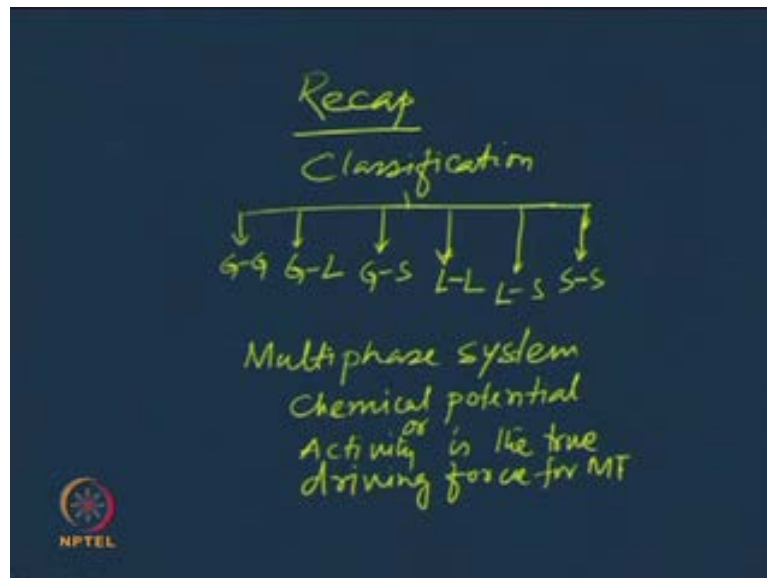


**Mass Transfer Operation-I**  
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**Module - 1**  
**Diffusion Mass Transfer**  
**Lecture - 2**  
**Molecular Diffusion**

(Refer Slide Time: 00:37)



Welcome to the second lecture on mass transfer operation. Before going to the second lecture, we will just have a recap on the first lecture, what we have done. In this lecture, we have introduced you the objectives of the course, and then the overall plan of the course syllabus, and then we have given you the introduction to mass transfer. What is mass transfer and what are the common examples of mass transfer? For example, we said, if we add a lump of sugar in a cup of tea, then there is a mass transfer, where sugar particles diffuses throughout and form the unit form solution. There are some industrial examples like the separations of CO<sub>2</sub>, which is a greenhouse gas; by using absorption is a mass transfer operation.

We have also classified the multiphase systems classification, and we have seen there are 6 phases of contact: Gas-gas system, gas-liquid system, gas-solid system, liquid-liquid system, liquid-solid system, and solid-solid system; and we have explained based on the thesis contact, what are the examples in each category. And then we have seen what are

the mechanism of mass transfer, and then the concentration gradient or the chemical potential gradient for mass transfer. As we can see, if there is a multiphase system, for multiphase system, then we have seen the chemical potential or activity, or activity is the true driving force for mass transfer.

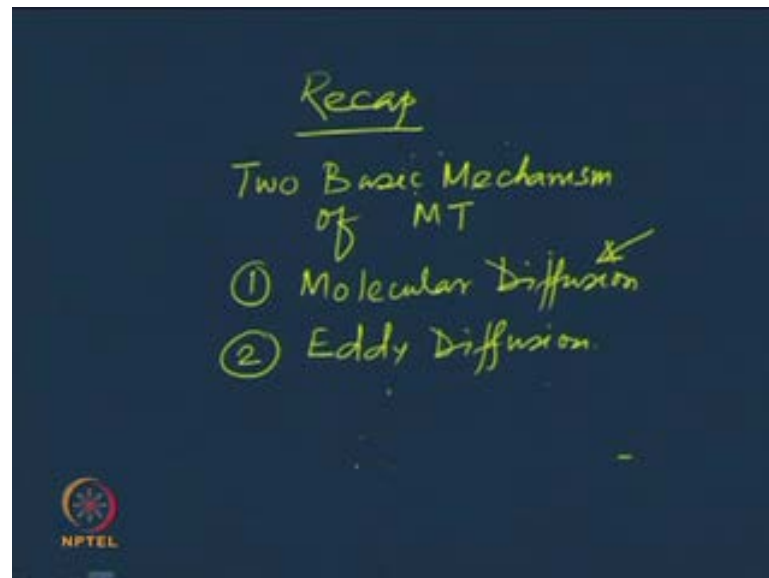
But in general, we consider mass transfer or we analyze mass transfer in a single phase system. In a single phase system or each phase, separately we analyze.

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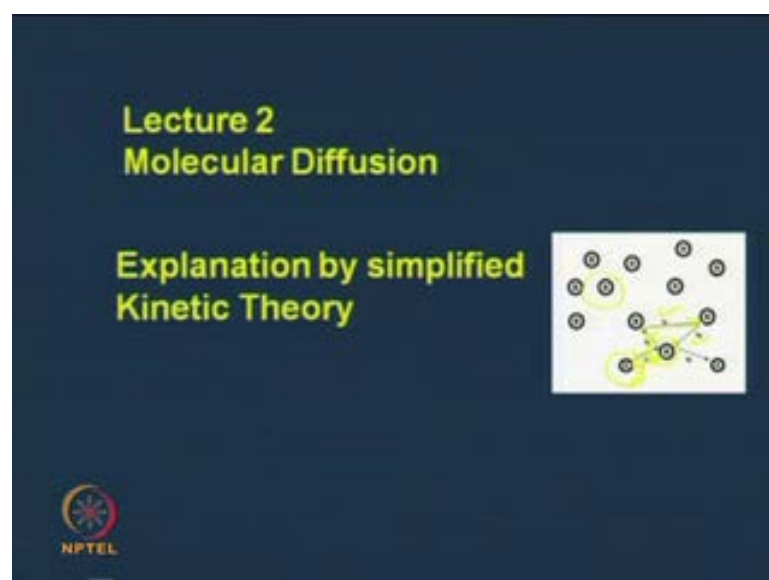
So in each phase, concentration is the driving force. For a single phase, the driving force is the concentration difference.

