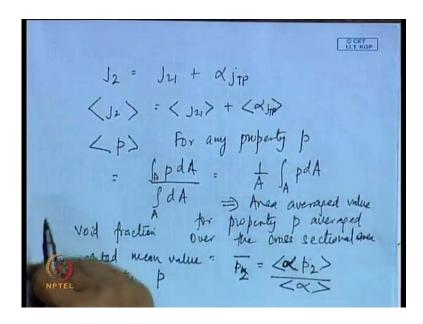
## Multiphase Flow Prof. Gargi Das Department of Chemical Engineering Indian Institute of Technology, Kharagpur

## Lecture No. # 16 Drift Flux Model (Contd.)

Well, good morning to all of you. So, today we have come almost to the final portion of the drift flux model, see in the last classes what we had derived is we had derived what is a drift flux model, and then the concept of drift flux and then how the drift flux can be incorporated into different expressions of the mixture properties like the mixture density the in situ velocities and so on and so forth.

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And finally, we had derived the final expression of the drift flux model which gives us as J2, this is equal to J21 plus alpha j. This was for the final expression we had derived from which we had calculated alpha, and as and accordingly that alpha was substitute in the different expressions. Now, the first thing which I would like to tell you in this class is when we had written down this particular expression, this particular expression this assumes that J2, J21, they are constant over the entire cross sectional area. Is it not? This was the first thing that we had assumed that well we take an averaged value of these particular parameters averaged over the entire cross sectional area.

Now, usually we find that this can be a very drastic assumption for most of the flow situations for most of the flow situations we find that usually they keep on varying across the cross section. So, corrected expression for the in order to incorporate the average quantities averaged over the entire cross section the best thing will be to average it out. Now, whenever we write down averaged over any over the cross section we usually denote it by this particular symbol what we mean is that actually whenever we are writing this expression what we mean is that all these quantities are averaged over the entire cross section.

Where this particular quantity say J2 or for any particular property p for any property p your this particulars, this squarish brackets they basically mean integral pdA by integral over dA integrated over the entire cross sectional area or in other word this is 1 by A integrated over a integral pdA.

So, therefore, you can very well understand that when I put this brackets across the individuals terms of these expressions what I mean is, this is the average volumetric flux of component to averaged over the entire cross section this is nothing but basically integral J2 dA by A this is the average drift flux which is averaged over the entire cross section and this is the product of volumetric concentration and volumetric flux which is averaged over the entire cross section.

Well just like to make a correction they are all referred to the two phase values now therefore, we find that all of them are the average quantities where as I have told you this particular bracket for any property this simply denotes the area averaged value averaged over the cross sectional area and the void fraction there are two terms one is since for single phase flow this is a sufficient definition the area averaged.

Now, value of each property or rather for any property this is nothing but the area averaged value for property p averaged over the entire cross section averaged over the cross sectional value, sorry averaged over the cross sectional area and when we are having two phases then we know that both the phases do not occupy the entire cross sectional area, see phase one occupies A1 part of the area phase two occupies A2 part of the area under that condition there is one additional definition which is void fraction averaged weighted mean value.

Or void fraction averaged mean value the void fraction weighted mean value means it is weighted against the void fraction this is for any particular property for phase I or k whatever it is void fraction weighted mean value of property p this is pk bar this is nothing but alpha p say if it is p2 then alpha p2 by alpha.

If it is p1 then it is 1 minus alpha p2 into by alpha. So, this is one particular term which is very important. So, if you observe this term you find that here alpha jTp will nothing will be equal to nothing but alpha into jTp bar isn't it something of this sort. So, what it is that we will be noticing or alpha into p2 sorry alpha jTp yeah this is going to be in the other particular fashion.

So, therefore, we find that there are 2 particular definitions which we have to we have to keep in mind this we have already got in your single phase flows for any property p. The area averaged value when the area is averaged over the entire cross sectional area, this can be given by this particular form and the weighted mean value of the property that is weighted over the entire or the void fraction weighted mean value it is can be expressed in this particular form agreed.

So, accordingly we find that if this is true then accordingly the different mixture properties which we get they should be averaged over the entire cross sectional area. So, therefore, just like I have written it down for J2 similarly for rho Tp also I can get the expression.

I TP = <X>1\_ + (1-40) P,
P, P\_ = constant because transverse pr.
gradient within a channel is
relatively small. O CET nseighted mean valueity  $\overline{U_2} = \langle X | U_2 \rangle = \langle J_2 \rangle$   $\overline{U_2} = \langle X | U_2 \rangle = \langle X \rangle$ 

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Say suppose, I get it for rho Tp what was it this was alpha rho 2 plus 1 minus alpha rho 1 isn't it. Now, for this particular case it is the mixture density averaged over the entire cross section this will be alpha rho 2 plus 1 minus alpha into rho 1. Where we assume that rho 1 and rho 2 they are constant over they do not vary over the cross section and this particular assumption remember this is a valid assumption, because the transverse pressure gradient constant, because we find that the transverse pressure gradient within a channel is relatively small.

