refer Slide Time: 48:26)



Handwritten mathematical derivations for Laplace transforms of spatial derivatives:

$$L\left(\frac{\partial^2 u}{\partial t^2}\right) = s^2 U(x, s) - s U(x, 0) - \frac{\partial u}{\partial t} \Big|_{t=0}$$

$$L\left(\frac{\partial u}{\partial x}\right) = \frac{dU}{dx}(x, s)$$

Proof:

$$L\left(\frac{\partial u}{\partial x}\right) = \int_0^\infty e^{-st} \frac{\partial u}{\partial x} dt$$

$$= \frac{d}{dx} \int_0^\infty e^{-st} u dt$$

$$= \frac{dU}{dx}$$

$$L\left(\frac{\partial^2 u}{\partial x^2}\right) = \frac{d^2 U}{dx^2}$$

Similarly, one can prove that Laplace of del square u del t square is same as s square U x s minus s u x at 0 minus del u del t at t is equal to 0. Similarly, one can proof Laplace of del u del x is nothing but d U d s, where x this is a function of u is a function of x and s. So, this we can proof Laplace of del u del x is nothing but 0 to infinity e to the power minus s t del u del x d t, so this integral is over t so we can take del u del x over we can take d d x outside.

So, outside it becomes d d x 0 to infinity e to the power minus s t u d t, so what is this this will be nothing but capital U, the Laplace transform of f of t of small u therefore this is nothing but d u d x.

Similarly, one can prove that Laplace of del square u del x square is nothing but d square u d x square, so with this you can get different derivative with respect the Laplace transform of various derivatives are presented in the s domain from t domain.

(Refer Slide Time: 50:25)

* Ex: $\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial x^2}$ ✓

at $t=0$, $u = 1 + \sin(\pi x)$ ✓

at $x=0$, $u=1$ ✓

at $x=1$, $u=1$ ✓

Take Laplace transform on both sides:

$$\int_0^\infty e^{-st} \frac{\partial u}{\partial t} dt = \int_0^\infty e^{-st} \frac{\partial^2 u}{\partial x^2} dt$$

$$\Rightarrow sU(x,s) - u(x,0) = \frac{\partial^2 U}{\partial x^2}$$

$$\Rightarrow \boxed{\frac{\partial^2 U}{\partial x^2} - sU = -(1 + \sin(\pi x))} \checkmark$$

With this, we will be in a position to formulate the first example to take up the first example that is $\frac{\partial u}{\partial t}$ is equal to $\frac{\partial^2 u}{\partial x^2}$ at t is equal to 0 u is equal to $1 + \sin \pi x$ and at x is equal to 0, we have u is equal to 1 at x is equal to 1, we have u is equal to 1. See this governing equation is a linear and homogeneous, we have a non-homogeneous term as an initial conditions and both the boundary conditions are non-homogeneous.

So, therefore we are going to solve this equation using Laplace transform. So, what we do? We take Laplace transform on both sides, if we do that it will be multiplied by e to the power minus $s t$ and integrate from 0 to infinity $\frac{\partial u}{\partial t} dt$ from 0 to infinity e to the power minus $s t \frac{\partial^2 u}{\partial x^2} dt$.

So, this becomes $s U$ of x and s minus u at time t is equal to 0 is equal to $\frac{\partial^2 u}{\partial x^2}$, we have already proved that and what is u at time t is equal to 0 that is the initial condition. So, therefore we will be getting the governing equation of $\frac{\partial^2 u}{\partial x^2}$ minus $s u$ is equal to minus $1 + \sin \pi x$.

So, what is essentially the message is that by using this the integral transform, we are able to get down the partial differential equation into an ordinary differential equation. If you look into the similarity transformation integral method, as well as the Laplace transform, we have seen that in all the cases the partial differential equation has boil

down into an ordinary differential equation and the solution of ordinary differential equations are quite simpler.

So, we take up this problem in the next class and solve this problem completely. So, I stop here, in this class; next, we will talk about more detail the solution of this problem or then I will be taking up couple of more examples of how to of application of Laplace transform for solution of partial differential equations, which will be more common in our transient chemical engineering processes, thank you very much.