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The mechanism of mass transfer as we said, there are two basic mechanism of mass transfer: One is molecular mass transfer, which is based on the molecular diffusion, and second mechanism is convective mass transfer, which is based on the Eddy diffusion. So in this lecture, we will start with the molecular diffusion phenomena and other related examples on this topic.

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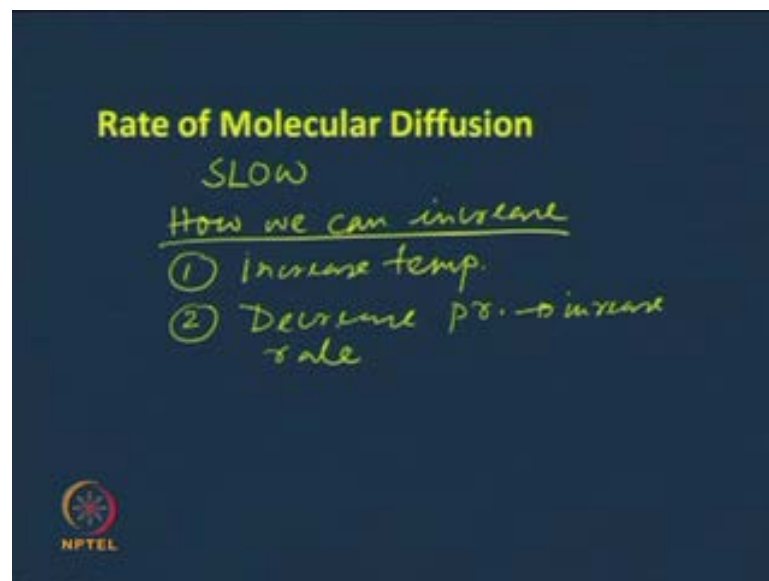


So molecular diffusion as we said in the last class, it is the diffusion of the molecules by virtue of their thermal energy. Since the diffusion of molecules by molecular diffusion

occurs by thermal energy, the rate of diffusions is slow. We can explain this molecular diffusion mechanism by simple kinetic theory, like in case of gas molecules, suppose there are A and B type of molecules are present in a system. So, the A molecule diffuses in a straight manner until it collides with the other molecule in the system. And then, it changes its direction and path and then it again travels in a straight path. So, the motion is known as the Brownian motion and the path is zig-zag. But the total distance travel if we considered, suppose time  $t_1$ ,  $t_2$ ,  $t_3$ , and  $t_4$ . So, total time is  $t$  up to  $t_4$  and the molecule A travels up to this point. Then the net distance travel by the molecule is a fraction of the total distance travelled by the molecule.

The total distance travelled by the molecule is the mean free path of the molecule, and then the rate of diffusion is defined the total distance travelled per unit time. Since the total distance travelled by molecule is a fraction of the net distance travel, so the rate of diffusion is slow.

(Refer Slide Time: 07:18)



So, molecular rate of molecular diffusion is slow, how we can increase this rate? There are two ways we can increase this rate: One is increase temperature. If we increase the temperature, the molecular motion will increase and the rate of molecular diffusion will increase, and second, decrease the pressure. If we decrease the pressure of the systems, the number of collisions will reduce. If the number of collisions reduces, the net distance

travel or mean free path of the molecule will be more or higher, and the rate of molecular diffusion will be more.

(Refer Slide Time: 08:40)

**Effect of Barrier on Molecular Diffusion**

Rate of evaporation of  $H_2O$   
at  $25^\circ C$  under complete  
vacuum =  $3.3 \text{ kg/m}^2 \text{ s}$   
of water surface

Place a stagnant layer  
at 1 atm pr. and thickness  
=  $0.1 \text{ mm}$  above the water  
surface



So, another effect on molecular diffusion is the barrier. Like if we consider rate of evaporation of water at 25 degree centigrade under complete vacuum, and it is roughly 3.3 kg per meter square second of water surface.