So, therefore, this is a reasonably this rho 1 rho 2 being constant is a reasonably valid assumption and under that condition the mixture density. The correct expression is in this particular form remember after we finish the drift flux model we will not be putting curly brackets everywhere just because it is very cumbersome, but we will imply that when we just say alpha it is the area averaged values it is implied that when after this topic is over when we write alpha we mean this.

Unless otherwise stated because every time writing this down is difficult. So, when you are just expressing it alpha in this particular way it is the mean averaged values. In the same way we find say the Axial component of the weighted main velocity suppose the u2 Axial component of weighted mean velocity of phase two. So, this is going to be u2 bar if we write this is alpha u2 divided by alpha agreed.

Now, we know what is alpha u2 equal to alpha u2 equals to this is the void fraction multiplied by the in situ velocity of component two. So, therefore, gives you J2 so therefore, please remember that Axial component of the weighted mean velocity of phase two u2 bar is the average J2 divided by the average alpha, please remember this is not equal to this u2 bar which is equal to this.

This is not equal to averaged u2 this is the weighted mean this is the cross sectional average the void fraction weighted mean velocity this is the cross sectional averaged velocity, these two are not equal why this is equal to the cross sectional average of J2 divided by the cross sectional average of alpha whereas, this means J2 by alpha over which the cross section is taken. Are these concepts clear to you?

Please try to understand these concepts they are extremely important the thing is in this particular case, we get this is the weighted mean average velocity and this is the cross sectional average velocity.

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LI.T. KGP  $\langle U_{2} \rangle = \int_{A} \int U_{2} dA$   $= \langle J_{2}^{1} \rangle = \int_{A} \int (J_{2}) dA$   $\overline{U}_{2} = \langle J_{2} \rangle = \int_{A} \int \int J_{2} dA$   $= \langle J_{2} \rangle = \int_{A} \int \int J_{2} dA$   $= \int \int J_{2} dA$ 

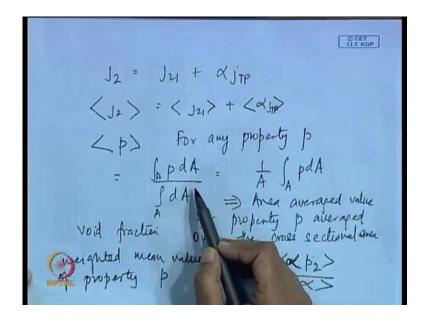
What does this means this u 2 bar it means this means integral u2 dA 1 by A or in other words, what it means if this is equal to J2 by alpha this means 1 by A integral J2 by alpha dA that means, for each particular point you measure J2 you measure alpha you divide the two get the product then get the quotient. And then that quotient you integrate over the entire cross sectional area divided by the area that gives you the weighted mean average velocity, and when you talk of u2 bar that gives a cross sectional average velocity and when you talk about the waited mean average velocity this means J2 by alpha which is nothing but equal to 1 by A integral J2 dA by 1 by A integral alpha dA now, by comparing these two expressions. Is it clear why this is not equal to this?

This is the cross sectional average velocity of component two this is the weighted mean velocity of component two. So, they are grossly different for this what you have to do, you have to measure the local or the in situ J2 at the every point, the local or the in situ alpha at every point, divide the two find the quotient then, that quotient you integrate in this particular case it is much more easier what you do you find the cross sectional average J2.

Finding out cross sectional average J2 is very easy this is nothing but Q2 by A. So therefore, this is an input parameter or this is a measurable quantity similarly this alpha it is just the average alpha. So, it is the area average alpha which you can very easily measure either by the conductivity probe technique or the radiation accumulation

technique and so on and so forth. So, therefore, this is a much more friendly quantity or a much more determinable quantity as compared to this. So, therefore, these concepts have to be very clear.

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Now, remember one thing certain concepts you have already learnt in single phase flows for example, this area averaged value this you have learnt in single phase flows is not it. In single phase flows very frequently you are you are suppose to find out the area average velocity for which you have given a velocity profile, you integrate the velocity profile over the entire area divided by the area, you get the your cross sectional averaged velocity or in other words you integrate the entire profile, you get the volumetric flow rate of that particular fluid over that particular area.

So, this area averaged value of this of this property the properties averaged over the entire cross sectional area you are already familiar with is not it, but the weighted main value the this is also a pretty I should say a pretty straight forward it is just the weighted main value which gives you the void fraction means, the total distribution divided by the void fraction or divided by the area over which it is distributed for p2 it is alpha p2 by alpha if it would have been p1 it is 1 minus alpha p1 by alpha.