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**Effect of Barrier on Molecular Diffusion**

Rate of Diffusion  
reduces about 600 times

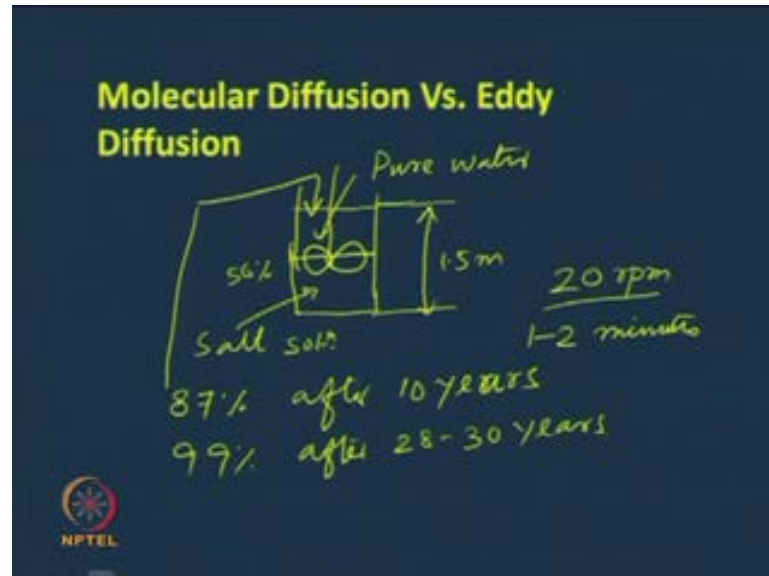
Place a stagnant layer  
at 1 atm pr. and thickness  
=  $0.1 \text{ mm}$  above the water  
surface



Now, if we place a stagnant layer at 1 atmosphere pressure and the thickness of the layer is around say 0.1 millimeter above the water surface, then the rate will decrease by about

600 times. The rate of diffusion reduces is about 600 times. So, the effect of barrier on molecular diffusion is very important.

(Refer Slide Time: 11:04)



Now, if we compare the difference between the molecular diffusion and Eddy diffusion, which one is faster and how they compare each other? Now, consider tank of total height say 1.5 meter and 50 percent of it port with a salt solution. Without disturbing, if we place another 50 percent by pure water and then leave it undisturbed, it can be calculated that this salt concentration at the top layer will reach around 87 percent after 10 years, and it will reach around 99 percent after 28 to 30 years.

So, we can see how slow this process is and, but instead of keeping it stagnant condition undisturbed condition, if we place one-third between the 2 layer and star it with 20 RPM revolution per minute, then it will take hardly 1 to 2 minutes to reach complete uniformity. So the Eddy diffusion is much faster compared to the turbulent diffusion. Now in mass transfer, we have to have some units to represent the flux, and we know the concentration in each phase is the driving force for mass transfer. So, we need to know the concentration unit. The concentrations are represented in different ways.

(Refer Slide Time: 13:36)

**Concentrations**

Mass Concentrations for component i

$$\rho_i = \frac{M_i}{V}$$

Total mass Concentration

$$\rho = \sum_{i=1}^n \rho_i$$

Mass fraction

$$w_i = \frac{\rho_i}{\sum_{i=1}^n \rho_i} = \frac{\rho_i}{\rho}$$
$$\sum_{i=1}^n w_i = \sum_{i=1}^n \frac{\rho_i}{\rho} = \text{Sum of mass fraction}$$


One is mass concentration. This is for component i. This is defined as  $\rho_i$  is equal to  $M_i$  by  $V$ . So, the total mass concentration can be written as  $\rho$  is equal to summation over  $i$  is equal to 1 to  $n$ , if there are  $n$  components in the mixture, it will be  $\rho_i$ ; and the mass fraction is defined as  $w_i$  which is equal to  $\rho_i$ , summation over  $i$  is equal to 1 to  $n$   $\rho_i$ , so which is equal to  $\rho_i$  by  $\rho$ ; and sum of the mass fraction summation over  $i$  is equal to 1 to  $n$   $w_i$  will be equal to summation over  $i$  is equal to 1 to  $n$   $\rho_i$  by  $\rho$ . So, this is the total sum of mass fraction.

(Refer Slide Time: 15:43)

**Concentrations**

Molar Concentrations

$$C_i = \frac{P_i}{RT}$$

Total molar concentration

$$C = \sum_{i=1}^n C_i$$

Total molar conc. for ideal Gas mixture

$$C = \frac{1}{RT} \sum_{i=1}^n P_i = \frac{P}{RT}$$


So, other concentration representation is the molar concentrations, and it is defined as  $C_i$  for component  $i$  is equal to  $p_i$  by  $RT$ . So, the total molar concentration we can represent it,  $C$  is equal to summation over  $i$  is equal to 1 to  $n$   $C_i$ . Total molar concentration for ideal gas mixture we can write,  $C$  is equal to  $1$  by  $RT$  summation over  $i$  is equal to 1 to  $n$   $p_i$  is equal to  $p_t$  by  $RT$ .

(Refer Slide Time: 17:29)

**Concentrations**

Mole fraction of component  $i$   
(Liquids & solid)

$$x_i = \frac{C_i}{C}$$

$$y_i = \frac{C_i}{C} \quad (\text{Gaseous})$$

$$= \frac{p_i}{p_t} \quad (\text{ideal gas mix})$$

Sum of mole fraction

$$\sum_{i=1}^n x_i = 1, \quad \sum_{i=1}^n y_i = 1$$

NPTEL

Mole fraction of component  $i$  for liquid and solid system can be represented as  $x_i$  is equal to  $C_i$  by  $C$ . For gaseous component, it is represented by  $y_i$  which is equal to  $C_i$  by  $C$ . If the gas components are ideal gas mixtures, then this will be  $p_i$  by  $p_t$  for ideal gas mixture, and then summation of mole fraction, we will get summation over  $i$  is equal to 1 to  $n$   $x_i$  will be 1, and summation over  $i$  is equal to 1 to  $n$   $y_i$  should be 1.

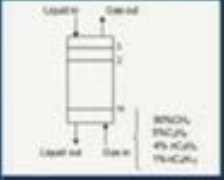
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### Example 1.1

The feed gas to an absorber has the following composition at 313 K and 200 kPa in the fig 1.

Calculate

- Composition of the feed gas in terms of mass fractions.
- Total mass concentration of the feed gas.



Now, let us take an example to calculate this mole fraction. Suppose the feed gas to an absorber has the composition 90 percent methane, 5 percent ethane, 4 percent normal propane, and 1 percent butane. These are at following temperature: 313 Kelvin and 200 kilo Pascal pressure. Now, we have to calculate the composition of feed gas in terms of mass fractions and the total mass concentration of the feed gas.

(Refer Slide Time: 20:01)

### Solution of Example 1.1

(i) Basis: 100 Kmol of feed

| Components                  | Kmol | Mol Wt | Mass (kg)             | Mass Fraction              |
|-----------------------------|------|--------|-----------------------|----------------------------|
| $\text{CH}_4$               | 90   | 16     | $90 \times 16 = 1440$ | $\frac{1440}{1808} = 0.80$ |
| $\text{C}_2\text{H}_6$      | 5    | 30     | 150                   | 0.08                       |
| $n\text{-C}_3\text{H}_8$    | 4    | 40     | 160                   | 0.09                       |
| $n\text{-C}_4\text{H}_{10}$ | 1    | 58     | 58                    | 0.03                       |
|                             | 100  |        | 1808                  | 1.0                        |

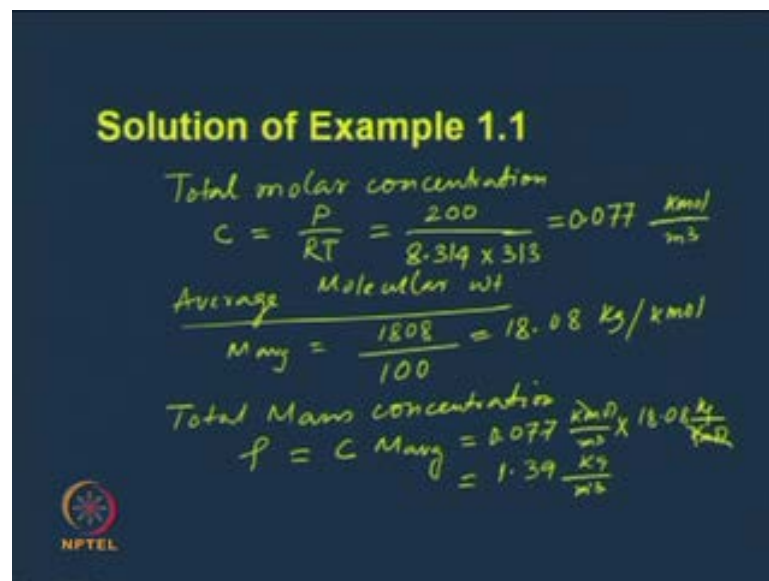


So for 1, for calculation of the mass fractions, let us take a basis. So, consider basis: 100 Kmol of feed.

So, let us develop the table. We have components and then Kmol, molecular weight of each component, mass in terms of kg, and then mass fraction. So, component we have CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, normal propane C<sub>3</sub>H<sub>8</sub>, C<sub>4</sub>H<sub>10</sub> and this is as the basis is 100 mole Kmol of feed; so, 90 percent of this component. So, it will be 90, 5 percent of this, and then 4 percent of nC<sub>3</sub>H<sub>8</sub>, and 1 percent of. So, total will be 100 Kmol. As we have taken the basis, we know the molecular weight 16, 30, 40, and then 58.

We can calculate the mass Kmol of each. Each is, we multiplied by the molecular weight will give you the mass. So, 90 into 16 will be 1440, and then this one will be 150, 40 multiplied by 4 160, and then 58 multiplied by 1 58. So, total mass is 1808 kg, and then the mass fractions will be equal to 1440 divided by the total mass 1808. So, it will be 0.80. Similarly, the next one is 0.08, and then 0.09, and 0.03. So, sum of all these is 1.0. So, this is mass fractions; the first questions is answered and then the second one to calculate the total mass concentration.