So, therefore, this particular property considering the effective area over which it is divided, the previous one was over the total area this is the effective area over which it is distributed or divided. So, that particular effective area is considered and from there we

get the void fraction or the weighted mean average property of any particular parameter. So, accordingly considering these particular things or these particular concepts what has been done the different mixture properties they can be defined.

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LI.T. KGP <PTP = <x>PL + (1-60) P, P, PL = constant because transverse pr. gradment within a channel is relatively small.  $d = \langle d \rangle$ Axial component of weighted mean velocity of phase 2  $U_2 = \langle d | u_2 \rangle = \langle l 2 \rangle$ 

For example, the rho Tp it can be defined the local in situ velocities can be defined.

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$$\overline{u_{1}} = (+-\frac{4}{4}) + \frac{1}{4}$$

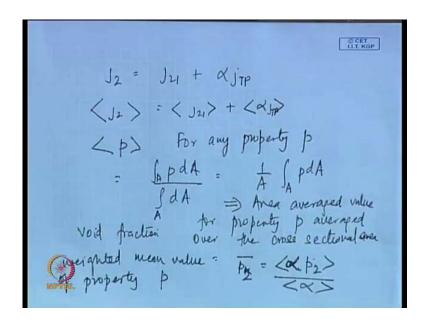
$$= \frac{2(1-2)}{2(1-2)} + \frac{1}{4}$$

$$= \frac{2(1-2)}{2(1-2)} + \frac{1}{4}$$

$$\overline{u_{1}} = \frac{2}{4} + \frac{1}{4} + \frac{1}$$

Similarly, you can define a u1 well in this particular case u1 would have been given as it is nothing but 1 minus alpha u1 or rather it is better written as u1 bar equals to 1 minus alpha u1 divided by 1 minus alpha. So, at each point you find it out and then you do it similarly suppose, we would like to define uTp the two phase mixture velocity it is nothing but rho Tp uTp divided by rho Tp. So, therefore, this is given as alpha again rho2 is taken as constant u2 bar plus 1minus alpha rho1 u1 bar divided by rho Tp. This is the thing and in the same way if you find out the volumetric flux the volumetric flux say jTp this is J1 plus J2 this is nothing but alpha u2 plus 1 minus alpha u1. So, in this particular way we can continue we can define all the different properties. Now, let us see how easily we can introduce some particular correction to the three dimensional drift flux model in order to arrive at the one dimensional flow situation.

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So, the basic definition which I had put it in this particular case is that this was the actual drift flux model which we can define is not it. From this particular model or from this particular concept now, the very rational approach to obtain the one dimensional drift flux model will be to integrate the three dimensional drift flux model over a cross sectional area, and then we can introduce proper mean values. We can integrate this by using this particular formulae over the entire flow field and over the entire cross sectional area and then we can introduce proper mean values.

Now, remember one thing whenever we have to deal with this particular equation finding out J2 is very easy it is nothing but Q2 by A as I have already written down here this particular J2 this is nothing but Q2 by a J21 it can be found out by it is just the average drift flux averaged over the entire area. So, this also can be found out easily now for finding out alpha into jTp what you have to do for each particular point you have to measure alpha at each particular point you have to measure jTp you have to multiply the 2 and then you have to integrate the entire functional form. Now, this is not very easy. So, a simplified approach is that if we can replace this by some other easily measurable or input parameters. Now, how to do this now for this particular thing now, certain things that I have told you this needs to be replaced.

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D CET LLT. KGP  $\langle J_{L} \rangle = \langle J_{21} \rangle + \langle X \rangle_{TP} \rangle$   $\langle X \rangle_{TP} \rangle \neq \langle X \rangle \langle J_{TP} \rangle$ Nomentium fluw in a pipe with Avelo oity profile and uniform density  $P \int u^{L} dA = A P \langle U^{2} \rangle$   $A P \langle U^{2} \rangle \neq A P \langle U^{2} \rangle$   $A P \langle U^{2} \rangle = Convection factor$  $<math>A P \langle U^{2} \rangle = Convection factor$   $A P \langle U^{2} \rangle = 1 for fruly 1d case$ 

Now, if I write down the equation once more J21 plus alpha jTp now, this term we know that definitely alpha jTp this is not equal to this term isn't it and this is a measurable parameter where this alpha jTp is nothing but Q1 by plus Q2 by A and alpha can also be measured. So, instead of this if we can replace it by this term along with some other corrections then probably my equation becomes a little more friendly, is it not? So, if that can be done then it becomes slightly little more easier. Now, how to do this now if you remember in single phase flow see single phase flow whatever wherever we get stuck we refer resort to single phase flows what has been done for single phase flows accordingly we would like to do it here.