(Refer Slide Time: 24:02)



**Solution of Example 1.1**

Total molar concentration  

$$C = \frac{P}{RT} = \frac{200}{8.314 \times 313} = 0.077 \frac{\text{kmol}}{\text{m}^3}$$

Average Molecular wt  

$$M_{\text{avg}} = \frac{1808}{100} = 18.08 \text{ kg/kmol}$$

Total Mass concentration  

$$\rho = C M_{\text{avg}} = 0.077 \frac{\text{kmol}}{\text{m}^3} \times 18.08 \frac{\text{kg}}{\text{kmol}} = 1.39 \frac{\text{kg}}{\text{m}^3}$$

NPTEL

So to calculate the total mass concentration, we can calculate total molar concentration first. So, C is equal to p by RT. So, pressure is given 200 kilo-Pascal, and RT we can write, 8.314 into temperature 313 Kelvin. So, it will be around 0.077 Kmol per meter cube. Then average molecular weight we can calculate. M average will be the total molecular weight is 1, the mass is given 1808 divided by 100 is equal to 18.08 kg per Kmol. So that, the total mass concentration, which is rho is equal to C into M average

will be equal to C is given, 0.77 Kmol per meter cube multiplied by M average 18.08 kg per Kmol; it will be Kmol, Kmol cancel out. So, it will be 1.39 kg per meter cube. So, this is the total mass concentration.

(Refer Slide Time: 26:30)

**Example 1.2**

A liquid mixture contains 30wt%  $\text{NaNO}_3$  and 70wt%  $\text{H}_2\text{O}$ . The solution temperature is 300K and the density of the solution is assumed to 1050  $\text{kg/m}^3$ . Calculate

- The composition in terms of mole fractions.
- The total molar concentrations.



Now, let us take another example to calculate the mole fractions and total molar concentrations. A liquid mixture contains 30 weight percent sodium nitrate, and 70 weight percent water. The solution temperature is 300 K, and at this temperature, the density of the solution is assumed as 1050 kg per meter cube. Now, calculate the composition in terms of the mole fraction and the total molar concentrations.

(Refer Slide Time: 27:07)

**Solution of Example 1.2**  
Basis: 1 kg of liquid mixture

| Component         | Mass (kg) | Mol Wt. | Kmol   | Mol Fraction |
|-------------------|-----------|---------|--------|--------------|
| NaNO <sub>3</sub> | 0.3       | 85      | 0.0035 | 0.08         |
| H <sub>2</sub> O  | 0.7       | 18      | 0.0389 | 0.92         |
| Total             |           |         | 0.0424 | 1.0          |



Similarly like previous case, we can take a basis, say 1 kg of liquid mixture. We can develop the table like earlier: Component, mass, molecular weight, Kmole, and mole fraction. So component is sodium nitrate and water; the percentage is given 30 weight percent. So, this is 0.3 kg and this is 0.7 kg. Molecular weight is 85 and 18, and this is Kmole if you calculate, it will be 0.0035 and this is 0.0389. So, the total Kmole is 0.0424, and then mole fraction is this Kmole 0.0035 divided by total mole, this is the total mole 0.0424. So then, this is will be equal to 0.08 and similarly for this Kmole, the mole fractions will be 0.92. So, the total mole fraction is 1.0.

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**Solution of Example 1.2**

Average Molecular Wt.

$$M_{avg} = \frac{1 \text{ kg}}{\text{Total kmol}} = \frac{1 \text{ kg}}{0.0424 \text{ kmol}}$$
$$= 23.585 \frac{\text{kg}}{\text{kmol}}$$

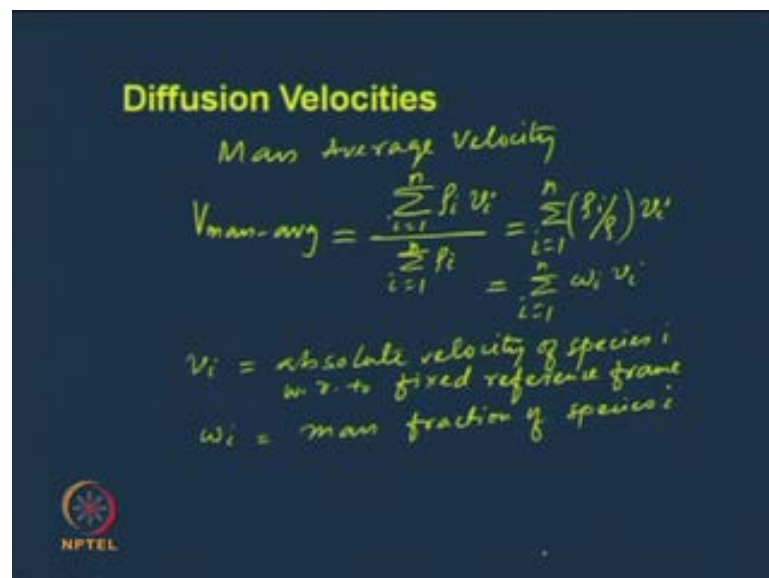
Total Molar Conc.

$$C = \frac{\rho}{M_{avg}} = \frac{1050 \text{ kg/m}^3}{23.585 \text{ kg/kmol}}$$
$$= 44.52 \frac{\text{kmol}}{\text{m}^3}$$


Now, to calculate the total molar concentration, we can calculate average molecular weight. So, this is M average is equal to 1 kg is the basis divided by total Kmol is equal to 1 kg divided by 0.0424 Kmol. So, this is 24 k mole. So, this is equal to 23.585 kg per Kmol. Now the total molar concentration is defined as C is equal to rho by M average. So rho is given, which is 1050 kg per meter cube divided by M average, which is 23.585 kg per Kmol. So, this is 44.52 Kmol per meter cube. This is the total concentration. So, this way we can calculate the molar and mass concentration.