Now, in single phase flows if you remember that when we had considered your the momentum flux and say suppose when we considered the momentum. If you remember the momentum correction factor and the kinetic energy correction factors alpha beta in single phase flows there what we did just to keep the matters simple, what we did was

momentum flux say in a pipe with velocity profile and uniform density. So, this is given as integral u square dA where this is nothing but A rho u square is not it now, we knew that this A rho u square this is not equal to A rho isn't it and, but this is a much more easily measurable parameter.

So, why because you just measure the velocity profile and then you integrate it find out the profile and then you square it, but for this particular case you have to measure the velocity at each and every point you have to square it then, you have to find out the profile then you have to integrate it. So, in single phase flows what we did we just took the ratio of these two and expressed it as a correction factor if you remember that this was the exact thing which we were done in Bernoulli's equation.

If you remember Bernoulli's equation the basic equation it is just u square by 2 plus z g delta p by rho plus delta u square by 2 plus and then we introduced a correction factor alpha there is it not? The alpha was the kinetic energy connection factor why did we introduce it, we introduced it just for this particular reason just for because if we introduce a correction factor then we can take up the average velocity and we can square it and we can use it.

But otherwise it is actually the velocity profile for each particular point the velocity has been to be measured it has to be squared. Accordingly, the profile changes that profile has to be determine that has to be integrated and then we can introduce it remember this. So, therefore, in single phase flows what we had done for kinetic energy even for momentum flux when the density is constant, and there is a velocity profile what we did how to express those things we had introduced a suitable correction factor.

What was the correction factor there for simplicity a correction which was nothing but the ratio of this divided by this particular ratio this was introduced as a correction term keeping in mind that this particular correction factor will be equal to unity for truly one dimensional case and not far from unity for the general case. So, it has to be u square alright.

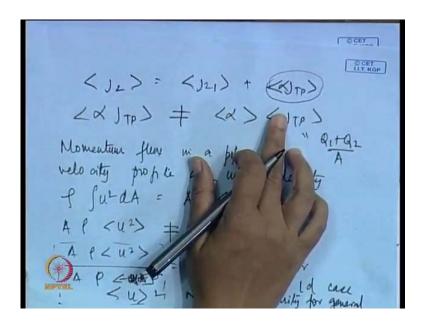
So, therefore, usually what is the concept of a single phase flows? In single phase flows we find that more or less the ratio of these they are not very far from unity and for truly one dimensional case they become unity, because for truly one dimensional case. What is the case the velocity is the same for all points in the cross section, so therefore, this correction factor which is equal to 1 for truly one dimensional case and not far from unity for the general case. So, therefore, in these particular way the correction terms were introduced. Similarly, we the similar approach was taken for this particular term here this alpha jTp instead of alpha jTp if we can replace it as alpha average jTp averaged into a correction factor then, situation becomes simpler provided the correction factor equals unity for truly one dimensional case it is not far removed from unity for the general case.

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LI.T. KGP Dis In bution

So, therefore, keep it just by using this particular concept it was thought that in the same way suppose we can refer this as the ratio this particular. This can also be introduce as a correction factor and then using the correction factor we can write down the equation as J2 equals to J21 plus say alpha jTp into the correction factor, this factor will be equal to unity for the general case for the truly one dimensional case not much removed from unity for the general case, and then we find that in this particular equation this can be obtained from Q2 by A. A measurable parameter this is Q1 plus Q2 by A again a measurable parameter alpha can be obtained from your simply void fraction measurements and j21 from the drift flux correlations, we had already discussed the different drift flux correlations they are all for truly one dimensional cases.

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So, therefore, this becomes much more easier now, this correction factor was first it was proposed by your Zuber and Findlay this is usually known as a distribution parameter. This is defined as C0 which can be defined as the C0 can be defined as alpha jTp by this is the definition or in other words if you break it down this is 1 by A integral alpha jdA divided by 1 by A integral alpha dA into 1 by A integral jdA see, if this particular till this portion it is clear to you or not, is it clear to you? Just to make corrections to the simple one dimensional theory what we did we first wrote down the actual equation in the form of average quantities. Now all these quantities there area average quantities, where this area average quantities can be defined in this particular form.

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CET LLT. KGP uniform densit

And next after this what we did once this could be defined then we found that more or less this can be obtained from a easily measurable parameter this is also the area averaged value this creates a problem. Now, this is a product of two particular quantities which vary which might vary across the cross section. So, therefore, what has to be done the volumetric concentration has to be measured on each and every point your the overall volumetric flux has to be measured at each and every point then the product has to be made and then it has to be integrated.