Now, another term in case of mass transfer is the velocity of diffusion or diffusion velocities. The diffusion velocities are defined either in terms of mass average velocity or molar average velocity.

(Refer Slide Time: 32:41)



**Diffusion Velocities**

Mass Average Velocity

$$V_{\text{mass-avg}} = \frac{\sum_{i=1}^n \rho_i v_i}{\sum_{i=1}^n \rho_i} = \frac{\sum_{i=1}^n (\rho_i / \rho) \rho v_i}{\sum_{i=1}^n \rho_i} = \sum_{i=1}^n w_i v_i$$

$v_i$  = absolute velocity of species  $i$  w.r. to fixed reference frame  
 $w_i$  = mass fraction of species  $i$

NPTEL

So for mass average velocity, it is defined in terms of mass concentration  $V$  mass average is equal to summation over  $i$  is equal to 1 to  $n$   $\rho_i V_i$  divided by summation over  $i$  is equal to 1 to  $n$   $\rho_i$ , which we can write equal to summation over  $i$  is equal to 1 to  $n$   $\rho_i$  by  $\rho$  into  $V_i$  is equal to summation over  $i$  equal 1 to  $n$   $w_i V_i$ .  $V_i$  is equal to absolute velocity of species  $i$  with respect to fixed reference frame, and  $w_i$  is the mass fraction of species  $i$ .

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**Diffusion Velocities**

$$V_{mol-avg} = \frac{\sum_{i=1}^n C_i v_i}{\sum_{i=1}^n C_i}$$

$$= \frac{\sum_{i=1}^n (C/c) v_i}{\sum_{i=1}^n (C/c)}$$

$$= \sum_{i=1}^n x_i v_i$$

$x_i = \text{mol. fra. of species } i$



Now molar average velocity we can define  $V_{mol}$  average is equal to summation over  $i$  is equal to 1 to  $n$   $C_i v_i$  divided by summation over  $i$  is equal to 1 to  $n$   $C_i$ . So, this equal to we can write, summation over  $i$  is equal to 1 to  $n$   $C_i$  by  $c$  into  $v_i$ , is equal to summation over  $i$  is equal to 1 to  $n$   $x_i v_i$ ;  $x_i$  is the mole fraction of species  $i$ .

(Refer Slide Time: 36:22)

**Example 1.3**

A gas mixture containing ( $H_2=15\%$ ,  $CO=30\%$ ,  $CO_2=5\%$  and  $N_2=50\%$ ) flows through a tube of 1 inch diameter, at 15 bar total pressure. If the velocities of the respective components are 0.05m/s, 0.03m/s, 0.02m/s and 0.03m/s, calculate the mass average and molar average velocities of the mixture.

Rename  $H_2:1$ ,  $CO:2$ ,  $CO_2:3$ ,  $N_2:4$

Molar av. vel.

$$V_{mol-avg} = \frac{1}{C} (C_1 v_1 + C_2 v_2 + C_3 v_3 + C_4 v_4)$$

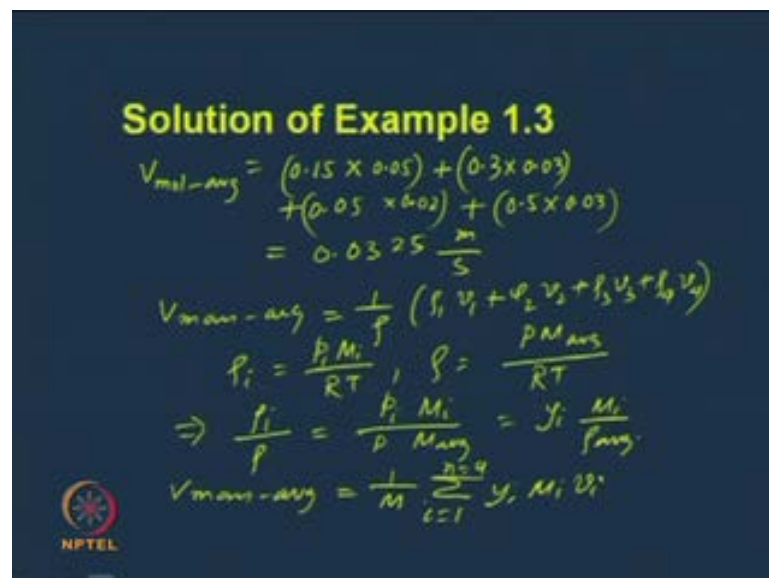
$$= (y_1 v_1 + y_2 v_2 + y_3 v_3 + y_4 v_4)$$


Now, let us take an example to calculate the average velocities. A gas mixture contains 15 percent hydrogen, 30 percent carbon monoxide, 5 percent  $CO_2$ , and 50 percent nitrogen. This flows through a tube of 1 inch diameter at 15 bar total pressure. If the

velocities of the respective components are given as 0.05 meter per second, 0.03 meter per second, 0.02 meter per second, and 0.03 meter per second; then, calculate the mass average and molar average velocities of the mixture.