For engineering applications this is something very difficult we would always like to keep matters simple while not sacrificing much on the accuracy of it. We would not like to go into something very complex do a lot of mathematics waste a lot of time and then get a very accurate results where a little less little loss on accuracy would not have been much loss to us, if the matters could have been made simple and we are doing it in several engineering applications.

In single phase flow also we have done it for the momentum correction factor kinetic energy correction factor etcetera etcetera. We had introduced a correction factor keeping in mind see whenever you introduce a correction factor something has to be kept in mind that for it reduces to some particular boundary conditions for example, the correction factor equals to 1 for truly one dimensional case and for other cases it is not very far suppose the correction factor becomes 5, 7, 10, 11 then it is not worth.

If it is not very far removed from unity then these particular concepts it works very well; that means, the correction is not very much is not it. It is a very small correction you can get this small correction by a larger number of mathematics or you can you can introduce some particular constant where that particular constant has to be evaluated accurately. So, these are the general concepts which we use even for single phase fluid flow. So, based on these concepts what we decided was since finding out these particular term becomes difficult.

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O CET LLT. KGP

So, if we can break it down into two terms and then introduce a correction factor which is nothing but the ratio of the two then we can get this expression in a much more simpler much more user friendly form. And this particular correction term this is defined as a distribution parameter this or a Zuber and Findlay parameter. Since, they were the first researchers to propose this particular concept for 2 phase flow and accordingly this distribution parameter has been defined and this makes the above equation the form of the equation now becomes something of this sort, so this becomes the form of the equation now it becomes something of these sort.

So, therefore, in these particular term we find that if we can find out C0 and if can find out j21 then more or less this equation can be used for finding out alpha or for all practical purposes. This equation can be used once you can find out alpha from this equation this alpha can be substituted in rho Tp u2, u1 Kinetic energy terms the Momentum flux terms etcetera etcetera and all the terms can be deuced. Accordingly and these terms when they are when they are substituting the pressure drop expression that we have obtained from the homogeneous flow model we can get a much more accurate estimation of pressure drop as well.

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C CET <Jz>= <Jzi>+ Co <X><JTP  $\frac{2}{2} = \frac{2}{2} \frac{3}{2} \frac{3}{2} + \frac{2}{2} \frac{3}{2} + \frac{2}{2} \frac{3}{2} \frac{3}{2$ 

So, therefore, the next discussion goes on how to estimate this C0 once we have certain ideas about estimating C0 it becomes much more easy. Now, before that I would like to write these particular expression is usually written in a slightly different form. What is the form the original expression is something of this sort usually dividing throughout by alpha what do we get something of this sort.

Where we know the this particular term what is this? This is nothing but alpha u2 by alpha isn't it which is nothing but u2 bar the weighted mean velocity as I have already defined and so, therefore, u2 bar equals to j21 by alpha plus C0. So, therefore, this can be defined and we know that this is a much more convenient term as compared to u2 bar this is a much more convenient term because this can directly be related to input parameters like the overall volumetric flow rate and the mean volumetric concentration and so, therefore, it is a much more means input parameter as compared to this and so, therefore, we define this particular equation by considering the weighted mean average velocity.

This is given as u2 is nothing but Q2 by A or in other words in terms of measurable parameters if you write this is nothing but Q2 by A alpha this is equal to C0 Q1 plus Q2 by A plus J21 by alpha. In this particular way we can write it down or in other words we can write it as u2 bar equals to j2 by alpha equals to u2j this can again be written down as u2j is not it, because this is alpha into u2j if you remember the basic definition of J21 what was the basic definition of J21 alpha into u2 minus J which is nothing but alpha

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So, therefore, if you write down J21 by alpha this is nothing but alpha u2j by alpha it is nothing but u2j bar isn't it. So, therefore, the previous equations which we were writing this particular equation or this particular equation we can also write it down as u2 bar isnothing, but it is u2j bar plus C0j. So, in this particular way also we can write down the equation in terms of two weighted mean average values. The weighted mean average value of the velocity of phase two and the weighted mean average value of the drift velocity. So, from this particular expression we can get the expression of alpha this is equal to Q2 minus A J21 divided by C0 into Q1 plus Q2. So, therefore, if Q2 and Q1 they are measured A is known if J21 is known and C0 is known alpha can be very well determined till this part. Is it clear to all of you?

So, for finding out J21 what do you need for finding out J21 you need two things one is dependence of J21 on alpha and the two thing is variation of alpha across cross section if

you know these two things then in that case because this J21 this is nothing but 1 by A j21 dA. So, therefore, you have to find out two things one is how j2 depends upon alpha. And how alpha varies across the cross section if these two data are known therefore, your J21 can be easily found out and one more thing that we also know is suppose say J21 is much smaller as compared to Q2. If j21 is much smaller then what happens to this particular expression.

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U.T. KGP U2 Dependence of

If your j21 much less than Q2 or Q2 by A then in that case your alpha becomes 1 by C0 Q2 by Q1 plus Q2 or in other words if the drift velocity or drift flux is very small that means, the two phases are moving at almost equal velocity under that circumstances we just need a distribution parameter in order to account for the non uniform velocity and void age profiles. And therefore, under that circumstances simply the homogeneous value has to be modified by the term one by C0 in order to account for the non uniform velocity and the void age profiles and accordingly the this particular correction it is found out, but under normal circumstances we find that generally we have this term J21 this is usually not very small we have to account for it.

And when we find that your j21 is also very small compared to Q2 by A and the more or less the velocity and void age profiles are flat across the cross section under that circumstance what happens a circumstance where j21 is much smaller as compared to Q2 by A that means, both the phases are moving at a more or less uniform velocity. And the your C0 is near to unity that means, the velocity and the void age profiles are more or less uniform that means, more or less it is a flat velocity profile and the dispersed phase is more or less uniformly dispersed in the channel or in the conduit geometry under that conditions C0 equals to 1 j21 is much less then Q2 by A for that for these two conditions what happens.

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CCET LLT. KOP LJ21 > KL QL/A If conc. profile is uniform channel C/s Co = 1 across 021 essentially homogeneous becomes relation between mean case , reduces to a straight origni at an angle of

The expression of alpha reduces to you can observe the expression of alpha where this is very small this term goes away and this is one term. So, therefore, it becomes the homogeneous flow value is not it. So, therefore, you please understand what does the drift flux model do it accounts for the relative motion of the two phases it accounts for the non uniform velocity and the void age profile. So, this is the thing which I would like you to know that for if concentration profile is uniform across channel cross section C0 equals to 1 if you u2j is much less than Q2 by A then for these two cases we get flow becomes essentially homogeneous.

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CET LLT, KGP  $\frac{\langle j_{22} \rangle}{\langle z_{x} \rangle} = \frac{\langle z_{x} \vee z_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle z_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle z_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} + \frac{\langle u_{23} \rangle}{\langle z_{x} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} + \frac{\langle u_{23} \rangle}{\langle u_{23} \rangle} = \frac{\langle u_{23}$ E Defendence of Jay on & E Vanation of & across of s > J22 2 2 f J J21) dA \*

And then what happens in this particular case the relation between your when this happens under that particular circumstance what happens if we go a little further, we find that this has become equal to unity this term has gone off then the relation between this and this it gives you a straight line passing through the origin at an angle of 45 degrees to the x axis or the y axis. So therefore, under that circumstance what happens relation in this case relation between mean velocity and flux reduces to a straight line through the origin at an angle of 45 degrees or in other words for such a circumstance.

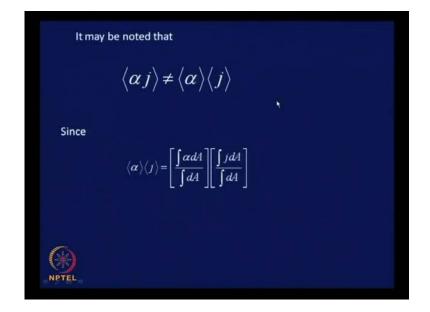
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If we plot your u2 bar with j we get a straight line through the origin isn't it we get such a straight line. And the thing is what we usually do we and this gives you the homogeneous flow theory now, for this particular case what we get is that usually what we do whenever we get in a experimental data we try to plot it on this particular curve with the 45 degrees line on it and then we see this spread of this data from this spread of the data, we try to understand how much it has deviated from the homogeneous flow theory accordingly we introduce corrections.

Do you understand usually whenever we have any particular experimental data what we do we usually with when it is for fully developed velocity and void profile for fully developed velocity and void profile, what we try to do is we make such a plot and then in that particular plot we substitute the data around this 45 degrees line and then we find out that usually data point will be clustering around this particular line. The amount of spread it has from this line that particular spread tells us how much it has deviated from the drift flux theory and whether we should go or how much it has deviated from the homogeneous flow theory and whether we should go for some correction or not and in what way should we introduce the correction whether C0 is important or whether j21 is important usually we find that j2 is important and some particular j21 has to be incorporated there. Now, the next thing which I would like to discuss is the estimation of C0 how we can estimate C0 or how the C0 can be obtained for different particular flow situations.

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Now, if you see here I have already written down in this ppt. if you observe then you find that in the ppt I have written down the basic equations if you observe this ppt then you find that in the particular ppt I have written down the basic equations you can always go through them and you can find out that more or less the basic things are written here. So, C0 is the ratio of the average of product of flux and concentration to the product of the averages.