Now, rename the components as H<sub>2</sub> is 1, CO as 2, CO<sub>2</sub> as 3, and nitrogen as 4. So, we can write the molar average velocities, that is  $V_{mol-avg}$ ; from the definition it is  $\frac{1}{C} \sum c_i v_i$  by C summation over we can just expand the summation like  $c_1 v_1 + c_2 v_2 + c_3 v_3 + c_4 v_4$ . Now if we substitute, the velocities are given and the concentration of each term if we substitute, then we will be able to calculate the total molar average velocity. So in this case we can write, this will be  $y_1 v_1 + y_2 v_2 + y_3 v_3 + y_4 v_4$ .

(Refer Slide Time: 39:13)



**Solution of Example 1.3**

$$V_{mol-avg} = (0.15 \times 0.05) + (0.3 \times 0.03) + (0.05 \times 0.02) + (0.5 \times 0.03)$$

$$= 0.0325 \frac{m}{s}$$

$$V_{mol-avg} = \frac{1}{P} (p_1 v_1 + p_2 v_2 + p_3 v_3 + p_4 v_4)$$

$$p_i = \frac{p_i M_i}{RT}, \quad P = \frac{P M_{avg}}{RT}$$

$$\Rightarrow \frac{p_i}{P} = \frac{p_i M_i}{P M_{avg}} = y_i \frac{M_i}{M_{avg}}$$

$$V_{mol-avg} = \frac{1}{M} \sum_{i=1}^n y_i M_i v_i$$

NPTL

Now after substitution in this relation,  $V_{mol-avg}$  will be 0.15 into 0.05, plus 0.3 multiplied by 0.03, 0.05 multiplied by 0.02, plus 0.5 multiplied by 0.03. So, this will give you the total 0.0325 meter per second.

Now, to calculate the mass average velocity; so,  $V_{mass-avg}$  we can calculate, and we know this is  $\frac{1}{\rho} \sum \rho_i v_i$  plus  $\rho_2 v_2$  plus  $\rho_3 v_3$  plus  $\rho_4 v_4$ , and we know  $\rho_i$  is equal to  $p_i M_i$  divided by  $RT$  if it is ideal gas, and then  $\rho$  is equal to  $P M_{avg}$  by  $RT$ . So, we can get  $\rho_i$  by  $\rho$ , is equal to  $p_i M_i$  by  $P M_{avg}$ . So, we can write  $y_i M_i$   $\rho_{avg}$ . If we substitute here, the equations would be  $V_{mass-avg}$ , is equal to  $\frac{1}{M} \sum_{i=1}^n y_i M_i v_i$ .

(Refer Slide Time: 41:51)

### Solution of Example 1.3

$$M_{avg} = y_1 M_1 + y_2 M_2 + \dots + y_4 M_4$$
$$= 24.9$$
$$V_{mass-avg} = \frac{1}{M_{avg}} (y_1 M_1 v_1 + \dots + y_4 M_4 v_4)$$
$$= 0.014 \text{ m/s}$$


So then we can calculate,  $M_{avg}$  as per our given data, which will be  $y_1 M_1$  plus  $y_2 M_2$  and  $y_4 M_4$ ; after substitution, it will be 24.9. So,  $V_{mass-avg}$  we can calculate using this correlations, which is  $1$  by  $M_{avg}$  into  $y_1 M_1 v_1$  plus  $y_4 M_4 v_4$ . After substitution, both  $M_{avg}$  and all this data, it will be 0.014 meter per second. So, this way, we can calculate the molar average velocity and mass average velocity for a given system.

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### Fluxes

Flux: rate of transport of a component  $i$  through unit area normal to the transport.

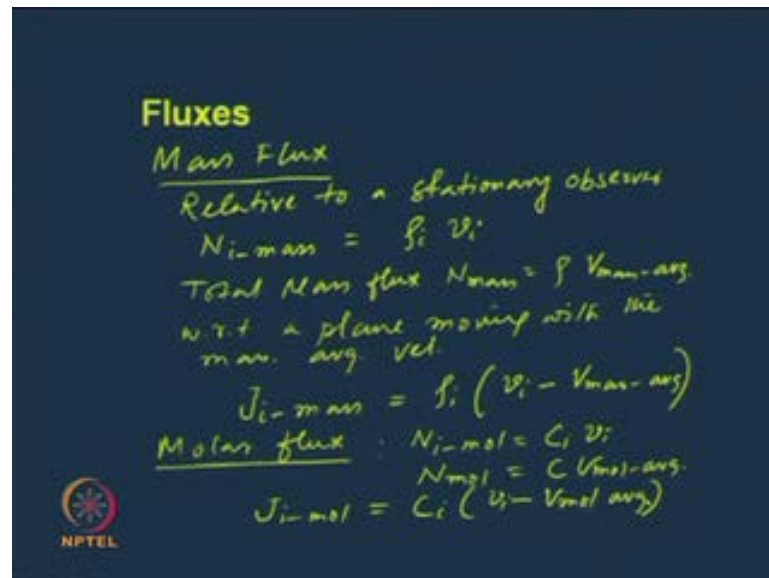
✓ Vector quantity.