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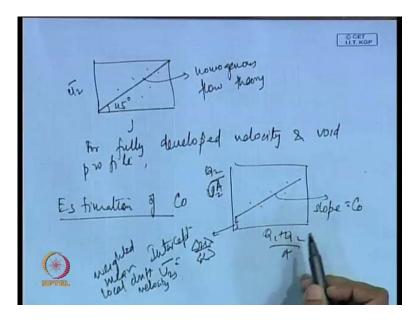
$$\frac{\left\langle j_{2}\right\rangle}{\left\langle \alpha\right\rangle} = \frac{\left\langle j_{21}\right\rangle}{\left\langle \alpha\right\rangle} + C_{0}\left\langle j\right\rangle$$

$$\frac{Q_{2}}{A\left\langle \alpha\right\rangle} = C_{0}\frac{Q_{1} + Q_{2}}{A} + \frac{\left\langle j_{21}\right\rangle}{\left\langle \alpha\right\rangle}$$

$$\left\langle \alpha\right\rangle = \frac{Q_{2} - A\left\langle j_{21}\right\rangle}{C_{0}\left(Q_{1} + Q_{2}\right)}$$
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This is the basic definition of C0 and then using this particular definition we come across this particular friendly equation based on input parameters from where alpha can be obtained by using this expression. Here we find if j21 and C0 is close to unity for fully may be when the velocity and the concentration profiles are flat and when j21 is much less compared to Q2 by A then, alpha reduces to the homogeneous flow value. Now, the usual trend to find how much your actual situation deviates from the homogeneous flow value. We usually plot this particular term with this particular term and then the deviation of the data from the 45 degrees line passing through the origin gives us an idea about the magnitude of C0 and j21 by alpha.

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So, next is estimation of C0 now, what are the different ways by which you can estimate C0 now, there are two ways the first thing is you construct such a type of plot now, if you construct such a type of plot then in that particular plot usually what we find is that it usually. Since, I have told you C0 is much not much removed from unity is not it. So, we find that if we make such a plot or in other words if we make a plot of say Q2 by Q1 plus Q2 by A then usually, we get a straight line the best fit curve is usually a straight line and can you tell me the slope of this straight line what it gives you and the intercept of this straight line what it gives and you can tell me what we get from the slope and the intercept of this particular straight line.

Slope gives you C0 and this gives you j21 by alpha isn't it. So, therefore, very simply usually we find that for fully developed velocity and void age profiles, please remember this for fully developed velocity and void age profiles usually we find that when we do such a plot it gives a best fit curve is a straight line. When the local drift velocity is constant or it is negligibly small in that particular case your slope it gives you the slope of this best fit line this gives you the value of the distribution parameters C0 and the intercept gives you the value of the weighted mean local drift velocity, this gives you the weight or in other word this gives you u2j which is nothing but the weighted mean local drift velocity.

So, this is one particular way by which we can find it out and we have done it several times what we do whenever we have to analyze experimental data first, we refer to such

a plot we find how much is the deviation. When we find the deviation is quiet large then we resort to this particular plot from where we can find out C0 we can find out u2j bar and once we find these out we can find out all the other qualities all the other parameters and, but this is usually done for fully developed velocity and void age profiles when it is varying with time definitely for temporal variations we cannot resort to this, but apart from this we find that there are certain other ways also by which we can find out C0 what are the other ways, if we go to the basic definition of C0 what was the basic definition.

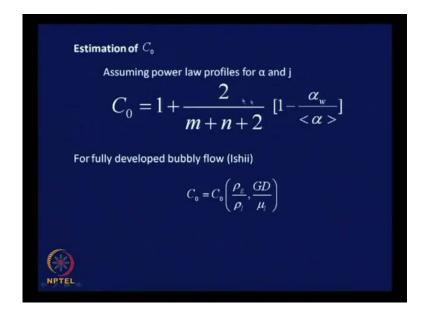
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So, the ways of finding out C12 is from this particular equation which is Q2 it gives you so, this particular equation and we plot this versus this then we can get C0 the other thing is what is the basic definition. Basic definition is alpha J by alpha J or in other words if we go to the actual definition this is this is the other definition. So, what we can do from the velocity profile and the concentration profile also we can find out C0 this can be the other way is not it. Usually, what we assume we assume parabolic power law profiles usually the type of profiles, which we assume are power law profiles which give you J by J0 equals to 1 minus r by R whole to the power n.

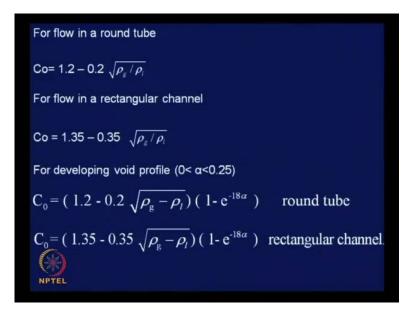
Usually we have such power law profiles even in single phase flow also you have found out that usually we deal with the power law type of profiles. So, when we have such type of profiles where you remember that alpha is the average volumetric concentration at any particular radial location r alpha 0 is at the center and alpha w. It is at the wall it is usually equal to 0 same thing j0 is at the center and this is the radius and this is the radial distance. So, for such a situation we find that C0 it can be given as 1 plus 2 by m plus n plus 2 into 1 minus your alpha by alpha. So, this I have already written down in the ppt.

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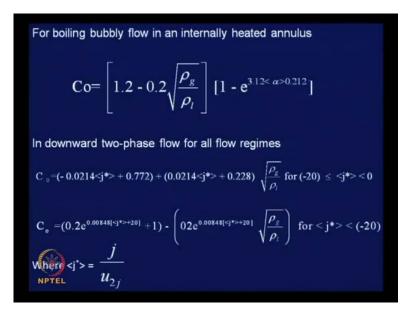


If you observe the ppt then you find that this particular C0. It has been derived for power law profiles of alpha and J several researchers have walked on different aspects of your drift flux model, and how to find out C0 and it has been found several researchers have proposed different particular values of C0. Some people have said that C0 it is a function of density ratio as well as the Reynold's number.

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And accordingly, several different definitions of C0 have been proposed which you can use for as the case may be they are imperial co-relations which have been derived for a large number of data for example, for fully developed flow in a round tube please remember C0 has been expressed as a function of rho g by rho l again for fully developed flow in a rectangular channel. It has been developed in this particular way when it is not fully developed then in that case the expressions are given here and accordingly I have written down a large number of expressions from where your C0 can be obtained under different conditions, but please remember these were all for more or less parabolic type of void age profiles where we assume that the void age is much more higher at the center as compared to the walls. But if the situations change say by some example may be say there is a heat flux and there is intense vaporization at the walls. So, under that condition the profile instead of becoming this it becomes this particular shape from concave it becomes convex. (Refer Slide Time: 50:55)



So, in such particular cases we find that the C0 calculation has to be done from the basic equation that I have written down here.

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LT. KGP law profiles - (n) m - (n) m  $\sim \begin{array}{c} c_{0} = 1 + \frac{2}{m + m + 2} \\ c_{0} \approx 1 - 1 \cdot 2 \end{array}$ 

From this particular basic equation it has to be done for two particular cases one is when there is heat flux and there is intense vaporization at the walls. So, therefore, there is a larger vapor concentration at the walls as compared to the center the other is when we are introducing air through say a porous wall then in that case what happens in the developing region there is greater concentration of air bubbles at the wall as compared to the center.

For such particular cases we cannot use the c zero values which I have written down in my ppt they are mostly for fully developed flow cases or for those particular cases which have a convex sort of a profile. So, for anything else C0 has been the has to be derived from the basic equation which I have written down and one more thing also which I would like you to remember in this particular case is usually by whatever way you find out C0. Usually, C0 it varies from 1 to1.2 as I have told you it does not deviate much from unity it varies it lies close to unity and usually from normal circumstances it has a maximum value of say 1 to 1.2 or 1 to 1.1 it does not vary more than that.

And finally, the last word of caution which I would like to give you regarding the drift flux model is see in this particular model we considered the volumetric flux velocity everything has vectors. If that is the case then the direction becomes very important for example, for all the cases co-current up flow co-current down flow I have been considering the upward direction as positive that is why j2 was positive for counter current flow j 1 was negative when liquid was flowing down etcetera. So, remember 1 thing sign convention is very important as far as the drift flux model is concerned.

There are several sign conventions which we take the first one is usually the direction of flow is taken as positive or the upward direction is taken as positive. Now, we find that most of the two phase flow analysis what we do we give more importance to the dispersed phase that is why we have defined alpha as the volumetric concentration of the dispersed phase is not it.

We do not define 1 minus alpha we talk in terms of alpha we usually talk in terms of j21 rather than j12 isn't it. So, usually we find that the direction of motion of the dispersed phase or the discontinuous phase is taken as positive there can be situation where the direction of gravitational force is taken as positive you can do whatever the case may be. But remember one thing whatever direction you are taking as positive you have to you have to define that in the beginning of the problem considering this direction as positive the following momentum analysis follows. So, this has to be referred to before you do any problem sign convention is very important for the drift flux model.

So, this completes our drift flux model and from the next class we are going to start the two fluid model or the separated flow model thank you very much.