Fixed  $\swarrow$  mass avg. Velocity  
                  or  
                  molar " "



So now, we will discuss on the flux. The flux is defined as the rate of transport of a component through unit area normal to the transport, and this flux is a vector quantity. This flux maybe defined with respect to co-ordinate fixed in step fixed co-ordinate, or it may be defined with respect to a moving plane, moving with a mass average velocity or molar average velocity.

(Refer Slide Time: 44:37)



**Fluxes**

Mass Flux  
 Relative to a stationary observer  
 $N_{i-mass} = \rho_i v_i$   
 Total Mass flux  $N_{mass} = \rho V_{mass-avg}$   
 w.r.t a plane moving with the mass avg vel.  
 $J_{i-mass} = \rho_i (v_i - V_{mass-avg})$

Molar flux  
 $N_{i-mol} = C_i v_i$   
 $N_{mol} = C V_{mol-avg}$   
 $J_{i-mol} = C_i (v_i - V_{mol-avg})$

NPTEL

So, mass flux we can define relative to a stationary observer or plane. So  $N_{i-mass}$  is  $\rho_i v_i$ , and the total mass flux  $N_{mass}$  is  $\rho V_{mass-avg}$ . Similarly, if we calculate the mass flux with respect to plane moving with the mass average velocity, then we can define,  $J_{i-mass}$  is equal to  $\rho_i v_i$  minus  $V_{mass-avg}$ .

Similarly, the molar flux we can define with respect to fixed plane and that we can write,  $N_{i-mol}$  is equal to  $C_i v_i$ , and the total molar flux  $N_{molar-total}$  is  $C V_{mol-avg}$ , and if the flux is defined with respect to the molar average velocity, then  $J_{i-mol}$  we can write  $C_i v_i$  minus  $V_{mol-avg}$ .

(Refer Slide Time: 47:25)

**Relation between Fluxes**

$$J_{i-mass} = f_i (V_i - V_{mass-avg})$$
$$= f_i V_i - f_i V_{mass-avg}$$
$$N_{i-mass} = f_i V_i$$
$$J_{i-mass} = N_{i-mass} - f_i V_{mass-avg}$$
$$N_{i-mass} = J_{i-mass} + f_i V_{mass-avg}$$

Similarly

$$N_{i-mol} = J_{i-mol} + C_i V_{mol-avg}$$


The relations between these mass average and molar average velocities, we can write from the above correlations,  $J_{i-mass}$  is equal to  $\rho_i v_i - \rho_i V_{mass-avg}$ . So we can write,  $\rho_i v_i - \rho_i V_{mass-avg}$ , say  $N_{i-mass}$  we know  $\rho_i v_i$ . So,  $J_{i-mass}$  is equal to  $N_{i-mass} - \rho_i V_{mass-avg}$ . So,  $N_{i-mass}$  will be  $J_{i-mass} + \rho_i V_{mass-avg}$ . Similarly, we can derive molar flux  $N_{i-mol}$  is equal to  $J_{i-mol} + C_i V_{mol-avg}$ .

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Q1. What is the SI unit of molar flux:

$$\text{Flux} = \frac{\text{kmol}}{\text{m}^2 \text{ s}}$$

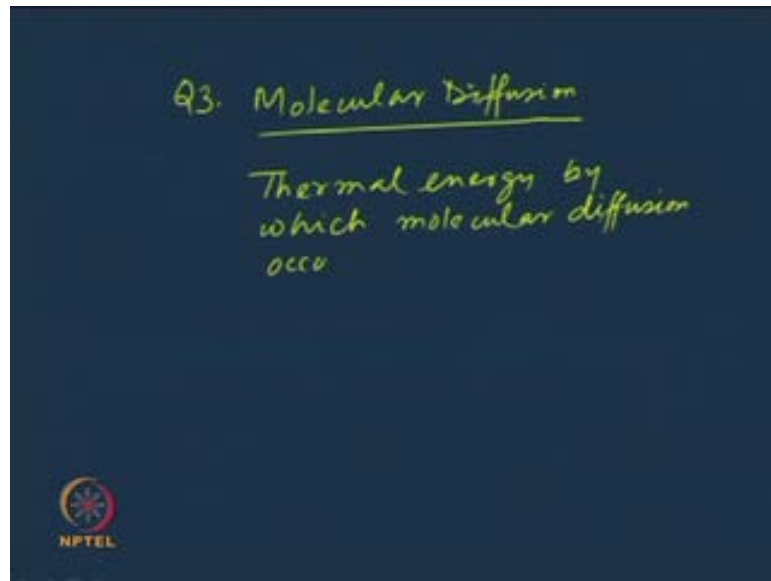
Q2. Under what conditions the mass avg vel. & the molar avg velocity should be same?

Ans: When the molecular wt of both components are same.



So if we ask the question, what is the SI unit of molar flux? As we define, it is the rate of transfer per unit area per unit time. So, it will be Kmol per unit area and time; so Kmol per meter square second. Second question: Under what condition, the mass average velocity and the molar average velocity should be same? The answer is, when the molecular weight of both the components are same then the total mass average velocity and the molar average velocity should be same.

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Another question if we ask, what are the basis for molecular diffusion or what are the driving force for molecular diffusion or the cause of molecular diffusion? It is the thermal energy by which diffusion occurs.